



Introduction:

- Diesel is a commonly used fuel source and a large contributor towards global warming largely due to its substantial emissions of carbon dioxide.
- In its place, dimethyl ethers (DME) have been proven to be a promising alternative to the fuel as it comes with many eco-friendly benefits:



• Our experiments aim to discover a catalyst which can most effectively aid in the creation of DME, with the eventual goal of using it in a reactive distillation column in order to produce it on a larger scale.

Methods:

- 4 different catalysts were used in this experiment:
 - Amberlyst 15 Dry (A15D)
 - Amberlyst 35 Wet (A35W)



<u>A15D</u>

Surface Area: 53 m²/g Avg. Pore Diameter: 300 Å Acid Site Conc.: 4.7 eq/kg Max Op. Temp.: 120 °C



<u>A16W</u> Surface Area: 30 m²/g Avg. Pore Diameter: 250 Å Acid Site Conc.: 4.8 eg/kg Max Op. Temp.: 130 °C



<u>A35W</u>

Surface Area: 50 m²/g Avg. Pore Diameter: 300 Å Acid Site Conc.: 5.2 eq/kg Max Op. Temp.: 150 °C Figure 1. Catalyst properties

• ~0.500g of each catalyst were placed in an oven (excluding A15D) for a minimum of 24 hours at 65°C in order to evaporate any traces of water from their pores.





Figure 2a. MIcroscopic image of Amberlyst Catalyst BEFORE drying



Figure 2b. MIcroscopic image of Amberlyst Catalyst AFTER drying

Fuel of the Future: **Stimulating the Production of Dimethyl Ethers** Through Catalysts Abegail Gagelonia, Danish Dar, Selam Demoz

Department of Clean Technologies, Northern Alberta Institute of Technology (NAIT)

 Amberlyst 16 Wet (A16W) • Amberlyst 36 Wet (A36W)



A36W Surface Area: 33 m²/g Avg. Pore Diameter: 240 Å Acid Site Conc.: 5.4 eq/kg Max Op. Temp.: 150 °C



- Each catalyst was reacted with pure methanol using a Methanol Mini Reactor Loop to dehydrate the methanol and produce dimethyl ether gas. The Opentrons Robot was then used to inject the product into 20mL vials at 50min intervals.
- Within the reactor, all catalysts were subjected to specific conditions:

Temperature: 130°C

Pressure: 135psi

• The vials were placed into a gas chromatograph (GC). • The quantity of DME that was produced during the reaction was able to be analyzed through the use of this machine.



Figure 3. The average production of DME produced during 50 minute intervals represented by the integration area number given by the gas chromatograph. This graph averages 4 different runs through the methanol reactor using each catalyst. Pure methanol ran through the reactor at 0.22 mL/min and filled 7 vials over the course of 6 hours.



Figure 4. The average production of methylal produced during 50 minute intervals represented by the integration area number given by the gas chromatograph. This graph averages 4 different runs through the methanol reactor using each catalyst. Pure methanol ran through the reactor at 0.22 mL/min and filled 7 vials over the course of 6 hours.





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