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**UNIVERSITY OF ALBERTA**

**DILUTION OF CIRCULAR WALL JET IN CROSSFLOW**

**BY**

**JOHN KIPKETER LANGAT**



**A THESIS**

**SUBMITTED TO THE FACULTY OF GRADUATE AND**

**RESEARCH IN PARTIAL FULFILLMENT OF THE**

**REQUIREMENT FOR THE DEGREE OF**

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**IN**

**WATER RESOURCES ENGINEERING**

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**EDMONTON, ALBERTA**

**SPRING, 1994.**



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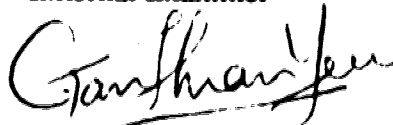
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## **ABSTRACT**

**Dilution of turbulent circular wall jets discharging perpendicular to crossflow ambients has not received much attention compared to studies on free turbulent jets in crossflows. An effluent diffuser designed as a circular wall jet is an efficient means of enhancing dilution of waste discharges from both industrial and municipal treatment plants under river conditions. The outfall is located at / or near the bed in order to utilize the whole flow depth in mixing and therefore this increases the efficiency of effluent dilution within the mixing zone. The present study considers the dilution characteristics of a circular wall jet in river-like crossflows and its comparison with the free jet discharging perpendicularly from the bed. The location of the jet takes into account the limited depths available for mixing in most shallow rivers.**

**This thesis presents the results of an experimental study on the dilution produced in circular wall jets discharging perpendicular to a freestream. The deflected wall jets were explored for dilutions up to 100:1 for downstream distance  $x$  up to about 200 times the jet nozzle diameter. Dilution characteristics of the jet were studied by first performing a similarity analysis on the 3-dimensional concentration distributions. Non-dimensional concentration profiles were found to be similar both in the vertical and the transverse directions. Minimum dilutions were considered along the axial distance of the jet for the flow regimes defined by the momentum dominated near field, the far field and the passive plume regions. For practical purposes, a mean equation was developed to describe the minimum dilution in the mixing region. The correlation was found to be of similar magnitude with the results of the free jets. The growth rate of the jet, both in the vertical and the transverse directions was also**

investigated. The results indicated that the lateral spread of the deflected jet is about twice that in the vertical direction. This characteristic of wall jets takes advantage of the available mixing space since most rivers have widths several times larger than the flow depth, and consequently increase the effluent dilution.

Effect of the flow depths on the tracer dilution was also studied. The results indicated significant reduction in tracer dilution for freestream flow depths less than 10 times the jet nozzle diameter. This problem prevails for effluent discharged into shallow rivers due to early surfacing.

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## TABLE OF CONTENTS

<b>1.0 INTRODUCTION .....</b>	<b>1</b>
1.1 General.....	1
1.2 Turbulent Jet Mixing in Crossflows .....	2
1.3 The Present Investigation .....	4
<b>2.0 LITERATURE REVIEW .....</b>	<b>6</b>
2.1 General.....	6
2.2 Description of Circular Turbulent Jets .....	7
2.2.1 Simple Axisymmetric Jet.....	7
2.2.2 Circular Jet in Crossflow	
Preliminary discussion .....	10
2.2.3 Diffusion of Circular Jets in Crossflow .....	12
2.2.4 Dilution of Circular Jets in Crossflow .....	14
<b>3.0 LABORATORY INVESTIGATIONS .....</b>	<b>19</b>
3.1 General.....	19
3.2 Experimental Arrangement.....	19
3.2.1 The Flume .....	19
3.2.2 Jet Arrangement.....	20
3.3 Calibration of the Fluorometer .....	21
3.4 Sampling Procedure .....	22
3.4.1 Sampling Rake Arrangement.....	22
3.4.2 Preliminary Investigations .....	24
3.4.3 Test Series.....	25
3.4.4 Error Estimation.....	27

<b>4.0 EXPERIMENTAL RESULTS AND ANALYSIS.....</b>	<b>40</b>
4.1 General.....	40
4.2 Boundary Limits of the Momentum Dominated Flow Regimes .....	41
4.2.1 Momentum Dominated Near Field Regime .....	41
4.2.2 Momentum Dominated Far Field Regime .....	43
4.3 Experimental Results .....	44
4.3.1 Parameters Considered .....	44
4.3.2 Presentation of the Results.....	45
4.4 Analysis .....	46
4.4.1 Concentration Profiles .....	46
4.4.2 Minimum Dilution .....	47
4.4.3 Length Scale Analysis .....	53
4.4.3.1 Vertical Scale, $b_z$ .....	53
4.4.3.2 Transverse Scale, $b_\theta$ .....	54
<b>5.0 CONCLUSIONS AND RECOMMENDATIONS .....</b>	<b>116</b>
5.1 Conclusions.....	116
5.1.1 Interpretation of the Experimental Results .....	116
5.1.2 Comparison with Previous Studies .....	118
5.2 Recommendations.....	119
References.....	121
<b>APPENDICES</b>	
I. Photographic Representation of the Circular Wall Jet Diffusion in Crossflow .....	126
II. Experimental Dilution Data .....	130
III. Centerline Wall Jet Trajectories for the Momentum Dominated Flow Regimes .....	161

## **LIST OF TABLES**

<b>TABLES</b>	<b>DESCRIPTION</b>	<b>PAGE</b>
3.1	Details of Experiments of Circular Wall Jet in Crossflow .....	35
3.2	Fluorometer Scale Error Estimation .....	36
3.3	Error Estimation .....	37

## **APPENDIX**

<b>II</b>	Experimental Dilution Data of Circular Wall Jet in Crossflow .....	130
-----------	--	-----

## LIST OF FIGURES

FIGURE	DESCRIPTION	PAGE
2.1	Simple Axisymmetric Turbulent Jet in Stagnant ambient.....	17
2.2	Turbulent Circular Jet Discharge in Crossflow .....	18
3.1	Velocity Profiles across the Flume .....	32
3.2	Calibration Curve for the Fluorometer .....	33
4.1	Boundary Limits for the Momentum Dominated Regions .....	56
4.2	Definition Sketches of Circular Wall jet in Crossflow .....	57
4.3 ( a )	Transverse Concentration Profiles ( $\eta - \xi$ plane ) for the Velocity Ratio $\alpha = 4$ and the downstream distance $x = 5$ mm .....	58
4.3 ( b )	Transverse Concentration Profiles ( $\eta - \xi$ plane ) for the Velocity Ratio $\alpha = 4$ and the downstream distance $x = 100$ mm .....	59
4.3 ( c )	Transverse Concentration Profiles ( $\eta - \xi$ plane ) for the Velocity Ratio $\alpha = 4$ and the downstream distance $x = 285$ mm .....	60
4.4	Concentration Profiles of $C / C_0$ against $z$ for the Velocity Ratio $\alpha = 2$ along the Centerline of the Jet .....	61
4.5	Concentration Profiles of $C / C_0$ against $z$ for the Velocity Ratio $\alpha = 4$ along the Centerline of the Jet .....	62
4.6	Concentration Profiles of $C / C_0$ against $z$ for the Velocity Ratio $\alpha = 6$ along the Centerline of the Jet .....	63
4.7	Concentration Profiles of $C / C_0$ against $z$ for the Velocity Ratio $\alpha = 8$ along the Centerline of the Jet .....	64

<b>4.8</b>	<b>Concentration Profiles of <math>C / C_0</math> against <math>z</math> for the Velocity Ratio <math>\alpha = 12</math> along the Centerline of the Jet .....</b>	<b>65</b>
<b>4.9 ( a )</b>	<b>Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction for Velocity Ratio <math>\alpha = 2</math> and MDNF regime .....</b>	<b>66</b>
<b>4.9 ( b )</b>	<b>Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction for Velocity Ratio <math>\alpha = 2</math> and MDFF regime .....</b>	<b>67</b>
<b>4.9 ( c )</b>	<b>Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction for Velocity Ratio <math>\alpha = 2</math> and PP regime .....</b>	<b>68</b>
<b>4.9 ( d )</b>	<b>Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction for Velocity Ratio <math>\alpha = 2</math> and Combined MDNF and MDFF regimes .....</b>	<b>69</b>
<b>4.10 ( a )</b>	<b>Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction for Velocity Ratio <math>\alpha = 4</math> and MDNF regime .....</b>	<b>70</b>
<b>4.10 ( b )</b>	<b>Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction for Velocity Ratio <math>\alpha = 4</math> and MDFF regime .....</b>	<b>71</b>
<b>4.10 ( c )</b>	<b>Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction for Velocity Ratio <math>\alpha = 4</math> and PP regime .....</b>	<b>72</b>
<b>4.10 ( d )</b>	<b>Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction for Velocity Ratio <math>\alpha = 4</math> and Combined MDNF MDFF regimes .....</b>	<b>73</b>
<b>4.11 ( a )</b>	<b>Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction for Velocity Ratio <math>\alpha = 6</math> and MDNF regime .....</b>	<b>74</b>
<b>4.11 ( b )</b>	<b>Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction for Velocity Ratio <math>\alpha = 6</math> and MDFF regime .....</b>	<b>75</b>
<b>4.11 ( c )</b>	<b>Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction for Velocity Ratio <math>\alpha = 8</math> and PP regime .....</b>	<b>76</b>

4.11 ( d )	Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction for Velocity Ratio $\alpha = 6$ and Combined MDNF and MDFF regimes .....	77
4.12 ( a )	Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction for Velocity Ratio $\alpha = 8$ and MDNF regime .....	78
4.12 ( b )	Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction for Velocity Ratio $\alpha = 8$ and MDFF regime .....	79
4.12 ( c )	Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction for Velocity Ratio $\alpha = 8$ and PP regime .....	80
4.12 ( d )	Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction for Velocity Ratio $\alpha = 8$ and Combined MDNF and MDFF regimes .....	81
4.13 ( a )	Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction for Velocity Ratio $\alpha = 8$ and MDNF regime .....	82
4.13 ( b )	Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction for Velocity Ratio $\alpha = 8$ and MDFF regime .....	83
4.13 ( c )	Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction for Velocity Ratio $\alpha = 8$ and PP regime .....	84
4.13 ( d )	Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction for Velocity Ratio $\alpha = 8$ and Combined MDNF and MDFF regimes .....	85
4.14 ( a )	Similarity Profiles of Concentration Distribution in the Vertical Direction for MDNF regime .....	86
4.14 ( b )	Similarity Profiles of Concentration Distribution in the Vertical Direction for MDFF regime .....	87

4.14 ( c )	Similarity Profiles of Concentration Distribution in the Vertical Direction for PP regime .....	88
4.14 ( d )	Similarity Profiles of Concentration Distribution in the Vertical Direction for Combined MDNF and MDFF regimes .....	89
4.15	Transverse Concentration Profiles of $C / C_0$ against $\eta$ Perpendicular to the Jet axis for the Velocity Ratio $\alpha = 2$ .....	90
4.16	Transverse Concentration Profiles of $C / C_0$ against $\eta$ Perpendicular to the Jet axis for the Velocity Ratio $\alpha = 4$ .....	91
4.17	Transverse Concentration Profiles of $C / C_0$ against $\eta$ Perpendicular to the Jet axis for the Velocity Ratio $\alpha = 6$ .....	92
4.18	Transverse Concentration Profiles of $C / C_0$ against $\eta$ Perpendicular to the Jet axis for the Velocity Ratio $\alpha = 8$ .....	93
4.19	Transverse Concentration Profiles of $C / C_0$ against $\eta$ Perpendicular to the Jet axis for the Velocity Ratio $\alpha = 12$ .....	94
4.20	Non - Dimensional Profiles of Concentration Distribution in the Transverse Direction for the Velocity Ratio $\alpha = 2$ .....	95
4.21	Non - Dimensional Profiles of Concentration Distribution in the Transverse Direction for the Velocity Ratio $\alpha = 4$ .....	96
4.22	Non - Dimensional Profiles of Concentration Distribution in the Transverse Direction for the Velocity Ratio $\alpha = 6$ .....	97
4.23	Non - Dimensional Profiles of Concentration Distribution in the Transverse Direction for the Velocity Ratio $\alpha = 8$ .....	98
4.24	Non - Dimensional Profiles of Concentration Distribution in the Transverse Direction for the Velocity Ratio $\alpha = 12$ .....	99
4.25	Similarity Profiles of Concentration Distribution in the Transverse Direction .....	100

4.26	Characteristic Minimum Dilution $C_o / C_m$ against $\alpha x / d$ for the Velocity Ratio $\alpha = 2$ of the Deflected jet .....	101
4.27	Characteristic Minimum Dilution $C_o / C_m$ against $\alpha x / d$ for the Velocity Ratio $\alpha = 4$ of the Deflected jet .....	102
4.28 ( a )	Characteristic Minimum Dilution $C_o / C_m$ against $\alpha x / d$ for the Velocity Ratio $\alpha = 6$ , $D / d = 20$ and $d = 12.7$ mm of the Deflected jet .....	103
4.28 ( b )	Characteristic Minimum Dilution $C_o / C_m$ against $\alpha x / d$ for the Velocity Ratio $\alpha = 6$ , $D / d = 10$ and $d = 12.7$ mm of the Deflected jet .....	104
4.28 ( c )	Characteristic Minimum Dilution $C_o / C_m$ against $\alpha x / d$ for the Velocity Ratio $\alpha = 6$ , $D / d = 5$ and $d = 12.7$ mm of the Deflected jet .....	105
4.29	Characteristic Minimum Dilution $C_o / C_m$ against $\alpha x / d$ for the Velocity Ratio $\alpha = 8$ of the Deflected jet .....	106
4.30 ( a )	Characteristic Minimum Dilution $C_o / C_m$ against $\alpha x / d$ for the Velocity Ratio $\alpha = 12$ and $d = 6.35$ mm of the Deflected jet .....	107
4.30 ( b )	Characteristic Minimum Dilution $C_o / C_m$ against $\alpha x / d$ for the Velocity Ratio $\alpha = 12$ and $d = 12.7$ mm of the Deflected jet .....	108
4.31	Comparison of Characteristic Minimum Dilution $C_o / C_m$ against $\alpha x / d$ for all the Jet Discharges of the Deflected jet .....	109
4.32	Comparison of Characteristic Minimum Dilution $C_o / C_m$ against $\alpha x / d$ for all the Jet Discharges with the Results of Hodgson ( 1991 ) and Wright ( 1977 ) of the Deflected jet .....	110



<b>4.33</b>	<b>Generalized Scales for the Vertical Concentration Profiles of the Deflected Jet .....</b>	<b>111</b>
<b>4.34 ( a )</b>	<b>Unified General Scale for the Vertical Concentration Profiles of the Deflected Jet .....</b>	<b>112</b>
<b>4.34 ( b )</b>	<b>Relation of the Vertical Scale .....</b>	<b>113</b>
<b>4.35</b>	<b>Generalized Scales for the Transverse Concentration Profiles of the Deflected Jet .....</b>	<b>114</b>
<b>4.36</b>	<b>Generalized Positive and Negative Transverse Scales.....</b>	<b>115</b>

## **APPENDIX**

<b>III</b>	<b>Centerline Wall Jet Trajectories for the Momentum Dominated Flow Regimes.....</b>	<b>161</b>
------------	--	------------

## LIST OF PLATES

PLATE	DESCRIPTION	PAGE
<b>3.1</b>	<b>Flume Arrangement</b>	
	( a ) Side View .....	34
	( b ) Inside of Flume .....	34
<b>3.2</b>	<b>Jet Nozzle Arrangement</b>	
	( a ) Location of the Nozzles.....	35
	( b ) Diffusion of the Jet .....	35
<b>3.3</b>	<b>Rotameter .....</b>	<b>36</b>
<b>3.4</b>	<b>Turner Model 10 Fluorometer .....</b>	<b>37</b>
<b>3.5</b>	<b>Sampling Rake</b>	
	( a ) Sampling Position inside the Flume.....	38
	( b ) Sampling Probes Arrangement .....	38
<b>3.6</b>	<b>Samples Holder</b>	
	( showing 60 ml plastic bottles and delivery tubes ) .....	39

## APPENDIX

<b>I</b>	<b>Photographic Representation of Circular Wall Jet Dilution.....</b>	<b>126</b>
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## NOTATIONS

<b>a</b>	<b>cross - section area of the sample delivery tubes</b>
<b>b</b>	<b>length scale in the velocity distribution for a simple jet</b>
<b>b<sub>c</sub></b>	<b>length scale in the concentration distribution for a simple jet</b>
<b>b<sub>z</sub></b>	<b>length scale on the z - direction</b>
<b>b<sub>η</sub></b>	<b>length scale on the transverse η - direction</b>
<b>C</b>	<b>concentration at a section of the jet</b>
<b>C<sub>0</sub></b>	<b>initial jet concentration at the nozzle</b>
<b>C<sub>m</sub></b>	<b>maximum jet concentration at a section</b>
<b>d</b>	<b>jet nozzle diameter</b>
<b>D</b>	<b>depth of the freestream flow</b>
<b>k</b>	<b>diffusion coefficient ratio</b>
<b>k<sub>1</sub></b>	<b>empirical constant in a simple jet</b>
<b>l<sub>m</sub></b>	<b>momentum length scale [ = M<sup>1/2</sup> / U ]</b>
<b>M</b>	<b>kinematic momentum flux at the jet nozzle</b>
<b>R</b>	<b>Reynolds number of the jet</b>
<b>r</b>	<b>radial distance to any point from the axis of a simple jet</b>
<b>u</b>	<b>velocity at any point of a simple jet in the axial direction</b>
<b>U</b>	<b>freestream velocity</b>

$u_m$	maximum jet velocity at a section
$U_0$	initial velocity of the jet at the nozzle
$x$	co - ordinate direction along the freestream
$x_0$	downstream $x$ co - ordinate of the deflected jet where momentum dominated near field ends
$x_f$	downstream $x$ co - ordinate of the deflected jet where momentum dominated far field ends
$y$	co - ordinate direction along the original direction of the jet perpendicular to the freestream
$y_c$	centerline co - ordinate on the $y$ - axis of the deflected jet
$z$	vertical ( depth wise ) co - ordinate direction above the channel bed
$\alpha$	the ratio of the jet velocity to the ambient freestream velocity
$\delta$	elevation of the maximum concentration axis above the bed at a section
$\nu$	kinematic viscosity of the fluid
$\theta$	angle of the jet deflection from the original orientation
$\xi$	distance along the centerline axis of the deflected jet
$\xi_m$	axial co - ordinate of the deflected jet at the end of the potential core
$\xi_f$	axial co - ordinate of the deflected jet at the end of momentum dominated far field
$\eta$	transverse co - ordinate direction normal to $\xi$
$\zeta$	vertical co - ordinate direction normal to $\xi$
$\rho$	density of the jet fluid

## **1.0 INTRODUCTION**

### **1.1 General**

A circular jet discharging at an angle into a moving free stream is of practical interest in the developments associated with waste disposal into rivers, lakes and into the atmosphere. The wastes which result from increased urbanization and industrialization have continuously increased the pollutant loadings of both the hydrosphere and the atmosphere. Examples of waste disposal issuing as a jet at an angle to the moving ambient fluid include the emission of industrial smoke into the wind, treated municipal waste and other industrial wastes into rivers. The aim of these jet discharges is to produce significant mixing in a relatively short distance.

The present study investigates the dilution of a circular wall jet in crossflow. The jet induced turbulence provides the initial mixing and the subsequent dilution of the pollutants and is greatly influenced by the design of the outfall. The interaction which occurs in a jet discharging normal to the streamflow enhances the mixing process and results in high dilutions compared to jets in stagnant or co-flowing ambients. Sufficient knowledge of pollutant concentration distributions within this reach of the river where the outfall is located is important. Outfall design would involve taking into considerations the shallow nature of natural streams and the pollutant control standards imposed to protect against indiscriminatory disposal of toxic effluents into rivers.

The advantages of locating the outfall near or at the stream bed are:

- I. most industrial wastes are colored and would be aesthetically objectionable if discharged near the surface of the rivers. Discharges near the bed would**

utilize the whole depth of flow in the river to diffuse the unpleasant color before surfacing.

II. effluent temperatures are normally slightly higher than that of the receiving waters ( about  $1^{\circ}\text{C}$  -  $5^{\circ}\text{C}$  difference ) due to the biological processes in the retention ponds before release into the river. Effluents therefore tend to float in a stratified manner in the river flow and this could be minimized by locating the jet diffuser near the bed.

A possible disadvantage is the possible erosion of the river bed in the vicinity of the outfall. To minimize the problem, provision of protection works would be necessary, such as constructing a concrete apron or stone pitching the sections that may be affected by the jet. A wall ( or bed ) jet diffuser similar to the present model and currently in use was designed by N. Rajaratnam and A. Charbannou for the Cariboo Pulp mill in Quesnel, in northern British Columbia which discharges into the Fraser river.

## **1.2 Turbulent Jet Mixing in Crossflows**

Initial concentration of effluents at the outfall may be much higher than the allowable receiving stream concentration. A zone therefore exists where significant dilution occurs in a relatively short distance, normally referred to as the initial dilution or mixing zone. Gowda ( 1984 ) described this zone as a limited use zone because the effluent concentrations often exceed the set standards of the receiving stream. Circular turbulent jets discharging the effluent perpendicular to the free stream flow is one of the effective schemes of achieving this significant dilution. In some cases, the effluent is discharged upwards into the free stream from a submerged outfall embedded in the

middle of the crossflow ( Wright, 1977; Hodgson and Rajaratnam, 1992 ). To use the limited flow depth in crossflows such as shallow rivers, it is preferable to delay the effluents from surfacing by locating the jet on or near the bed and discharging normal to the freestream as a wall ( bed ) jet. It is assumed that the ratio of the stream flow depth (  $D$  ) to the jet diameter (  $d$  ) is large enough to minimize disturbance of the free surface in the stream by the jet. Therefore, the parameter (  $D / d$  ) will be considered not important in this analysis of the circular wall jet in crossflows. ( It should be mentioned that in our case, the wall jets should be called bed jets but following the general practice in Fluid Mechanics, they are referred to as wall jets, where all boundaries are referred to as walls. )

The work of Hodgson and Rajaratnam ( 1988 ) broadly classified deep water and shallow water jets based on the parameter  $\alpha d / D$ , where  $\alpha$  is the ratio of the jet velocity,  $U_0$  to the free stream velocity,  $U$ . A photographic study of circular jets discharging into river-like shallow flows showed that the critical value for the parameter  $\alpha d / D$  is about 0.34. Larger values of this parameter correspond to shallow water jets and smaller values to deep water jets. In the present work, values of  $\alpha d / D$  are as large as 1.2, and the jet showed no surface effects indicating that it behaved as a deep water jet. Use of the same parameter to categorize wall jets is therefore not applicable because the growth towards the surface is only through diffusion and the jet momentum is not in the direction of the freestream depth.

Simple axisymmetric circular turbulent jets discharging into a large quiescent ambient is first considered. Considering the region of developed flow, the dilution along the axis of a simple jet is approximated by the expression ( Rajaratnam, 1983 ):

$$\frac{C_0}{C_m} = k_1 \frac{x}{d} \quad (1.1)$$

where  $C_0$  and  $C_m$  are respectively the concentrations at the jet nozzle of diameter  $d$ , and maximum concentration at an axial distance of  $x$  downstream of the nozzle and  $k_1$  is an empirical constant determined through experiments. The work of Hodgson and Rajaratnam ( 1989 ) found that  $k_1$  is approximately equal to 0.19.

Several studies have been conducted on the mixing of circular jets in crossflows of large extent ( Rajaratnam, 1976 ). One of the more significant studies in this area is the work of Wright ( 1977 ). Recently, Hodgson and Rajaratnam studied the dilutions of circular jets in rivers, including shallow flows ( Hodgson and Rajaratnam, 1992 ).

### 1.3 The Present Investigation

Most of the research work on circular turbulent jets in crossflow have emphasized the momentum characteristics compared to the concentration measurements. The present work emphasizes the practical importance of the jet dilution issuing as a wall jet in crossflows as applied in hydraulics.

The objective of the experimental investigation was to study the main dilution characteristics of circular wall jet in ambient flows normal to the jet discharge and to compare with the existing work for the momentum dominated regimes of the free jet. To understand the problem, general mixing characteristics of turbulent jets in crossflow were first considered, developing from the simple case of the axisymmetric jet. Review of the existing work on the free jet in crossflows formed the basis of studying dilution characteristics of circular wall jet in crossflow. The analysis of the dilution data was based on the flow regimes defined by the momentum dominated near field and far field regions of the jet. The results were then compared with those of



the free jet conditions investigated by Wright ( 1977 ) and Hodgson and Rajaratnam ( 1992 ).

## **2.0 LITERATURE REVIEW**

### **2.1 General**

Circular jets in crossflows have attracted the attention of researchers because of their practical importance in several fields. List ( 1982 ) indicated that the earliest work on the subject of jets was by Young ( 1800 ) who recognized that the angle of expansion of turbulent jets was not a function of the jet velocity. A simple axisymmetric jet discharging into a stagnant ambient is well understood, but significant differences occur with complex turbulent shear flows when the ambient is changed to a crossflow. The earliest published work on jets in crossflow was carried out by Ruggeri et al, 1949 ( see Rajaratnam, 1976 ) who investigated jet penetration in a wind tunnel. Hodgson (1991) tabulated a comprehensive summary of the previous experimental work on jet discharges in crossflows but none of the 33 references dealt with a wall jet.

To achieve a significant degree of mixing in the immediate vicinity of the outfall, effluent discharges into the environment, especially in rivers, need to be momentum dominated and because of the shallow nature of the rivers the outfalls need to be located near the bed. Such arrangements will maximize the mixing process within the depth of the river and delay the surfacing of the discharges. Dilutions up to 50 : 1 in the initial dilution zone, have been reported when a jet diffuser is used compared to an outfall which relies solely on the river turbulence as in the case of passive plumes ( Hodgson, 1991 ).

To understand the main characteristics of a circular wall jet in crossflow, previous experimental investigations on the well understood free turbulent jets will be reviewed in this chapter. The simple axisymmetric turbulent jet discharging into a

stagnant ambient will be described and compared with a wall jet of similar conditions. This will be followed by the description of the basic components of free circular jet discharges in crossflow. The knowledge on the free jet will be used as a basis for understanding the conditions of a wall jet with similar discharges in crossflow.

## 2.2 Description of Circular Turbulent Jets

The characteristics of the circular jet in crossflow can be better understood by first describing the simple free jet issuing into a stagnant ambient and then moving the ambient as a crossflow. In this section existing experimental observations on simple axisymmetric wall jets will be discussed. This will be later applied when discussing the effects of the wall on dilution of circular jets in crossflow. Free turbulent jets discharge into a stagnant ambient with boundaries sufficiently far away, while the wall jet discharges tangentially and grows along a wall (Abramovich, 1963). It is useful to note that if the Reynolds number  $R$  of the jet, defined as  $R = U_0 d / \nu$  where  $\nu$  is the kinematic viscosity of the fluid, is greater than about 1000, the jet becomes turbulent fairly quickly (Fischer et al, 1979).

### 2.2.1 Simple Axisymmetric Jet

Consider a circular jet of diameter  $d$  and discharging with a uniform velocity  $U_0$  into a stagnant ambient. The jet is divided into two distinct regions (Fig. 2.1). The region near the jet nozzle with undiminished discharge velocity  $U_0$  is known as the potential core or flow development region. In the core, the flow is essentially potential with little or no turbulence and extends to about  $6d$  (Abraham, 1960;

Rajaratnam, 1976 ). The end of the potential flow occurs when the turbulence generated by the shear at the boundaries spreads to the axis of the jet.

The next zone, known as the fully developed flow region, occurs beyond the end of the potential core. The mean velocity  $u_m$  along the centerline decays with the axial distance  $x$ . Rajaratnam ( 1983 ) found that the velocity and concentration scales decay inversely with the distance along the jet axis and are described by the following equations:

$$\frac{u_m}{U_0} = \frac{6.13}{x/d} \quad (2.1)$$

$$\frac{C_m}{C_0} = \frac{5.34}{x/d} \quad (2.2)$$

where:

$U_0$  is the initial velocity of the jet at the nozzle

$u_m$  is the maximum jet velocity at any section

$x$  is the axial distance from the jet nozzle to that section

$d$  is the diameter of the jet nozzle

$C_0$  is the initial concentration in the jet

$C_m$  is the maximum concentration at the section considered.

The radial distributions of velocity and concentration are also known to be similar. These distributions are well described by the following equations:

$$\frac{u}{u_m} = \exp \left[ - \ln 2 \left( \frac{r}{b} \right) \right] \quad (2.3)$$

$$\frac{C}{C_m} = \exp \left[ - \ln 2 \left( \frac{r}{b_c} \right) \right] \quad (2.4)$$

where:

$u$  is the velocity at a point at a section

$r$  is the radial distance to the point from the jet axis

$b$  is the length scale ( distance to the point where  $u = 1/2 u_m$  )

$b_c$  is the length scale ( distance to the point where  $C = 1/2 C_m$  ) and

$C$  is the concentration at a point.

The variation of the length scale  $b$  used in the velocity distribution for the circular turbulent jets has been found to be a linear function of the axial distance  $x$  from the nozzle, given by:

$$b = 0.096 x \quad ( 2.5 )$$

Similarly, the growth of the concentration length scale  $b_c$  was found to be a linear function of the axial distance but with a greater slope and is given as:

$$b_c = 0.096 k x \quad ( 2.6 )$$

where  $k$  is an empirical coefficient.

The work of Rajaratnam ( 1983 ) found the diffusion coefficient ratio  $k$  to have a constant value of about 1.17 in the whole region of the developed flow.

The work of Sforza and his associates ( 1966 ) and that of Rajaratnam and Pani ( 1974 ) considered three-dimensional turbulent wall jets. The shape of the nozzles used in the studies included a square, a circle and a rectangle with an aspect ratio close to unity. Experimental observations were carried out in the fully-developed region to find out the velocity distributions and the growth of the jet both in the vertical and the lateral directions.

The results on the three-dimensional wall jet indicated that the center plane velocity distributions in the vertical direction were reasonably similar along the longitudinal distance greater than 10 times the nozzle height ( or diameter ). The classical wall jet similarity curve ( plane turbulent wall jet issuing tangentially to a smooth wall, surrounded by a stagnant ambient of the same fluid of infinite extent ) also described well the distributions of the three - dimensional jet. The results of the length scales indicated that both the vertical and the horizontal scales were linear functions of the longitudinal distance downstream of the nozzle. From the length scales, it was found that the lateral scale grows about 4 to 5 times faster than the vertical scale. The wall shear coefficient was also found to increase to a constant value beyond the downstream distance equal to 50 times the square root of the nozzle cross - sectional area. By neglecting the shear on the wall, these authors considered the problem could be analyzed in a manner similar to that of three-dimensional free jets.

### **2.2.2 Circular Jet in Crossflow: Preliminary discussion**

When a moving ambient perpendicular to the jet discharge is introduced to replace the stagnant conditions in the axisymmetric jet, the jet is described as a circular jet discharge into a crossflow. Free turbulent jet discharge in an infinite depth of the crossflow prevails when the walls ( or boundaries ) are sufficiently far away ( Abramovich, 1963 ) and do not influence the growth of the jet in the momentum dominated region.

The main characteristics of jets in crossflow are defined by considering a circular jet of diameter  $d$  discharging with an initial velocity  $U_0$  perpendicular to a moving free stream of velocity  $U$  ( Figure 2.2 ). The jet would initially penetrate at

right angles to the ambient flow but eventually be deformed by the crossflow and deflected from its original course to approximately the ambient flow direction. Rajaratnam and Gangadhariah ( 1980 ) indicated the cause of the jet deflection as the result of the pressure field exerted near the jet nozzle by the free stream as well as the entrainment of the ambient fluid. Deflected jets experience three zones of flow, as opposed to two for the simple jet.

The cone-shaped potential core forms the central region of the jet near the nozzle characterized by the shear free flow and undiminished total pressure ( Rajaratnam, 1976 ). Studies by Pratte and Baines ( 1967 ), Keffer and Baines ( 1971 ) and Rajaratnam and Gangadhariah ( 1980 ) have identified the length of the potential core in crossflows to be shorter than that of the simple jet because of the extra shear exerted by the crossflow. Accurate determination of the core length has not been achieved yet. Hodgson ( 1991 ) analyzed the measurements from the above mentioned studies and found that this length varies from 1 to 4 times the jet diameter for velocity ratios  $\alpha$  greater than 10. Other approximations have considered extrapolating backwards the centerline velocity profile on a log-log plot to the point where  $u_m = U_0$ . This method was found by Hodgson ( 1991 ) to overestimate the length when data from Keffer and Baines ( 1963 ) for velocity ratios  $\alpha = 4, 6$  and 8 were used. According to Rajaratnam ( 1976 ), the end of the potential core is located on the jet centerline for  $\alpha > 4$ . Platten and Keffer ( 1971 ) noted a downwind displacement of the core length by the crossflow for weak jets with velocity ratios  $\alpha < 2$ .

The zone after the potential core where the jet undergoes major deflection is the second flow region known as the zone of maximum deflection and the jet axis here changes orientation from the original normal direction to almost parallel with the free

stream flow . Turbulent mixing causes the outer layers of the jet to lose some of their momentum through entrainment of free stream fluid and become susceptible to the deflection of the crossflow. In this region therefore, the cross-section of the jet is deformed from the original circular to a kidney shape ( Abramovich, 1963 ), which houses two counter-rotating vortices. As the jet continues interacting with the crossflow, it entrains more ambient fluid. This results in a growth in size and strength of the vortex pair and increases the total flow of the jet. Some decay of maximum velocity and hence the concentration in this region occurs along the curvilinear axis of the jet. According to Hodgson ( 1991 ) the maximum deflection zone extends to an axial distance (  $\xi$  ) of about 15 to 20 times the jet diameter.

The third flow region is referred to as the vortex zone and occurs when the cross-section of the jet is almost completely occupied by the vortex pair. Further entrainment increases the size of the vortices and both the jet velocity and direction approach those of the ambient crossflow. Pratte and Baines ( 1967 ) and Fearn and Weston ( 1979 ) noted in their investigations the presence of the vortices at distances as near as  $x = 10 d$  and as far as  $x = 1000 d$  downstream of the jet nozzle. The strength of the vortices decrease with distance downstream of the jet.

### **2.2.3 Diffusion of Circular Jets in Crossflow**

Several investigations have been carried out examining the structure of the velocity and pressure fields of the jets in crossflow ( Sherif and Fletcher, 1989 ). Initial studies were conducted in air medium and using pitot tubes to measure the total and dynamic pressure heads in the jet. The axis of the jet was then located by the points of maximum pressure ( Jordinson, 1956 ). Similar experiments were carried out by



Gordier ( 1959 ) using water instead of air, to measure the distribution of the total pressure in the jet in a water duct. Gordier found that the results were similar to those of the air jet.

The introduction of the Hot - Wire Anemometry ( HWA ) in the early 1960's and the Laser Doppler Anemometry ( LDA ) in the mid 1970's improved the understanding of the jet discharges. Both instruments were able to measure the velocity profiles, jet axis trajectory, the turbulence and the vortex structures of the deformed jet.

Rajaratnam and Gangadhariah ( 1980 ) studied experimentally the behaviour of circular jet in crossflow for four different discharges of velocity ratios  $\alpha = 2.73, 4.52, 7.05$  and  $23$ , in a water flume. The velocity and piezometric pressure distribution in the full cross-section of the deflected jet were measured using the pitot tube. The results predicted the shape of the deformed jet, the centerline trajectory, the velocity distribution, and the mass and momentum fluxes of the jet discharges.

Photographic investigations were also used in a number of studies to locate the jet axis trajectory and jet boundaries. Gordier ( 1959 ) located the jet penetration ( outer boundary ) and the width from photographs of a deformed jet in a water flume. Pratte and Baines ( 1967 ) used photographs to locate the jet axis trajectory, the width and thickness of a jet marked by oil aerosol discharging in an air crossflow. Similar photographic studies were carried out by Crowe and Riechbieter ( 1967 ) using smoke, while Margason ( 1968 ) used water vapour for the observations. Wright ( 1977 ) photographed extensively 60 different deflected jet discharges of dye for the velocity ratio  $\alpha$  between  $0.8$  and  $116$  for a downstream distance extending to a maximum of  $x / d = 113$ . Wright considered both the buoyant and non-buoyant jets in uniform and stratified crossflow and used his photographic trajectory plots to define the distinct

flow regimes which occurred in the deflected jet. Wright also defined a momentum length scale  $l_m = M^{1/2} / U$  as a criteria for separating the flow regimes.

#### 2.2.4 Dilution of Circular Jets in Crossflow

Investigations of dilution characteristics of circular jets in crossflow are not as numerous as the studies of the diffusion. Studies using temperature and other conservative tracers have added significant knowledge to the understanding of dilution of turbulent jet discharges. The following section summarizes the published experimental studies on dilution of jets in crossflow.

Patrick ( 1967 ) investigated both the velocity and concentration distributions of jet discharges in crossflow using nitrous oxide (  $\text{NO}_2$  ) as a tracer. The experiments were carried out in an air medium for 23 different jet nozzle discharges and velocity ratio  $\alpha$  between 8.5 and 54. Sampling was carried out using the pitot tube. The results indicated that the jet centerline dilution was a function of the axial distance (  $\xi$  ) of the jet. Centerline dilutions of up to 100 : 1 for the downstream distance of  $\xi / d = 50$  were reported.

The work of Fan ( 1967 ) considered the dilution of buoyant jet discharges in crossflow. The investigation was carried out in a water medium for 10 different discharges of salt solution through a jet orifice. The velocity ratios  $\alpha$  were between 4 and 16, and the densimetric Froude number  $F_\rho$  between 10 and 80. Crossflow simulation was done by towing the orifice. Concentration distributions within the flow field were determined using a conductivity meter or probe for downstream distances upto  $x / d = 250$ . Fan concluded from his results that the enhanced mixing was due to the self-generated turbulence of the jet.

Ramsey and Goldstein ( 1971 ) investigated the distribution of temperature for weak air jet discharges in crossflow, and velocity ratios  $\alpha = 0.1, 0.5, 1.0$  and  $2.0$ . They used both the hot-wire anemometry and a thermocouple to measure the temperature profiles. Their measurements covered a downstream distance of  $x / d = 10$ . The results indicated that the weak jets (  $\alpha = 0.1$  and  $0.5$  ) remained attached to the wall, while the stronger jets (  $\alpha = 1$  and  $2$  ) were clearly separated from the wall. Similar investigations were carried out by Kamotani and Greber ( 1972 ) for high velocity ratios,  $\alpha = 3.9$  and  $7.7$ . Their results indicated that the vortex structure was not established for the weaker jet discharge (  $\alpha = 3.9$  ), while the stronger jet discharge (  $\alpha = 7.7$  ) had a developed twin vortex structure typical of jet discharges in crossflow. The decay of the centreline temperature was found to be a function of the axial distance (  $\xi$  ). Initially the temperature decay was slower for the stronger jet but the dilution was found to be about the same beyond an axial distance of  $\xi / d = 70$ .

Chu and Goldberg ( 1974 ) carried out both the theoretical and experimental investigation on the location and dilution of buoyant jet discharges in crossflow. The experiments were carried out in a water medium for 8 different jet discharges of velocity ratios  $\alpha$  between  $6.3$  and  $44$ . Dyed salt solution was used as a tracer and both the measurements of salinity and the photography were used to interpret the results. Their conclusion indicated that the jet dilution was a function of the downstream distance and described by the two-thirds power law. It will be realized later the two-third power normally describes the dilution of the momentum dominated region of pure jets. The relatively high velocity ratios (  $\alpha > 3.5$  ) used by the authors in most of their tests explains the similarity of their results to those expected for the non-buoyant jets.

Wright ( 1977 ) investigated extensively the whole range of buoyant and non-buoyant jets discharging into uniform and stratified crossflows. Wright used dimensional considerations, photographic analysis and dilution measurements using Rhodamine B Extra dye as a tracer. The jet source was towed at a constant velocity discharging into a stagnant ambient in a flume. Concentration measurements were carried out for 20 non-buoyant jet discharges into unstratified crossflows and velocity ratios  $\alpha$  between 20 and 35. Relative concentration of samples along the jet trajectory were analyzed using a G.K. Turner Associates Model 111 fluorometer. Dilution analysis were carried out from measurements of the maximum concentrations along the jet centerline. The experimental results agreed with the theoretical formulations and indicated that distinct transitions occur between the various flow regimes of the jet. For the non-buoyant jets discharging into a uniform crossflow, Wright used both the dilution and trajectory plots to define the two slopes of the momentum dominated regions of the jet. The region described by the one-half slope near the jet nozzle was defined as the momentum dominated near field ( MDNF ) and the next region described by the two-thirds slope as the momentum dominated far field ( MDFF ). The data also indicated that the concentration centerline was located about 20 % higher than the centerline derived from the photographic analysis.

Hodgson and Rajaratnam ( 1992 ) conducted dilution studies in the laboratory with a similar approach to that of Wright ( 1977 ) and compared these results with some investigations in rivers. He considered flow velocity ratios  $\alpha$  between 1.46 and 10.55, and depth ratios between 15.7 and 41.3. The investigations were meant to simulate more closely the actual field situations for downstream distances in the range  $1.1 < \alpha x / d < 990$ . The results were well represented by a power law relation.

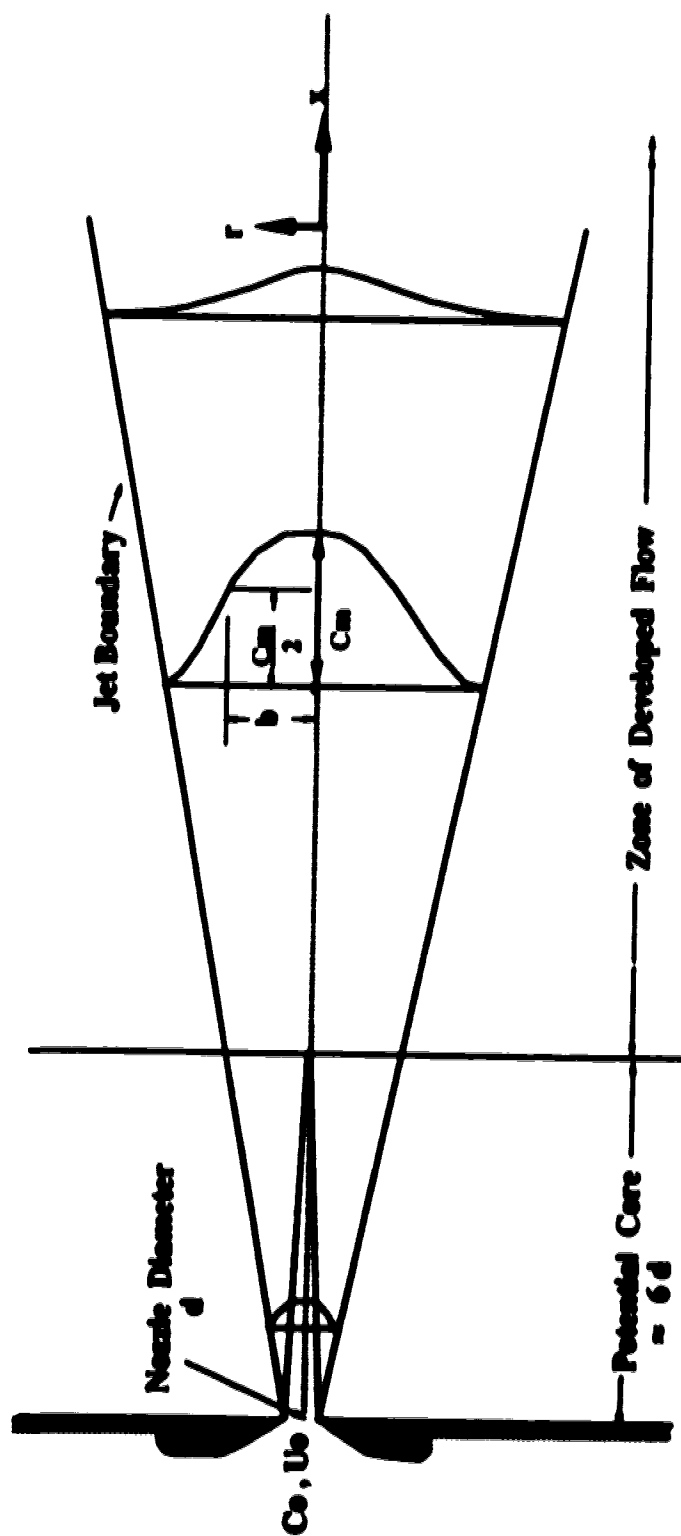


Fig. 2.1 Turbulent Circular Jet Discharge into a Stagnant Ambient

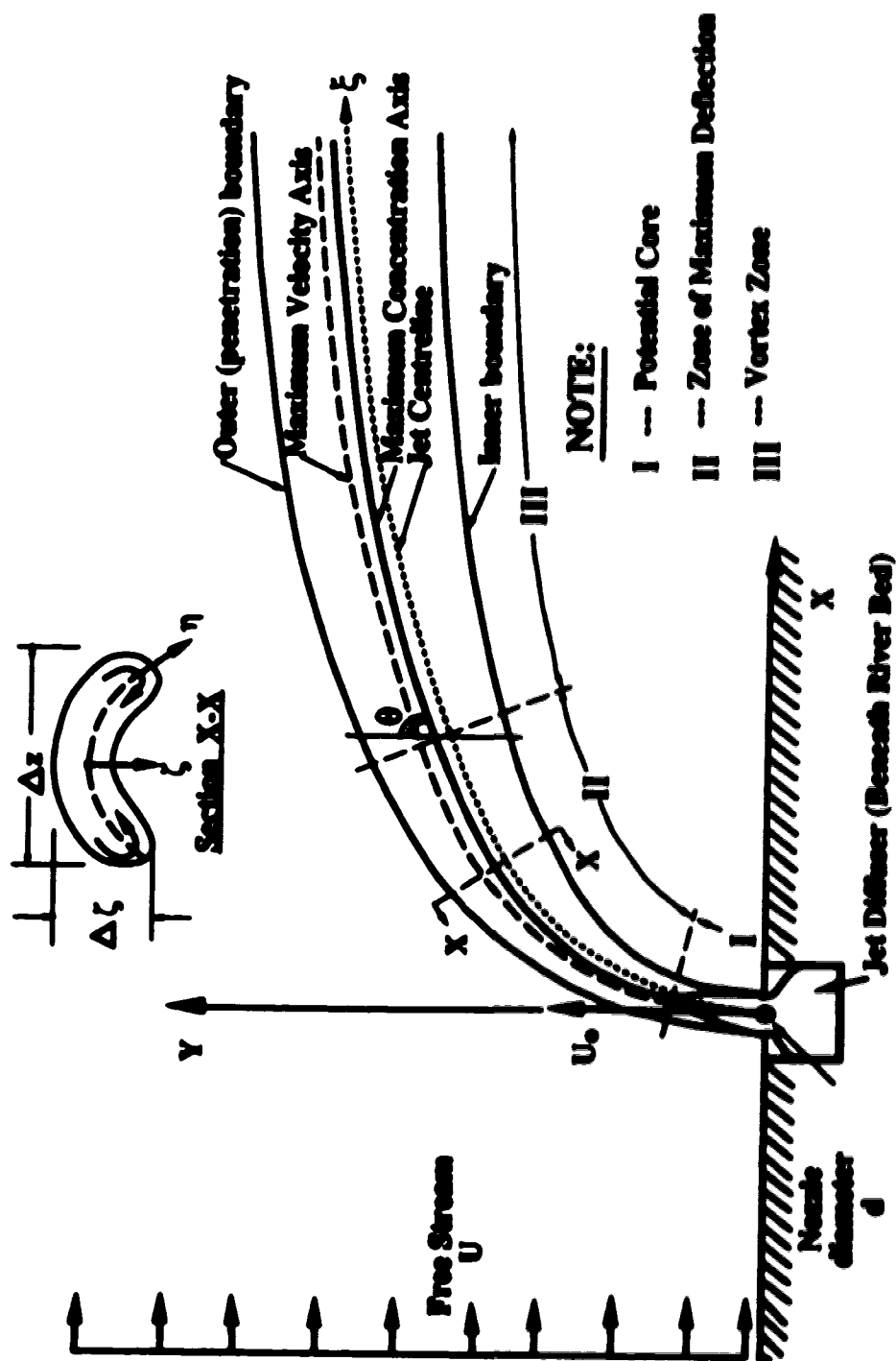


Fig. 2.2. Schematic Sketch of Turbulent Circular Jet Discharge in Crossflow (after Rajaratnam, 1976)

### **3.0 LABORATORY INVESTIGATIONS**

#### **3.1 General**

The laboratory study on the dilution of a wall jet in crossflows was carried out to simulate the prototype river conditions by introducing a freestream flow in the channel ( here referred to as crossflow ) with a flow depth (  $D$  ) to jet diameter (  $d$  ) ratio of similar magnitude to the actual field situation. The bed of the channel would not represent the true conditions prevailing in the river but assumed the effect is minimal on the model experimental results. The channel flow was from the laboratory sump water refilled from the regular city water. Temperatures remained constant at the ambient laboratory conditions of about  $20 ( \pm 0.5 )$  degrees Celsius throughout the experimental work.

Detailed discussion of the experimental procedure is presented in the following sections under three categories, namely: the experimental arrangement, calibration of the fluorometer and the sampling procedure.

#### **3.2 Experimental Arrangement**

##### **3.2.1 The Flume**

The experiments were carried out in a rectangular channel 0.91 m wide, 0.77 m deep and 36.5 m long ( Plate 3.1 ) in the University of Alberta's T. Blench Hydraulics Laboratory. The channel is fitted with an adjustable slope mechanism, and the freestream flow was provided by a pump located in the laboratory sump. The discharge was measured using an inline magnetic flow meter with a digital measuring

scale ( reading to 2 decimal points ) and calibrated for 1.0 VC unit to be equivalent to  $0.015 \text{ m}^3/\text{s}$ . The mean velocity in the channel section of the experiment was calculated from the measured discharge in the flume and the section flow area. The average velocity was also measured for 3 locations across the flume at distances of 80 mm, 220 mm and 450 mm ( center of the flume ) from the side wall using Prandtl-type pitot-static tube and transducers. The velocity profiles shown in Figure 3.1 clearly indicate that the wall effect extends as far as 80 mm into the freestream flow.

### **3.2.2 Jet Arrangement**

Well-designed nozzles of diameters equal to 6.35 mm and 12.7 mm were used to produce the circular wall jets and both were located at a distance of about ( 22.0 m ) downstream of the flume entrance. The nozzles were installed flush with the side wall of the flume with the bottom of the internal diameter at about the same level as the channel bed ( Plate 3.2 ). The jet flows were generated by a 1/3 horsepower Jacuzzi model SP125/B pump fitted with a bypass line and connected to a constant head tank by a nalgene 800 tubing of 25.4 mm ( 1-inch ID ) internal diameter and 3 mm wall thickness. The Rhodamine dye used as a tracer in the present study was mixed in a 900 litres tank connected to the pumping unit near its base, and received both the bypass line flow and the overflow from the head tank. Water used for mixing the dye was pumped from the same sump which provided the freestream flow.

The flow rate through the jet nozzle was measured by a calibrated Fischer rotameter rated in litres per minute ( Plate 3.3 ) and controlled by two gate valves, one on the bypass line and the other on the line connecting to the constant head tank and



the jet nozzle. The calibration of the rotameter was also checked by volumetric measurement.

The velocity at the jet nozzle was calculated from the rotameter discharge reading and the jet nozzle diameter. Velocity at the nozzle was maintained constant by the provision of the constant head tank on the flow line with an overflow arrangement.

### 3.3 Calibration of the Fluorometer

The analysis of the fluid samples was carried out in a Turner model 10 portable fluorometer ( Plate 3.4 ) by manually filling the 35 ml cuvette or a clear test tube, with the sample from each bottle container at a time. The fluorometer output reading is on a double scale from 0 to 10 on the upper scale or 0 to 3.16 on the lower scale and both scales are related to each other by a factor of 3.16. For convenience with the decimal points, the upper scale was used throughout the present work. The fluorometer was calibrated using diluted standards of the Rhodamine dye ( original market concentration of 20 % by weight of the dye and specific gravity of 1.19 ) solution corresponding to its range of 0.01 ppb to 55 ppb in order to derive the relation for interpreting the relative concentrations of the fluorescent dye in the sampled fluid. Standardized dye concentrations were plotted against the fluorometer output scale reading and the calibration indicated that the dye fluorescence is a linear function of the tracer concentration ( Figure 3.2 ). The calibration best fit line (  $r^2 = 0.999$  ) was expressed by the following relation:

$$C \text{ (ppb)} = \frac{5.56 \times \text{Scale Reading (0 - 10)}}{\text{Multiplier} \times \text{Range}} \quad (3.1)$$

The multiplier was either 1 or 100, while the range of sensitivity was 1, 3.16, 10 or 31.6 and the larger figures indicate low concentration levels of the tracer in the sampled fluid. The multiplier of 1 was constantly used throughout the analysis but the range was varied through all the sensitivities depending on the tracer concentration. The concentrations higher than the maximum reading of the fluorometer could be analyzed by making standard solutions of the dye. The initial concentration ( $C_0$ ) at the jet nozzle ranged from about 15 ppb to 20 ppb depending on the initial mixing of the dye in the 900 litres tank for the different jet discharges.

Consistency of the fluorometer calibration was checked by taking the readings of the standard solutions before and after the analysis of the samples. It was also necessary to turn on the fluorometer for about 20 minutes before carrying out the analysis of the fluid samples. The fluorometer is capable of measuring the fluorescence intensity of any chemical solution by simply installing the right kind of filter necessary for the particular solution and carrying out similar calibration procedure for the concentrations. The fluorometer could also be equipped with a continuous flow - through sampling procedure when using a single sampling tube.

### **3.4 Sampling Procedure**

#### **3.4.1 Sampling Rake Arrangement**

Assessment of the jet dilution in the crossflow was done by carrying out the concentration measurements using Rhodamine WT as a tracer in the jet fluid. Fluid samples were withdrawn by means of a rake comprising a minimum of 7 sampling

probes, each of 3.175 mm ( 1/8-inch OD ) and a wall thickness of 0.9 mm, aligned with the  $\xi$ -axis ( centerline trajectory ) of the jet. The  $\xi$ -axis at a section was determined from the photographic trajectory plots of the centerline ( Appendix III ) and by the injection of the food color dye prior to sampling the tracer dye. The angle of the jet deflection from its original perpendicular direction was measured by a protractor, attached to the top of the sampling rake.

The sampling rake shown in Plate 3.5 was made up of L-shaped brass tubes set at a spacing of 30 mm and held in position by a wooden bracket which was kept out of the water surface at all times during the experiments. The spacing between the tubes was adjustable depending on the position of the sampling and the width of the jet. A minimum of 10 mm spacing was used near the jet nozzle and a maximum of 40 mm was used in the region away from the nozzle, where the lateral concentration gradients were small. The probes were set to withdraw the samples at the same level in the transverse  $\eta$ -axis simultaneously, starting from the bed level and the first tube was sampling near the inner boundary of the jet.

The tracer samples were collected for different levels at a spacing of 5 mm in the  $z$ -axis until the level which marks the outer boundary of the jet growth in the vertical elevation. To be able to sample across the jet in the  $\eta$ -axis, a second set of sampling was carried out with the last probe sampling the outer boundary ( penetration axis ) of the jet and the other tubes located between the positions of the first setting. The procedure followed in the first setting is repeated during the second setting for all the levels. It was assumed that steady state flow conditions prevailed both in the jet nozzle and the channel discharges and therefore sampling at any particular location was not time dependent. The samples for the background channel flow were withdrawn concurrently by a similar probe located upstream but near the jet nozzle.

A siphoning system of vinyl nalgene premium tubings of 3.175 mm (1/8-inch ID) internal diameter and 2.0 m long was used to discharge the tracer samples and collect in 60 ml opaque plastic bottles marked with the positions of the sampling probes. The collection bottles were set up and contained in a wooden sample rack ( see Plate 3.6 ) positioned at an appropriate level to create a sampling velocity at the probe nozzle approximately equal to the main channel flow velocity and a continuous free flow in the tubings. All sample bottles were filled within the same amount of time but sufficient duration was allowed to eliminate the adsorption or desorption of the dye onto the delivery tubings. To minimize the loss of the dye fluorescence due to light, the samples were kept in a dark sample box until the concentration analysis of all the samples was completed.

### **3.4.2 Preliminary Investigations**

The preliminary runs were carried out while developing the operational procedures of the experimental arrangements by visual observations of the jet trajectories and measuring the local velocity profiles of the flow in the flume for comparison with the mean value used in the present study. Figure ( 3.2 ) gives the profiles for the 3 locations across the flume at the section of the jet nozzle ( mean channel flow velocity  $U = 0.60$  m/s ) which indicate that the mean velocity used is satisfactory in the region of the flow where the jet would be growing.

The centerline trajectory profiles of the various jet discharges were visually observed with the help of the colored dye and compared with the co-ordinate locations earlier obtained by Diebel and Rajaratnam ( 1980 ) for a similar circular wall jet

( Appendix III ). Adjustments of the centerline axis were made independently for each jet discharge where necessary during the actual investigations.

In addition to the observations in the flume, the jet discharge was timed to empty the 900 litres tank in order to evaluate the length of the tracer sampling time before refilling the tank. During this process the fluctuation of the dye concentration in the tank was observed to be negligible and assumed constant ( as the initial nozzle concentration,  $C_0$  ) during the actual sampling. It was found that the dye solution in the tank was only enough to carry out sampling for one section of the jet at a time ( running for about 3 hours ). For every set of sampling it was found that the initial jet nozzle concentration depends on the amount of the dye mixed in the tank and therefore not necessarily constant for the different sections of the jet. To unify a steady state condition of the jet for all the sections investigated, the concentrations were considered with reference to the initial nozzle value ( i.e.  $C / C_0$  ).

### 3.4.3 Test Series

The present study involved a total of 9 experiments, including five jet discharges (  $\alpha = 2, 4, 6, 8$  and  $12$  ), two jet nozzles of diameters (  $d$  )  $6.35$  mm and  $12.7$  mm, and three flow depth ratios (  $D / d$  ) of  $20$ ,  $10$  and  $5$ . The summary of the conditions investigated are given in Table 3.1.

Sampling procedure of the tracer concentration began with making standard solutions of the Rhodamine dye ( original market concentration is  $20\%$  by weight ). A standardized working solution of  $1.0 \times 10^5$  ppb ( parts-per-billion ) was made from the original solution and kept in a dark  $4$  litre bottle for use throughout the experiments. For every experiment, about  $20 - 30$  ml of the standard solution was

withdrawn with the help of a pipette and mixed thoroughly in the 900 litres tank. Tracer mixture in the tank was checked for uniformity by measuring the concentrations at different levels ( surface, center and bottom ) of the tank. A constant value of the concentration passing through the bypass line of the pumping unit and the overflow line of the constant head tank was used as the initial jet nozzle concentration (  $C_0$  ) because these flow lines were connected to the nozzle. The nozzle concentration was also checked after every sampling for any fluctuations which might have occurred. Also the temperature of the dye mixture was recorded before and after completing sampling each section of the jet. While the dye mixing was being carried out, a constant discharge was established in the flume.

The movement of the sampling rake perpendicular to the jet axis along the  $\eta$ -axis was restricted because errors could be introduced in the angular shift. The setting therefore was limited to two positions aligned with the centerline axis located by the jet deflection angle (  $\theta$  ) measured from the normal direction to the channel flow. For every setting the parameters noted were; the centerline axis co-ordinates (  $x, y_c$  ) at the section, the jet deflection angle (  $\theta$  ) and the sampling probe number which locates the centerline of the jet.

The sampling rack containing the bottles for collecting the tracer samples was positioned to determine the discharge velocity of the samples. This was carried out by calculating the discharge velocity (  $u_s$  ) from the time taken to fill the 60 ml bottles and dividing the discharge by the cross - sectional area (  $a$  ) of the siphoning delivery tube ( i.e.  $u_s = 60 \text{ ml} \cdot 1 / \text{time} \cdot 1 / a$  ). Repositioning was carried out until the velocity  $u_s$  was approximately in the range of the crossflow velocity  $U$  and the siphon system was free flowing without the interference of the bubbles in the tubings. This procedure was necessary to avoid the sampling probe acting as a sink in the

streamflow or causing obstruction to the tracer discharge. Flushing of the bubbles was carried out whenever they were found.

The jet discharge was allowed to stabilize once all the settings were done before collecting the samples. Sampling was carried out at elevation spacing of 5 mm ( z - axis ) over the whole jet region in order to minimize the chances of missing the peak concentration ( a characteristic maximum ) of the jet. The samples were analyzed manually in the fluorometer and the concentration results were corrected for the ambient flow fluorescence which fluctuated between 0.05 - 0.10 ppb, depending on the amount of fresh water fed into the sump.

#### **3.4.4 Error Estimation**

The most critical error evaluation was carried out for the concentration measurements using the fluorometer. Significant errors could occur, especially for low values of concentration because the lowest possible reading of the fluorometer scale was 0.05 units when manually operated. The analysis of the standard error introduced by the calibration was carried out using 13 observations of the standard solutions of Rhodamine ( diluted to known concentrations with distilled water ). The calibration data were compared with the scale reading and the data given in Table 3.2 indicate that the fluorometer scale reading introduces a standard error of 0.01 units ( equivalent to 0.002 ppb ). This result compared to the lowest recorded reading of 0.5 units of the fluorometer's upper scale gave an error of about 2 % of the tracer concentration. For a 50 : 1 dilution of the tracer, the error introduced in the concentration measurements was less than 1 %. Manual operation of the fluorometer was used and hence resulted in minimal errors compared to those obtained when the

automatic mode was in operation. Concentration errors due to desorption, adsorption, the bubbles in the tubing and the mixing process of making the standard solutions were found difficult to quantify, but may add or lower the actual concentration readings.

Other experimental errors were introduced during the measurements of the discharges, the crossflow and jet velocities and the angular measurements of the sampling probe co-ordinates. The error in the jet velocity resulted from the nozzle diameter machined to a precision of 0.025 mm and the rotameter discharge measurements with scale precision of 0.05 L/min. Linear measurements of the flume flow depth and the sampling spacing were carried out using the scale with a precision of 0.5 mm. Table 3.3 gives a summary of the experimental errors estimated for the parameters considered.



Experiment	Jet Diameter $d$ (mm)	DD	Jet Velocity $U_0$ (m/s)	Channel Velocity $U$ (m/s)	$\alpha$ ( $U_0/U$ )	Reynolds No $\frac{U_0 d}{\nu}$
A100	6.35	20	0.53	0.26	2	3145
A200	6.35	20	2.4	0.59	4	14243
A300	6.35	20	2.6	0.43	6	15430
A400	6.35	20	2.9	0.36	8	17210
A500	6.35	20	3.42	0.285	12	20296
B100	12.7	20	0.86	0.143	6	10207
B200	12.7	10	0.78	0.13	6	9258
B300	12.7	5	1.57	0.26	6	18635
B400	12.7	20	0.86	0.07	12	10207

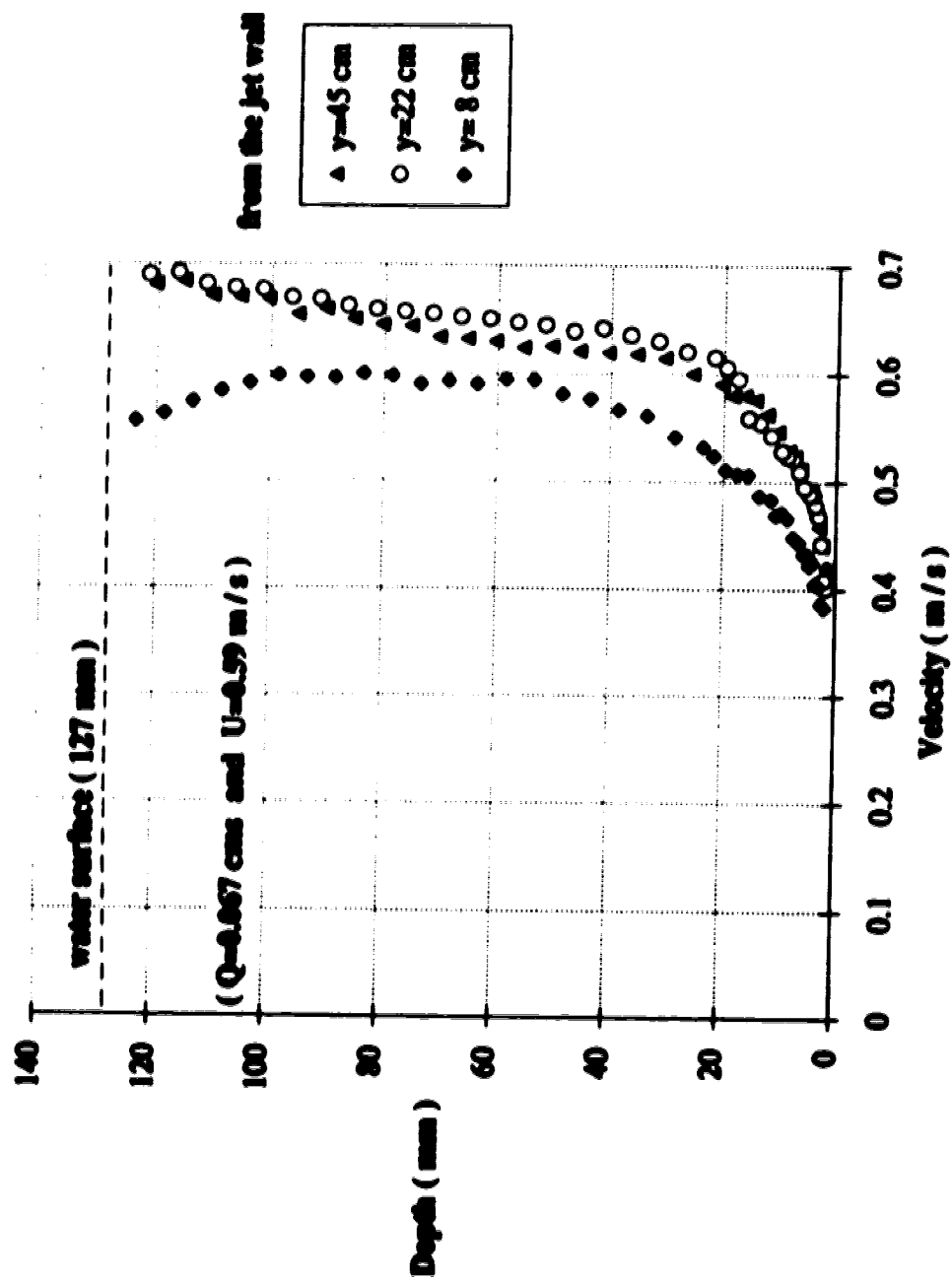
**Table 3.1 Details of Experiments of Turbulent Circular Wall Jet in Crossflow**

Standard Solution ( ppb ) ①	Scale Reading ( Upper ) ②	Calibration ( Equation ) ③	Difference ( 2 - 3 ) ④
50	8.9	8.962	-0.062
45	8.1	8.064	0.036
40	7.2	7.166	0.034
35	6.3	6.268	0.032
30	5.35	5.370	-0.020
25	4.5	4.472	0.028
20	3.5	3.574	-0.074
15	2.7	2.676	0.024
10	1.8	1.778	0.022
8	1.4	1.419	-0.019
6	1.05	1.060	-0.010
4	0.7	0.700	0.000
2	0.35	0.341	0.009
<b>Note:</b> Standard Deviation = 0.036 and Standard Error = 0.01 ( of the scale reading difference )			

**Table 3.2 Fluorometer Scale Reading Error Estimation**

Measurements	Precision	Error Estimation ( $\pm$ %)
Fluorometer ( Upper Scale )	0.05	< 2
Jet Discharge (L/min)	0.05	< 5
Jet Nozzle Diameter (mm)	0.025	< 1
Channel Discharge (L/sec)	0.05	< 5
Flow Depth (mm)	0.5	< 4
Sampling Spacing (mm)	0.5	< 5
Angular Alignment (degree)	0.5	< 5

**Table 3.3 Error Estimation**



**Fig. 3.1 Velocity Profiles across the Flame**

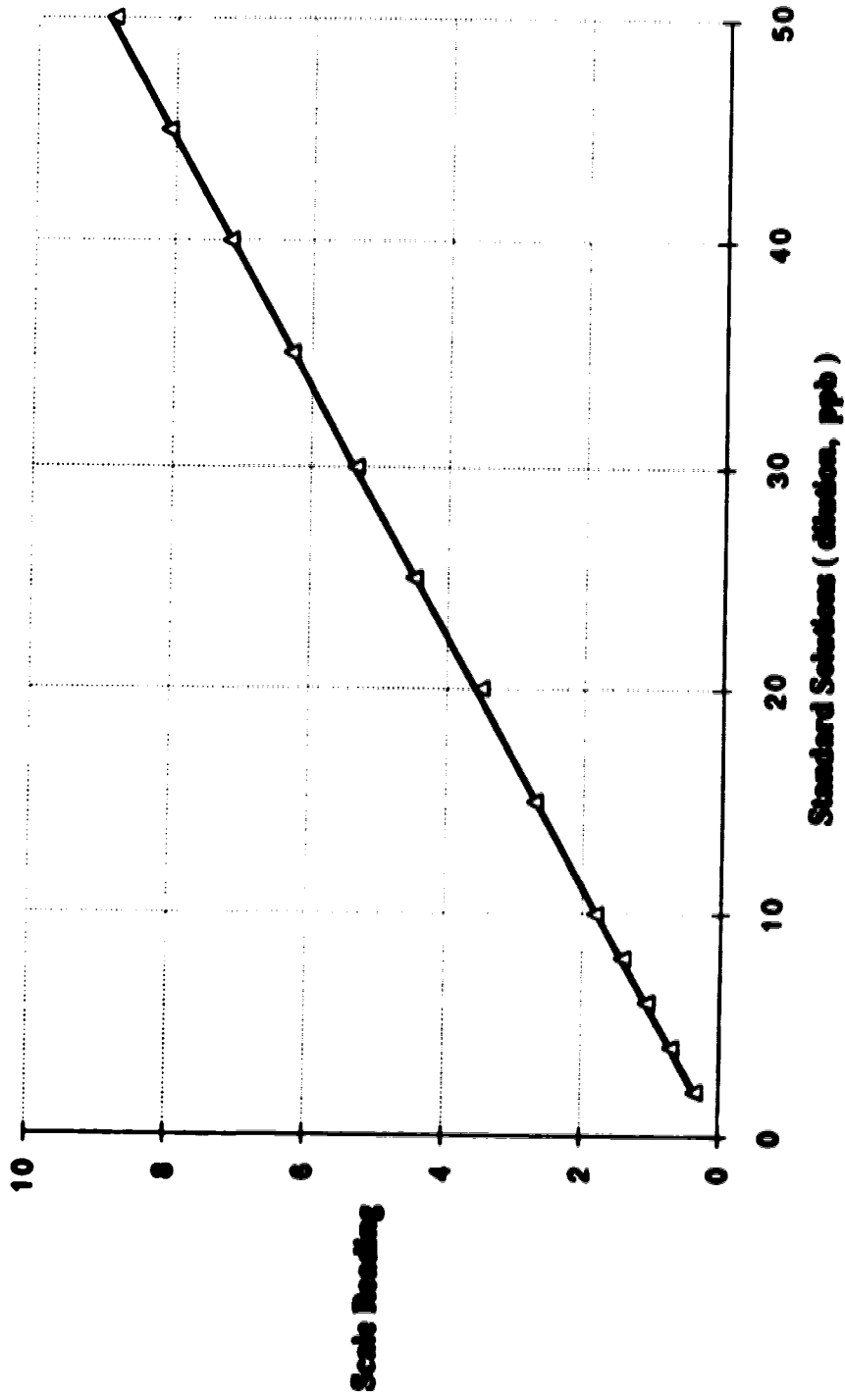
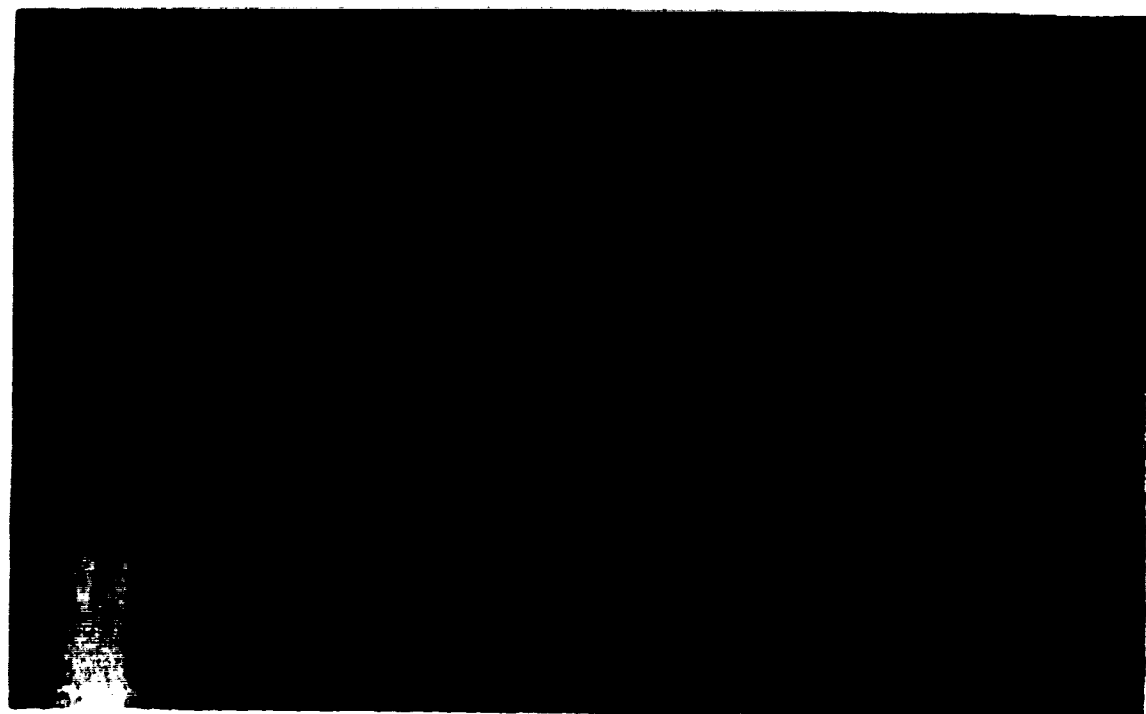


Fig. 3.2 Calibration Curve for the Fluorometer

**(a) Side View**

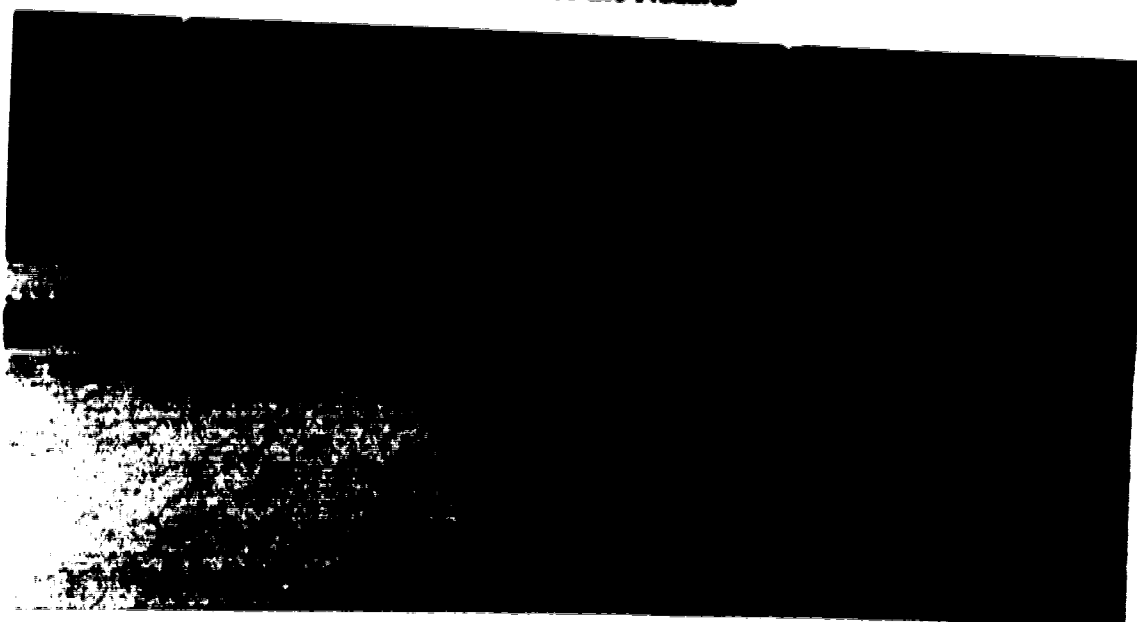


**(b) Sampling Position**



**Plate 3.1 Flame Arrangement**

(a) Location of the Nozzles



(b) Diffusion of the Jet:  $\alpha = 12$ ,  $\frac{D}{d} = 20$  and  $d = 6.35$  mm

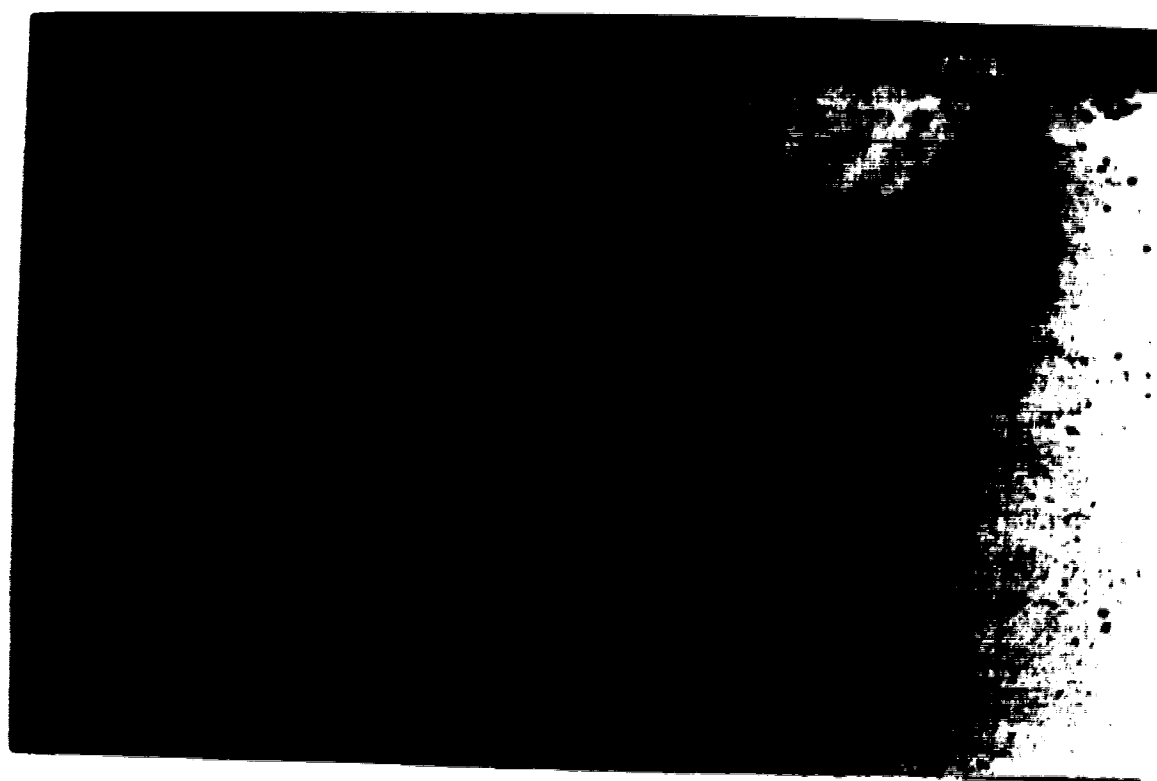
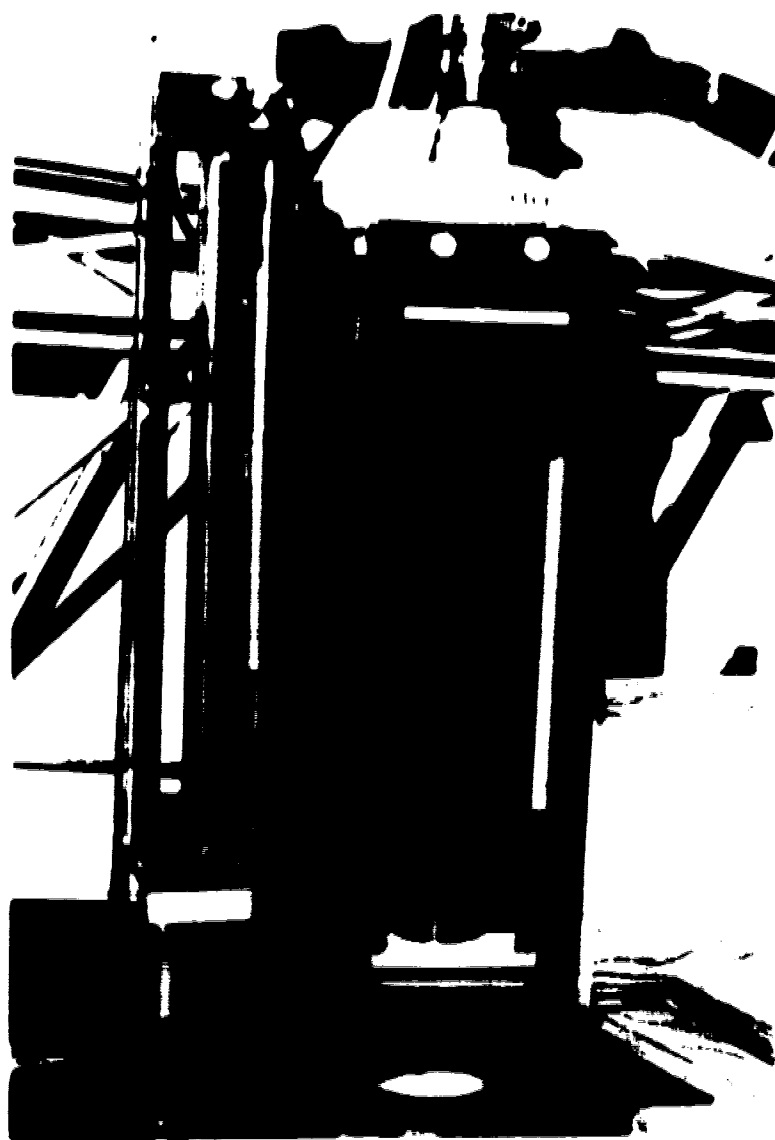
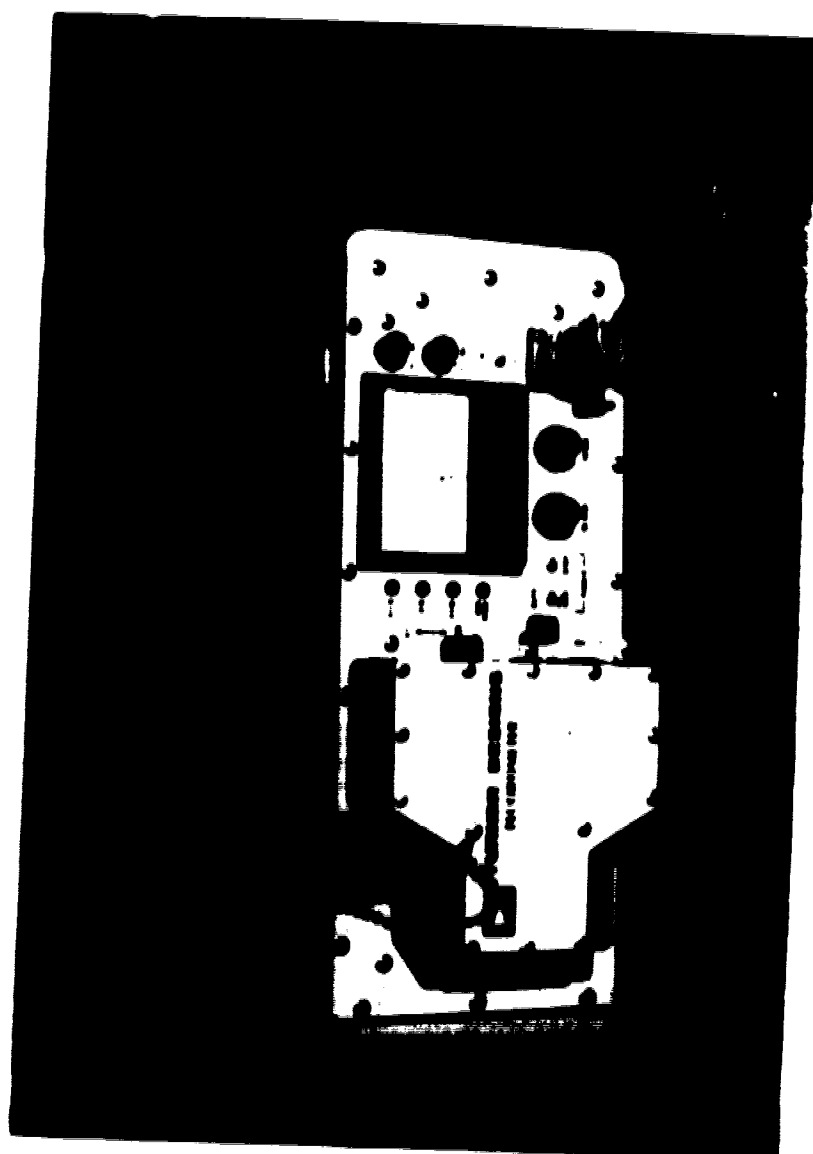


Plate 3.2 Jet Nozzle Arrangement



**Plate 3.3 Rotameter**





**Photo 3.4 Turner Model 10 Fluorometer**

**( a ) Sampling Position in the Flame**



**( b ) Sampling Probes Arrangement**



**Plate 3.5 Sampling Probe**

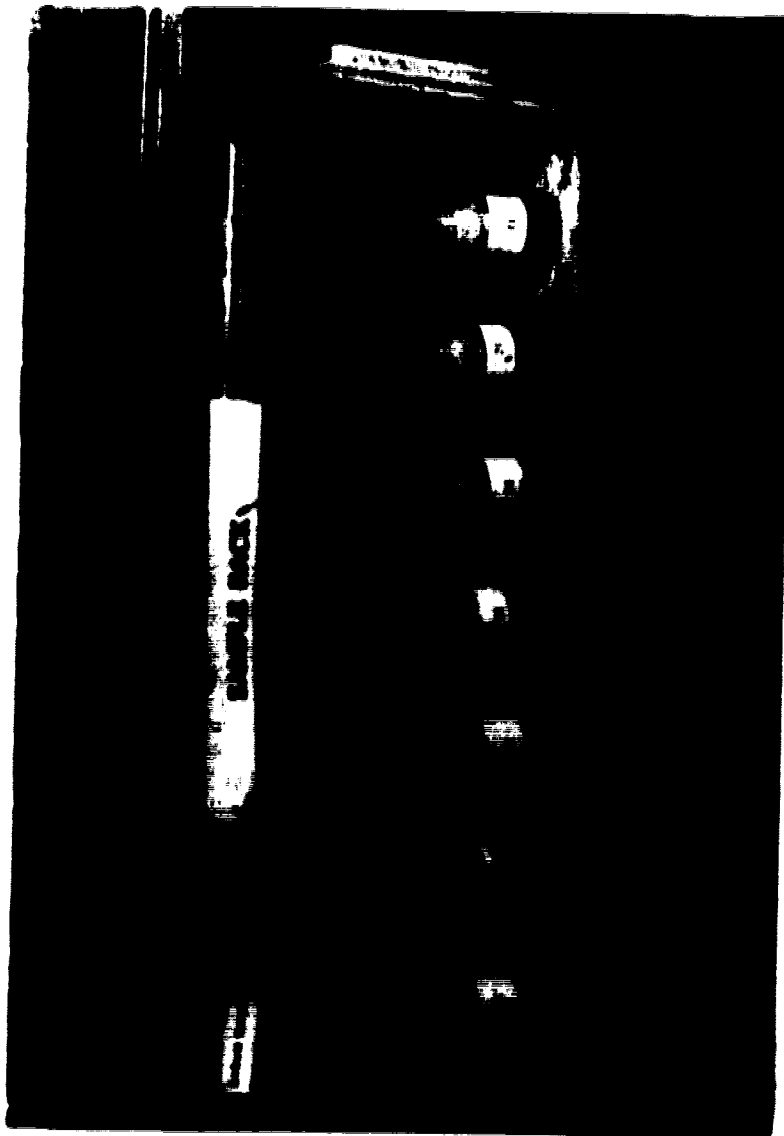


Plate 3.6 Sampling Rack (showing 60 ml bottles and delivery tubes )

## **4.0 EXPERIMENTAL RESULTS AND ANALYSIS**

### **4.1 General**

Interpretation of the concentration results in the following sections follows the objectives of identifying the main characteristics of dilution of circular wall jets in crossflow and comparing with those of the free jets.

The dilution of circular wall jet in crossflow is a complex three-dimensional problem and the present analysis considers the maximum concentration ( or minimum dilution ) to characterize the dilution problem. Since no published investigations exist on this problem, the present results are compared with those on dilution of the free circular jet ( Wright, 1977; and Hodgson and Rajaratnam, 1992 ). A generalized form of the results is suggested for practical purposes for predicting the minimum dilution (  $C_o / C_m$  ) along the non-dimensional distance  $\alpha x / d$  for each of the flow regimes earlier defined as the momentum dominated near and far fields, as well as the passive plume region at the end.

The growth of the jet both in the vertical (  $z - \xi$  plane ) and the transverse (  $\eta - \xi$  plane ) directions would be assessed from the concentration profiles, by comparing the trends of the length scales along the curvilinear distance (  $\xi$  ) of the jet. In addition, the effect of changing the jet nozzle diameter (  $d$  ) and the flow depth ratio (  $D / d$  ) would be considered.

The boundary limits of the momentum dominated flow regimes identified from the earlier results of Wright ( 1977 ) and Rajaratnam and Gangadhariah ( 1980 ) would be defined. The results of the present investigation would then be categorized graphically into the momentum dominated near field, the far field and the passive plume regions.

## **4.2 Boundary Limits of the Momentum Dominated Flow Regimes**

The analysis presented in this section defines the momentum dominated flow regimes of the deflected jet in crossflows. Based on existing works, the different mixing regions would be identified first for the free circular jet and then applied to the wall jet in crossflows.

The mixing process experienced by the effluents discharged into a receiving stream, from the review of the existing literature is considered to occur in two momentum dominated regimes; the near field region ( MDNF ) where  $y_c \ll l_m$  and the far field ( MDFF ) where  $y_c \gg l_m$ . In the MDNF, the jet is displaced by the crossflow but retains its similarity to jets in a stagnant ambient whereas in the MDFF, the diffusion of the jet is affected by the moving ambient. These two regimes are generally followed by what can be termed the passive plume region ( PPR ) where the velocity excess in the jet has decayed and the mixing and dilution is due to the turbulence in the ambient. However, the boundary limits of the regions were not clearly defined and now form part of the present analysis. The work of Wright (1977) on the momentum dominated trajectories and that of Rajaratnam and Gangadhariah (1980) on circular jets in crossflow are used in the present investigation to derive the limits of the three regimes.

### **4.2.1 Momentum Dominated Near Field Regime**

The photographic observations of Wright ( 1977 ) indicate that the intersection of the 1/2 and the 1/3 slopes on the data plot of  $y_c / l_m$  against  $x / l_m$  defines the co-

ordinates of the separation point between these two regimes. The point is given by  $y_c / l_m = 1.5$  and  $x / l_m = 1.0$ , where  $l_m$  is the momentum length scale  $(= M^{1/2} / U)$  as had earlier been defined. The trajectory relation for the momentum dominated near field flow regime, from dimensional analysis is given by ( Wright, 1977 ):

$$\frac{y_c}{l_m} = C_1 \left( \frac{x}{l_m} \right)^{1/2} \quad (4.1)$$

where  $C_1$  is the proportionality constant and a function of  $\alpha$ .

Let  $x_*$  to be the  $x$  co-ordinate where MDNF ends. Rewriting the above Equation 4.1 and substituting for  $y_c / l_m$  becomes:

$$\frac{x_*}{l_m} = \frac{2.25}{C_1^2} \quad (4.2)$$

The distance downstream of the freestream flow from the jet nozzle is given in a non-dimensional form as  $\alpha x / d$  and, therefore, Equation 4.2 becomes:

$$x_* = \frac{2 \alpha d}{C_1^2} \quad (4.3)$$

The coefficient  $C_1$  is derived from the experimental data using the general Equation 4.1 and plotted against the velocity ratio  $\alpha$ . The data are described by the equation ( Hodgson and Rajaratnam, 1988 ):

$$C_1 = 2.0 \cdot \frac{2.2}{\alpha^{2/3}} \quad (4.4)$$

Therefore, a plot of  $\alpha x_* / d$  against  $\alpha$  is given in Fig. 4.1 as the end limit of the MDNF or the lower limit of the MDFF.

#### 4.2.2 Momentum Dominated Far Field Regime

Similar analysis was followed to define the upper limit of the momentum dominated far field region. The centerline trajectory relation derived by Wright ( 1977 ) for this region is given by:

$$\frac{y_c}{l_m} = C_2 \left( \frac{x}{l_m} \right)^{1/3} \quad (4.5)$$

The proportionality constant  $C_2$  is again found to be a function of  $\alpha$ . The logarithmic plot of the coefficient determined from the experimental data was given by the equation ( Hodgson and Rajaratnam, 1988 ):

$$C_2 = 0.89 \alpha^{1/6} \quad (4.6)$$

The upper boundary of the MDFF could not be determined from Wright's trajectory plot and therefore a new basis was explored to define the limit. Based on the velocity field of the flow, the end of the MDFF was assumed to occur where the excess velocity in the jet above that of the ambient falls to about 1% of the initial velocity excess given as  $(U_m - U) = 0.01 (U_0 - U)$ . From the work of Rajaratnam and Gangadhariah ( 1980 ),  $(U_m - U) / (U_0 - U) = 0.01$  occurs approximately when  $\xi / \xi_0 = 10$  where  $\xi_0$  is the length scale in the velocity correlation and defined by the axial distance of the deflected jet from the virtual origin to the end of the potential core. The length scale is a function of  $\alpha$  and fitted by the logarithmic function given by:

$$\xi_0 / d = 1.5 \alpha^{0.43} \quad (4.7)$$

Pratte and Baines ( 1967 ) plotted the centerline penetration of the deflected jet against the distances along the  $\xi$  - axis and the data were described by a straight line with the equation:

$$\frac{y_c}{\alpha d} = 1.63 \left( \frac{\xi}{\alpha d} \right)^{1/3} \quad (4.8)$$

for all the data points beyond the potential core.

Let  $\xi_f$  and  $x_f$  be the axial distance and the downstream longitudinal distance of the deflected jet respectively at the end of the MDFF. Therefore, incorporating the above assumption into Equation 4.8 and combining with Equation 4.5 results in the following relation, for the end limit of the MDFF regime:

$$x_f = 5.47 \frac{\xi_f}{C_2^3} \quad (4.9)$$

A plot of  $\alpha x_f / d$  against  $\alpha$  is given in Figure 4.1. The figure indicates the three distinct regions delineated by the Equations 4.3 and 4.9 as the momentum dominated near field regime, momentum dominated far field regime and the passive plume regime which occurs beyond the upper boundary of the far field regime.

### 4.3 Experimental Results

#### 4.3.1 Parameters Considered

Concentrations across the section of the jet were sampled on a minimum grid of 5 mm by 5 mm near the nozzle to a maximum grid of 10 mm by 10 mm on the wider section of the jet to ensure that the peak concentration point was sampled. The grid system resulted in a minimum of about 80 co-ordinate points near the jet nozzle and a maximum of about 200 co-ordinate points for the fully grown jet, of concentration measurements for one section. An average of 10 sections were



investigated for each of the 5 jet discharges covering downstream distances as far as  $x = 4000$  mm ( or a maximum of  $\alpha x / d = 5000$  ).

Two jet nozzles of diameters of 6.35 mm and 12.7 mm were used for the range of velocity ratios  $\alpha$  of 2, 4, 6, 8 and 12. The ratio of the freestream flow depth (  $D$  ) and the jet nozzle diameter (  $d$  ) was maintained constant at 20 throughout the measurements, except for  $\alpha = 6$  where cases with  $D / d = 10$  and 5 were also investigated.

#### 4.3.2 Presentation of the Results

The concentration data were corrected to eliminate the ambient fluorescence and tabulated in Appendix II. Concentration measurements in all the sections were taken perpendicular to the jet axis. A similar procedure was used by Fan ( 1967 ) while Wright ( 1977 ) and Hodgson ( 1991 ) considered vertical cross-sections ( parallel to y-axis ) for the free jet. The data for the different transverse (  $\eta - \xi$  plane ) levels are presented, with the lowest level fixed at an elevation of 1.5 mm above the bed at the axis of the sampling probe centerline while touching the bed. The schematic sketch given in Figure 4.2 defines the planes considered in the presentation of the results. The unit for the tracer concentration is parts per billion ( ppb ).

## 4.4 Analysis

### 4.4.1 Concentration Profiles

Transverse concentration profiles (  $\eta - \xi$  plane ) were plotted for all the sections investigated. Sample plots for the velocity ratio  $\alpha = 4$  at locations in the near field (  $x = 5 \text{ mm}$  ) and the far field region (  $x = 100 \text{ mm}$  and  $285 \text{ mm}$  ) are given in Fig. 4.3 ( a ) - ( c ). Observation of the plots indicates no symmetry between the profiles near the bed and those on the upper half of the jet because of the boundary layer effect. The maximum concentration (  $C_m$  ) occurs at a distance  $\delta$  measured from the bed to the elevation of maximum concentration, then decreases to a constant value of the ambient fluorescence. It was also interesting to note the shift of the concentration peak for profiles near the bed, towards the outer part of the jet, and the profiles above the level  $z = \delta$  show a shift of their peaks towards the inside boundary of the jet. The shift for profiles near the bed is a result of the low boundary layer velocity which allows greater jet penetration. The maximum concentration is not symmetrically located on the visual centerline of the jet trajectory as observed in axisymmetric jets but occurs generally on the outer half-section of the jet width.

Double peaked concentration profiles appeared for the sections investigated in the maximum deflection zone. The possible explanation could be as a result of the vortex formation which could only be further investigated by plotting the contour profiles. This has not been considered in the present study. Concentration profiles for the locations far downstream indicated complete mixing and little change occurs in the concentration gradient throughout the flow depth where the jet momentum has diminished to ambient flow conditions.

#### 4.4.2 Minimum Dilution

Dilution of the tracer concentration at a section is explored by considering its characteristic minimum value which occurs at the location of maximum concentration in the jet. Minimum dilution is therefore given by the ratio of the initial concentration ( $C_0$ ) at the jet nozzle to that of the characteristic maximum concentration ( $C_m$ ). Both the vertical and the transverse planes containing the characteristic value are considered for the similarity test and the growth of the jet half-width ( where the instantaneous concentration is one half the maximum value, or  $C = 1/2 C_m$  ) length scales. The main features of the various flow regimes would be identified by presenting the analysis based on the momentum dominated near field, momentum dominated far field and the passive plume regions.

The vertical (  $z - \xi$  plane ) concentration profiles were considered by plotting the maximum value of  $C/C_0$  against the elevation  $z$  ( mm ) for all the sections and for each of the five jet discharges as given in Figures 4.4 - 4.8. The results clearly indicate the distributions assume the wall jet shape quickly and the profiles are not symmetrical along the maximum value as expected for the simple jet. This is because the jet growth is restricted near the bed. The plots also indicate that little dilution ( less than 2 : 1 ) occurs near the jet nozzle where the jet penetrates the ambient flow with its undiminished momentum. Most of the tracer accumulated in the lower one-third of the flow depth.

Similarity of the concentration profiles was tested by plotting non-dimensional values of  $C/C_m$  against  $z/b_z$  ( where  $b_z$  is the elevation measured from the bed where  $C = 1/2 C_m$  ), for all the flow discharges. Plots for the different flow regimes are given for each of the five jet discharges in Figures 4.9 - 4.14. The plots indicate reasonably similar concentration distributions on the outer edge of the jet but

noticeable scatter exists near the bed due to the boundary layer effects. Considering the data points away from the wall ( bed ), the concentration distributions for the sections in the momentum dominated near field all collapse into a single curve with minimal scatter. The jet dominates the flow in this region and is least affected by the crossflow ambient, and therefore the mixing processes are similar to those in the simple axisymmetric jet. As similarity trend is also shown by the data in the momentum dominated far field. However, some scatter is displayed by the data points on the outside periphery of the jet. This might be due to the effects of non-uniform velocity distribution of the crossflow.

The distributions for the passive plume region show a lot of scatter over the whole depth of the flow. This indicates that the characteristics of the flow regime are different from those of the momentum dominated regimes. Some trend, however, exists for most of the data points neglecting those near the wall. The jet mixing in the region has grown to the free surface and consequently the dilution is constrained.

Concentration distributions in the transverse (  $\eta - \xi$  plane ) direction were investigated by plotting  $C / C_0$  against the lateral distance  $\eta$  measured on both sides from the axis of the maximum concentration as the origin. The plots are given in Figures 4.15 - 4.19 for each of the five jet discharges. The profiles are fairly symmetrical and can be approximated to the Gaussian distribution, especially beyond the maximum deflection zone of the jet when the profiles become more uniform. Concentration profiles for the sections at downstream distance of about  $\xi = 50 d$  show minimum dilution of about 20 : 1 for each of the jet discharges. The spread of the jet growth to the inner wall occurred faster for the weaker jet discharge of  $\alpha = 2$  because of its smaller penetration and susceptibility to deformation by the crossflow ambient compared to the relatively stronger jets of  $\alpha = 4, 6, 8$  and 12.

Similarity plots of the transverse concentration profiles were obtained by plotting  $C / C_m$  against  $\eta / b_*$  ( where the jet half-width,  $b_*$  is the transverse distance measured from the axis of the maximum tracer concentration to the position where concentration is one-half the maximum value, or  $C = 1/2 C_m$  ). The plots for the momentum dominated regime are presented in Figures 4.19 - 4.24 for each of the five jet discharges and the combined distributions given in Figure 4.25. The distributions indicate similarity for the momentum dominated flow regimes. Limited scatter occurs for data points sampled near the inner wall boundary, which is expected because of the uneven distribution of the freestream velocity near the walls ( see cross-section velocity distributions, Figure 3.1 ).

Concentration distributions for the passive plume region were not included because the jet half-width,  $b_*$  could not be obtained due to a near uniform concentration profile across the jet flow in the region. This further supports the differences of the passive plume region from those dominated by the jet.

Next we study the decay of the maximum concentration (  $C_m$  ) along the downstream distance  $x$  by considering the minimum dilution ratio (  $C_o / C_m$  ). Patrick ( 1967 ) expressed the dilution ratio empirically as a function of the curvilinear distance (  $\xi$  ) of the deflected jet. Wright ( 1977 ) used dimensional considerations to define the dilution as proportional to the vertical distance (  $y_c$  ) of the centerline of the jet. For practical purposes and the convenience of measuring the downstream distance  $x$ , Hodgson and Rajaratnam ( 1992 ) reduced the dilution expression given by Wright to be a function of  $\alpha x / d$ . Similar consideration is adopted for the present analysis and the results compared to those of the free jet ( Wright, 1977; Hodgson and Rajaratnam, 1992 ) for the momentum dominated regions.

The power law form of minimum dilution given by Patrick ( 1967 ) is reduced with the help of the logarithms into a simple correlation with the downstream distance  $x$  . The choice of using the downstream distance  $x$  is however limited in the field application where river flow goes through a meandering reach and therefore prior knowledge of the river reach is necessary to ensure sufficient length of the initial dilution zone is available before locating the outfall. In the present investigation plots of the minimum dilution (  $C_0 / C_m$  ) against the downstream non-dimensional distance (  $\alpha x / d$  ) are given on the double-logarithmic scale for each of the jet discharges investigated in Figures 4.26 - 32 which cover the investigated range of  $\alpha x / d$  from 2.0 to 5000. The data indicate a general trend for the characteristic dilution and is fitted by two slopes of  $1/2$  and  $2/3$ , respectively. For a free jet in a crossflow, according to Wright (1977 ), the two flow regimes represent the momentum dominated near field ( MDNF ) and the momentum dominated far field ( MDFF ) regions of a circular jet in crossflow. The present consideration of a circular wall jet in crossflow indicates similar slope trends and, therefore, similar flow regimes prevail. The effect of the wall ( bed ) on the level of dilution would be assessed by comparing the two forms of the jet. The most significant observation of the two slopes is the transition limit. Based on the criteria earlier defined for the limits of the MDNF, MDFF and the PPR regions given in Figure 4.1, the transition for the slopes occur within 2 orders of magnitude (  $\alpha x / d < 100$  ) for the jet discharges with the velocity ratios  $\alpha = 2$  and 4 and fairly close to the criteria used. However, the transitions for the stronger jet discharges of velocity ratios  $\alpha = 6, 8$  and 12 are shifted more downstream and occur between the distance range of  $100 < \alpha x / d < 1000$ . This results suggest stronger wall jet flows behave as though the near field regimes are longer than those of the corresponding free jets. The extended length of the near field regime may be due to the underestimated crossflow velocity near the bed which is less than the mean

value used. For all the discharges considered, the plots indicate that dilutions less than 2 : 1 are generally non-linear and occur in the vicinity of the outfall ( $\alpha x / d < 10$ ).

The weakest jet, ( $\alpha = 2$ ) shows a more superior dilution as compared to the other jet discharges and also higher than Wright's near field ( $1/2$  slope). Dilutions of between 10 : 1 and 20 : 1, normally recommended within the vicinity of a jet diffuser is achieved by the jet discharge for  $\alpha x / d < 100$  and dilution of upto 100 : 1 occurs for  $\alpha x / d < 1000$ . The model for Hodgson (1991) achieved a maximum dilution of 50 : 1 at a downstream distance of  $\alpha x / d = 900$ , which extended only through the range for the initial dilution (or mixing) zone.

The jet discharge with velocity ratio  $\alpha = 4$  had similar range of dilutions with those of  $\alpha = 2$ . Dilutions of 10 : 1 upto 20 : 1 were achieved within the downstream distances of  $100 < \alpha x / d < 200$ . The initial dilution zone requirement of dilution of 50 : 1 was achieved by the jet discharge at a distance of about  $\alpha x / d = 700$ . The other jet discharges ( $\alpha = 6, 8$  and 12) indicated low dilutions ranging generally between 30 : 1 and 35 : 1 within downstream distances  $\alpha x / d < 1000$ .

Effect of the flow depth ratios ( $D / d$ ) on the dilution was also investigated by considering  $D / d = 10$  and 5 for  $\alpha = 6$ . The results are given in Figures 4.28 (b) and (c). For  $D / d = 10$ , the results for the momentum dominated near field compares well with those of Wright's equation and extends to a downstream distance of about  $\alpha x / d = 400$  for dilutions of approximately 20 : 1. The same jet discharge and that of  $D / d = 20$  fitted similarly well for the near field data for a downstream distance of about  $\alpha x / d = 300$  and dilutions of upto about 20 : 1. Further decrease of the flow depth ratio to  $D / d = 5$ , resulted in significant effects on the dilution because of the surfacing of the jet. The dilutions presented graphically in

Figure 4.28 ( c ) assumed an almost constant value of about  $C_o / C_m = 15$  for downstream distances  $(\alpha x / d)$  above 100.

The combined results given in Figures 4.31 and 4.32 indicate the lower jet discharge of  $\alpha = 2$  compares well with the results of Hodgson ( 1991 ) for the near field dilutions but more superior for downstream distances above  $\alpha x / d = 100$ . This may be explained by the change of the flow regime from the momentum dominated to the passive plume condition which show higher dilutions. Hodgson's results compare well with the data for  $\alpha = 4$  above  $\alpha x / d = 100$ . The higher jet discharges of  $\alpha = 6, 8$  and 12 maintained the momentum dominated near field characteristics similar to those of Wright's for distances up to three orders of magnitude  $(\alpha x / d = 1000)$ . The dilutions in the far field regime compare approximately well to those of Hodgson. Therefore, the results in the present investigation suggest that circular wall jet dilutions in the near field regime are represented well by the Wright's ( 1/2 slope ) solution , while for the far field regime are predicted by the results of Hodgson ( 0.56 slope ). However, the use of Wright's far field solution could also be applicable for the wall jet but the coefficient  $C_4$  used and hence the constant in the dilution equation will change and be higher than the given value of 0.223.

For convenience in estimating the dilutions in a practical situation, the results of the present study given in Figure 4.31 are described by a mean equation of the form:

$$C_o / C_m = 0.67 (\alpha x / d)^{0.63} \quad (4.10)$$

The above equation describes fairly well the data points in the momentum dominated near field because all the jet discharges behave similar in the regime. Distinct scatter of the data is shown in the far field because dilutions are more dependent on the



strength of the jet discharge. Dilutions of upto 100 : 1 are represented by the correlation.

#### 4.4.3 Length Scale Analysis

The concentration profiles for circular wall jet in crossflow have been shown to be similar both in the vertical,  $z - \xi$  plane ( depth-wise ) and the transverse,  $\eta - \xi$  planes. The following analysis considers the variation of the respective characteristic length scales along the curvilinear (  $\xi$  ) distance. The jet nozzle diameter  $d$  is used as a length scale to make the results non-dimensional.

##### 4.4.3.1 Vertical Scale, $b_z$

The vertical length scale  $b_z$  is measured from the bed (  $z = 0$  ) to the point where the concentration is one-half of the maximum value at the section (  $C = 1/2 C_m$  ). Figure 4.33 graphically shows the variation of  $b_z / d$  along the axial distance,  $\xi / d$  ( measured along the trajectory of maximum concentrations ) for the five jet discharges. The results indicate that the momentum dominated near field flow regime (  $\xi / d < 30$  ) is fitted by a unifying length scale described by the following relation:

$$\frac{b_z}{d} = 1.0 + 0.3 ( \xi / d ) \quad (4.11)$$

The variation of the scale in the momentum dominated far field appears to be a function of the flow velocity ratio  $\alpha$ . The weakest growth is shown by the jet discharge of velocity ratio  $\alpha = 2$ , while for  $\alpha = 4$  and 6,  $b_z$  grows at rates higher than that of  $\alpha = 2$ . Jet discharges of velocity ratios  $\alpha = 8$  and 12, grow at rates higher than

those of the weaker jets. However, all the jet flows grow with similar slopes and are described by the following relations:

$$\frac{b_z}{d} = 3.0 + 0.02 (\xi / d) \quad (\alpha = 2) \quad (4.12)$$

$$\frac{b_z}{d} = 6.0 + 0.03 (\xi / d) \quad (\alpha = 4 \text{ and } 6) \quad (4.13)$$

$$\frac{b_z}{d} = 10.0 + 0.03 (\xi / d) \quad (\alpha = 8 \text{ and } 12) \quad (4.14)$$

The dependence of  $\alpha$  of the scale in the momentum dominated far field region is shown by plotting  $\xi / \xi_{em}$  against  $b_z / \alpha d$  ( where  $\xi_{em}$  is the axial distance where  $x = \alpha d$  ) and given in Figures 4.34 ( a ) and ( b ). For velocity ratios  $\alpha$  greater than 4, the plot indicate the dimensionless distance  $\xi_{em} / d$  is a linear function of  $\alpha$ .

The variation of the vertical scale,  $b_z$  indicates that the wall jet grows at about 10 times faster in the momentum dominated near field compared to the momentum dominated far field regime.

#### 4.4.3.2 Transverse Scale, $b_o$

Transverse characteristic length  $b_o$  at a section is defined as the distance measured from the jet axis ( defined by maximum tracer concentration ) to the location where the instantaneous concentration is one - half the maximum value on either sides of the axis. The outer scale is conventionally considered positive and the inner scale negative. The transverse growth characteristics of the wall jet are derived graphically by plotting  $\xi / d$  against the absolute sum of the scale  $(+b_o + |-b_o|) / d$  and given in Figure 4.35. The results for all the five jet discharges fall into two

distinct flow regimes. For the first region defined by the momentum dominated near field, the variation is described by the linear relation:

$$\frac{(+b_* + |-b_*|)}{d} = 0.53 \frac{\xi}{d} \quad (4.15)$$

For the second flow region known as the momentum dominated far field, the corresponding relation is:

$$\frac{(+b_* + |-b_*|)}{d} = 7.5 + 0.075 \frac{\xi}{d} \quad (4.16)$$

Unique trends were observed when the transverse length scales for the growth on the outside ( positive ) and the inside (negative ) regions of the deflected jet were considered separately. The results given in Figure 4.36 ( a ) and ( b ) indicate that the transition between the momentum dominated near field and far field regions for the outside scale does not occur gradually whereas for the inner scale, there is a smooth transition.

Comparing these results to those obtained for the vertical scale easily, we can conclude that for circular wall jets in crossflow, the transverse growth is about two times that of the corresponding growth in the vertical ( depth - wise ) direction. These results support the fact that the wall ( bed ) restricts the vertical growth of the jet but favors the horizontal transverse growth and it is an advantage for dilution in shallow rivers where normally the widths are several times more than the flow depth.

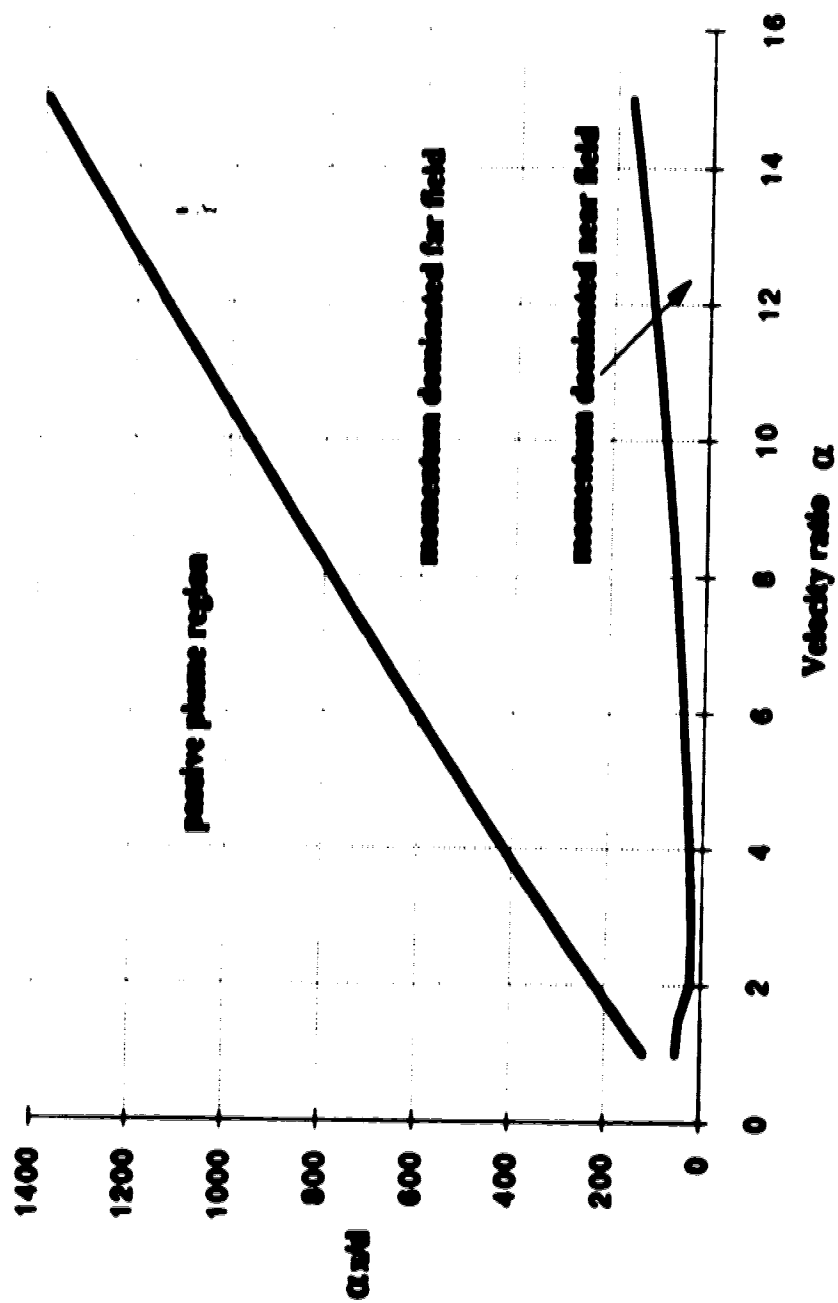
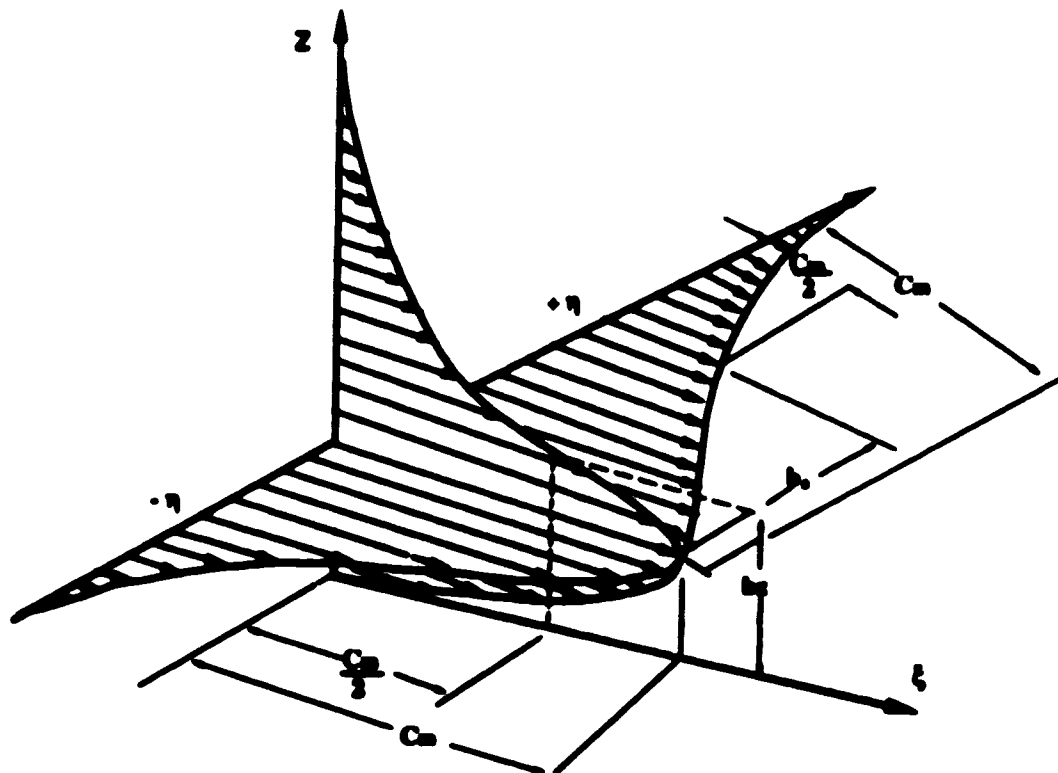
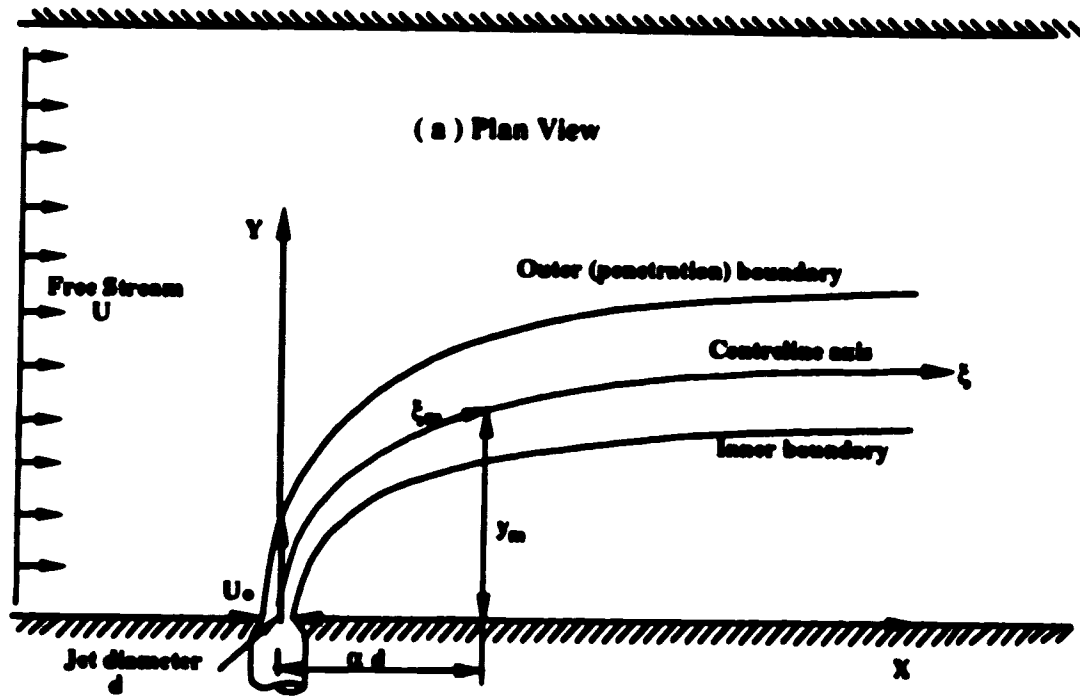


Fig. 4.1 Boundary Limits for the Momentum Dominated Regions



(b) Three-Dimensional Concentration Profiles of a Wall Jet

Fig. 4.2 Definition Sketches of a Circular Wall Jet in Crossflow

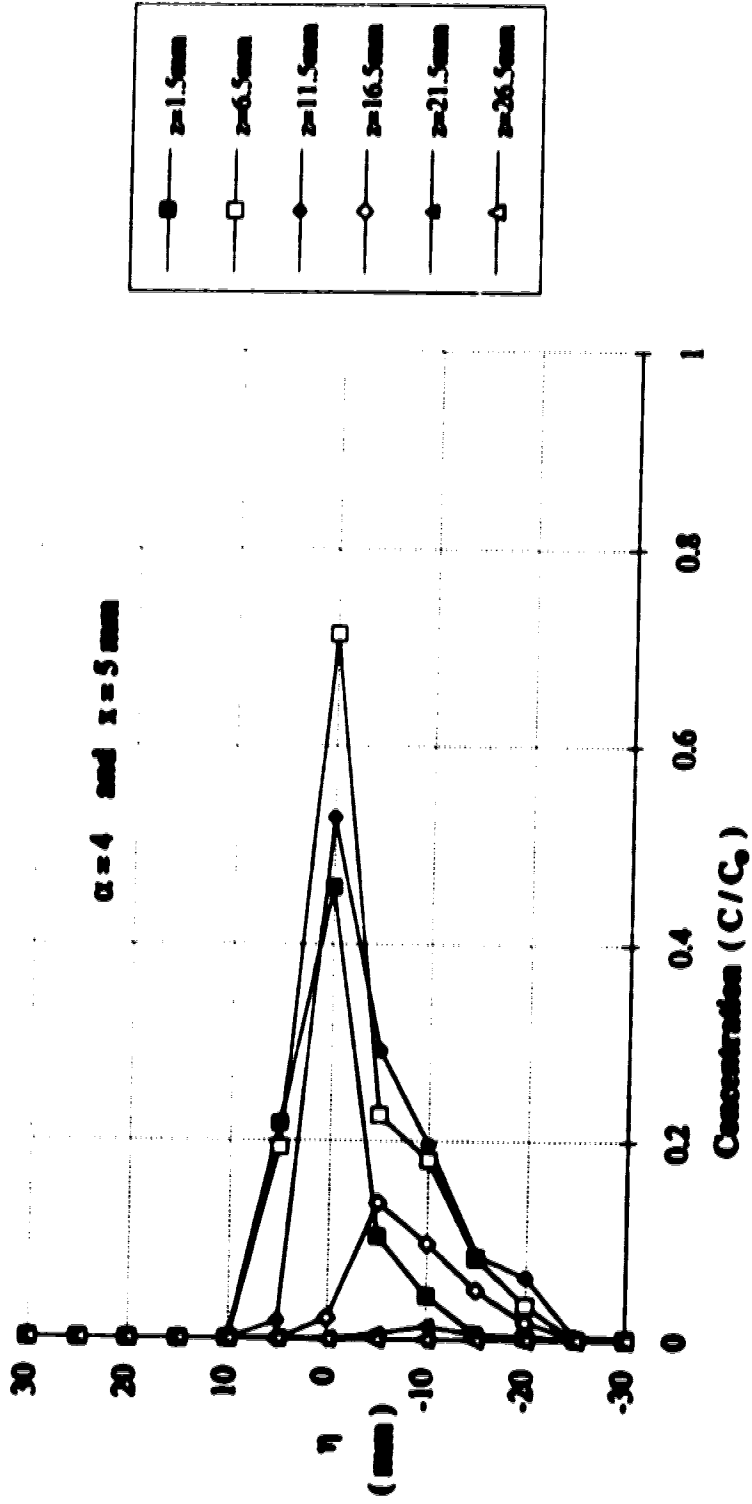


Fig. 4.3(e) Transverse Concentration Profiles

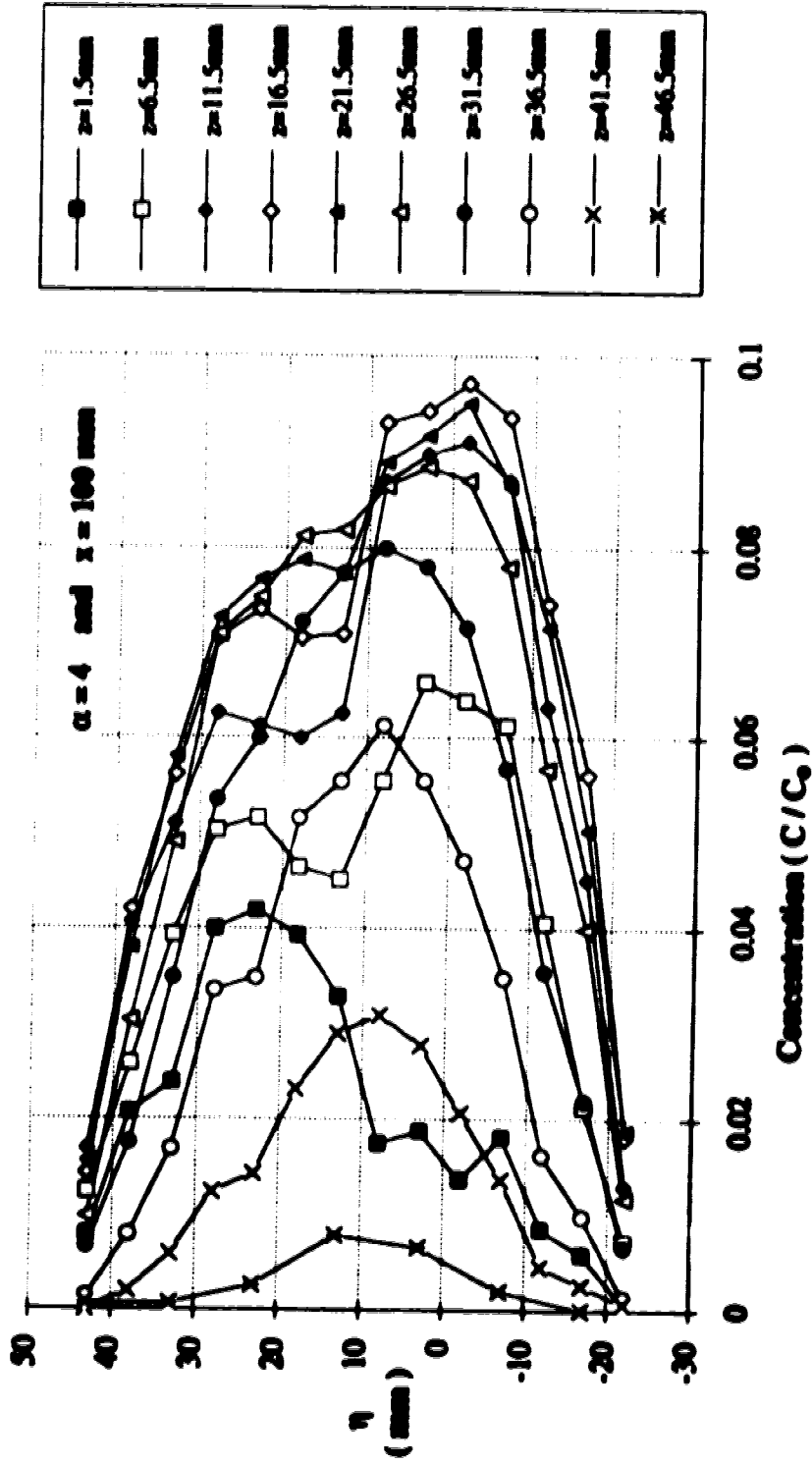


Fig. 4.3(b) Transverse Concentration Profiles

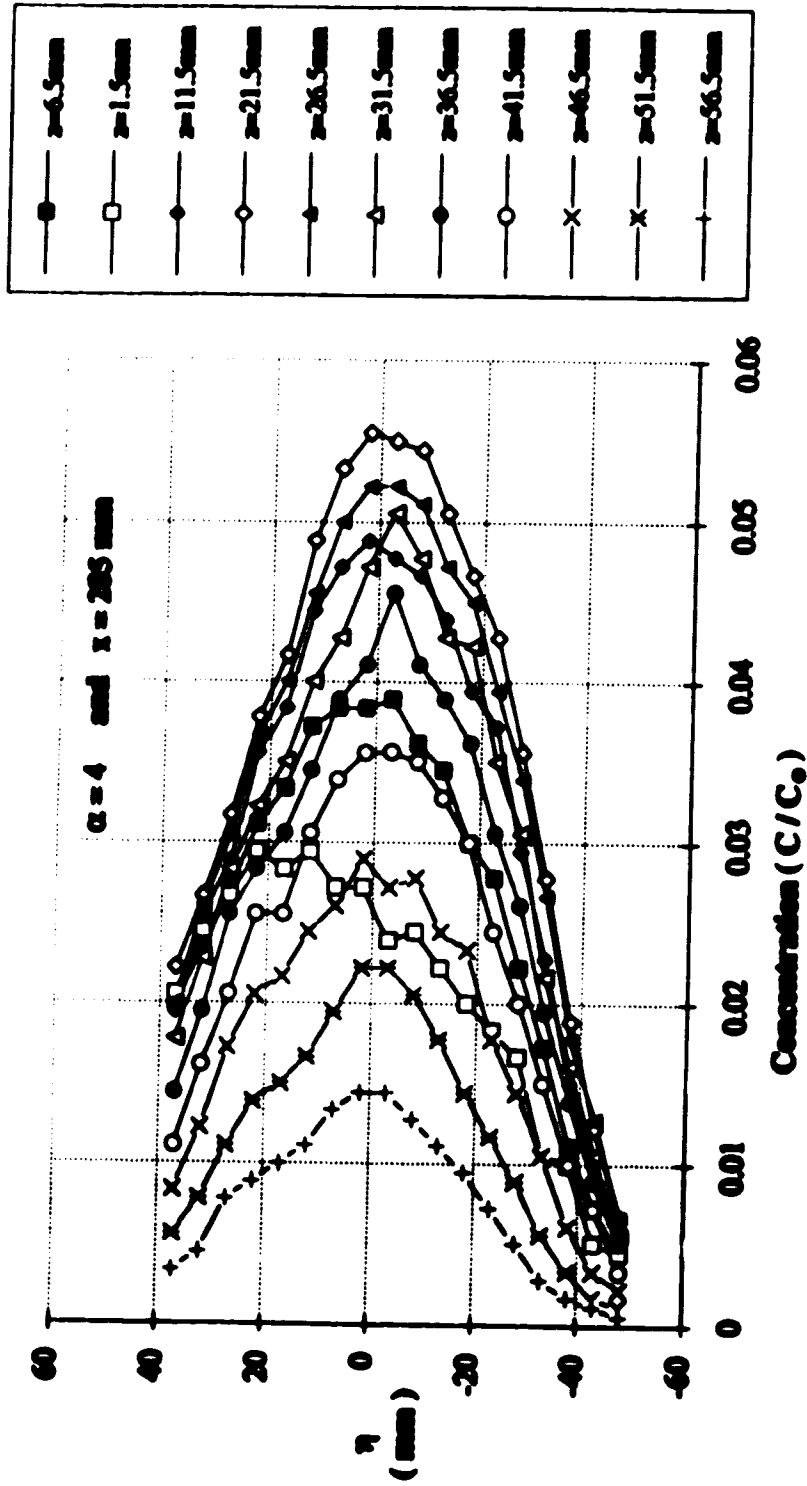


Fig. 4.3(c) Transverse Concentration Profiles



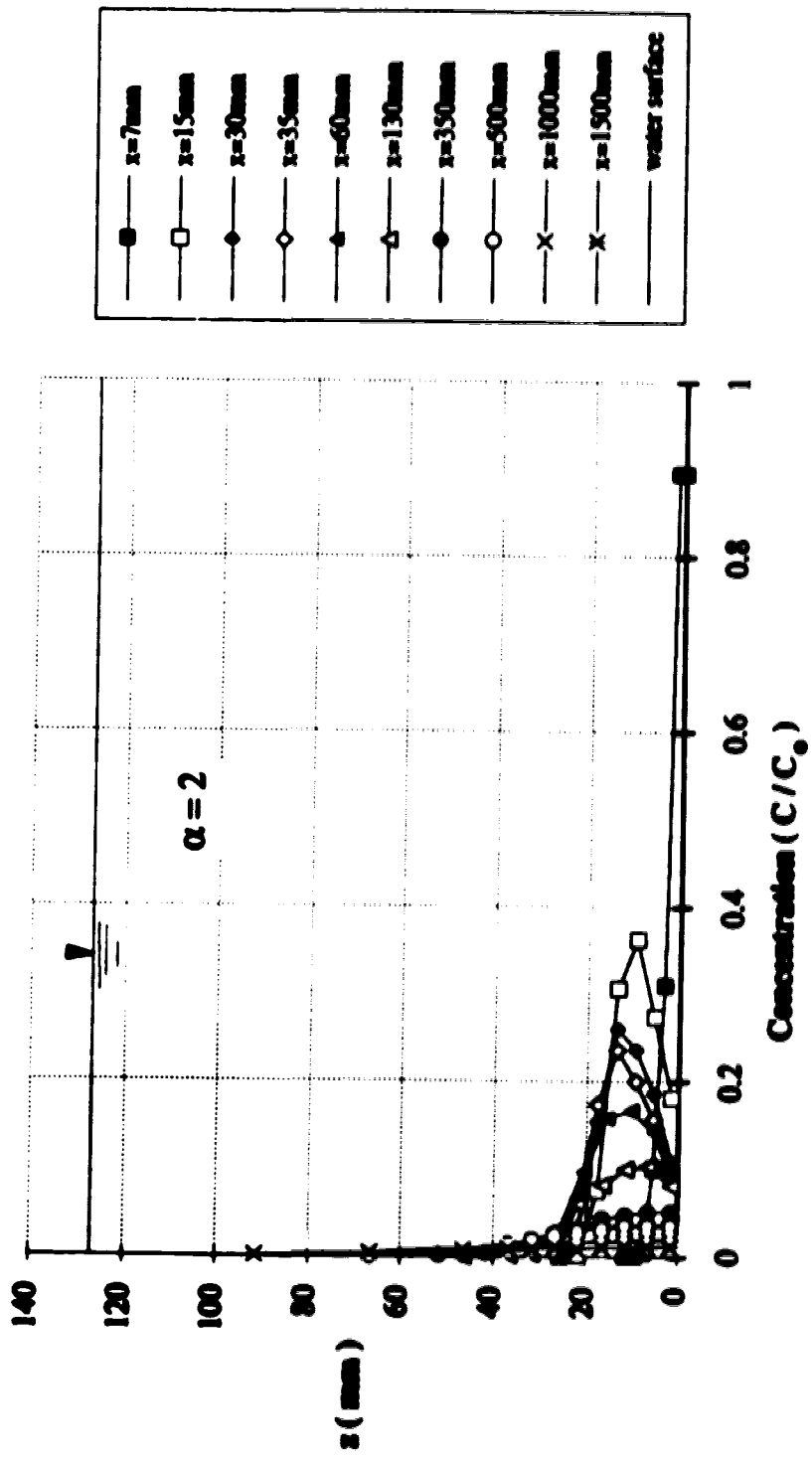


Fig. 4.4 Concentration Profiles along the Centreline of the Jet

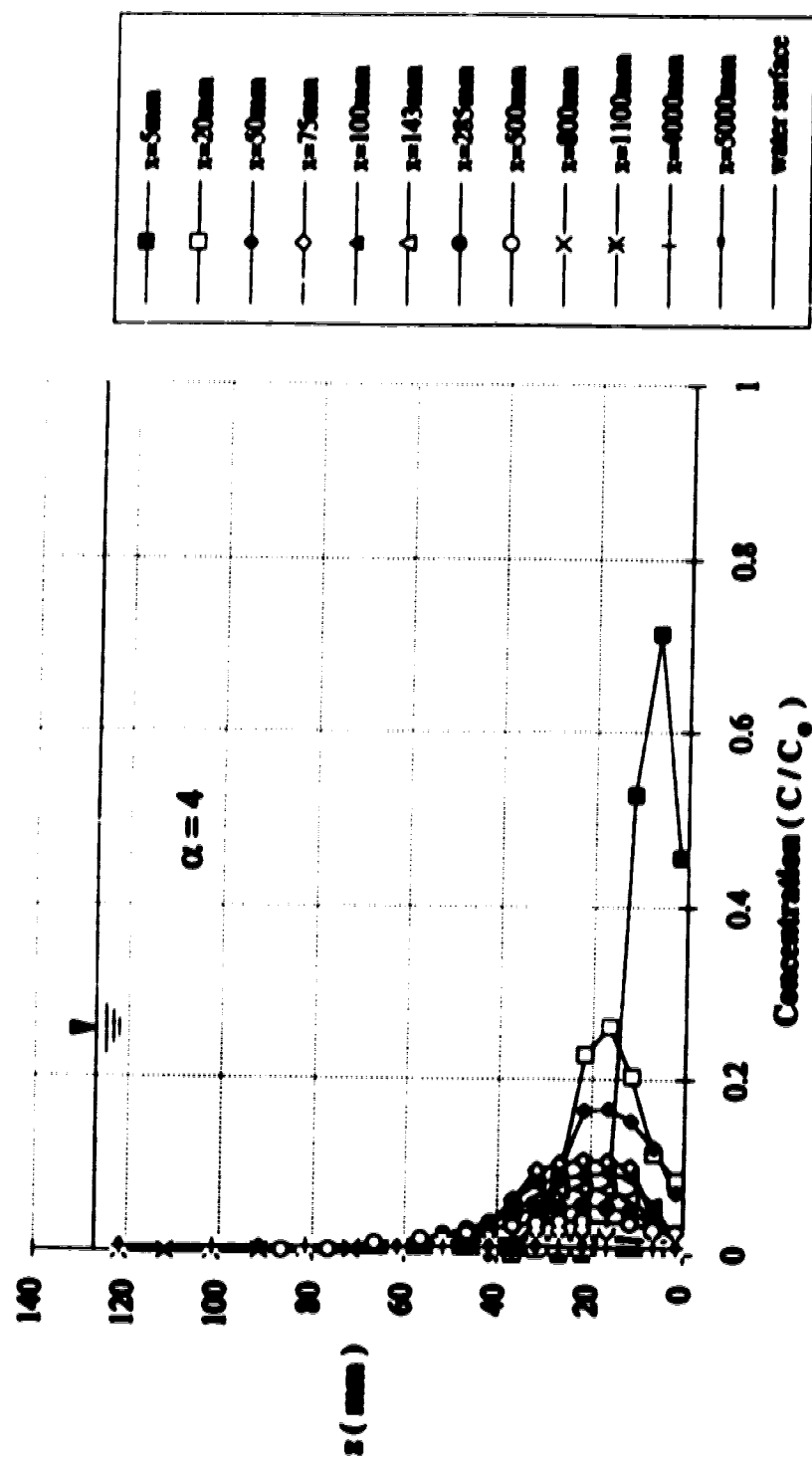


Fig. 4.5 Concentration Profiles along the Centreline of the Jet

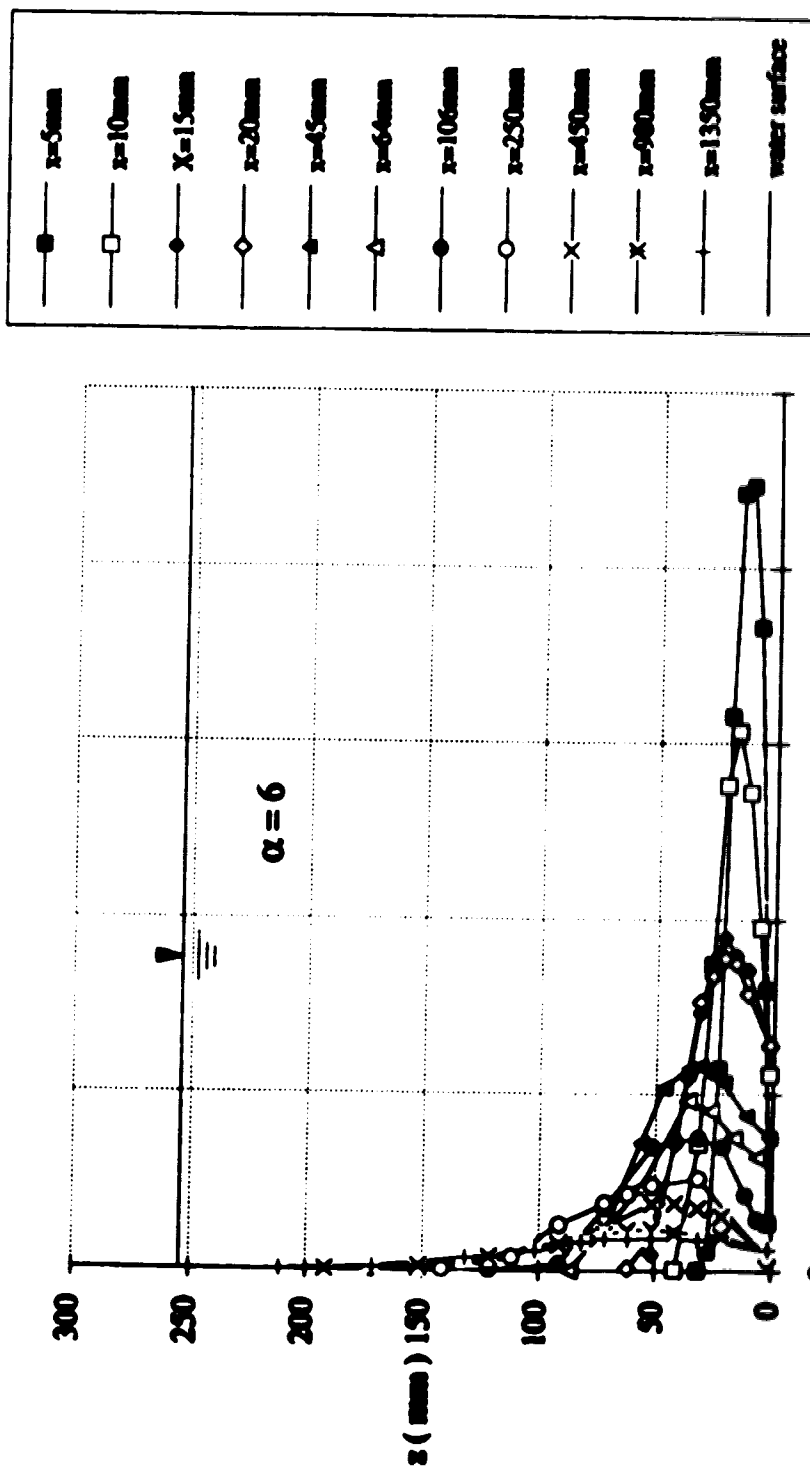


Fig. 4.6 Concentration Profiles along the Centerline of the Jet

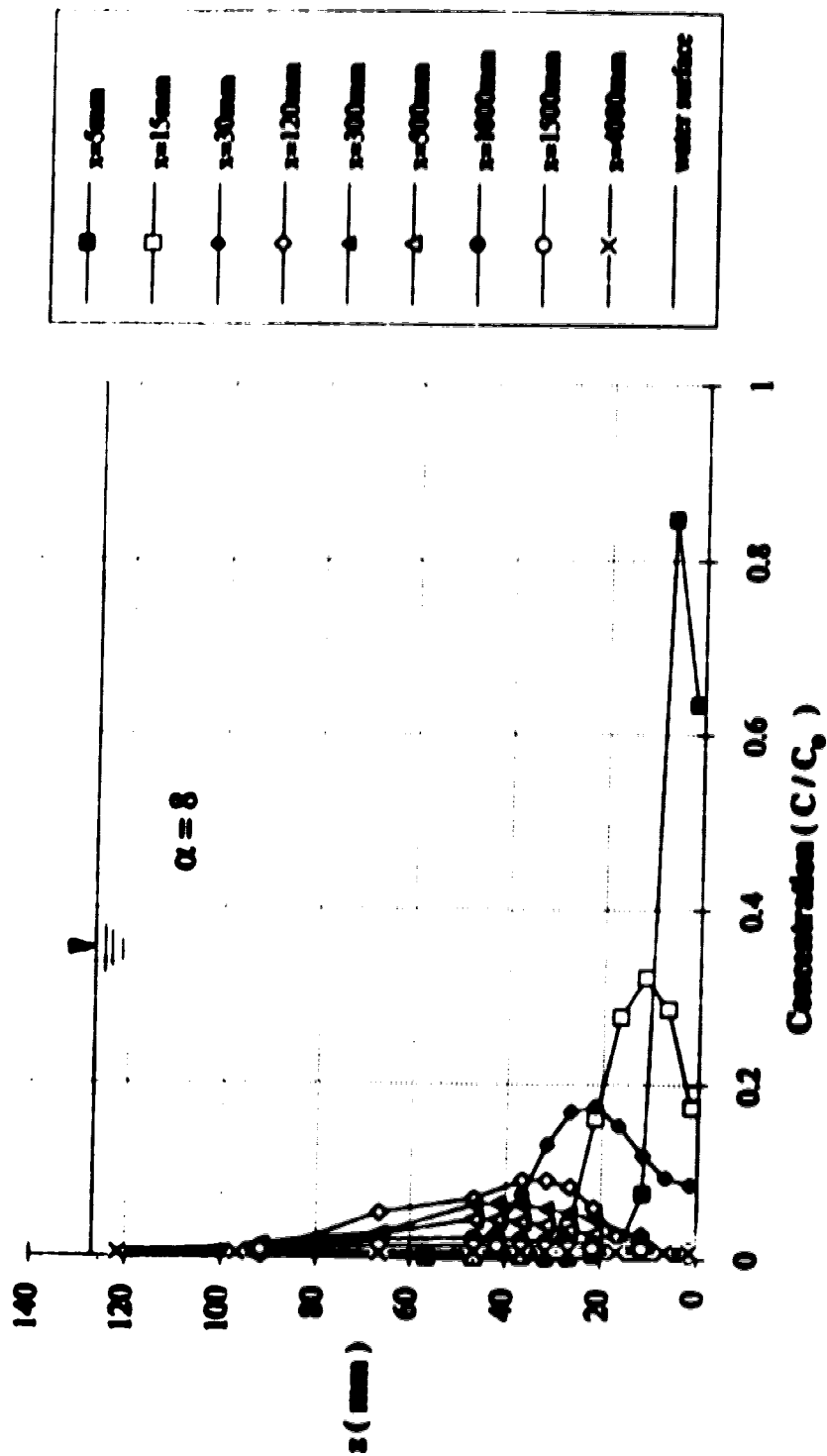


Fig. 4.7 Concentration Profiles along the Centerline of the Jet

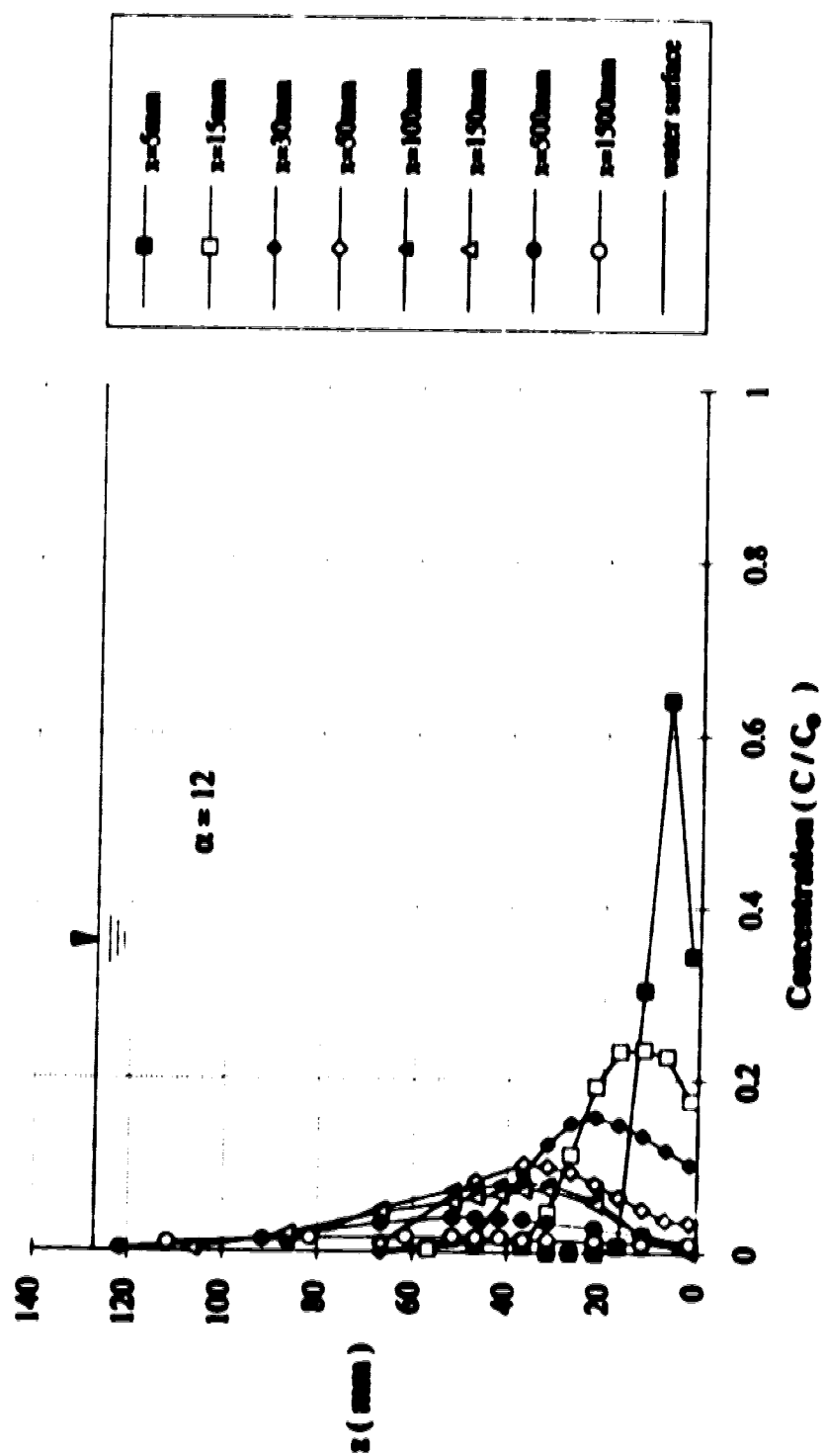


Fig. 4.8 Concentration Profiles along the Centerline of the Jet

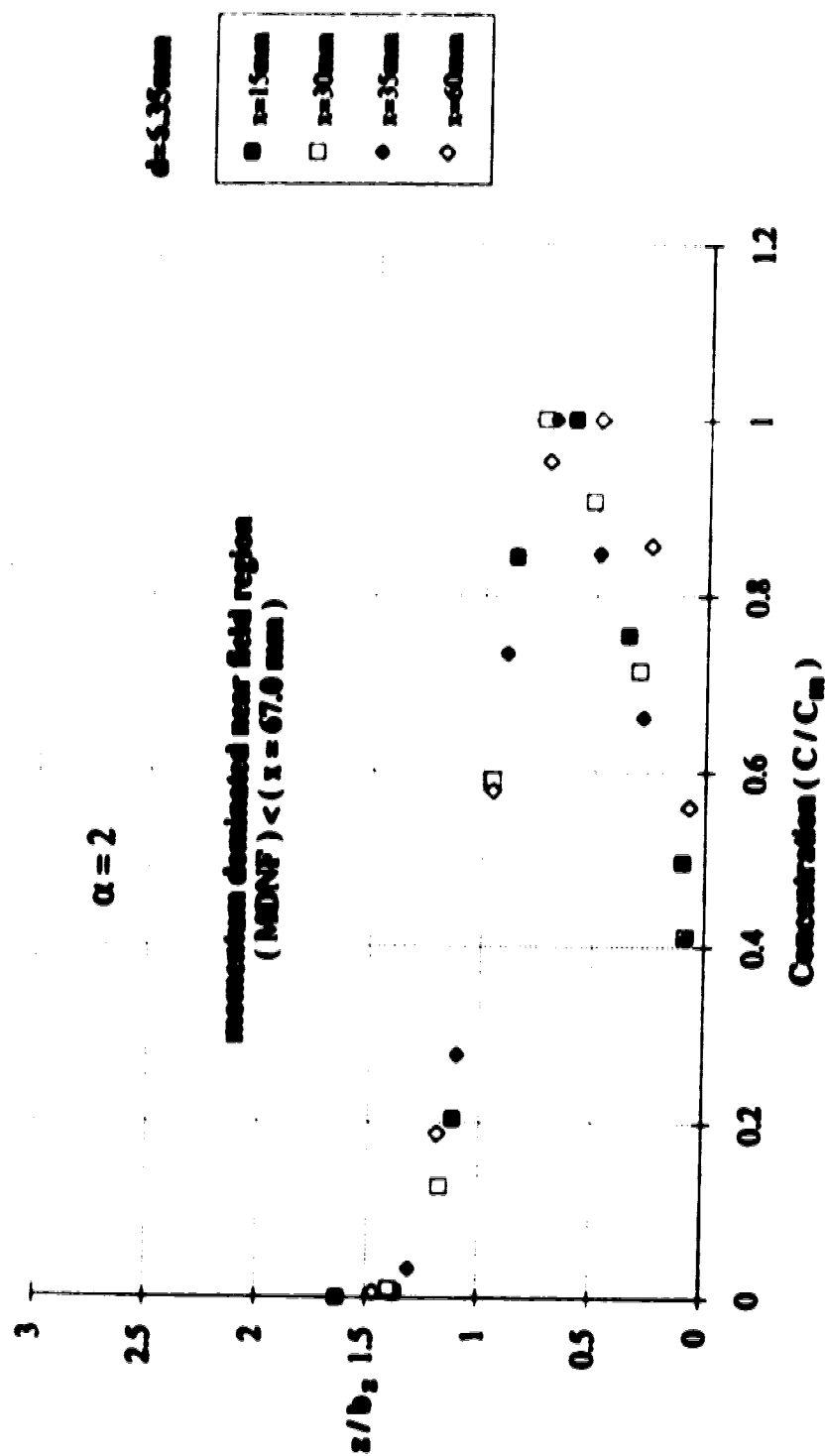


Fig. 4.9 (a) Non - dimensional Profiles of Concentration Distribution in the Vertical Direction

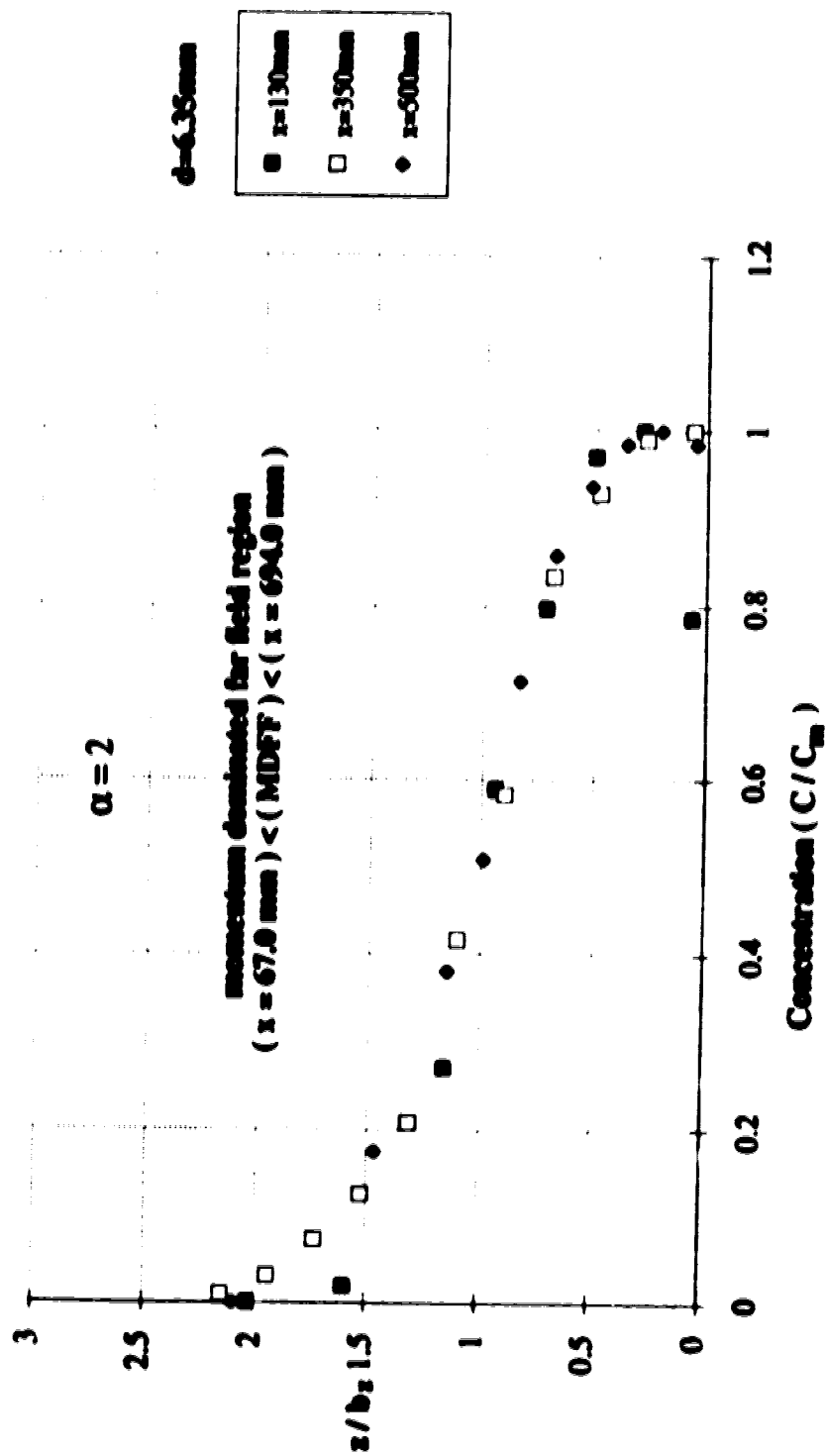


Fig. 4.9 (b) Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction

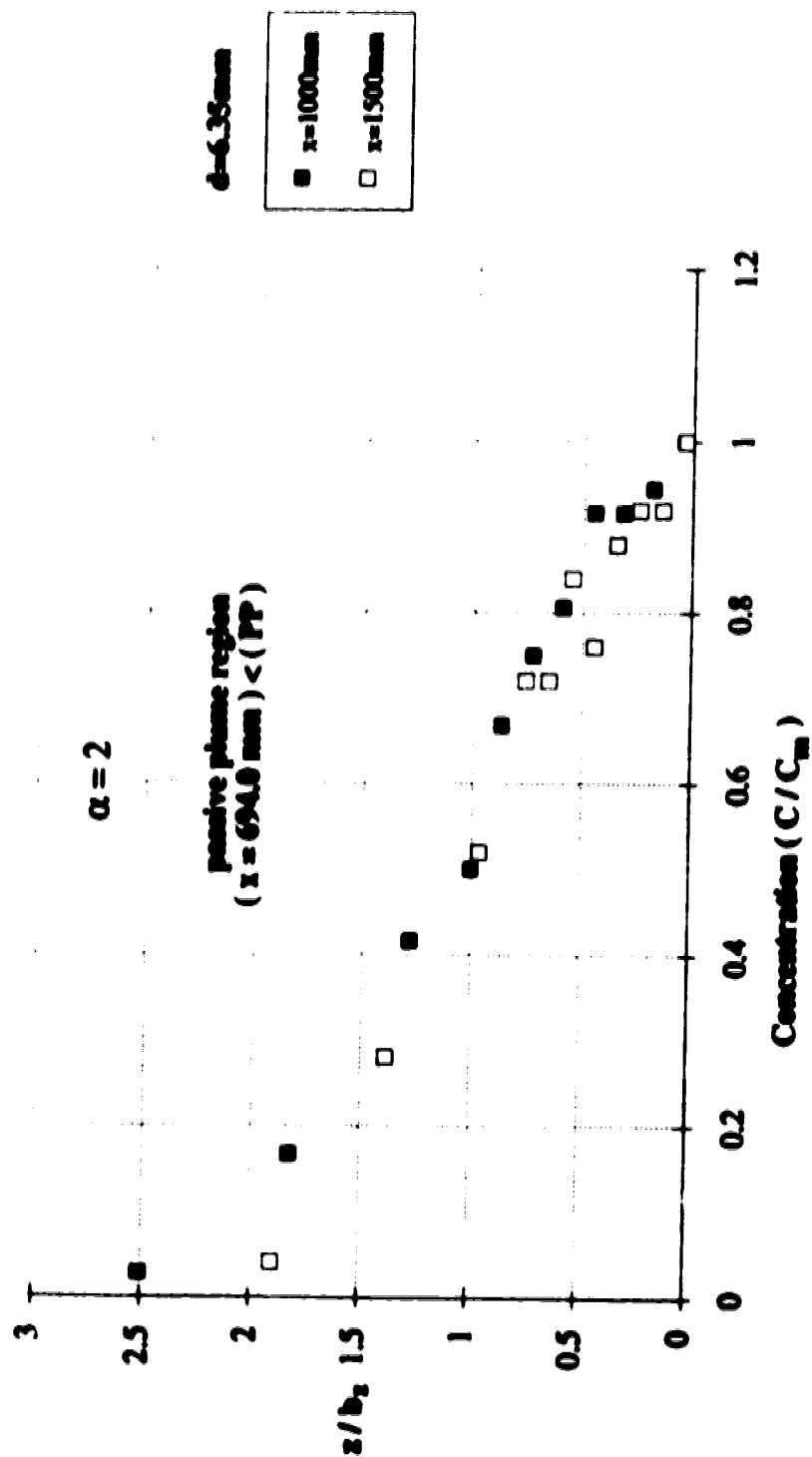


Fig. 4.9 (c) Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction



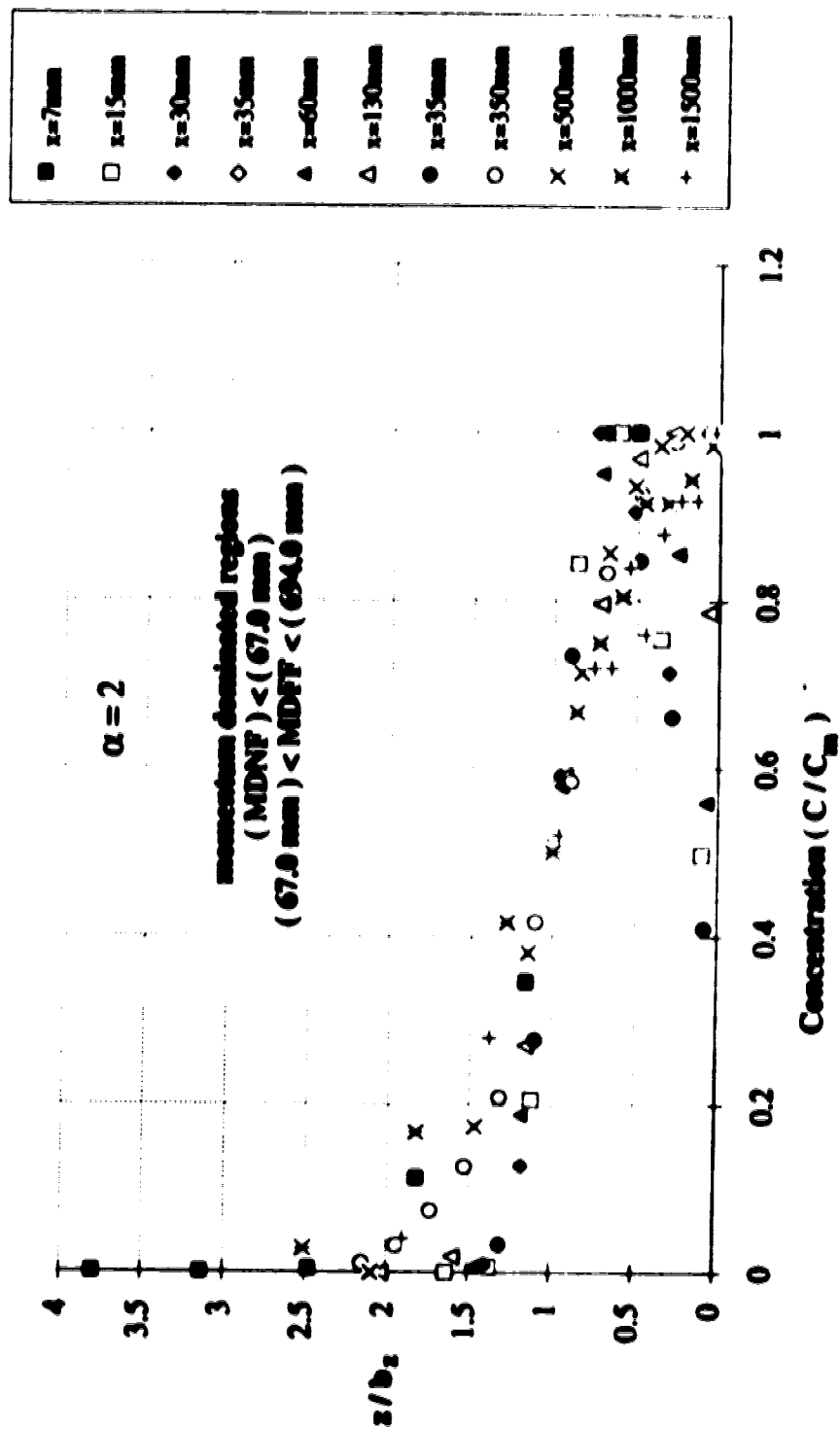


Fig. 4.9 (d) Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction

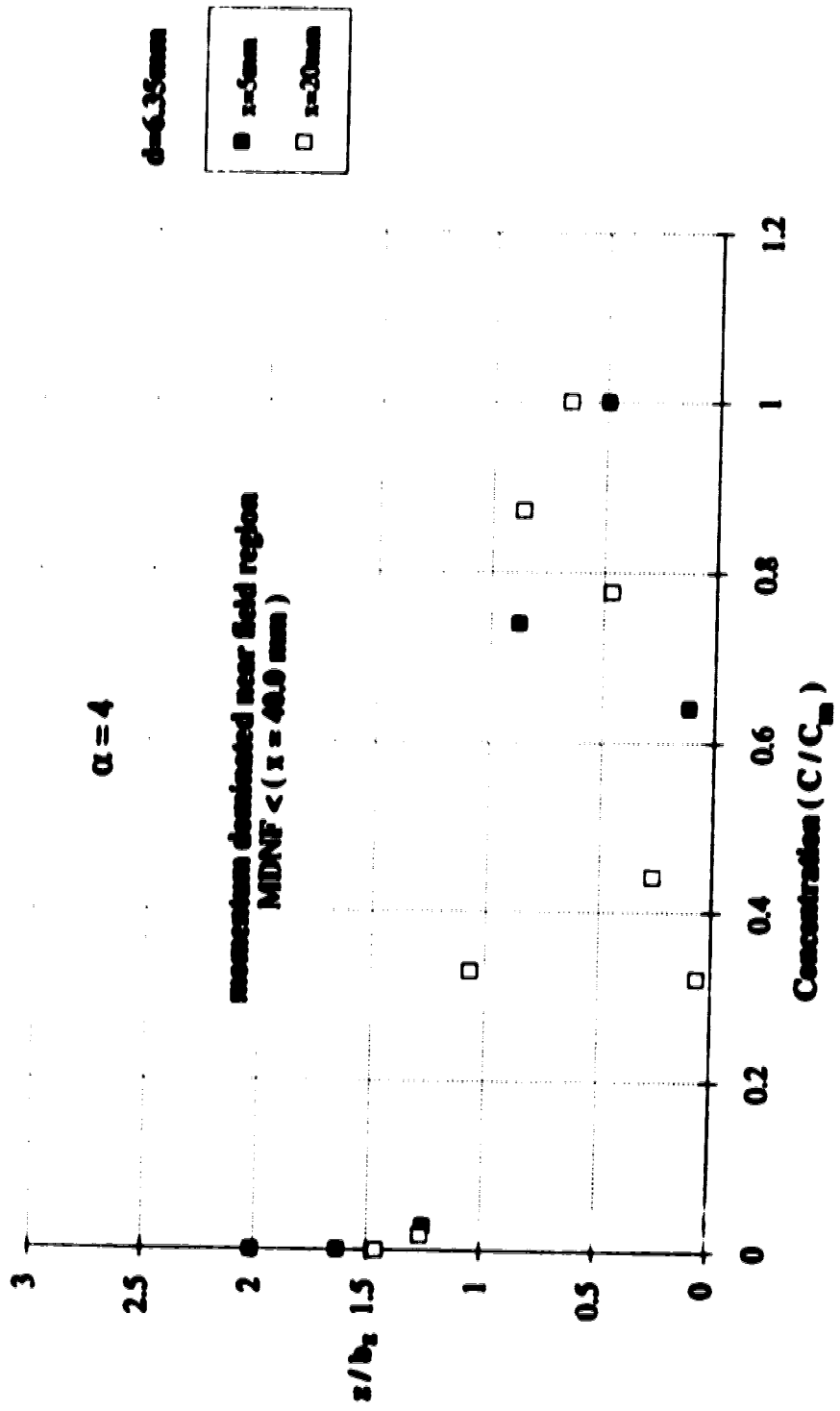


Fig. 4.10 (a) Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction

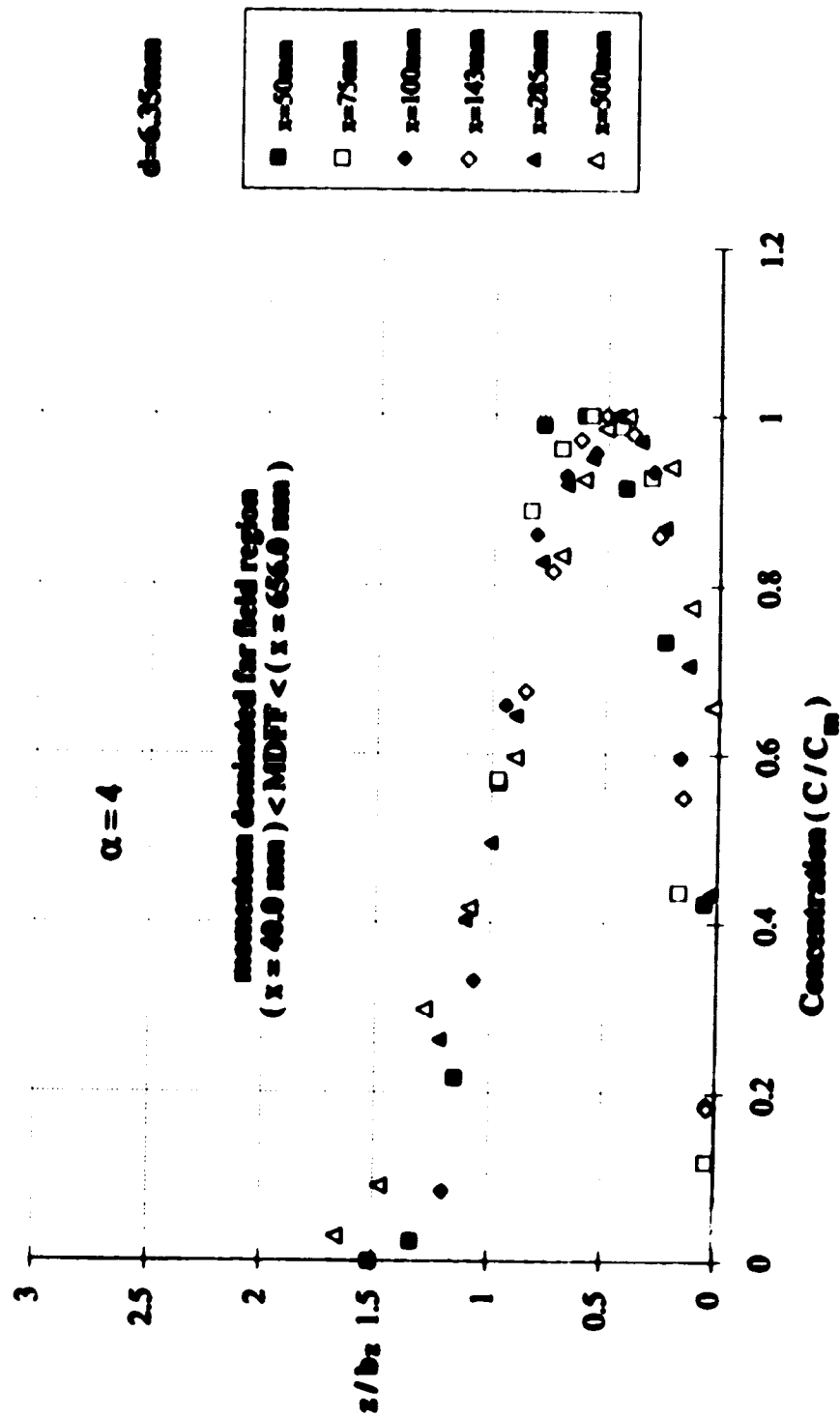
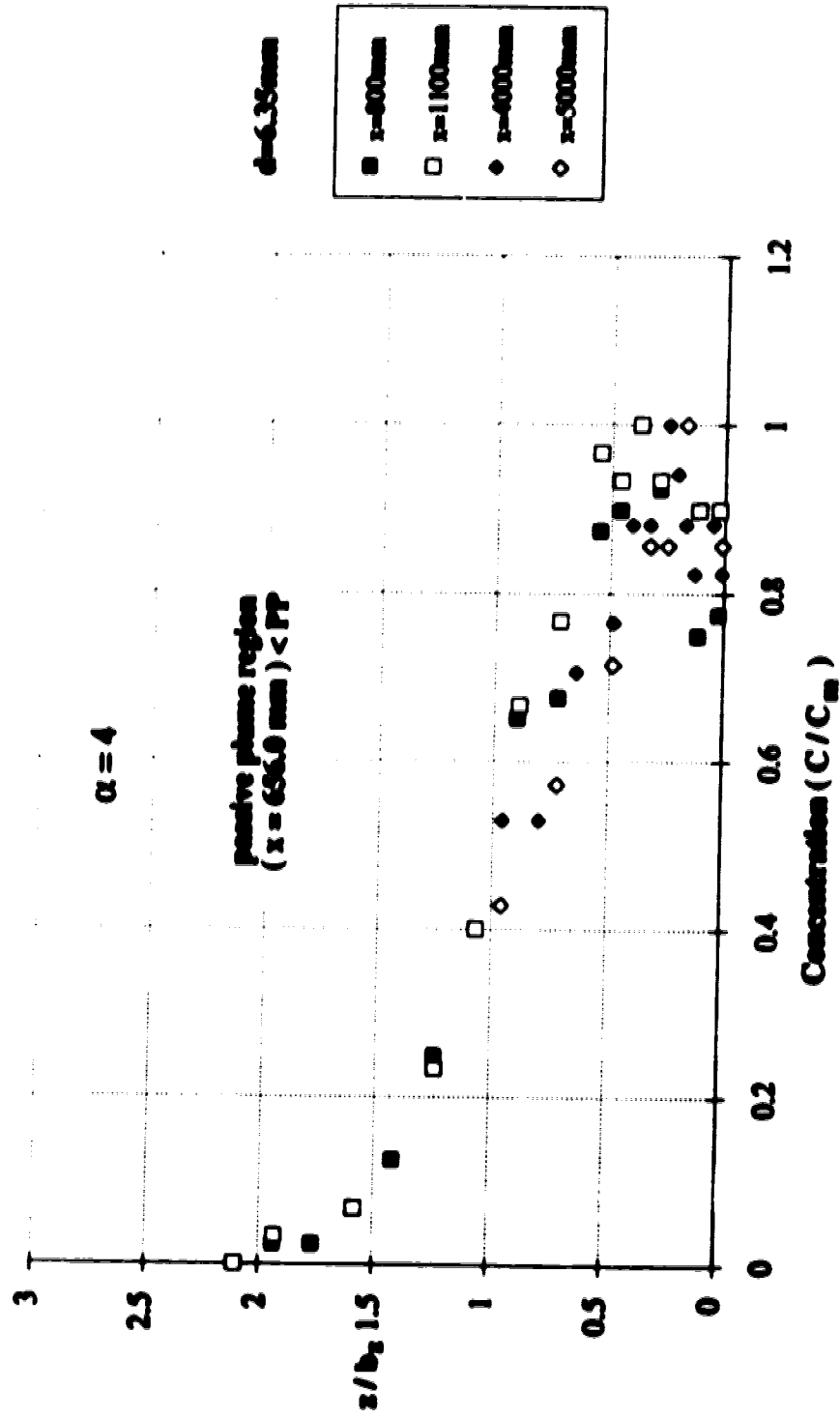
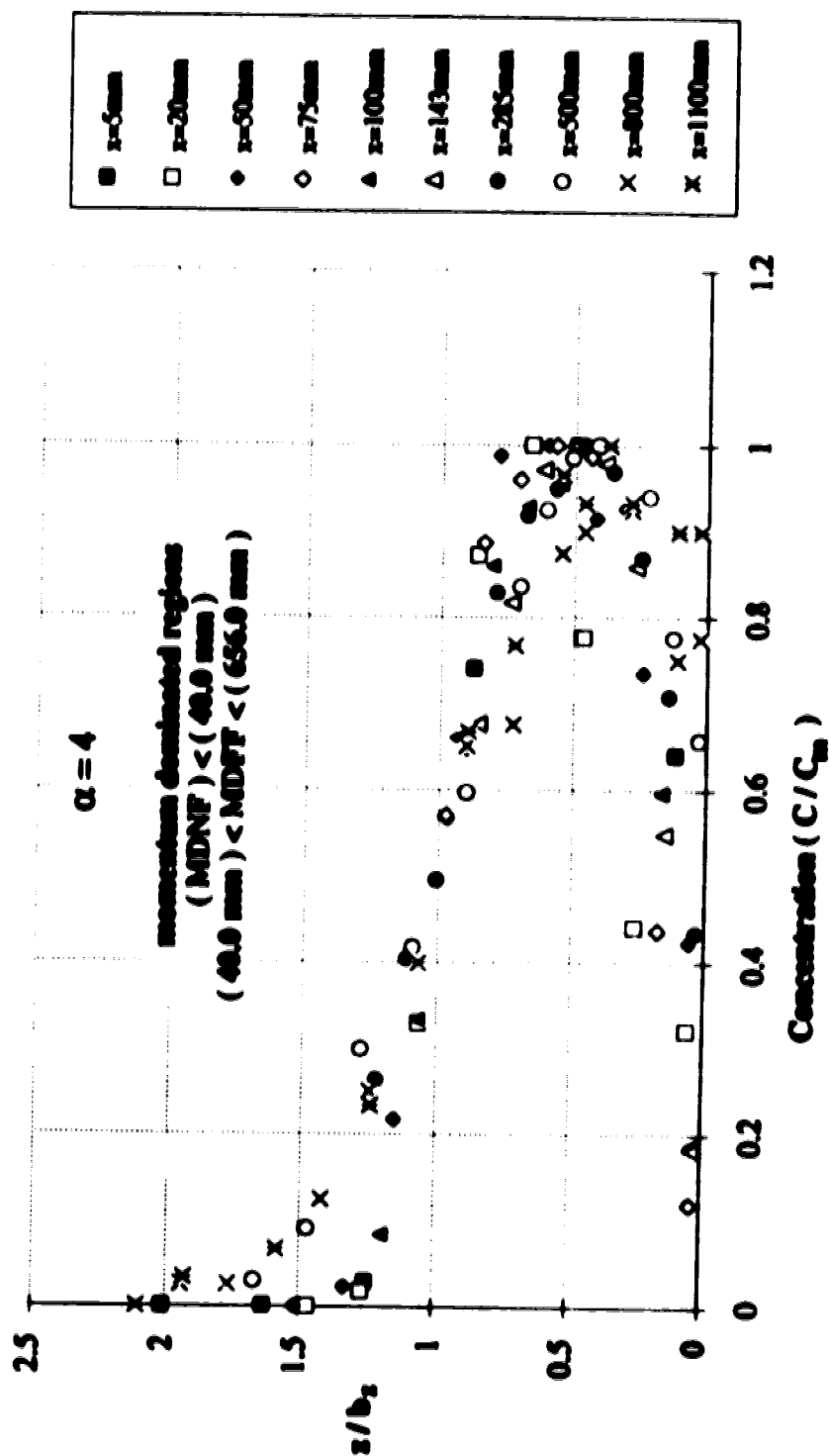


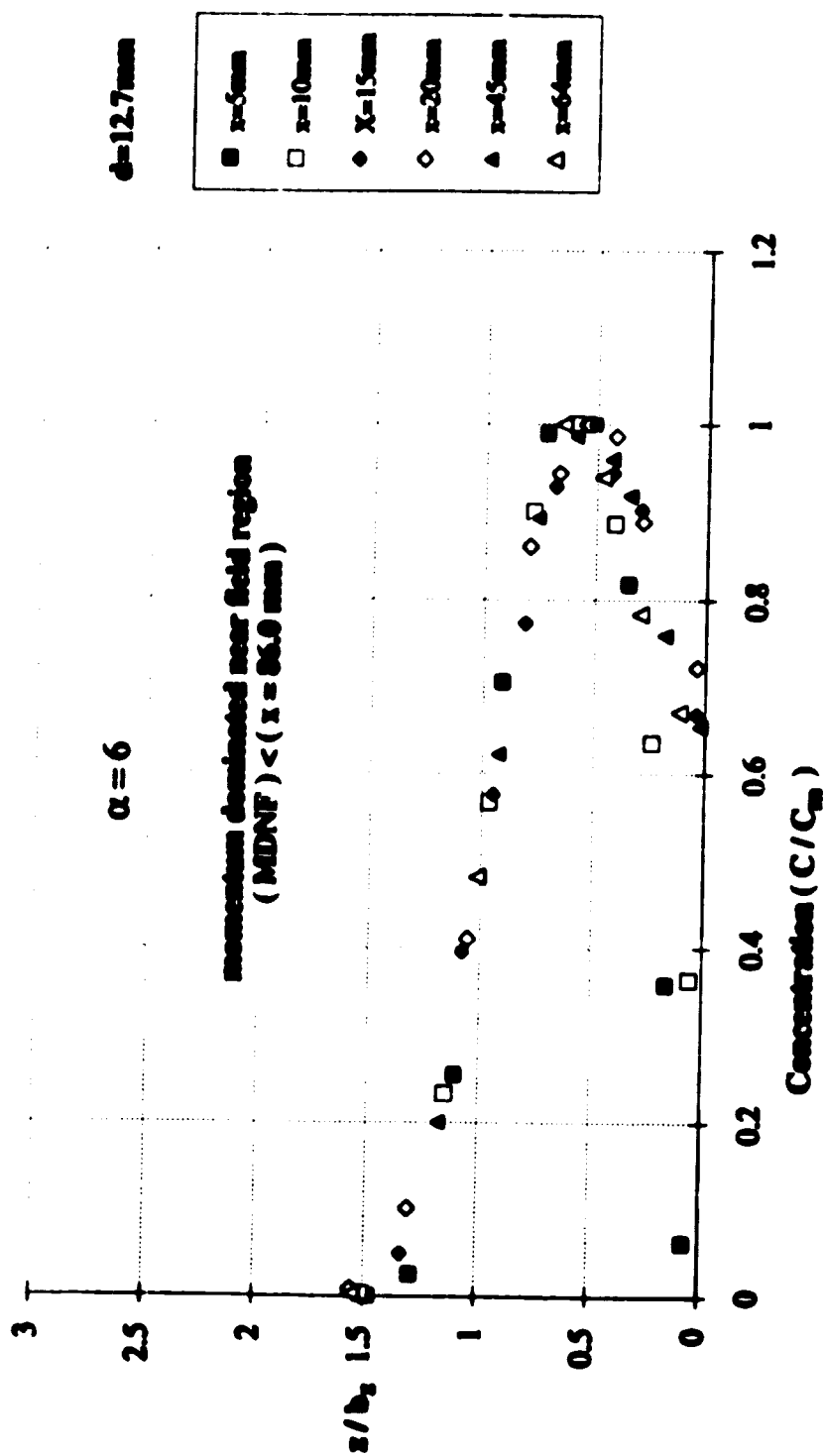
Fig. 4.10 ( b ) Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction



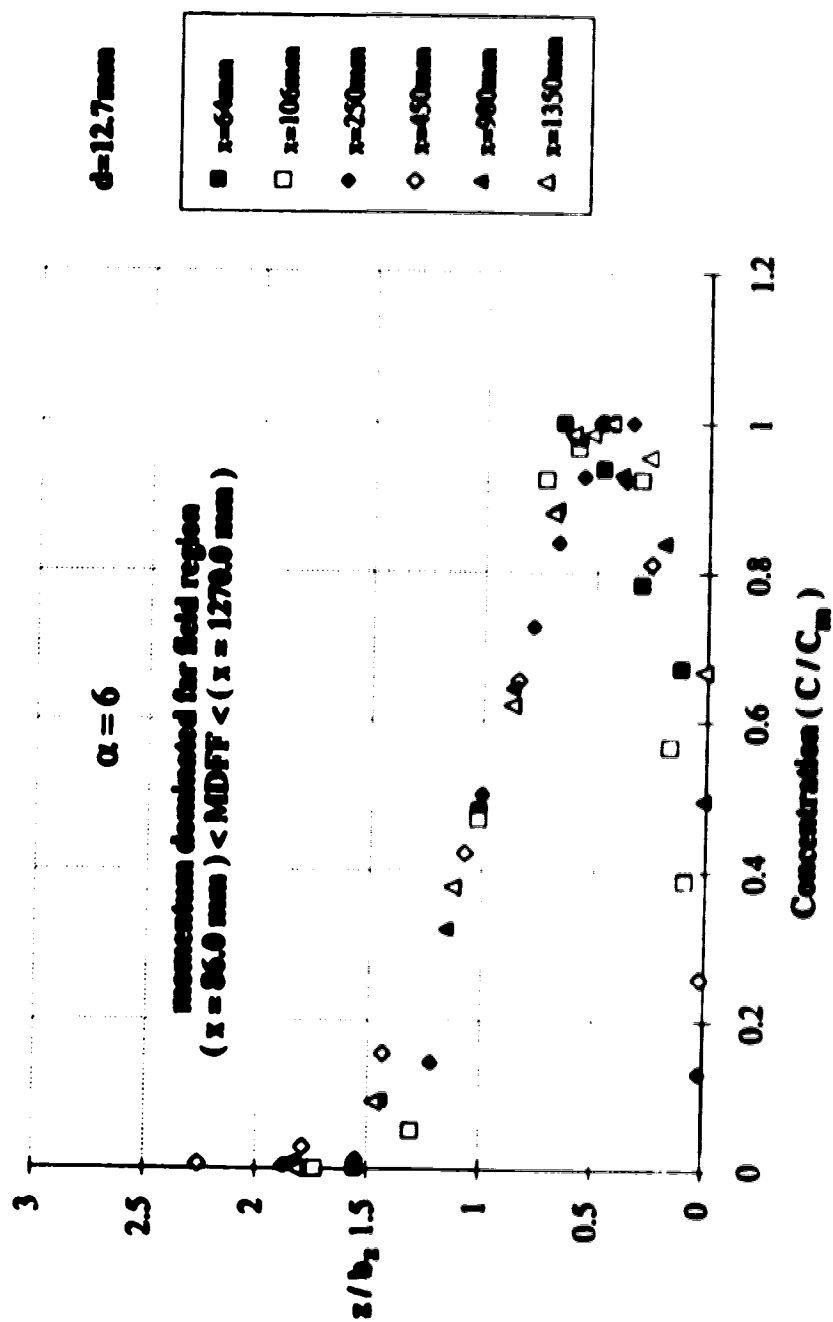
**Fig. 4.10 (c) Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction**



**Fig. 4.10 (d) Non - Dimensional Profiles of Concentration  
Distribution in the Vertical Direction**



**Fig. 4.11 (a) Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction**



**Fig. 4.11 (b) Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction**

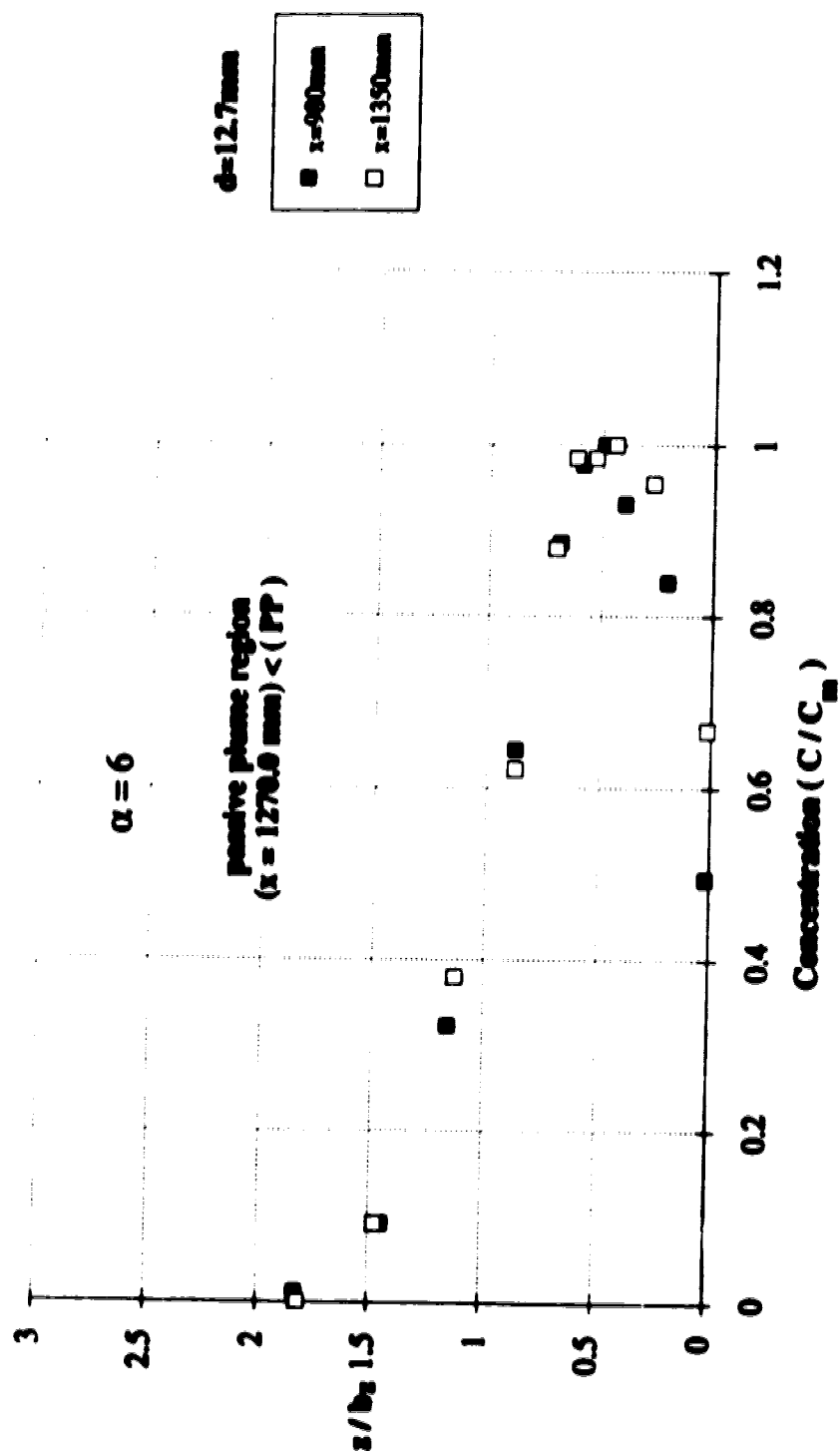


Fig. 4.11(c) Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction



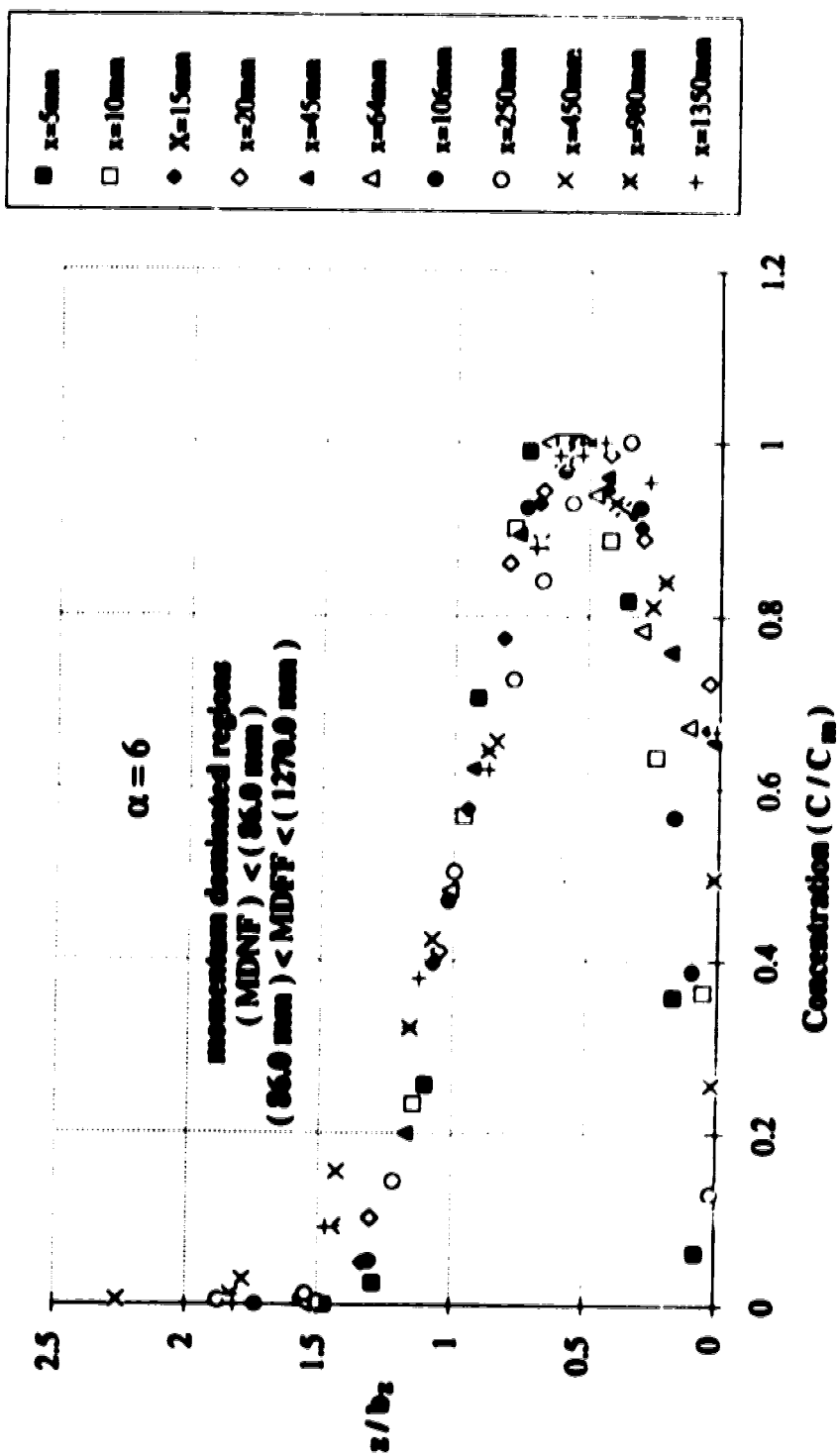


Fig. 4.11 (d) Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction

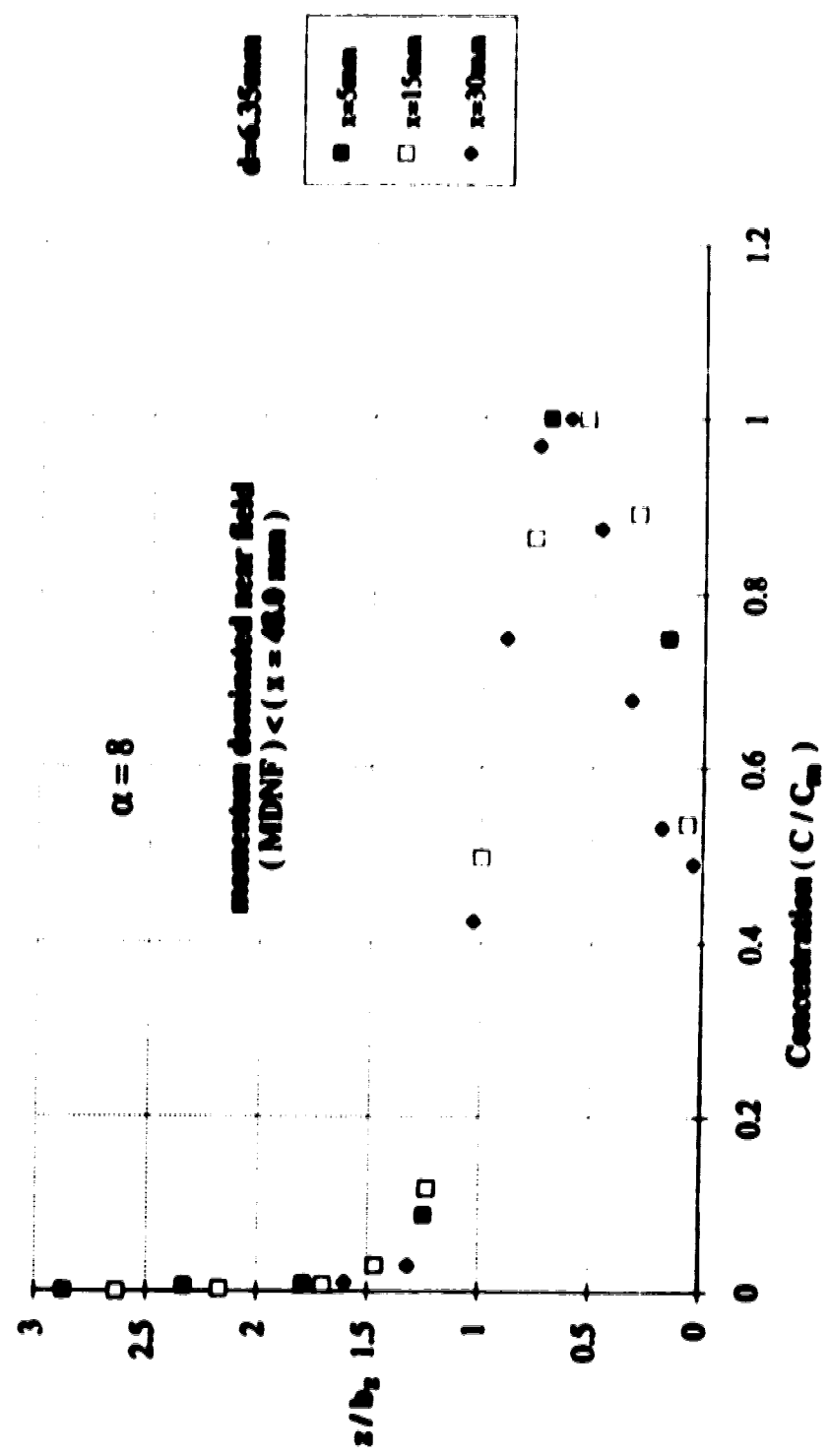
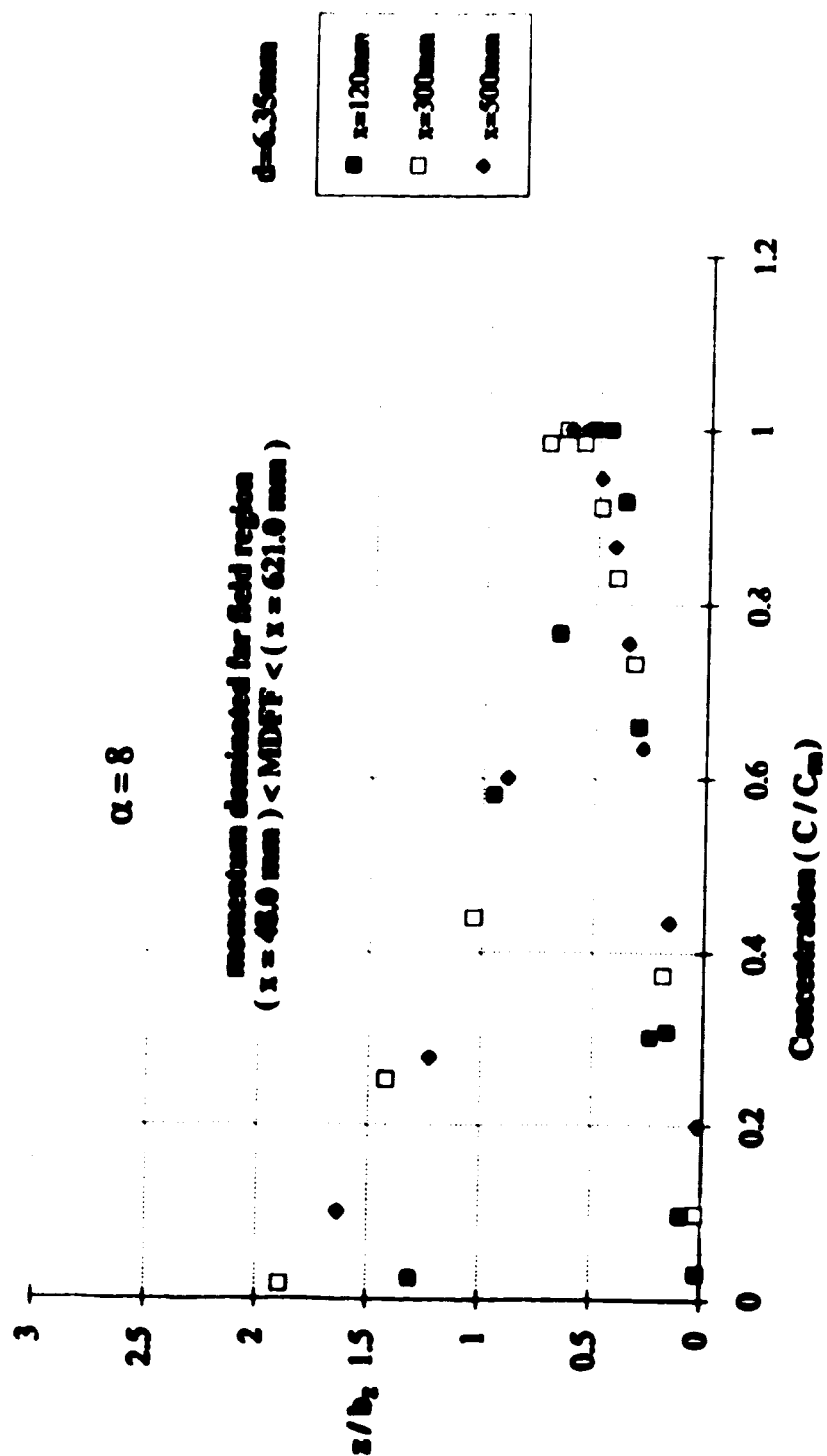


Fig. 4.12 (a) Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction



**Fig. 4.12 (b) Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction**

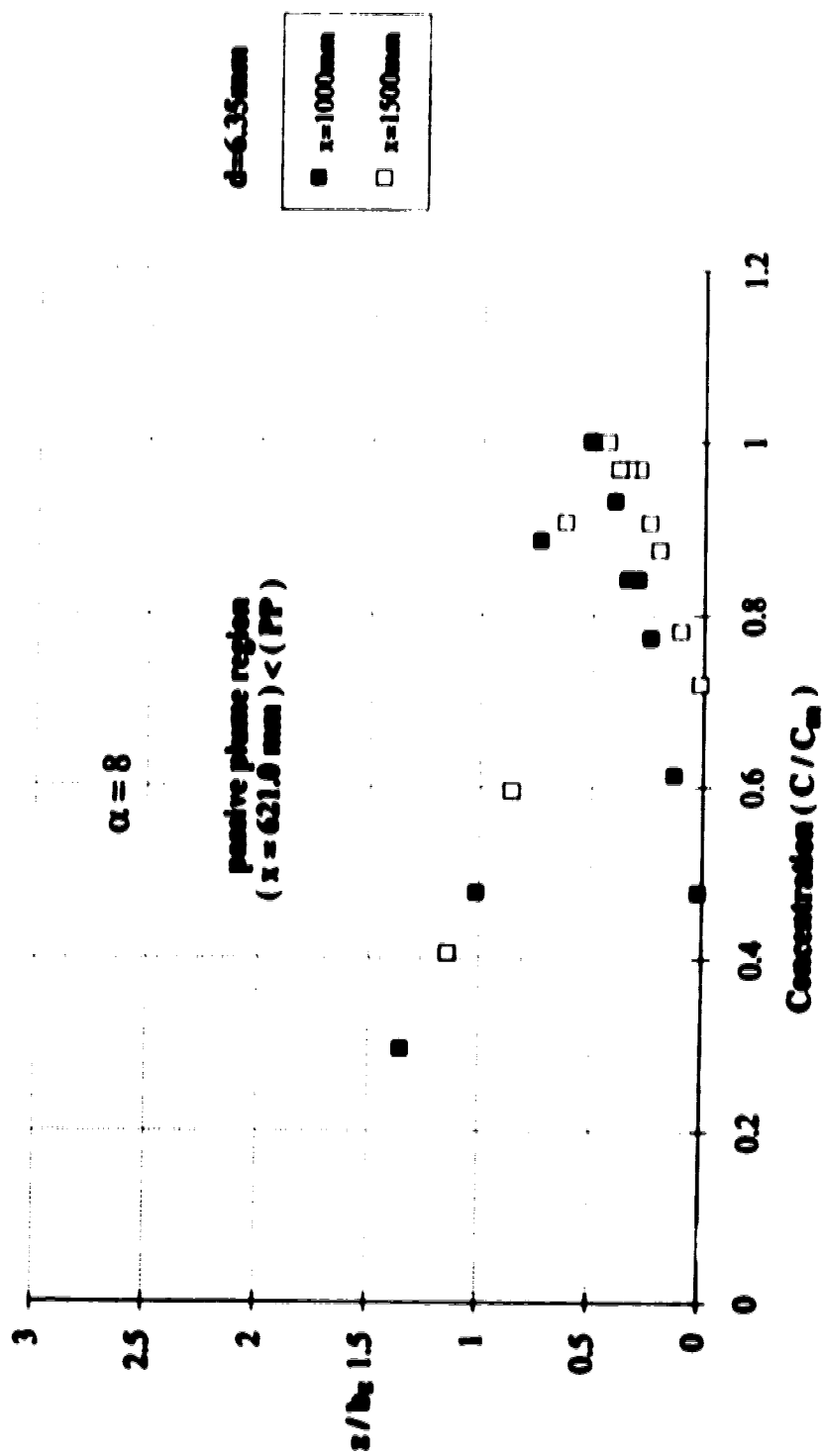
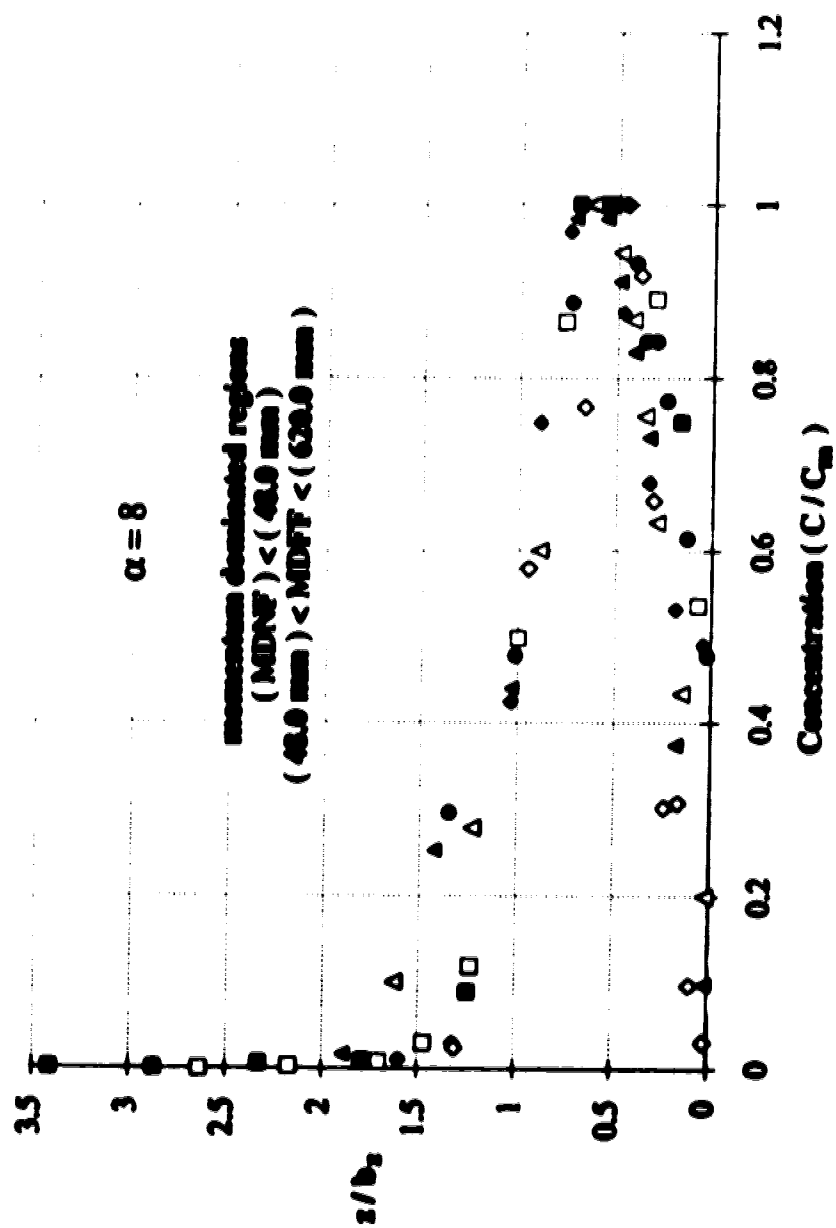


Fig. 4.12(c) Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction



**Fig. 4.12 (d) Non - Dimensional Profiles of the Concentration Distribution in the Vertical Direction**

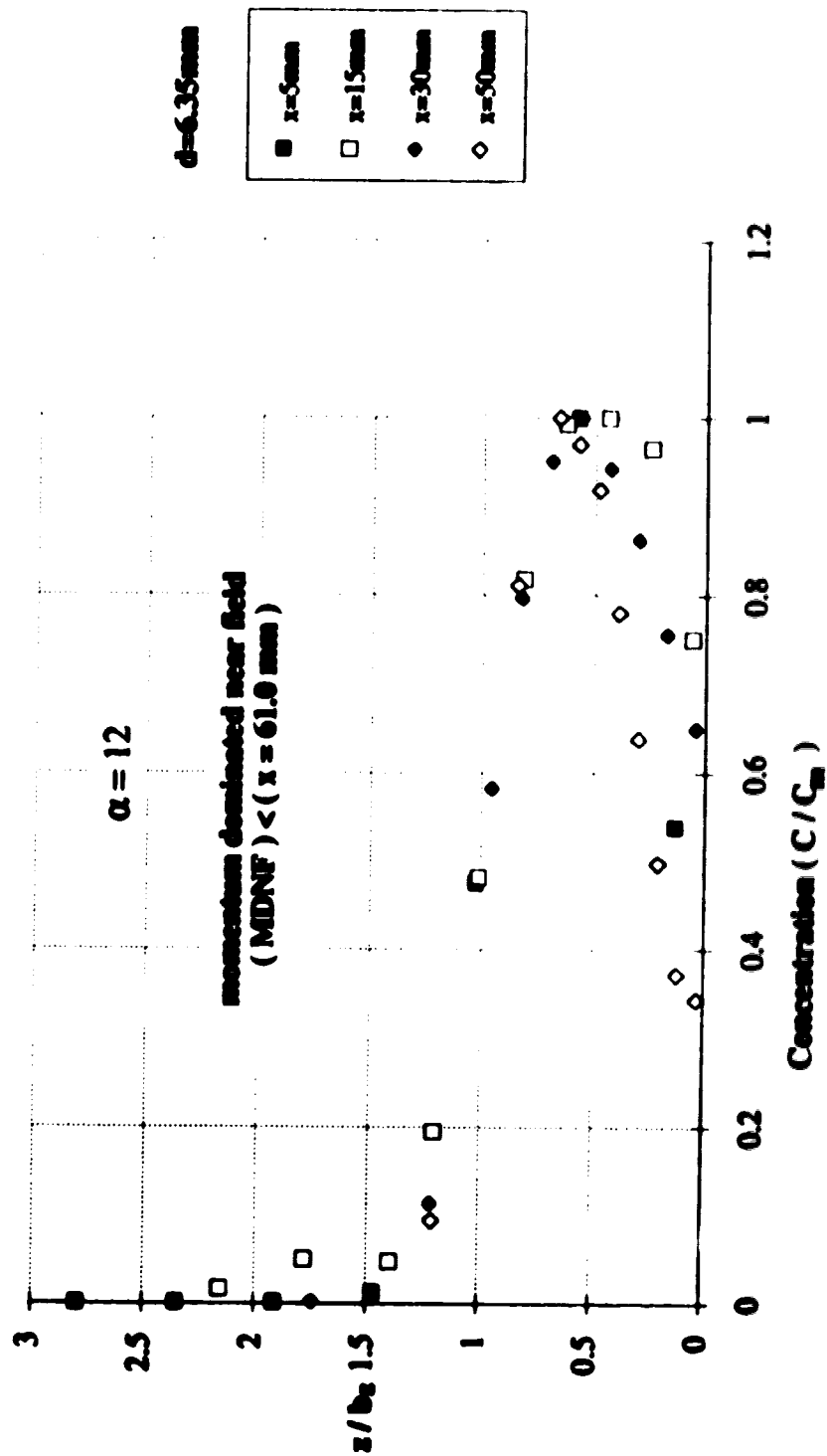


Fig. 4.13 (a) Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction

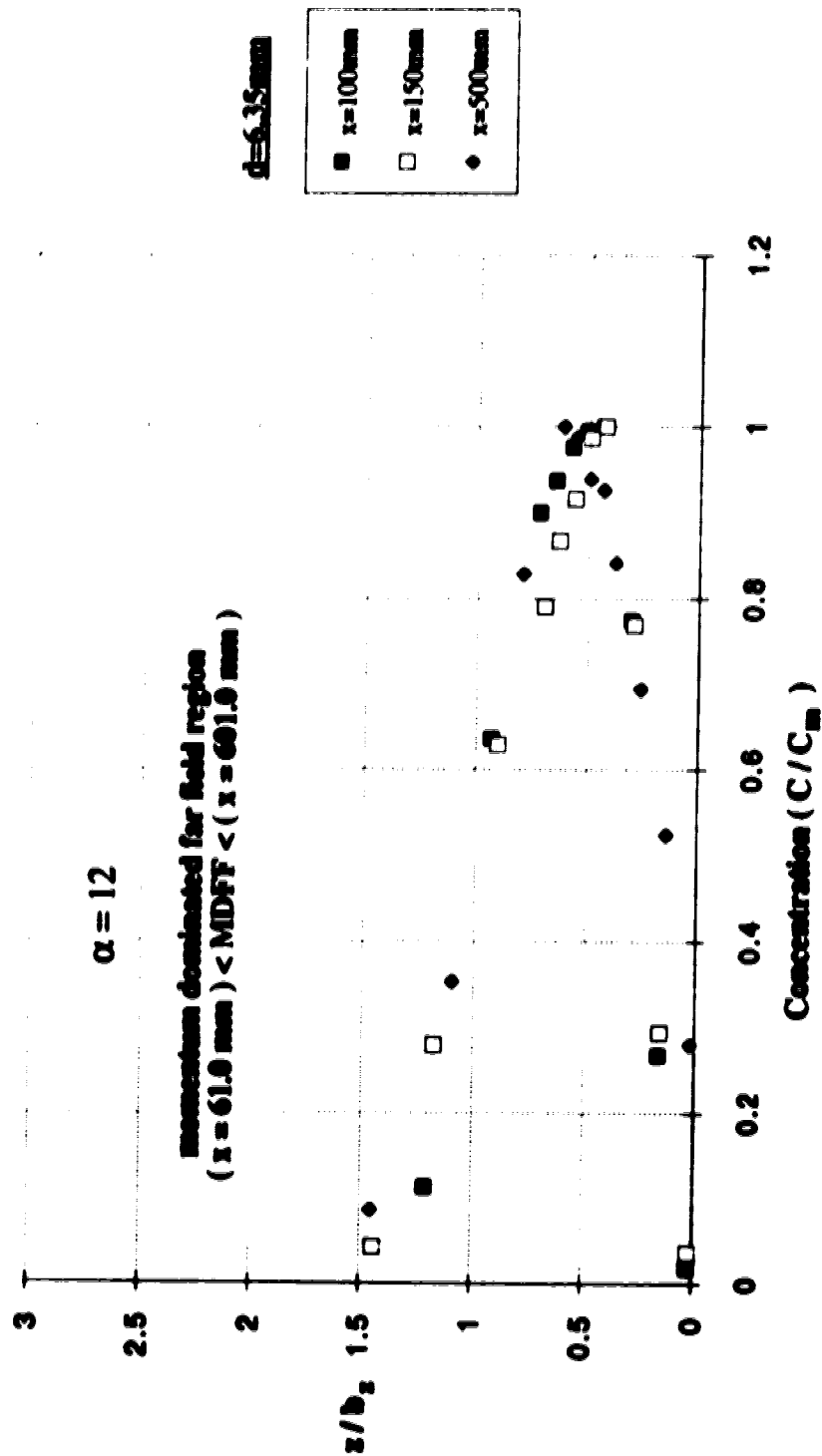


Fig. 4.13 (b) Non - Dimensional Profiles of the Concentration Distribution in the Vertical Direction

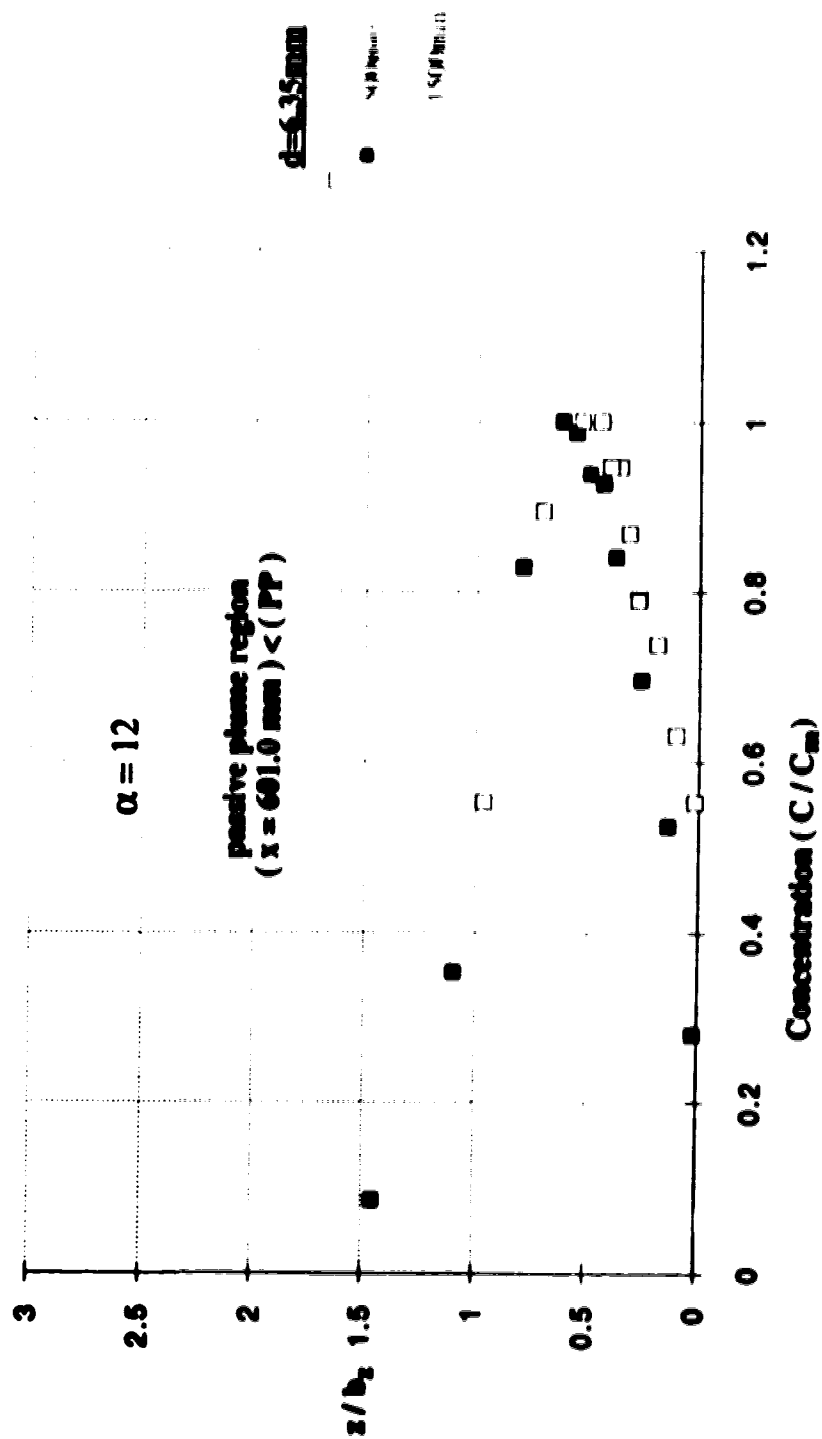
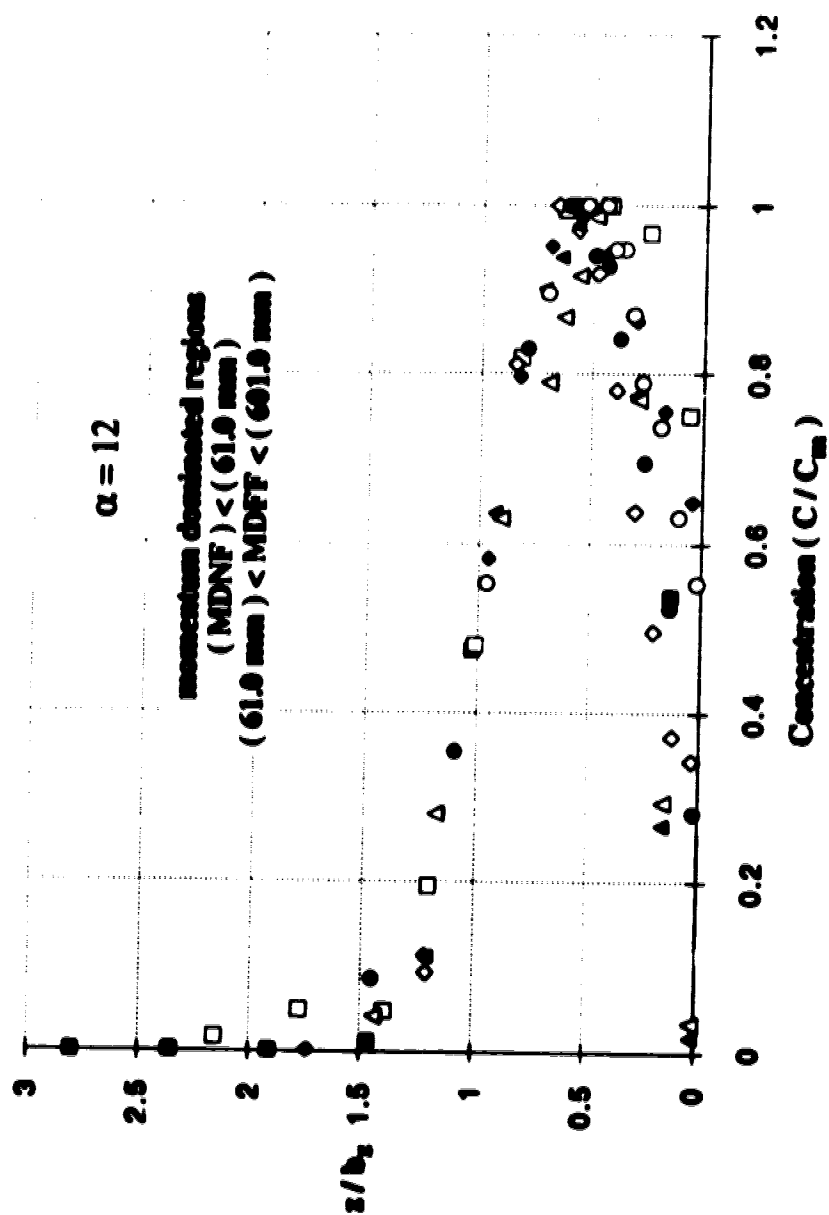


Fig. 4.13 (c) Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction





**Fig. 4.13 (d) Non - Dimensional Profiles of Concentration Distribution in the Vertical Direction**

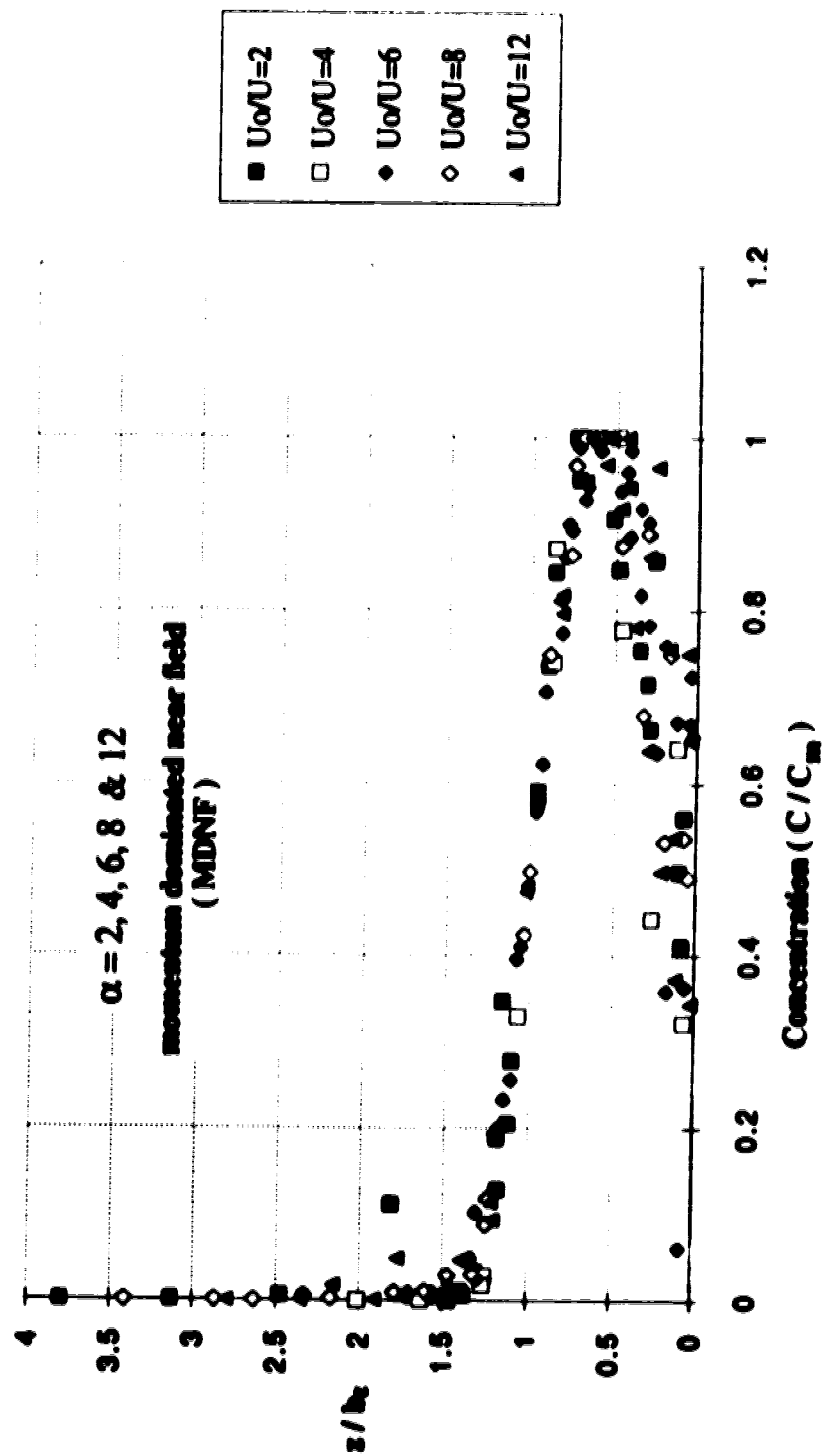


Fig. 4.14 (a) Similarity Profiles of Concentration Distribution in the Vertical Direction

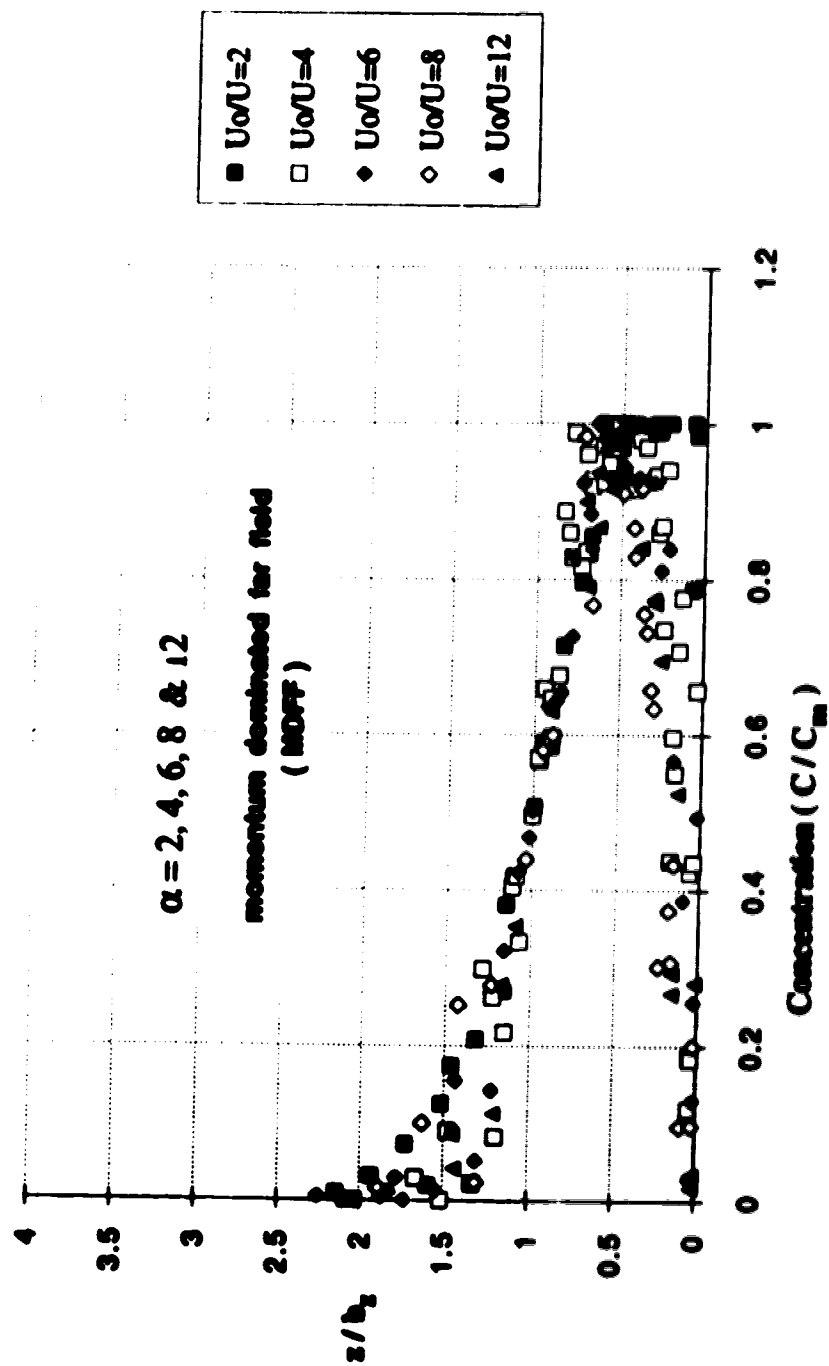


Fig. 4.14 (b) Similarity Profiles of Concentration Distribution in the Vertical Direction

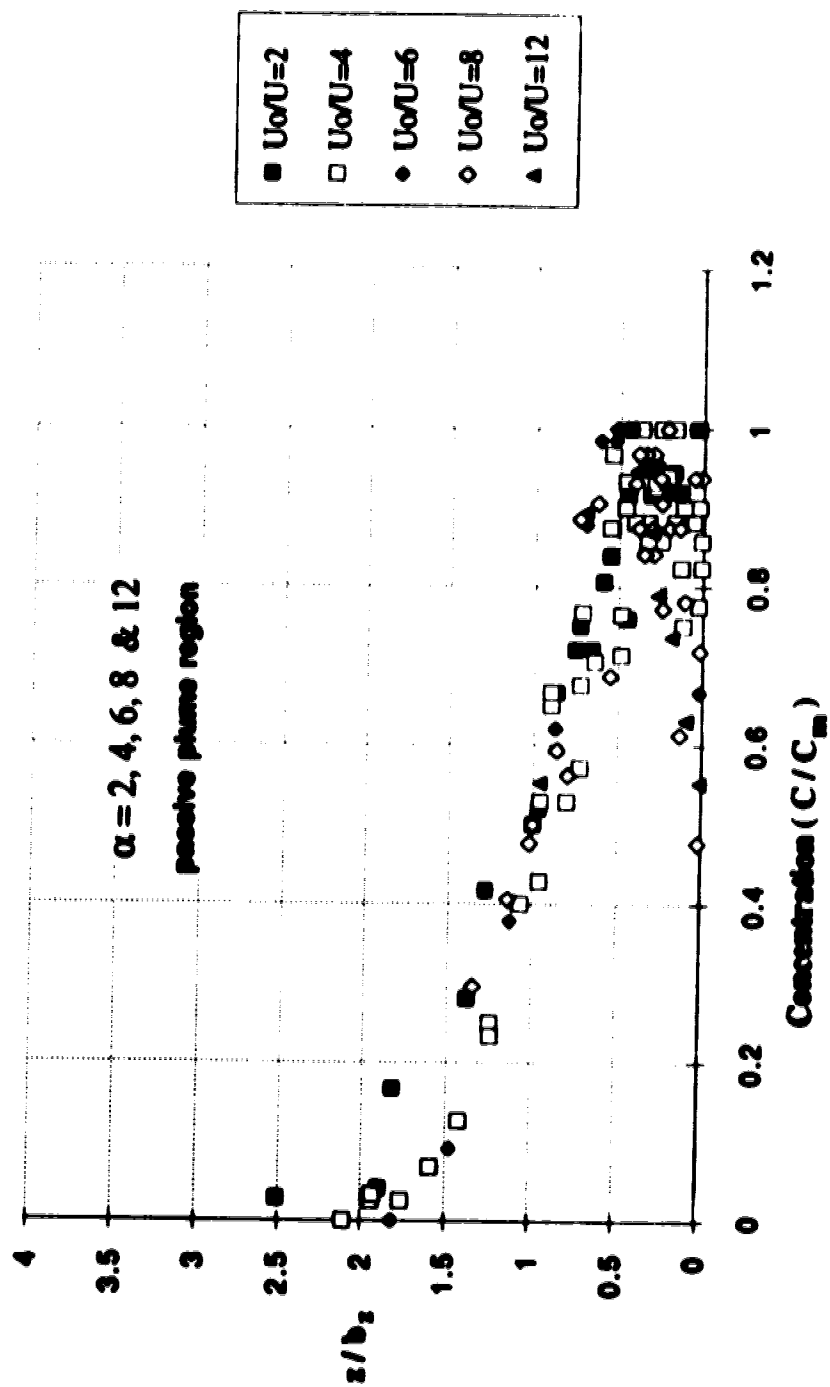


Fig. 4.14 (c) Similarity Profiles of Concentration Distribution in the Vertical Direction

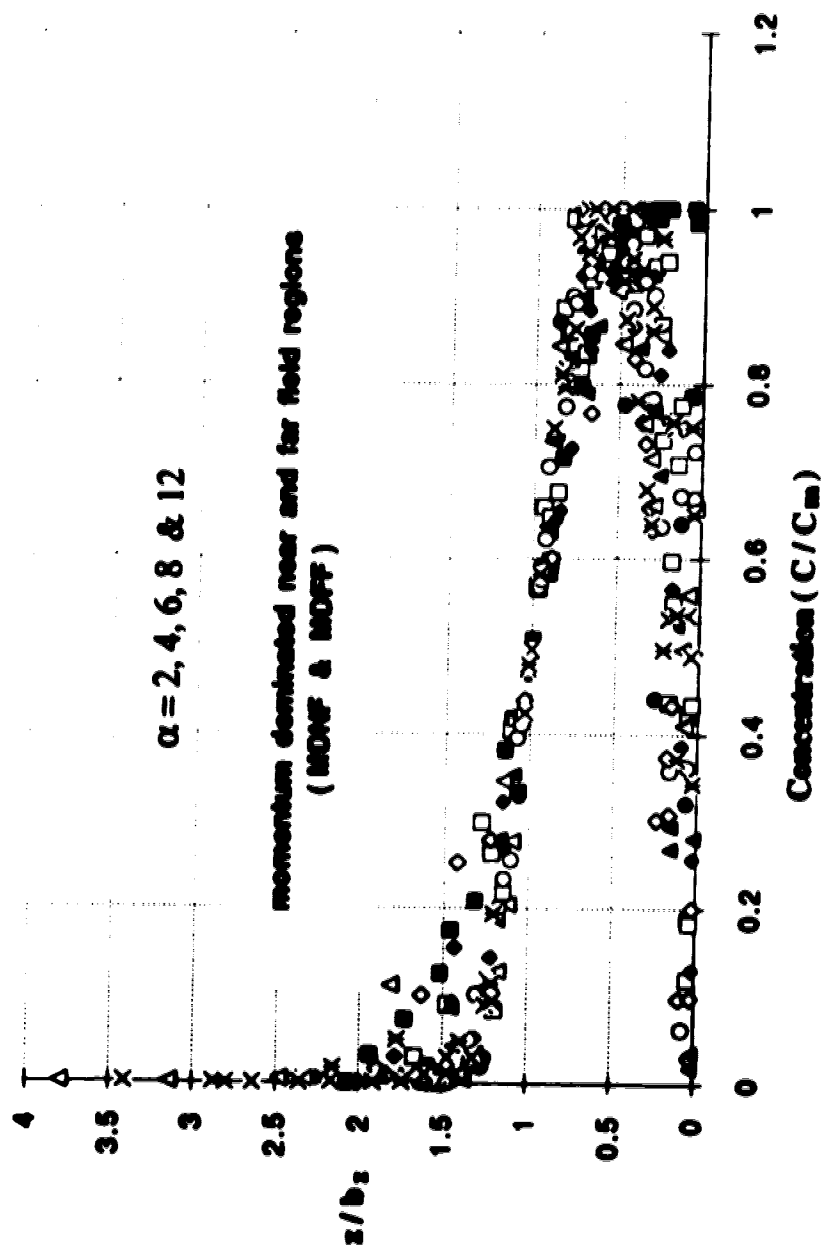


Fig. 4.14(d) Similarity Profiles of Concentration Distribution in the Vertical Direction

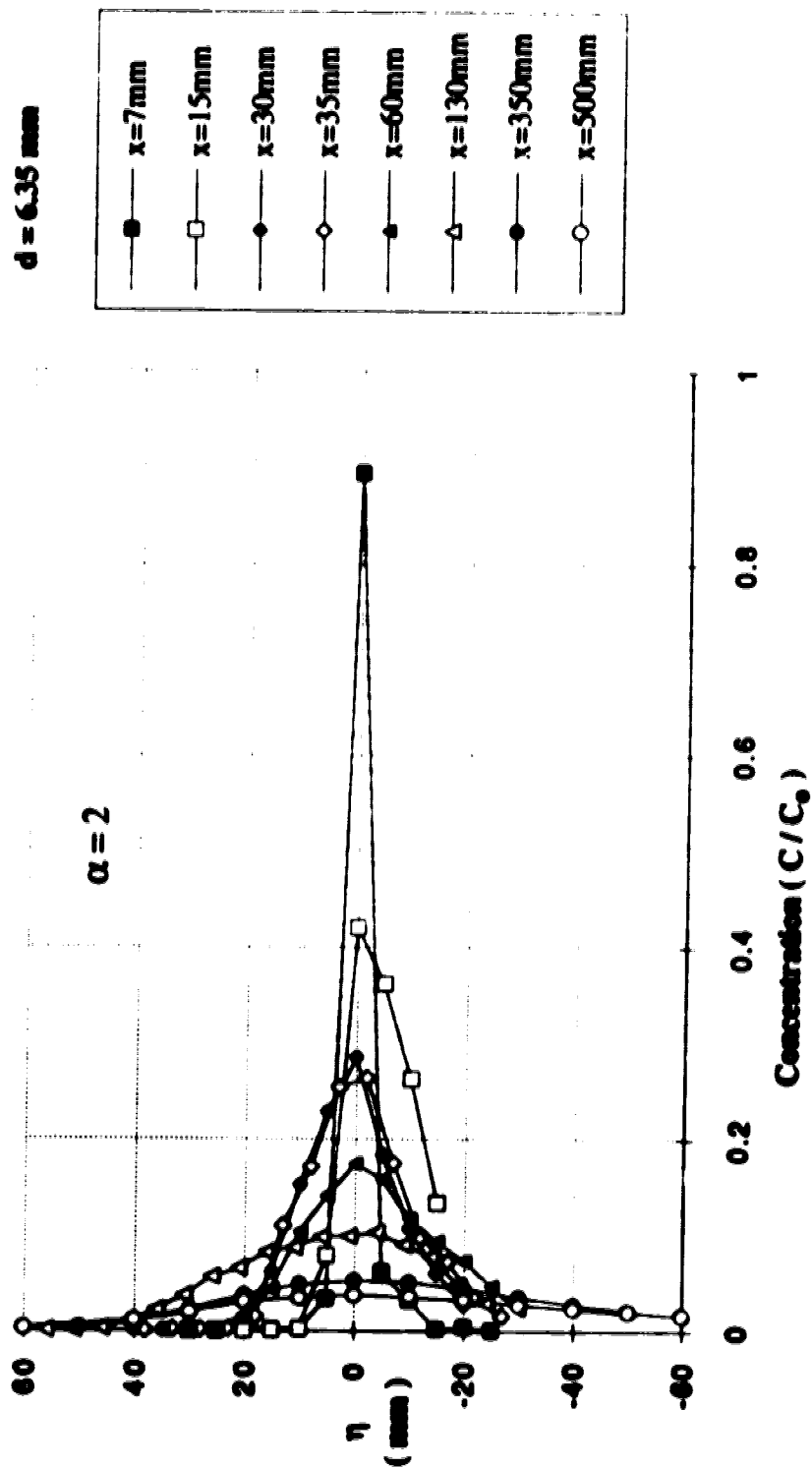
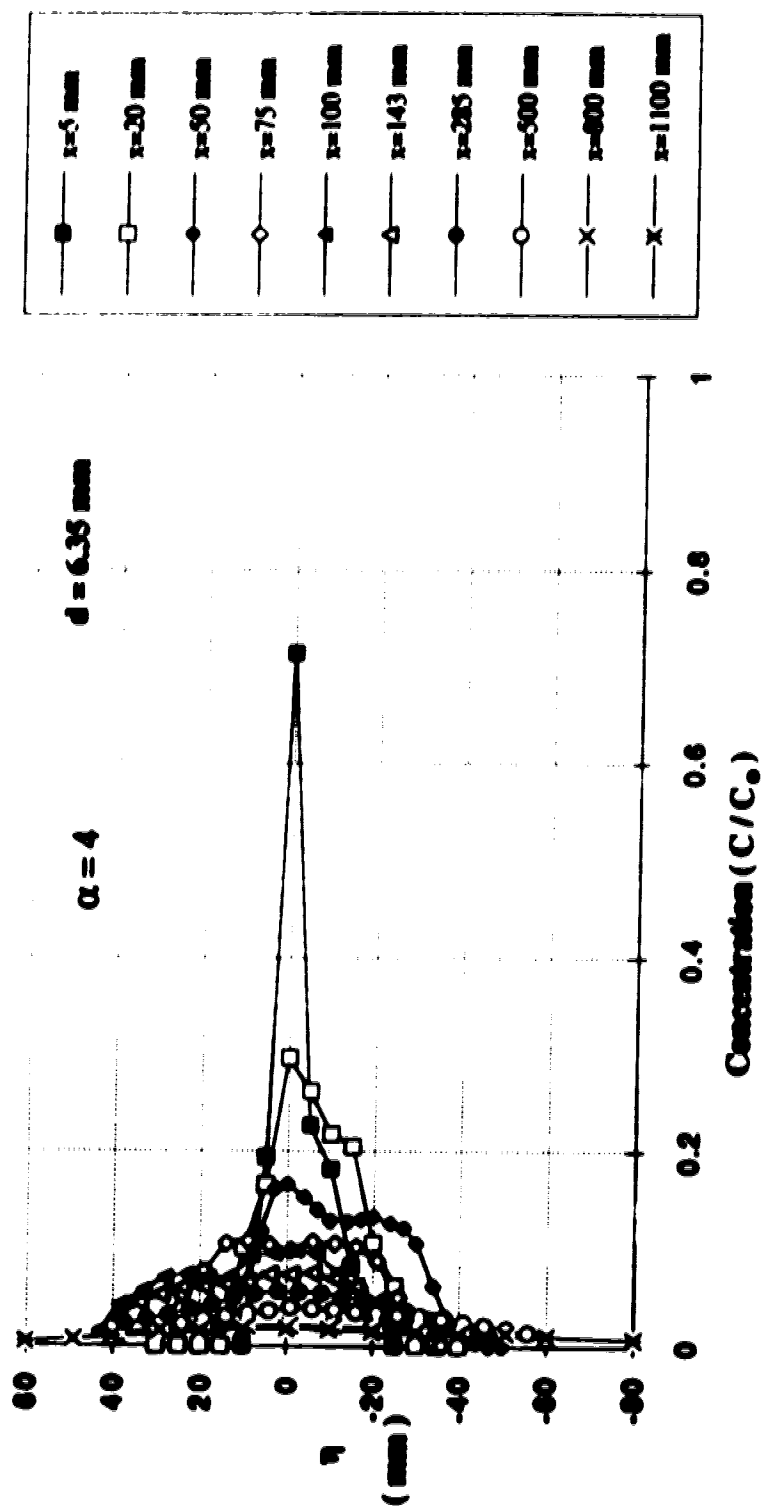


Fig. 4.15 Transverse Concentration Profiles Perpendicular to the Jet Axis



**Fig. 4.16 Transverse Concentration Profiles Perpendicular to the Jet Axis**

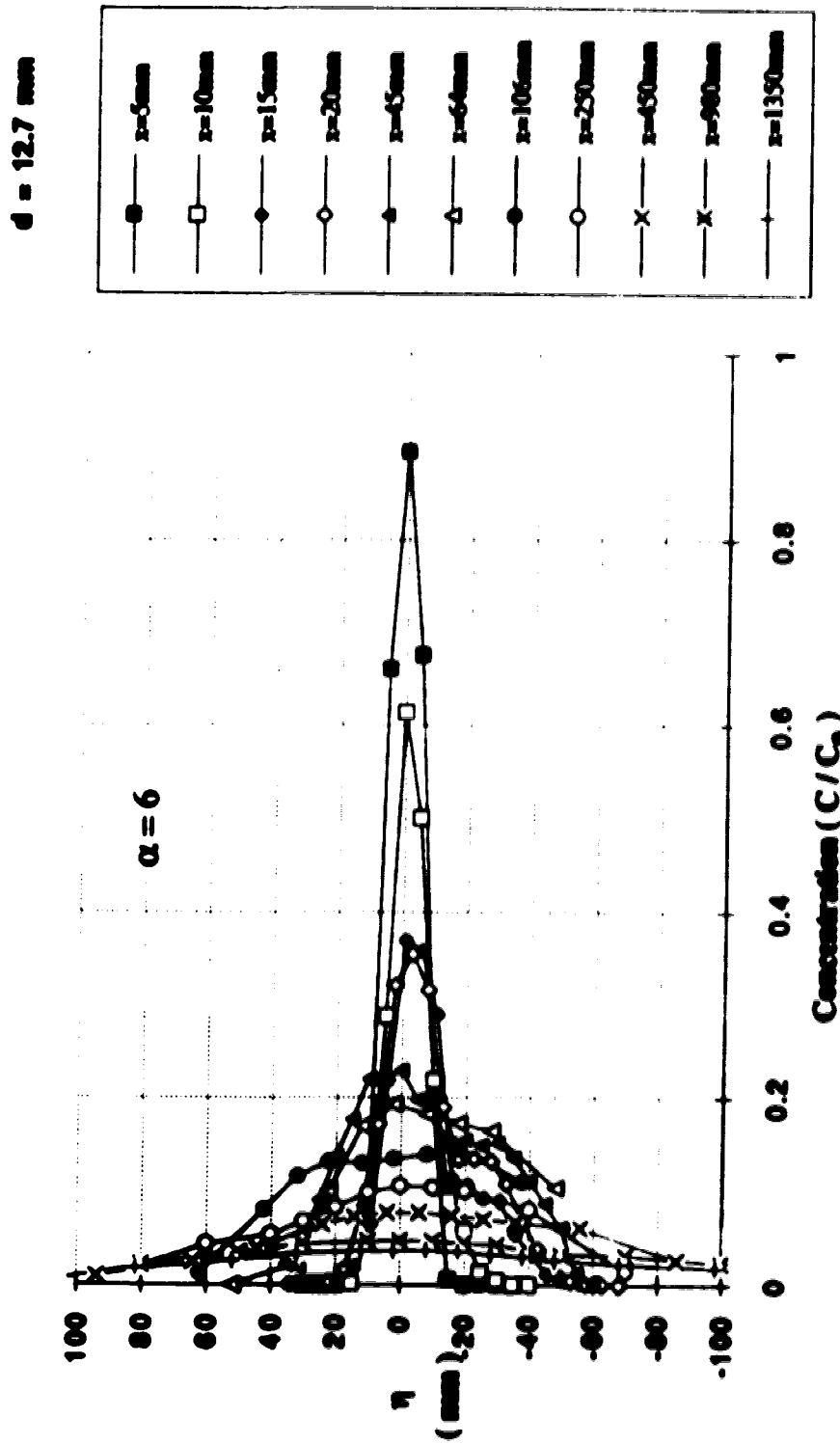


Fig. 4.17 Transverse Concentration Profiles Perpendicular to the Jet Axis



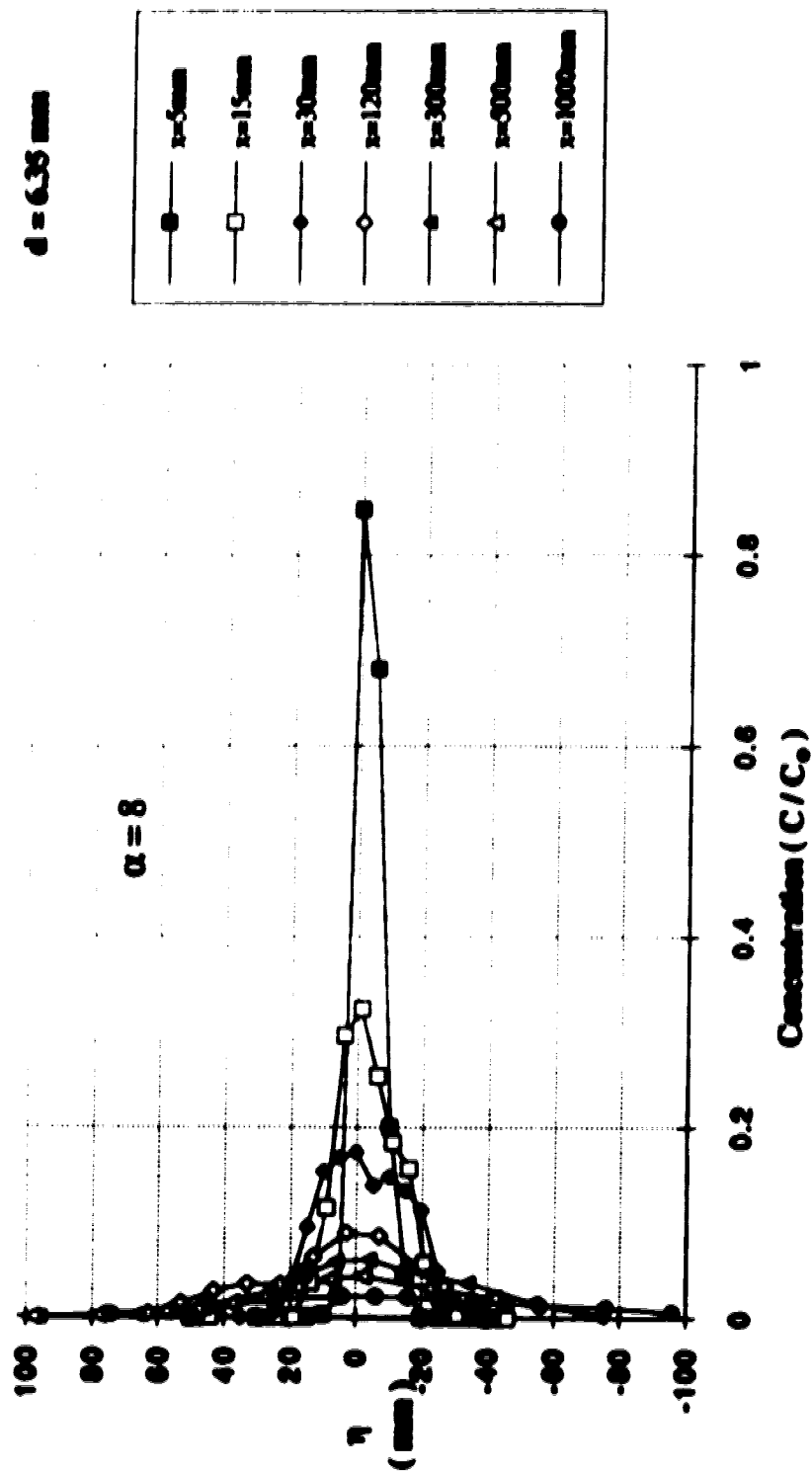


Fig. 4.13 Transverse Concentration Profiles Perpendicular to the Jet Axis

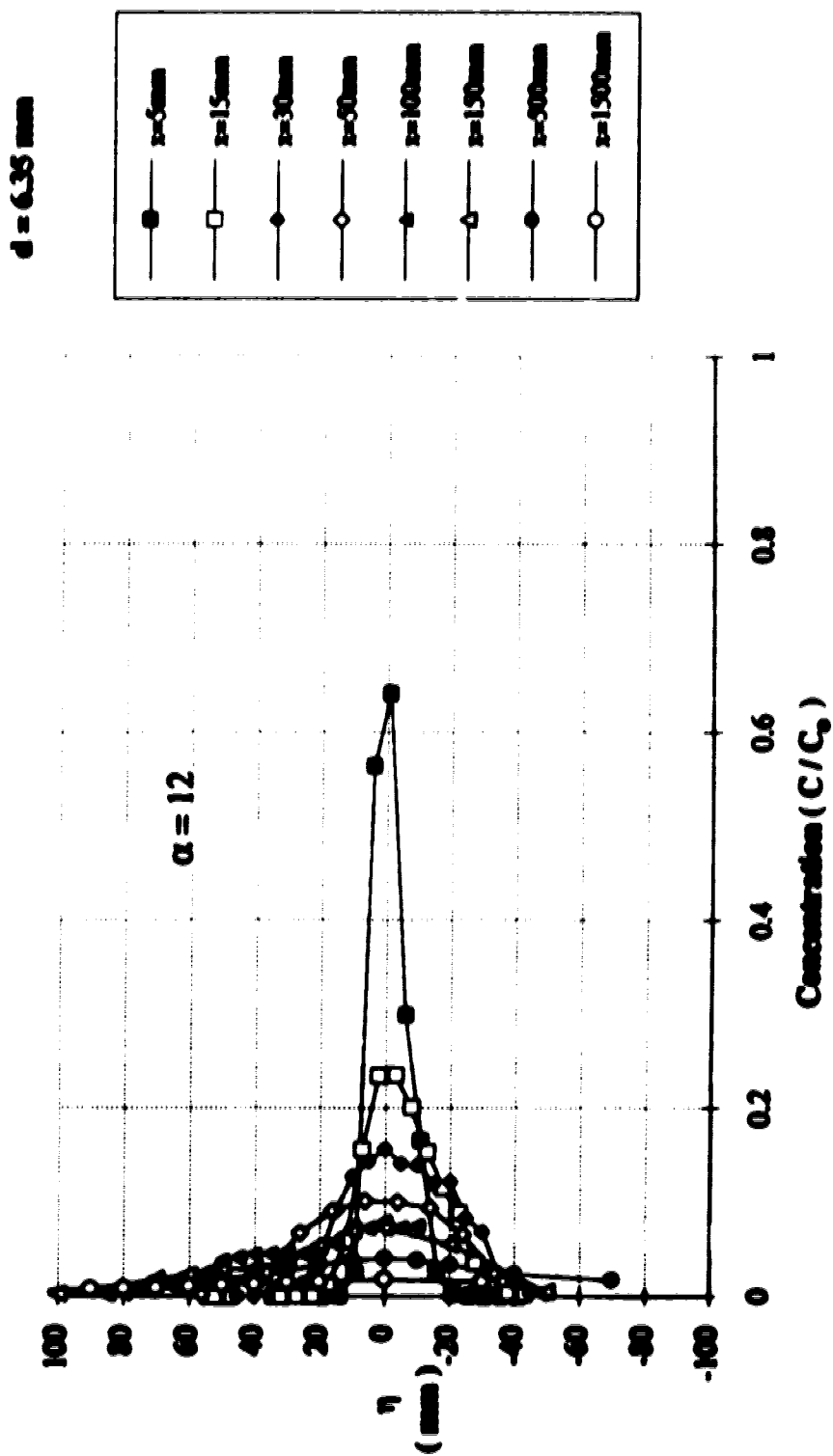


Fig. 4.19 Transverse Concentration Profiles Perpendicular to the Jet Axis

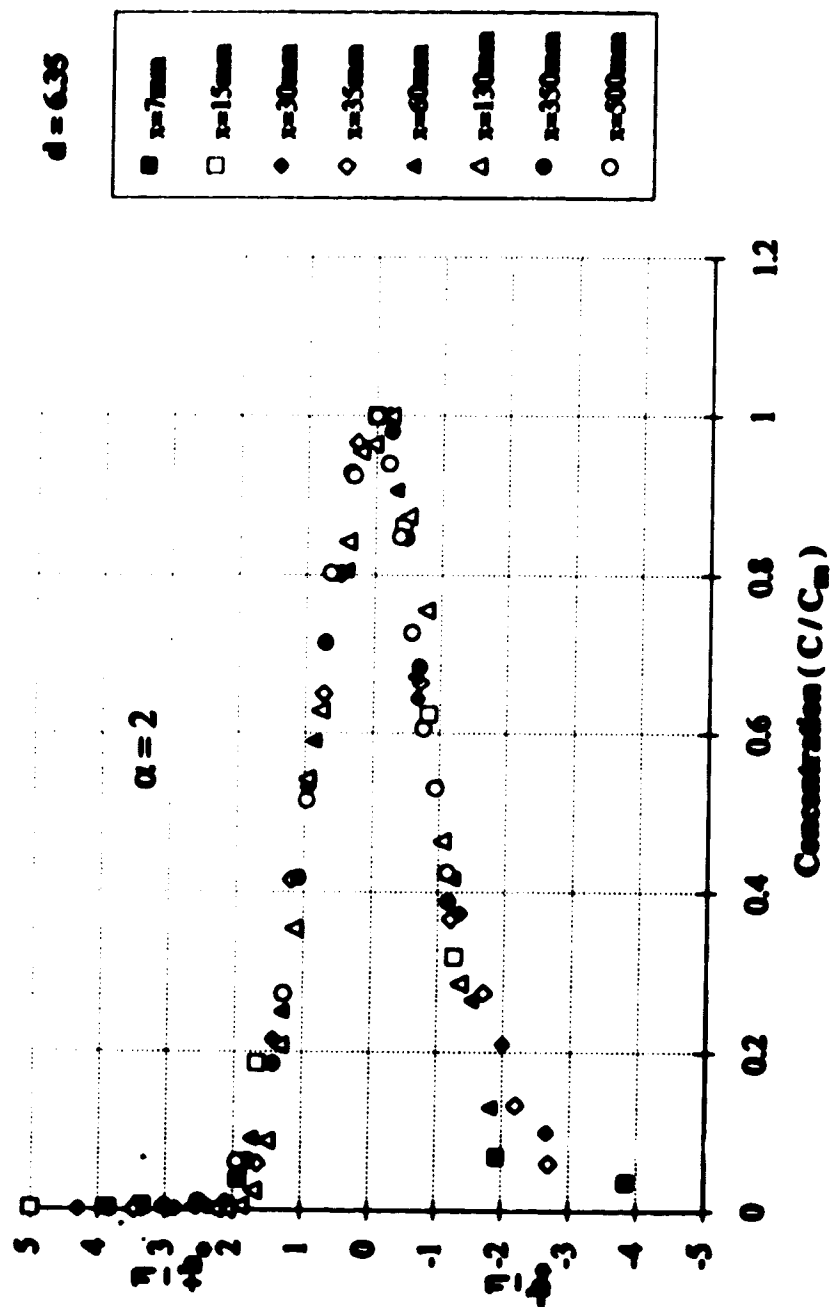
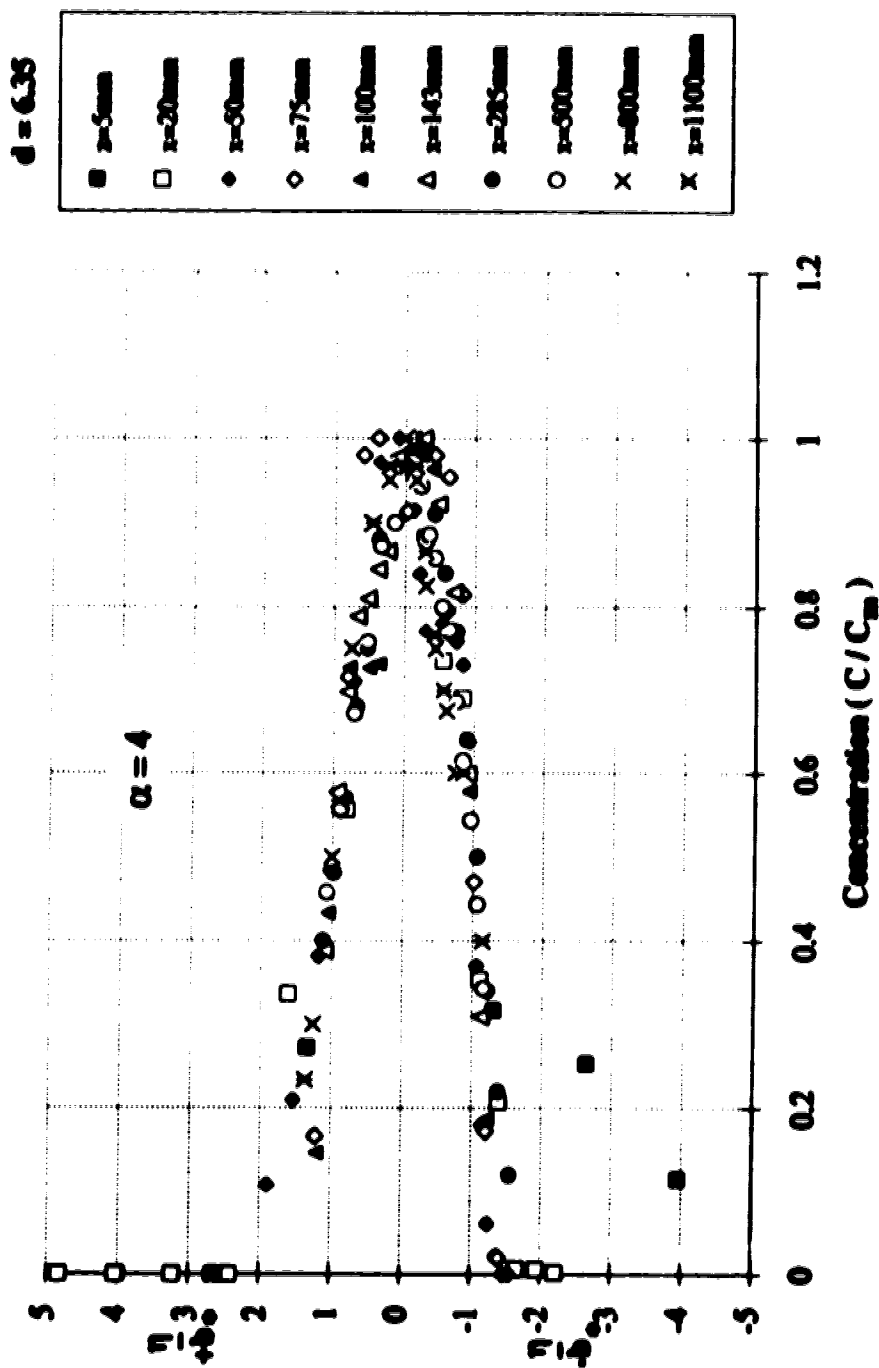


Fig. 4.20 Non - Dimensional Profiles of Concentration Distribution in the Transverse Direction



**Fig. 4.21 Non - Dimensional Profiles of Concentration Distribution in the Transverse Direction**

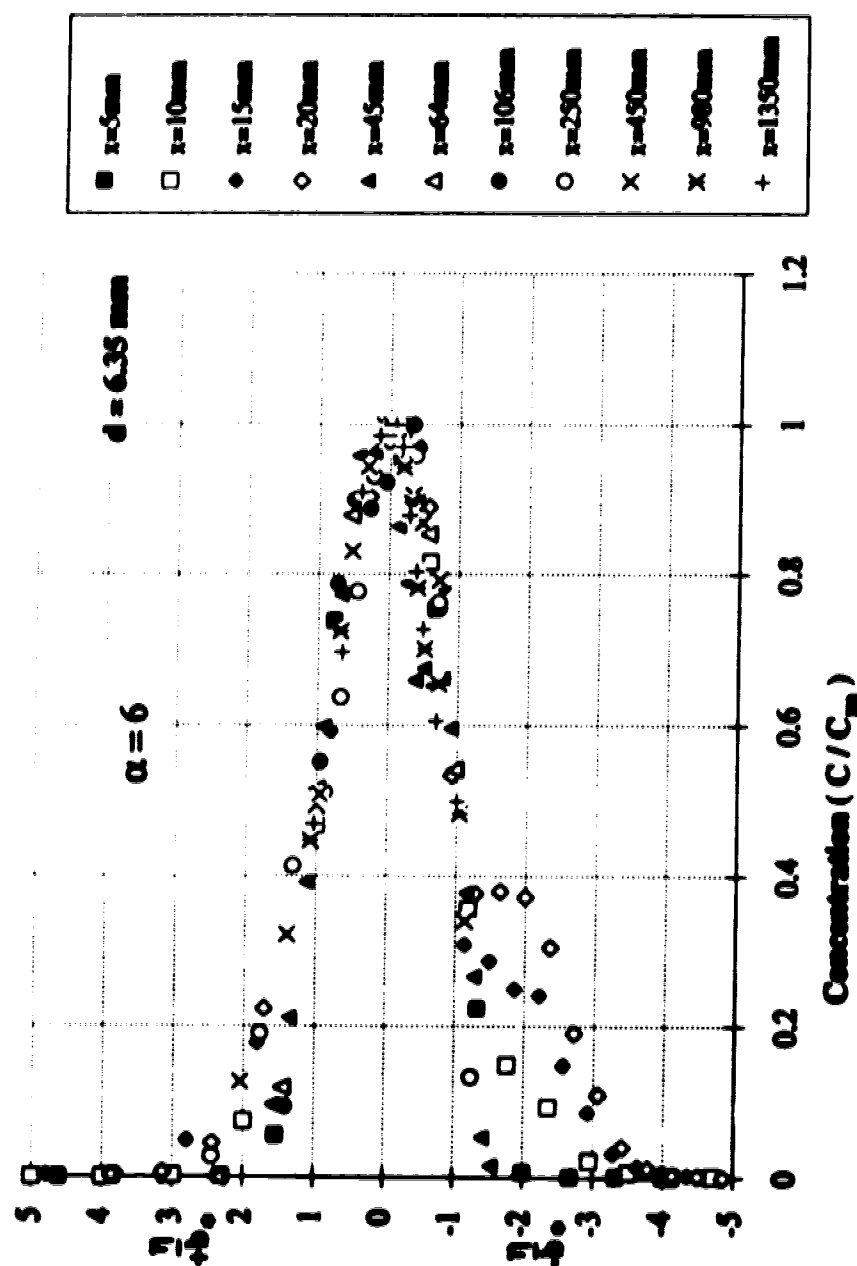
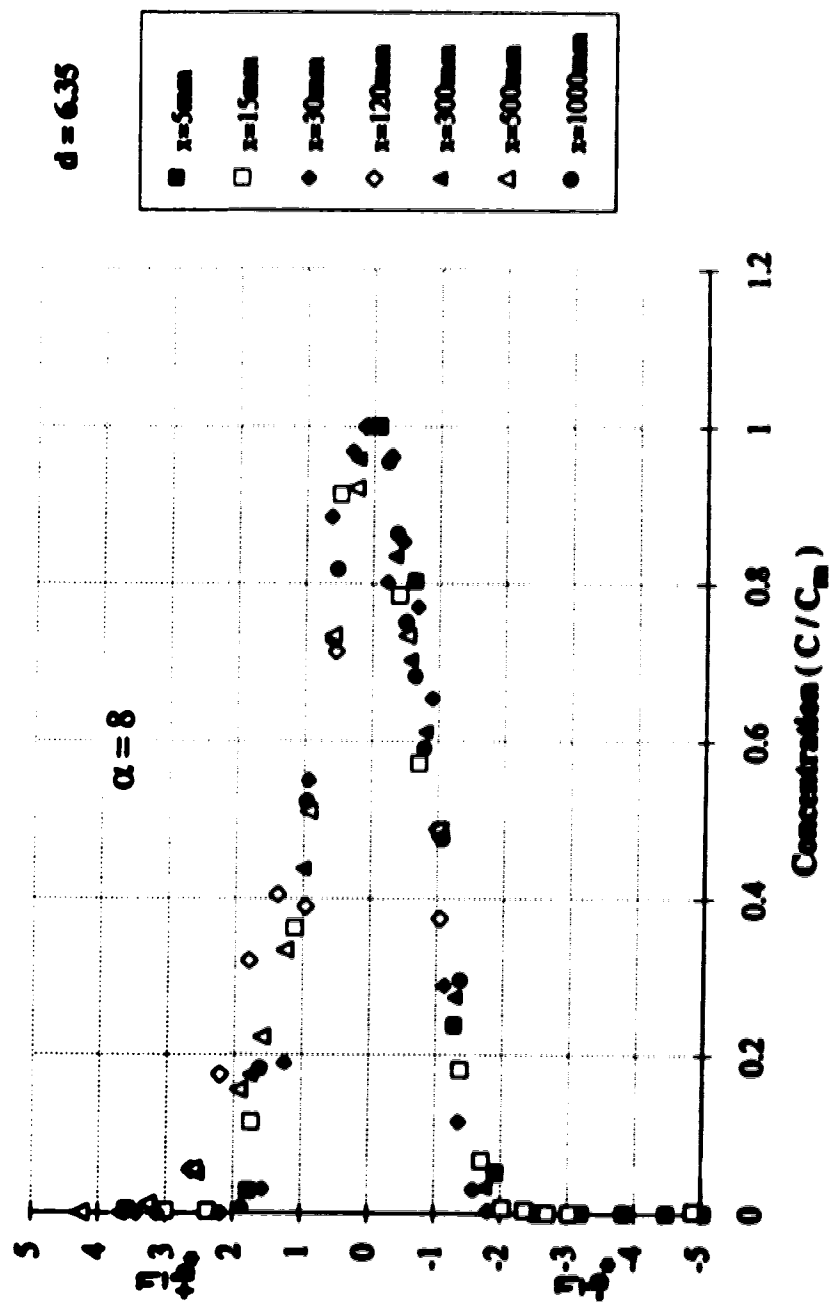
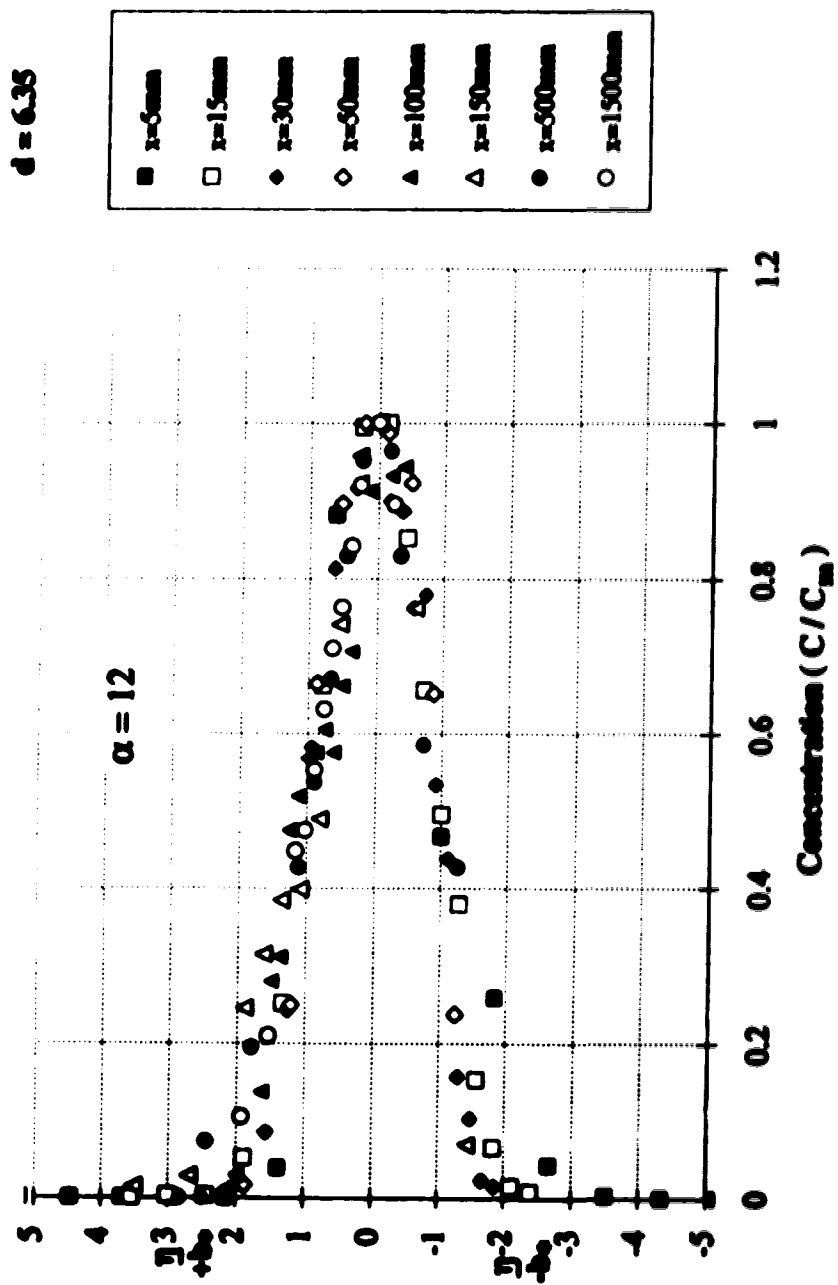


Fig. 4.22 Non - Dimensional Profiles of Concentration Distribution in the Transverse Direction



**Fig. 4.23 Non - Dimensional Profiles of Concentration Distribution in the Transverse Direction**



**Fig. 4.24 Non - Dimensional Profiles of Concentration Distribution in the Transverse Direction**

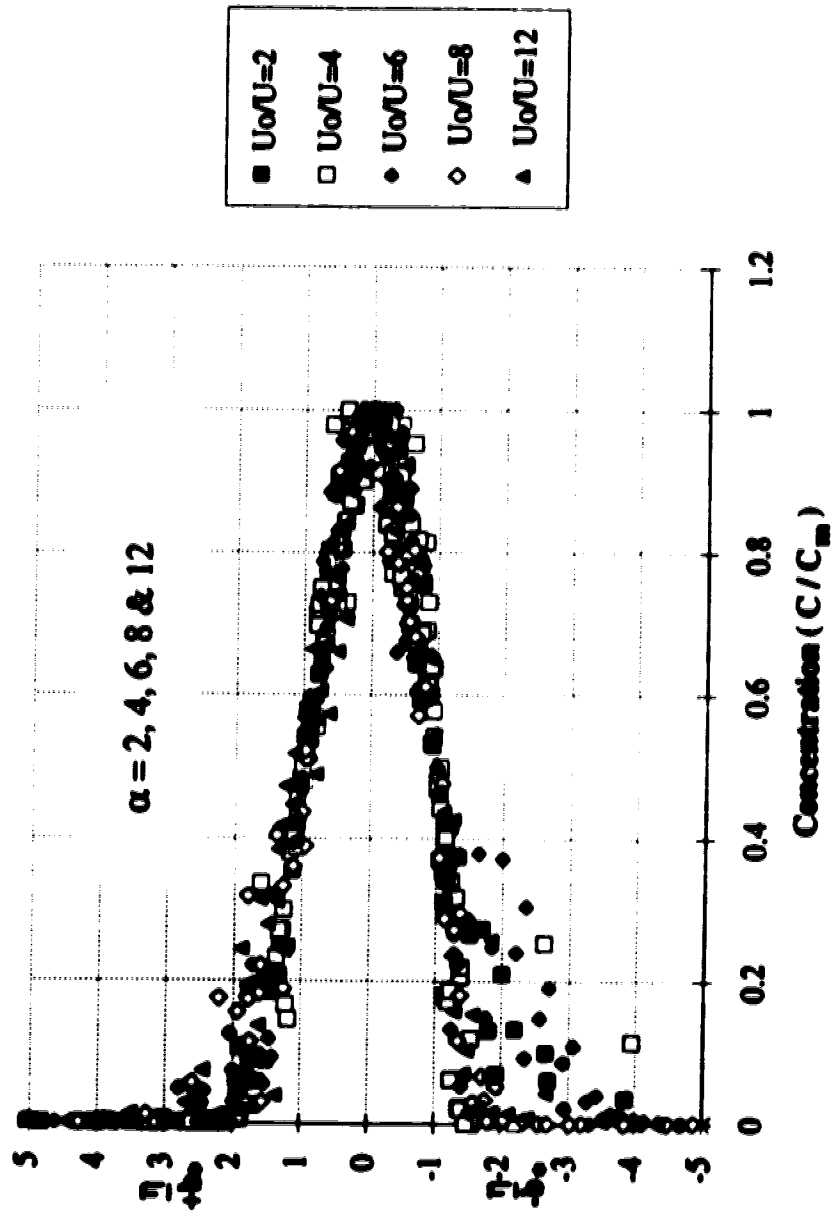


Fig. 4.25 Similarity Profiles of Concentration Distribution in the Transverse Direction



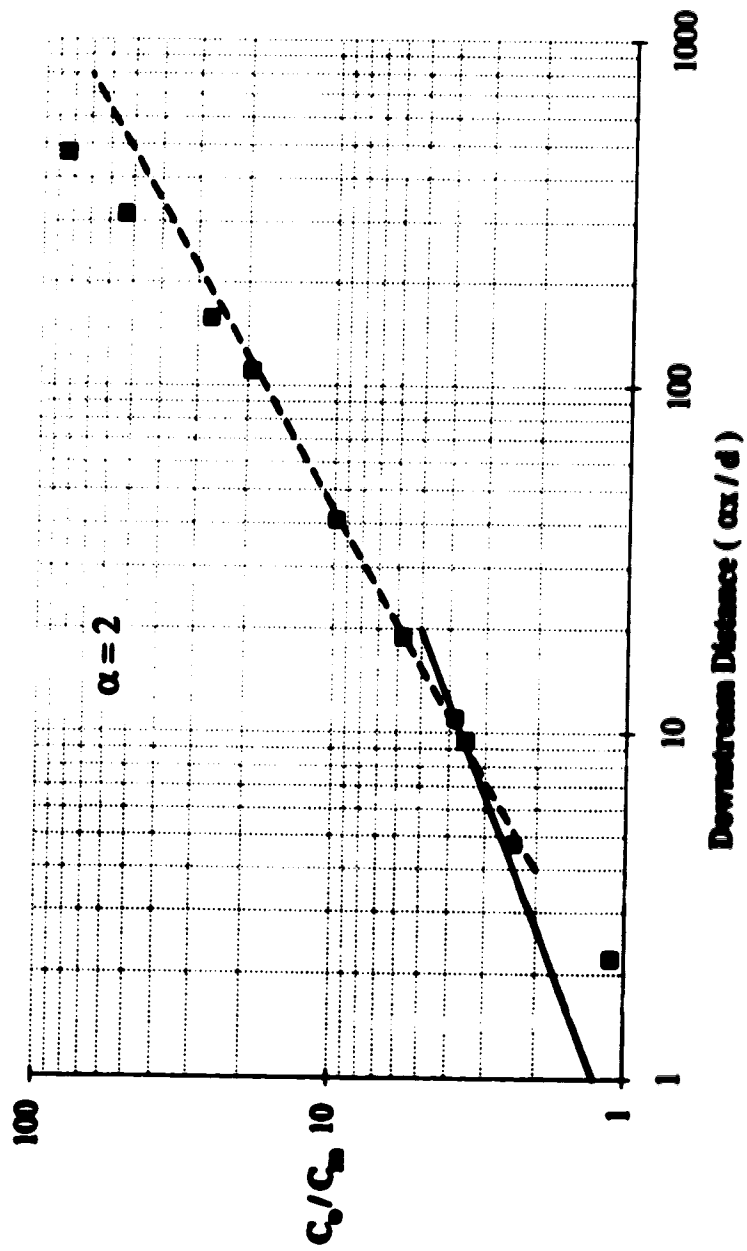


Fig. 4.26 Characteristic Minimum Diffusion of the Deflected Jet

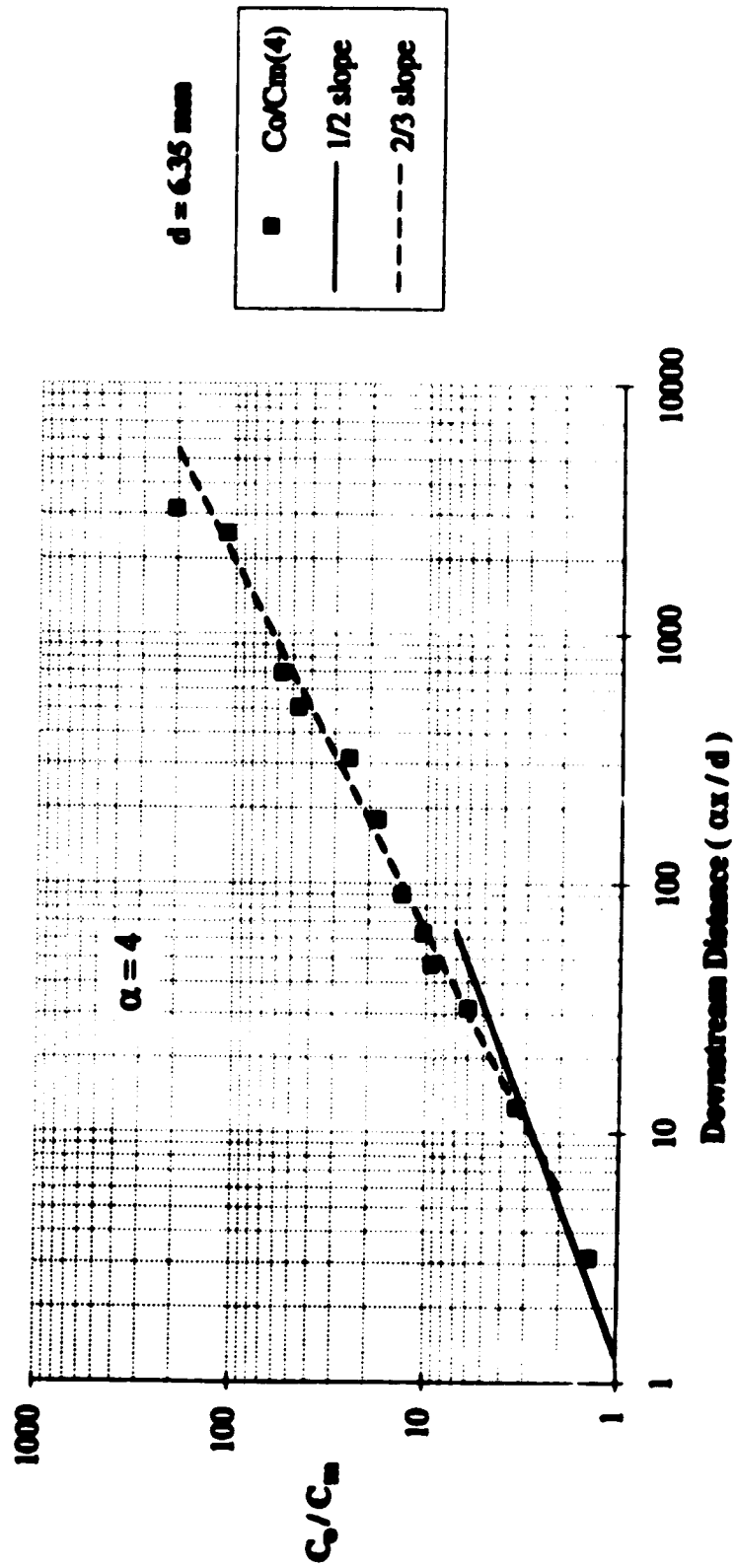


Fig. 4.27 Characteristic Minimum Division of the Deflected Jet

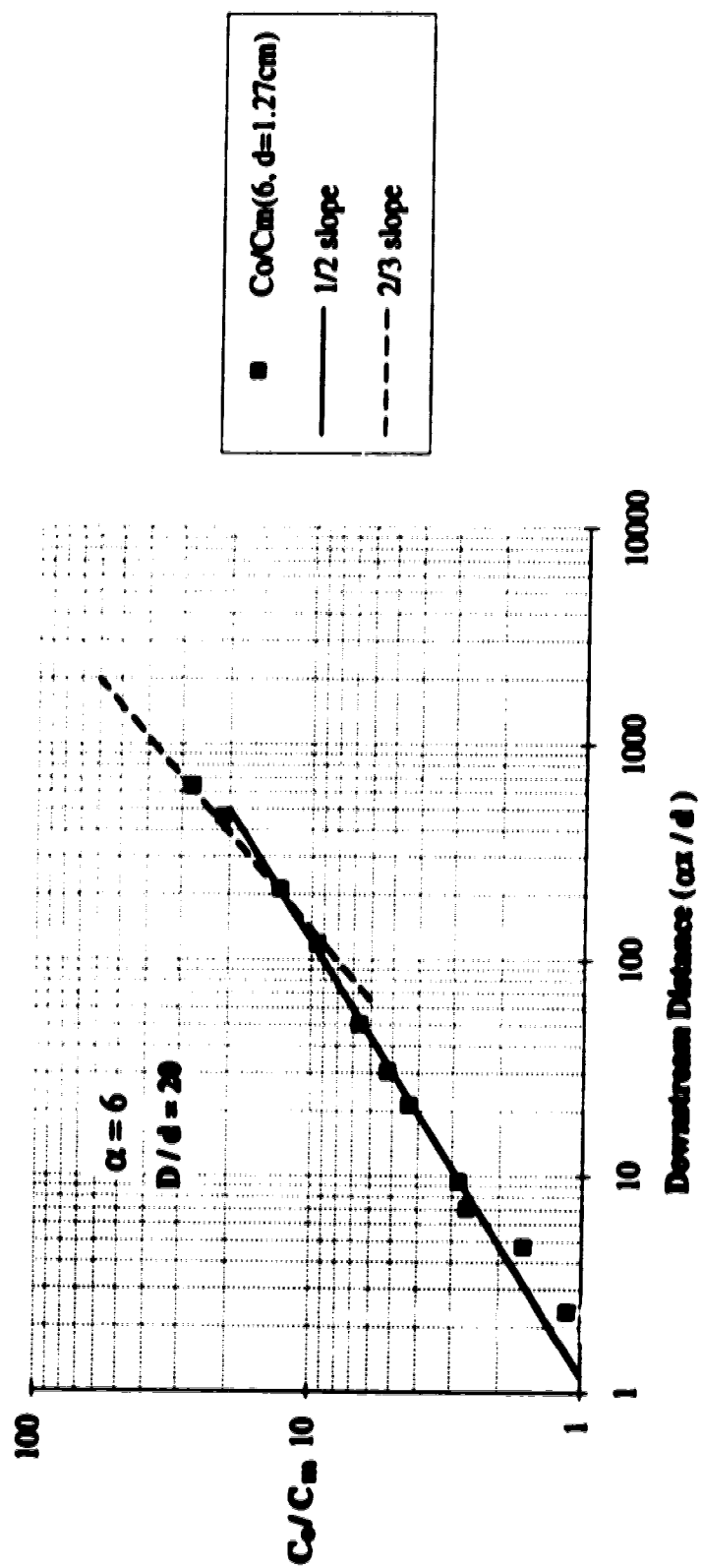


Fig. 4.28 (a) Characteristic Minimum Division of the Deflected Jet

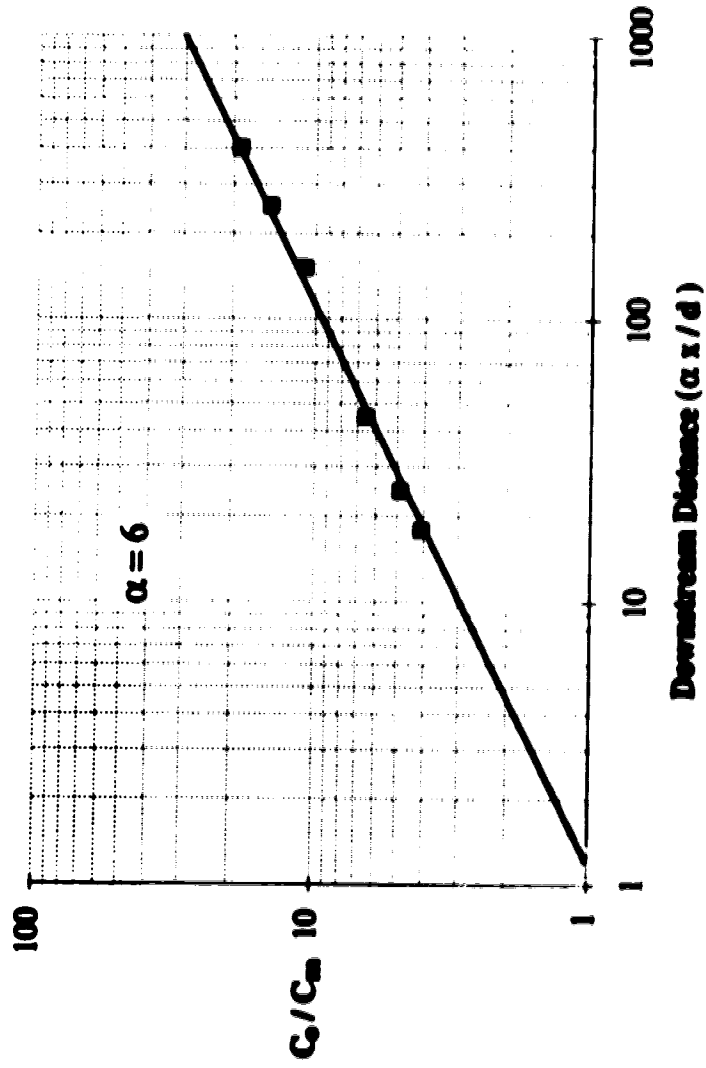


Fig. 4.28 (b) Characteristic Minimum Diffusion of the Deflected Jet

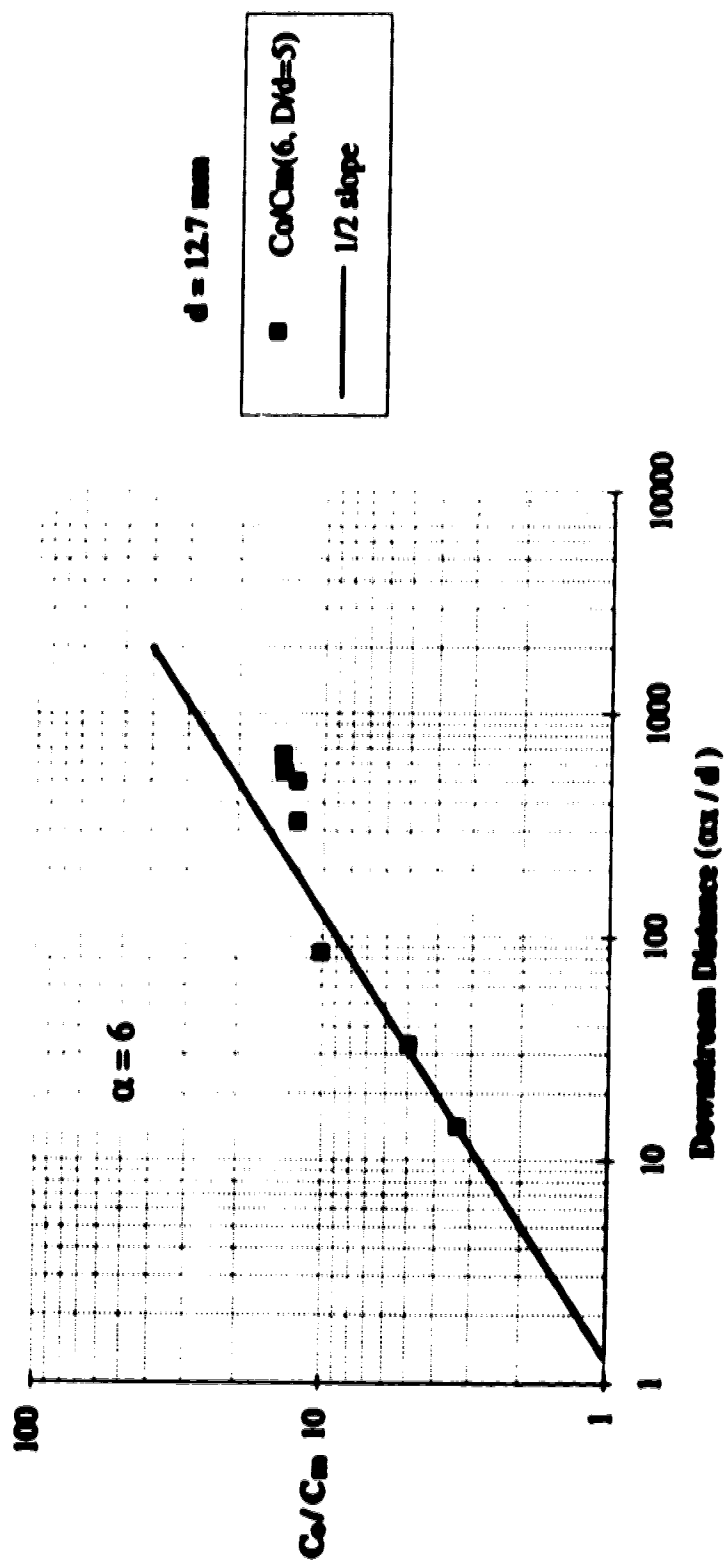


FIG. 4.28 (c) Characteristic Minimum Diffusion of the Deflected Jet

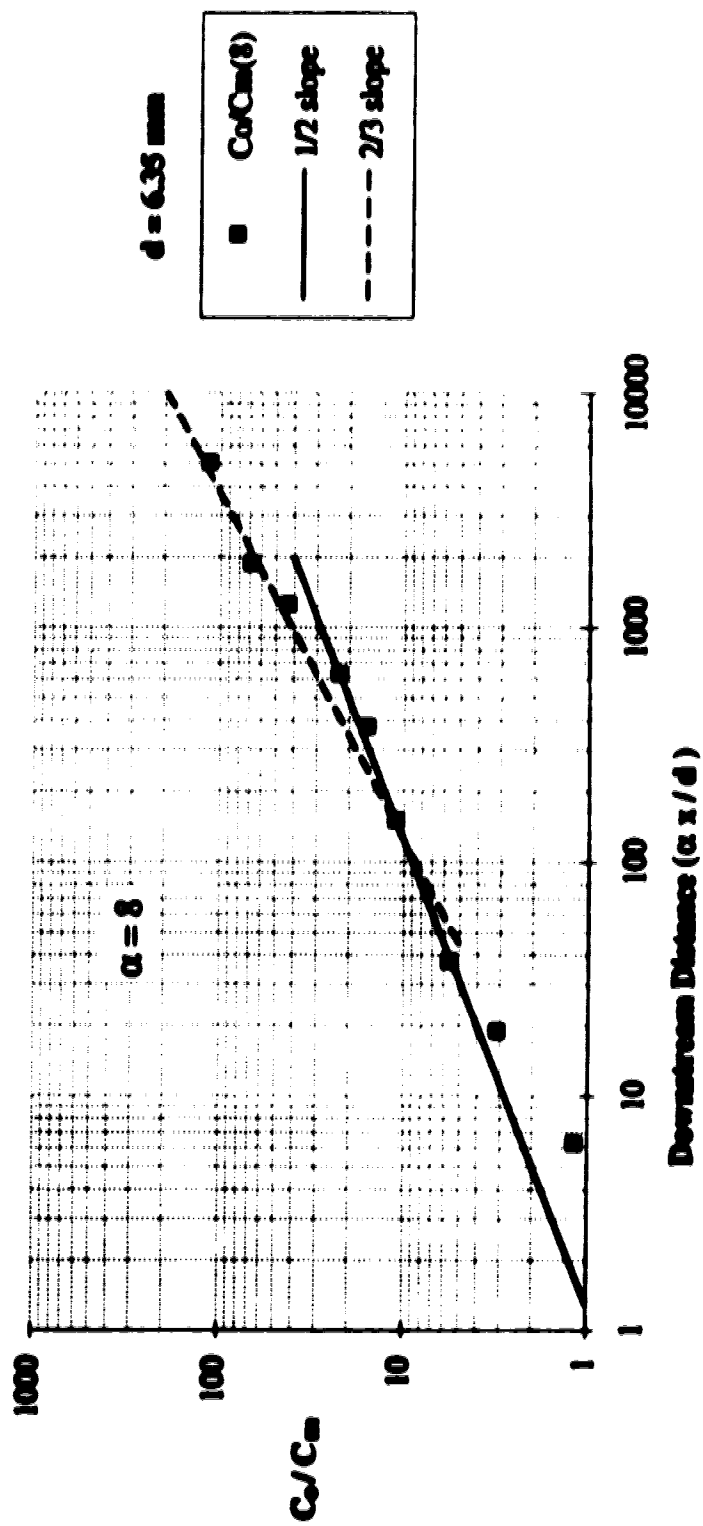


Fig. 4.29 Characteristic Minimum Dilution of the Deflected Jet

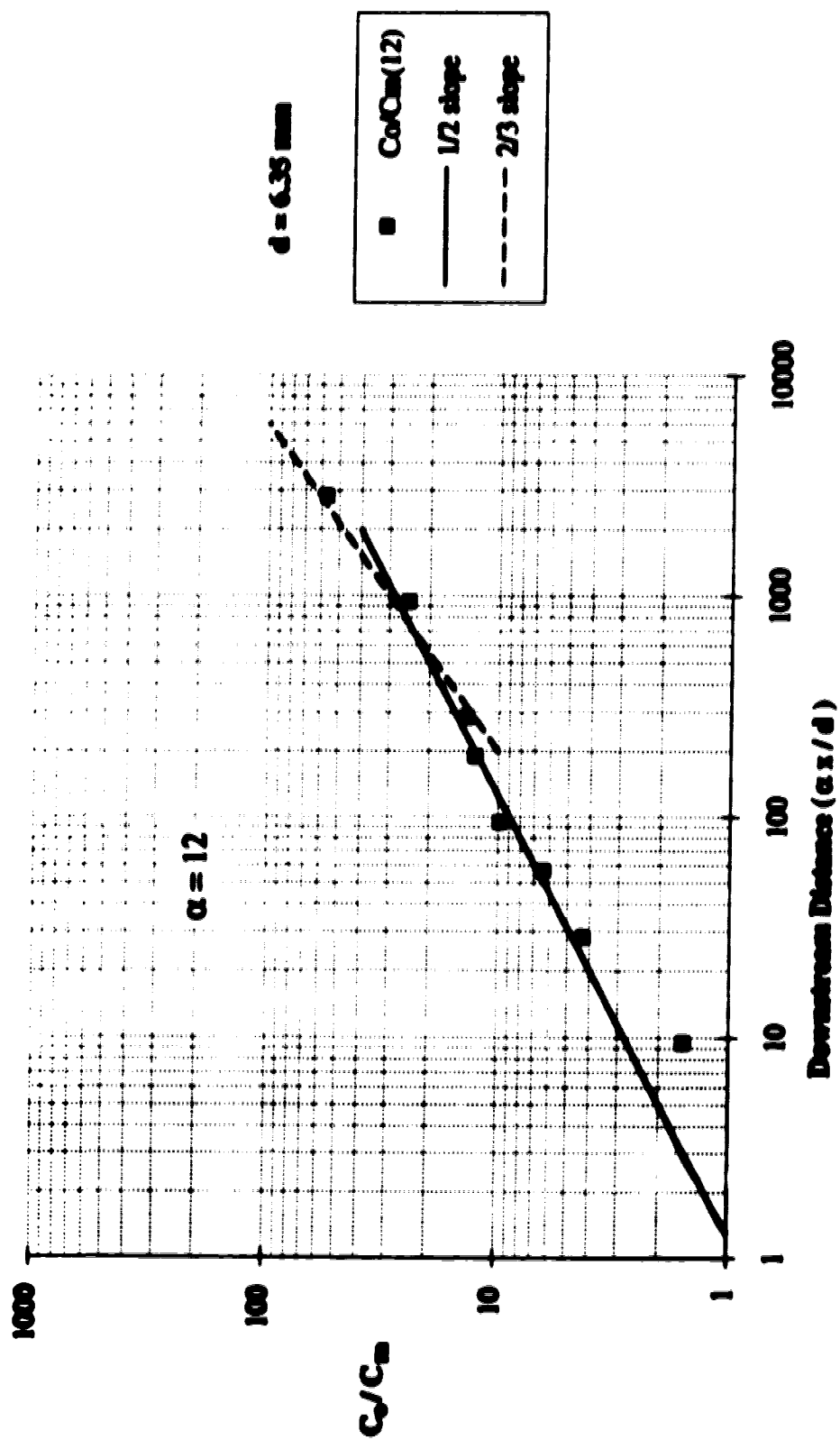


Fig. 4.39 (a) Characteristic Minimum Division of the Deflected Jet

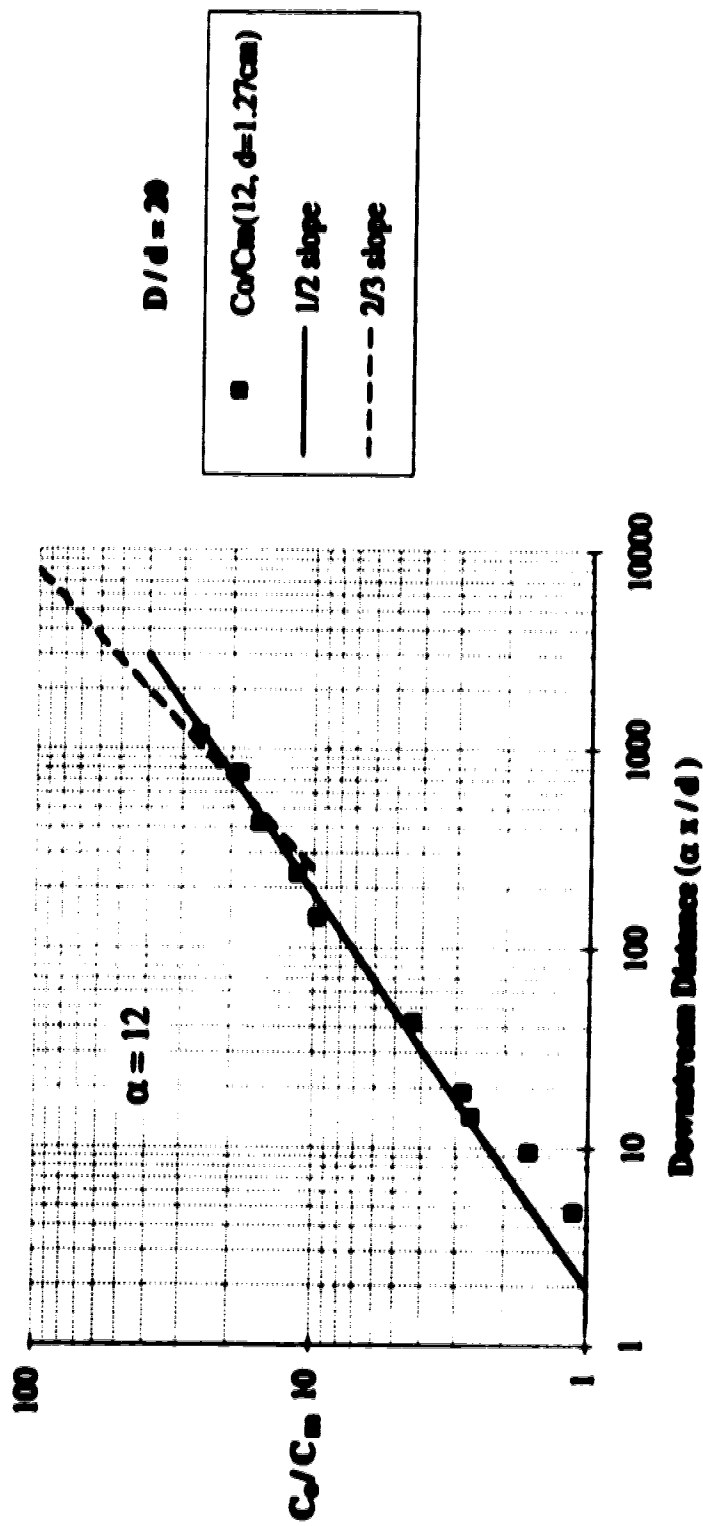


Fig. 4.39 (b) Characteristic Minimum Diffusion of the Deflected Jet



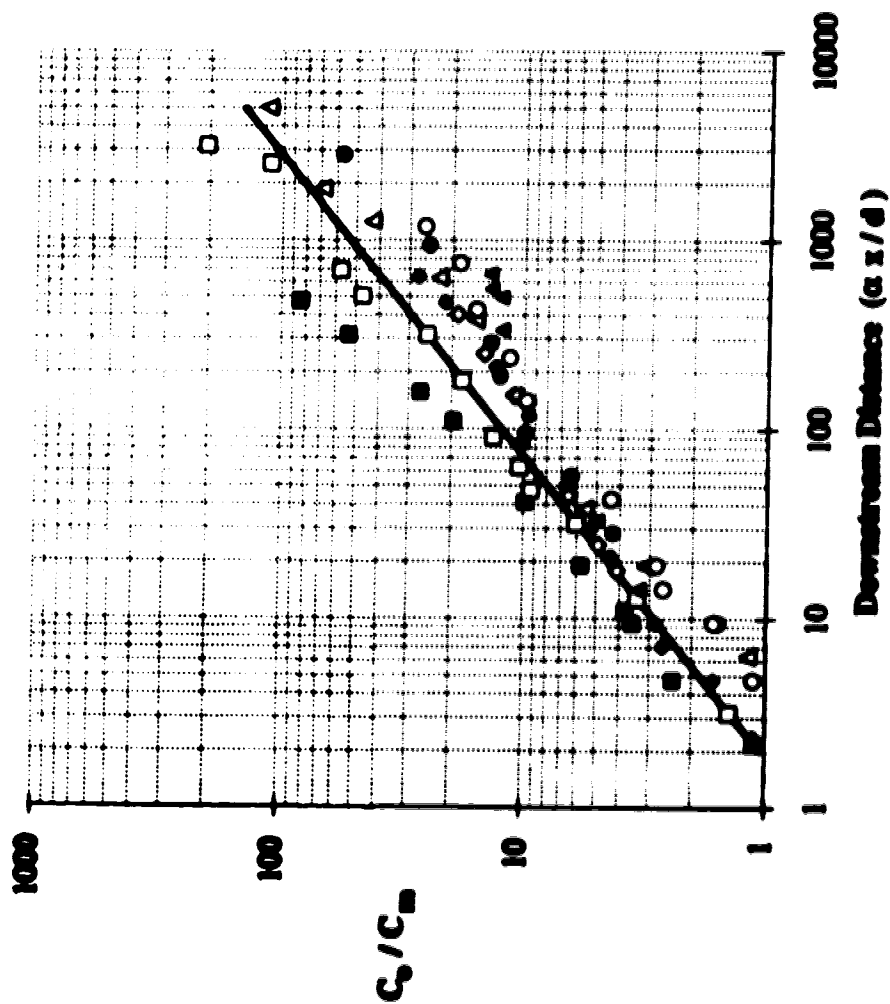
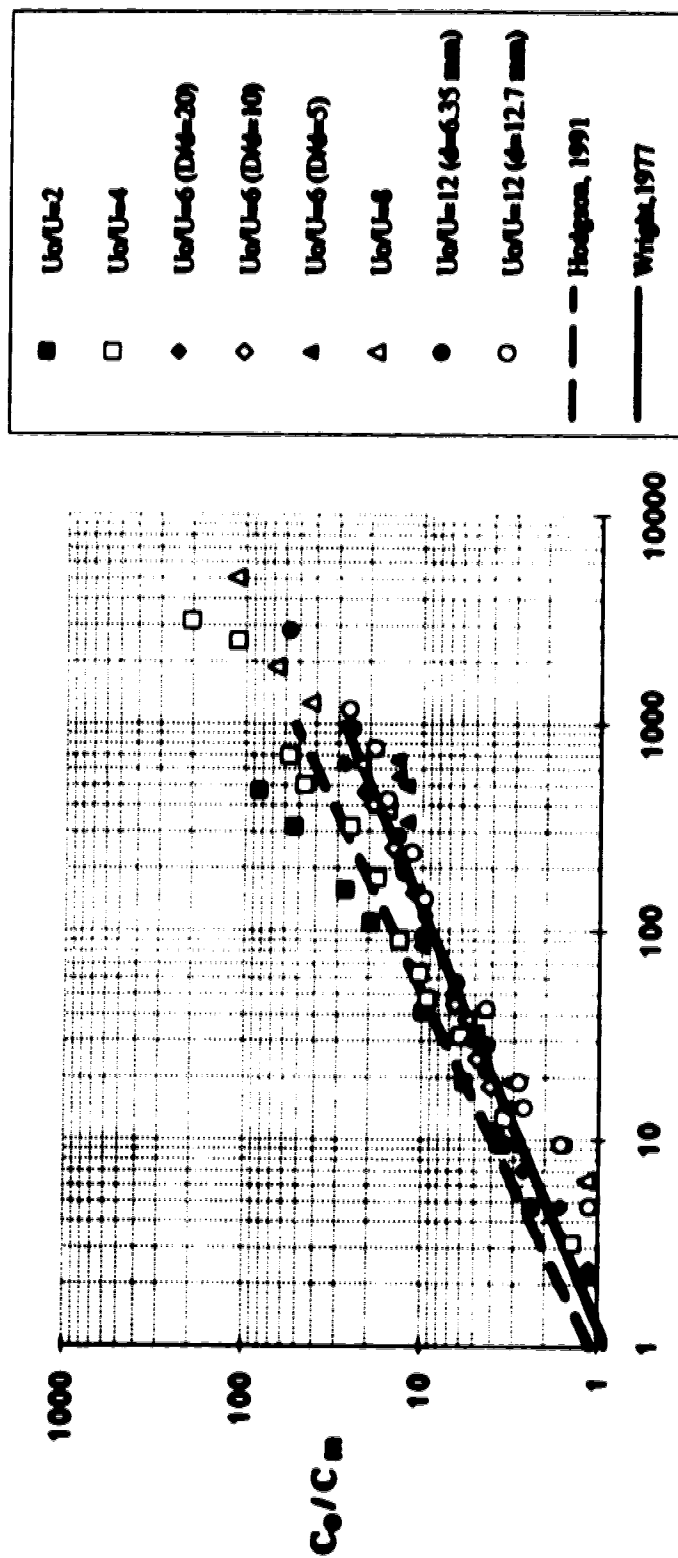


Fig. 4.31 Generalized Minimum Distance of the Deflected Wall Jet



**Fig.A.32 Comparison of Free and Wall Jet Minimum Distances**

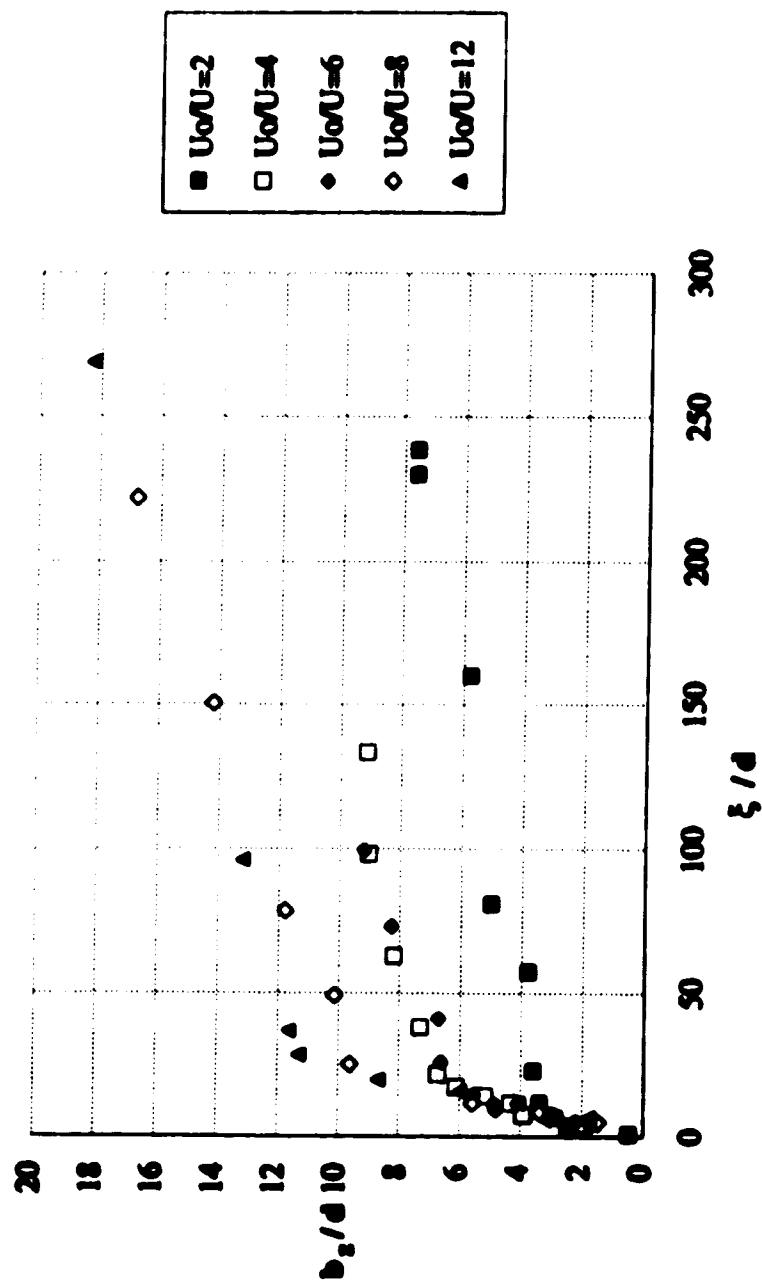


Fig. 4.33 Generalized Scales for the Vertical Concentration Profiles of the Deflected Jet

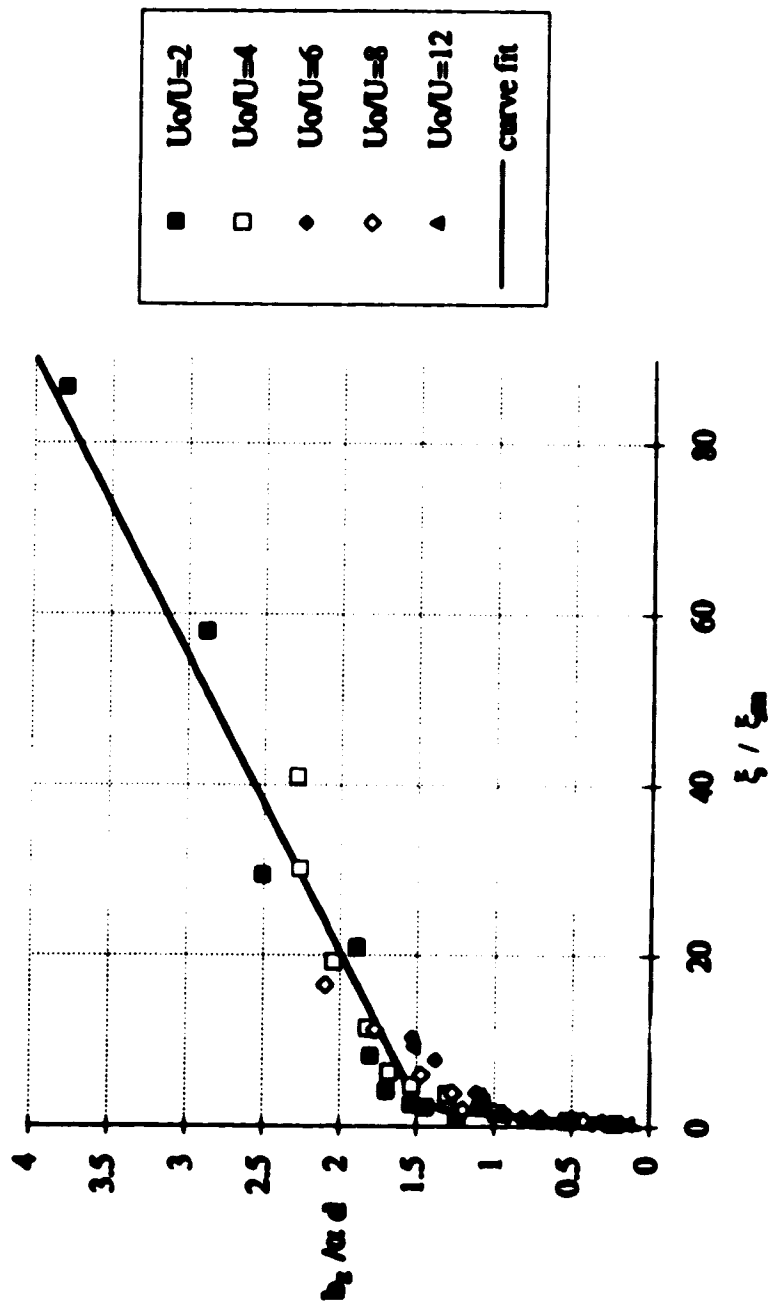


Fig. 4.34 (a) Generalized Scale for the Vertical Concentration Distribution of the Deflected Jet

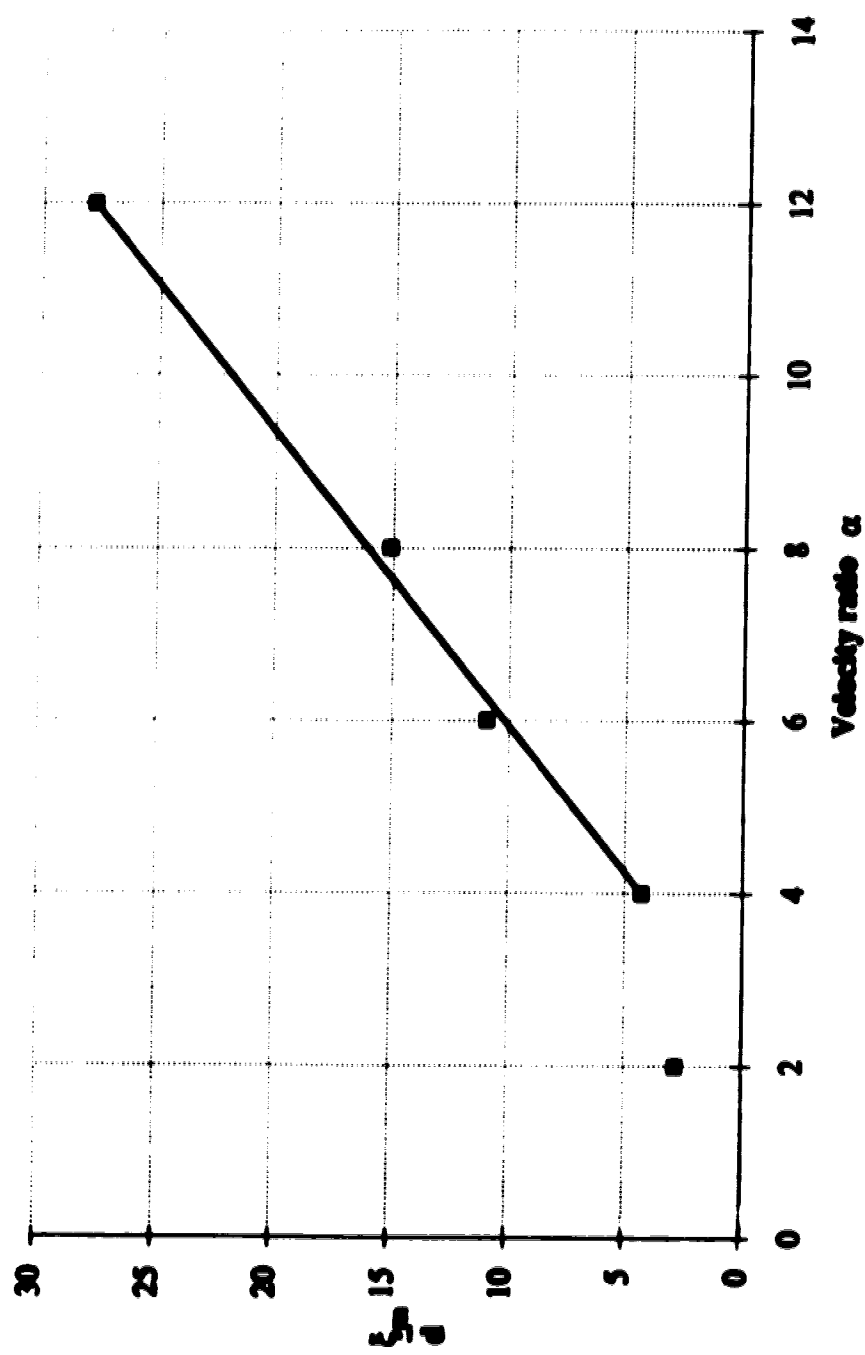


Fig.4.34 (b) Relationship of the Scale

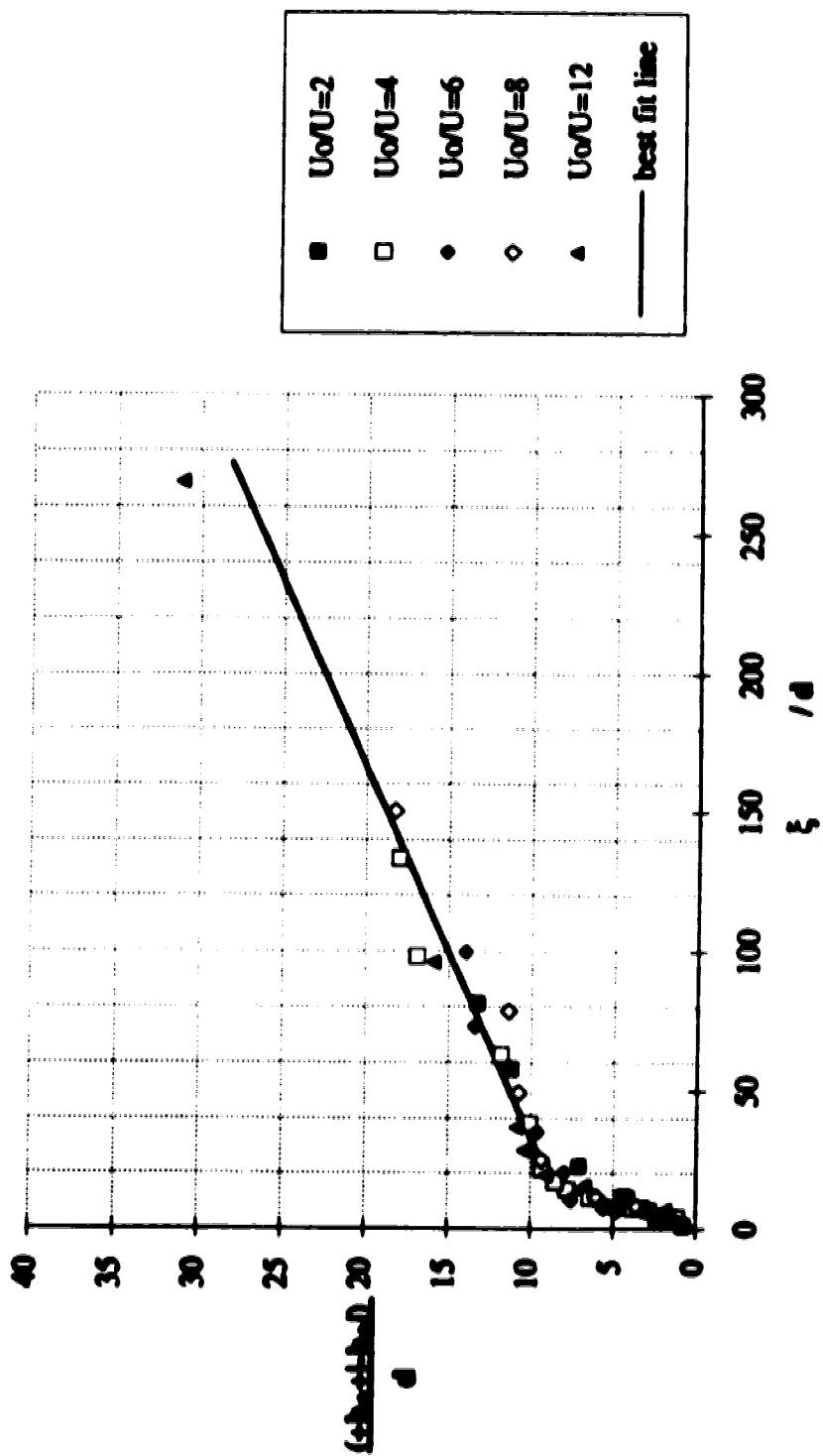
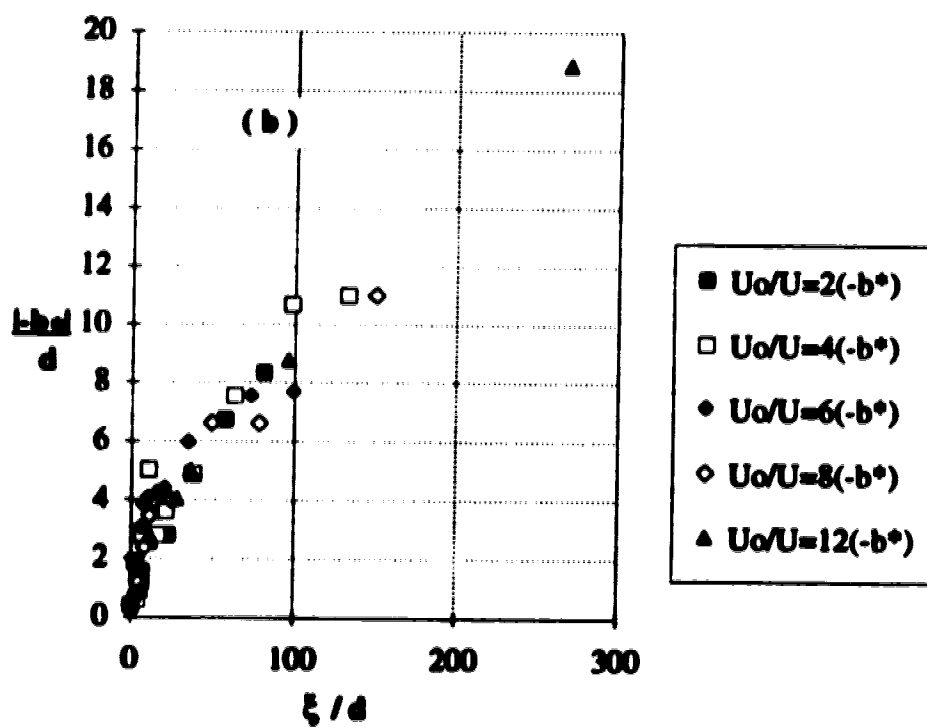
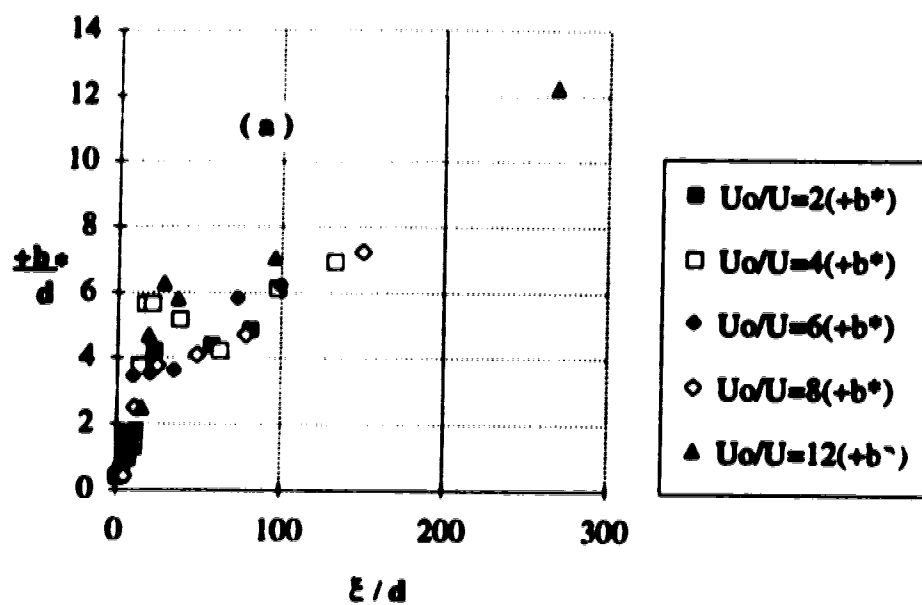


Fig. 4.35 Generalized Scales for the Transverse Concentration Profiles of the Deflected Jet



**Fig. 4.36 Generalized Positive and Negative Transverse Scales**

## **5.0 CONCLUSIONS AND RECOMMENDATIONS**

### **5.1 Conclusions**

The objective of the present study was to investigate the dilution characteristics of circular wall jets in crossflows. These include the similarity analysis of the concentration profiles both in the vertical and transverse directions, minimum dilution and the growth of the jet half - width. The maximum concentrations (  $C_m$  ) was used as a characteristic scale parameter. It is of practical importance to have knowledge of the maximum value of tracer concentration at any section of the jet because it is useful in assessing the extend of pollutant dilutions released into the environment.

The conclusions presented below are applicable for the region where the jet generated turbulence dominates the ambient flow conditions. The characteristics in the region where the jet strength has decayed to the ambient flow turbulence and referred to in the text as a passive plume condition, was not considered in detail but could be investigated under a separate study.

#### **5.1.1 Interpretation of the Experimental Results**

The similarity profiles of concentration distributions both in the vertical (  $z - \xi$  plane ) and the transverse (  $\eta - \xi$  plane ) are presented in Figures 4.14 and 4.25. The plots indicate that normalized concentration distributions for a circular wall jet in crossflow are preserved from section to section. This behavior is assumed to hold true under the boundary conditions of zero jet velocity at the wall where some scatter on the dilution data were observed, and the upper boundary of the free mixing region is marked by the jet decay to the ambient flow velocity (  $U$  ). The dimensionless plots of



both the momentum dominated near field and the far field regimes showed no observable distinction because the jet momentum dominates the mixing and hence controls the dilution in the regions. The concentration distributions in the passive plume region were not similar to those of the momentum dominated region.

The wall effect was shown by the scatter of dilution data for all the jet discharges. The generalized distributions in the vertical direction indicated that the boundary layer thickness  $\delta$  could be derived approximately by the elevation  $z = 0.5 b_z$ . Transverse concentration distributions were approximately symmetrical along the jet axis and could be described by the Gaussian distribution.

The minimum dilution ( $C_0 / C_m$ ) plots along the downstream distance  $\alpha x / d$  indicated a general trend of increase in tracer dilution shown by the data slope transition from  $1/2$  to  $2/3$ . The trends imply that the dilution along the axis of the jet are governed by the inter - dependent cross - sections with similar rates, or constant slope. Beyond the momentum dominated region, the stream turbulence influences mixing. The passive plume flow regime is shown by the data with steeper slope than the  $2/3$  of the momentum dominated far field. This feature was clearly distinct for the weaker jet with the velocity ratio  $\alpha = 2$  beyond the downstream distance  $\alpha x / d = 100$ .

The results have shown that dilutions of 50 : 1 were achieved by all the jet discharges within the momentum dominated far field regime. Dilutions in the range of 3 : 1 to 20 : 1 were attained in the momentum dominated near field depending on the strength of the jet discharge. These results indicate that the momentum dominated far field is a very important region in achieving significant dilutions within the initial dilution zone in river discharges.

The dilution data were correlated by a unifying equation which describes the whole region dominated by the jet. The relation ( Equation 4.10 ) is sufficient for practical purposes in estimating tracer dilution in rivers.

The length scale analysis for both the vertical and the transverse directions indicated that the jet grows faster in the momentum dominated near field than in the far field regime. The result is attributed to the dominance of the jet strength in the MDNF; while in the MDFF, the growth behavior is similar to that of a jet in a co - flowing stream. It was also found that the jet growth was about twice in the transverse direction compared to that in the vertical direction.

The transition between the momentum dominated near and the far fields occurred approximately at  $x / \alpha d = 1$  for  $\alpha = 2$  and 4. The stronger jets with velocity ratios greater than 4 had their transitions at distances  $( x / \alpha d ) > 2$ .

The effect of the freestream flow depth was also considered and found that significant reduction in the tracer dilution occurred for depths less than 10 times the jet nozzle diameter. This result indicates the restriction which occurs in the vertical mixing in shallow rivers.

### 5.1.2 Comparison with Previous Studies

Dilution of circular wall jet in crossflows has not been studied previously. The present results therefore, are compared with the investigations of Wright ( 1977 ) and Hodgson and Rajaratnam ( 1992) on circular free jets in crossflows.

The results plotted in Figure 4.32 show that the dilution characteristics of the wall jet discharges are fitted well by the results of Wright ( 1977 ) for the MDNF and

those of Hodgson and Rajaratnam ( 1992 ) approximates the MDFF. When each of the jet discharges was considered separately, the dilution of the wall jet in the MDFF were fitted well by a  $2/3$  - slope of the power law equation but with a higher constant coefficient than that given for the Wright's equation.

The transition from the MDNF to the MDFF, based on the trajectory plots of Wright, occurs approximately where  $l_m = x$ , and therefore reduces  $\alpha x / d$  to approximately  $\alpha^2$ . For  $\alpha$  varying between 2 and 12, corresponds to  $\alpha^2$  in the range of 4 to 144. This criteria was only met by the wall jet discharges of  $\alpha = 2$  and 4. For  $\alpha$  greater than 4, the transition values were greater than the  $\alpha^2$  values. Higher values may have been caused by the smaller resistance of low velocity of the crossflow near the bed.

## 5.2 Recommendations

The present investigation considered only the dilution characteristics of circular wall jet in crossflow. To complete the study of the jet requires an integration of all the other related hydraulic aspects. Some of the important characteristics recommended for further study include:

- I. detailed study of the concentration contours across the section of the jet.  
The study would identify the differences in the vortex structure of both the wall and free jets in crossflow.
- II. measurements of the bed shear as an indicator of the extent of the jet erosion of the river bed.

**III. detailed photographic study of the jet growth to compare with the known conditions of the free jet in crossflow.**

**IV. dilution study of buoyant jet discharges for comparison with the non-buoyant cases.**

**V. to carry out the dilution study under the prototype river conditions similar to the investigations of Hodgson and Rajaratnam ( 1992).**

**VI. to study the turbulence characteristics of the wall jet in crossflow.**

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## **APPENDIX I**

### **Photographic Representation of the Circular Wall Jet Diffusion in Crossflow**



**Plate I (a) Experiment No. A100:      Velocity Ratio ( $U_0/U$ ) = 2**  
 **$D = 127 \text{ mm}$ ,  $d = 6.35 \text{ mm}$**

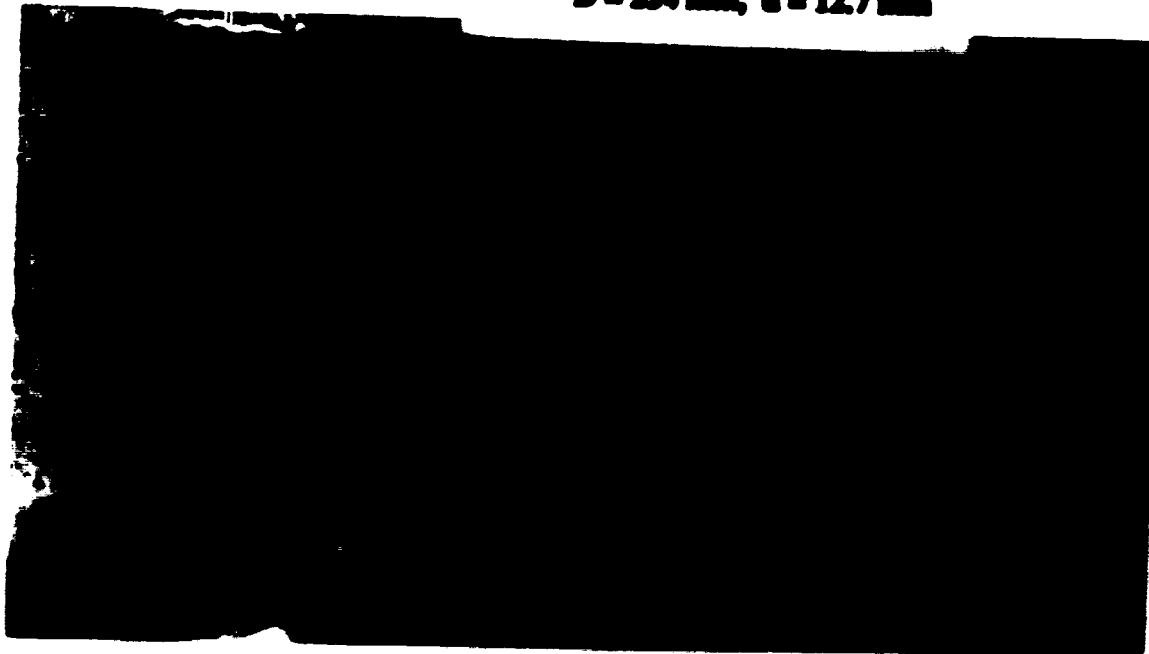


**Plate I (b) Experiment No. A200:      Velocity Ratio ( $U_0/U$ ) = 4**  
 **$D = 127 \text{ mm}$ ,  $d = 6.35 \text{ mm}$**



**Plate I (c) Experiment No. A300:      Velocity Ratio ( $U_0/U$ ) = 6**  
**D = 127 mm, d = 6.35 mm**

**Plate I (d) Experiment No. B100:      Velocity Ratio ( $U_0/U$ ) = 6**  
**D = 254 mm, d = 12.7 mm**

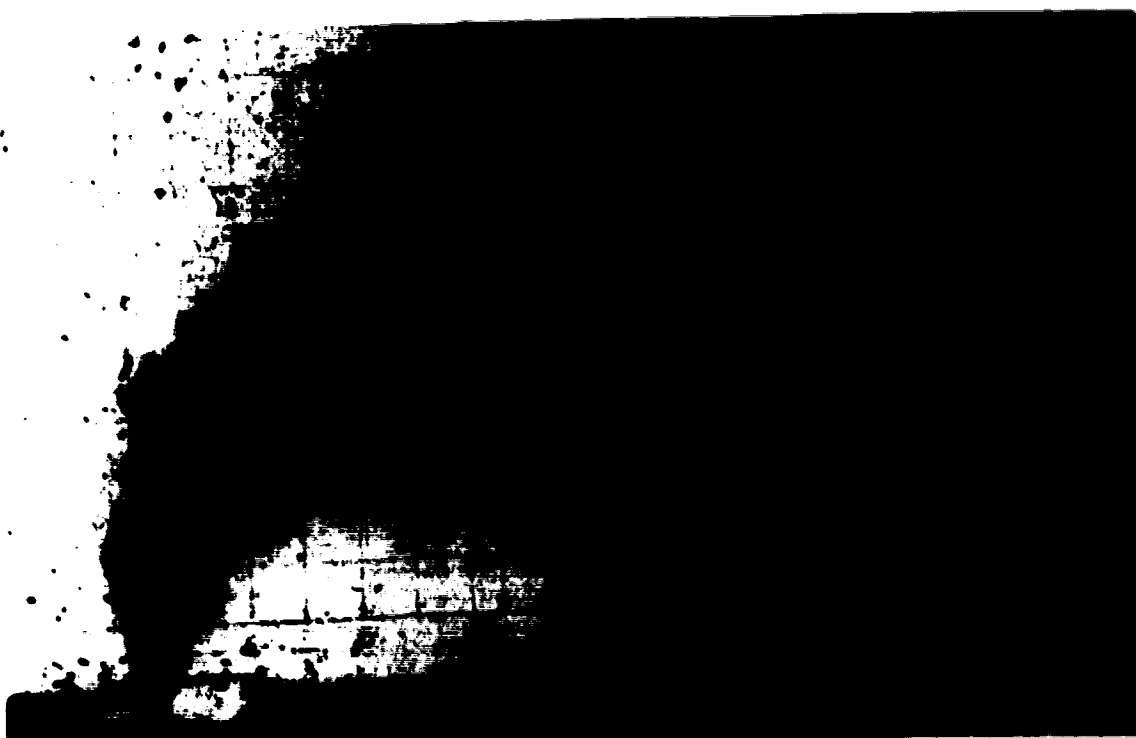




**Plate I (e) Experiment No. A400:**

**Velocity Ratio ( $U_0/U$ ) = 8**

**$D = 127$  mm,  $d = 6.35$  mm**



**Plate I (f) Experiment No. A500:**

**Velocity Ratio ( $U_0/U$ ) = 12**

**$D = 127$  mm,  $d = 6.35$  mm**

## **APPENDIX II**

### **Experimental Dilution Data**

Uo/U = 2		D/d = 20, d = 6.35 mm		(Concentration readings have been corrected for the ambient value)	
Note: Transverse measurements are referenced from the inner boundary of the deflected jet					
Experiment No. A101		Ambient Concentration = 0.062 ppb		Jet Nozzle Concentration = 13.9 ppb	
z = 1.5 mm		z = 7 mm, y = 5 mm		z = 9.5 mm	
$\eta$ (mm)	C (ppb)	$\eta$ (mm)	C (ppb)	$\eta$ (mm)	C (ppb)
0.0	0.009	0.0	0.026	0.0	0.053
5.0	0.053	5.0	0.035	5.0	0.026
10.0	0.035	10.0	0.062	10.0	0.044
15.0	0.040	15.0	0.008	15.0	0.026
20.0	0.053	20.0	0.079	20.0	0.018
25.0	12.431	25.0	1.304	25.0	0.009
30.0	0.066	30.0	0.035	30.0	0.018
35.0	0.026	35.0	0.018	35.0	0.009
40.0	0.035	40.0	0.026	40.0	0.000
45.0	0.026	45.0	0.018	45.0	0.000
Experiment No. A102: z = 15 mm, Ambient Con. = 0.062 ppb, Jet Nozzle Con. = 16.363 ppb		z = 13.5 mm		z = 17.5 mm	
z = 1.5 mm		z = 0.5 mm		z = 21.5 mm	
$\eta$ (mm)	C (ppb)	$\eta$ (mm)	C (ppb)	$\eta$ (mm)	C (ppb)
0.0	0.343	0.0	1.304	0.0	0.097
5.0	1.217	5.0	3.497	5.0	0.792
10.0	2.941	10.0	4.470	10.0	1.214
15.0	6.008	15.0	6.537	15.0	0.924
20.0	4.498	20.0	2.162	20.0	0.044
25.0	1.406	25.0	0.123	25.0	0.000
30.0	0.176	30.0	0.026	30.0	0.000
35.0	0.053	35.0	0.009	35.0	0.000
40.0	0.009	40.0	0.009	40.0	0.000
45.0	0.000	45.0	0.000	45.0	0.000
50.0	0.000	50.0	0.000	50.0	0.000
55.0	0.000	55.0	0.000	55.0	0.000
60.0	0.000	60.0	0.000	60.0	0.000
65.0	0.000	65.0	0.000	65.0	0.000
		z = 25.5 mm		z = 25.5 mm	
		$\eta$ (mm)	C (ppb)	$\eta$ (mm)	C (ppb)
		0.0	0.000	0.0	0.000
		5.0	0.018	5.0	0.018
		10.0	0.035	10.0	0.035
		15.0	0.018	15.0	0.018
		20.0	0.009	20.0	0.009
		25.0	0.000	25.0	0.000
		30.0	0.000	30.0	0.000
		35.0	0.000	35.0	0.000
		40.0	0.000	40.0	0.000
		45.0	0.000	45.0	0.000
		50.0	0.000	50.0	0.000
		55.0	0.000	55.0	0.000
		60.0	0.000	60.0	0.000
		65.0	0.000	65.0	0.000

Velocity Ratio ( $U_0/U$ ) = 2											
$D/d = 20$ , $d = 6.35$ mm (Concentration readings have been corrected for the ambient value)											
Note: Transverse measurements are referenced from the inner boundary of the deflected jet											
Experiment No. A103: $x = 30$ mm Ambient Conc. = 0.106 ppb, Jet Nozzle Conc. = 17.236 ppb											
$z = 1.5$ mm	$z = 3.5$ mm	$z = 5.5$ mm	$z = 7.5$ mm	$z = 9.5$ mm	$z = 13.5$ mm	$z = 17.5$ mm	$z = 21.5$ mm	$z = 25.5$ mm			
$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$C$ (ppb)
0.0	0.404	0.0	1.340	0.0	2.285	0.0	1.646	0.0	0.545	0.0	0.009
5.0	1.034	5.0	2.591	5.0	3.731	5.0	3.425	5.0	1.785	5.0	0.018
10.0	1.840	10.0	3.203	10.0	4.064	10.0	4.401	10.0	2.647	10.0	0.044
15.0	3.175	15.0	3.314	15.0	4.259	15.0	4.315	15.0	2.535	15.0	0.026
20.0	4.926	20.0	4.064	20.0	3.453	20.0	2.647	20.0	0.895	20.0	0.009
25.0	3.953	25.0	2.309	25.0	1.062	25.0	0.867	25.0	0.211	25.0	0.009
30.0	2.649	30.0	0.867	30.0	0.167	30.0	0.062	30.0	0.009	30.0	0.000
35.0	1.062	35.0	0.202	35.0	0.009	35.0	0.009	35.0	0.009	35.0	0.000
40.0	0.229	40.0	0.026	40.0	0.009	40.0	0.009	40.0	0.009	40.0	0.000
45.0	0.018	45.0	0.009	45.0	0.009	45.0	0.009	45.0	0.009	45.0	0.000
50.0	0.009	50.0	0.009	50.0	0.009	50.0	0.009	50.0	0.009	50.0	0.000
55.0	0.000	55.0	0.009	55.0	0.000	55.0	0.000	55.0	0.000	55.0	0.000
60.0	0.000	60.0	0.009	60.0	0.000	60.0	0.000	60.0	0.000	60.0	0.000
65.0	0.000	65.0	0.000	65.0	0.000	65.0	0.000	65.0	0.000	65.0	0.000
Experiment No. A104: $x = 35$ mm Ambient Conc. = 0.079 ppb, Jet Nozzle Conc. = 17.792 ppb											
$z = 1.5$ mm	$z = 3.5$ mm	$z = 5.5$ mm	$z = 7.5$ mm	$z = 9.5$ mm	$z = 13.5$ mm	$z = 17.5$ mm	$z = 21.5$ mm	$z = 25.5$ mm			
$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$C$ (ppb)
0.0	0.382	0.0	0.457	0.0	0.651	0.0	0.413	0.0	0.132	0.0	0.000
5.0	0.625	5.0	1.364	5.0	2.247	5.0	2.053	5.0	1.091	5.0	0.026
10.0	1.203	10.0	2.040	10.0	3.665	10.0	3.721	10.0	2.497	10.0	0.008
15.0	1.719	15.0	2.775	15.0	3.554	15.0	4.193	15.0	3.081	15.0	0.141
20.0	3.118	20.0	3.396	20.0	3.832	20.0	3.832	20.0	2.470	20.0	0.070
25.0	4.094	25.0	3.443	25.0	3.304	25.0	2.775	25.0	1.274	25.0	0.026
30.0	4.536	30.0	2.173	30.0	0.805	30.0	0.551	30.0	0.211	30.0	0.000
35.0	3.053	35.0	1.441	35.0	0.334	35.0	0.062	35.0	0.018	35.0	0.000
40.0	1.950	40.0	0.699	40.0	0.062	40.0	0.009	40.0	0.009	40.0	0.000
45.0	0.273	45.0	0.070	45.0	0.009	45.0	0.000	45.0	0.000	45.0	0.000
50.0	0.044	50.0	0.026	50.0	0.018	50.0	0.000	50.0	0.000	50.0	0.000
55.0	0.018	55.0	0.009	55.0	0.000	55.0	0.000	55.0	0.000	55.0	0.000
60.0	0.026	60.0	0.018	60.0	0.000	60.0	0.000	60.0	0.000	60.0	0.000
65.0	0.000	65.0	0.000	65.0	0.000	65.0	0.000	65.0	0.000	65.0	0.000



Velocity Ratio ( $U_0/U_1$ ) = 2											
D/d = 20, d = 6.35 mm (Concentration readings have been corrected for the ambient value)											
Note: Transverse measurements are referenced from the inner boundary of the deflected jet											
Experiment No. A105: z = 40 mm Ambient Conc. = 0.062 ppb Jet Nozzle Conc. = 17.507 ppb											
z = 15 mm		z = 25 mm		z = 40.5 mm		z = 105.5 mm		z = 165.5 mm		z = 215.5 mm	
$\eta$	C	$\eta$	C	$\eta$	C	$\eta$	C	$\eta$	C	$\eta$	C
(mm)	(ppb)	(mm)	(ppb)	(mm)	(ppb)	(mm)	(ppb)	(mm)	(ppb)	(mm)	(ppb)
0.0	0.796	0.0	0.757	0.0	1.345	0.0	0.959	0.0	0.352	0.0	0.044
5.0	0.000	5.0	1.001	5.0	2.209	5.0	1.876	5.0	0.836	5.0	0.176
10.0	1.273	10.0	2.007	10.0	2.996	10.0	2.913	10.0	1.662	10.0	0.396
15.0	1.025	15.0	2.407	15.0	2.904	15.0	2.765	15.0	1.681	15.0	0.545
20.0	2.004	20.0	2.400	20.0	2.718	20.0	2.635	20.0	1.273	20.0	0.361
25.0	2.705	25.0	2.710	25.0	2.654	25.0	2.098	25.0	1.014	25.0	0.194
30.0	3.052	30.0	2.304	30.0	1.523	30.0	0.939	30.0	0.229	30.0	0.079
35.0	2.459	35.0	1.598	35.0	1.069	35.0	0.405	35.0	0.114	35.0	0.009
40.0	1.801	40.0	0.856	40.0	0.229	40.0	0.044	40.0	0.018	40.0	0.000
45.0	0.764	45.0	0.352	45.0	0.123	45.0	0.009	45.0	0.000	45.0	0.000
50.0	0.273	50.0	0.079	50.0	0.018	50.0	0.000	50.0	0.000	50.0	0.000
55.0	0.000	55.0	0.000	55.0	0.000	55.0	0.000	55.0	0.000	55.0	0.000
60.0	0.000	60.0	0.000	60.0	0.000	60.0	0.000	60.0	0.000	60.0	0.000
65.0	0.000	65.0	0.000	65.0	0.000	65.0	0.000	65.0	0.000	65.0	0.000
Experiment No. A106: z = 15 mm Ambient Conc. = 0.070 ppb Jet Nozzle Conc. = 17.592 ppb											
z = 15 mm		z = 115.5 mm		z = 165.5 mm		z = 215.5 mm		z = 265.5 mm		z = 365.5 mm	
$\eta$	C	$\eta$	C	$\eta$	C	$\eta$	C	$\eta$	C	$\eta$	C
(mm)	(ppb)	(mm)	(ppb)	(mm)	(ppb)	(mm)	(ppb)	(mm)	(ppb)	(mm)	(ppb)
0.0	0.413	0.0	0.519	0.0	0.633	0.0	0.693	0.0	0.123	0.0	0.000
5.0	0.000	5.0	0.945	5.0	1.429	5.0	0.915	5.0	0.202	5.0	0.035
10.0	0.000	10.0	1.375	10.0	1.570	10.0	1.339	10.0	0.422	10.0	0.035
15.0	1.170	15.0	1.500	15.0	1.672	15.0	1.450	15.0	0.300	15.0	0.062
20.0	1.404	20.0	1.820	20.0	1.764	20.0	1.505	20.0	0.493	20.0	0.035
25.0	1.206	25.0	1.756	25.0	1.728	25.0	1.450	25.0	0.301	25.0	0.035
30.0	1.406	30.0	1.757	30.0	1.570	30.0	1.311	30.0	0.309	30.0	0.018
35.0	1.500	35.0	1.533	35.0	1.366	35.0	1.008	35.0	0.273	35.0	0.000
40.0	1.700	40.0	1.459	40.0	1.042	40.0	0.699	40.0	0.132	40.0	0.000
45.0	1.422	45.0	1.144	45.0	0.810	45.0	0.477	45.0	0.079	45.0	0.000
50.0	1.202	50.0	0.906	50.0	0.591	50.0	0.264	50.0	0.026	50.0	0.000
55.0	0.644	55.0	0.644	55.0	0.352	55.0	0.105	55.0	0.009	55.0	0.000
60.0	0.413	60.0	0.378	60.0	0.176	60.0	0.035	60.0	0.000	60.0	0.000
65.0	0.000	65.0	0.150	65.0	0.062	65.0	0.000	65.0	0.000	65.0	0.000
70.0	0.000	70.0	0.044	70.0	0.026	70.0	0.000	70.0	0.000	70.0	0.000
75.0	0.000	75.0	0.009	75.0	0.009	75.0	0.000	75.0	0.000	75.0	0.000
80.0	0.000	80.0	0.000	80.0	0.000	80.0	0.000	80.0	0.000	80.0	0.000
85.0	0.000	85.0	0.000	85.0	0.000	85.0	0.000	85.0	0.000	85.0	0.000

Velocity Ratio ( $U_0/U$ ) = 2											
D/d = 20, d = 6.35 mm (Concentration readings have been corrected for the ambient value)											
Note: Pressure measurements are referenced from the inner boundary of the deflected jet											
Experiment No. A167: z = 350 mm, Ambient Conc. = 0.063 pph, Jet Nozzle Conc. = 16.68 pph											
z = 1.5 mm	z = 6.5 mm	z = 11.5 mm	z = 16.5 mm	z = 21.5 mm	z = 26.5 mm	z = 31.5 mm	z = 36.5 mm	z = 41.5 mm	z = 46.5 mm		
$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	C
(pph)	(pph)	(pph)	(pph)	(pph)	(pph)	(pph)	(pph)	(pph)	(pph)	(pph)	(pph)
0.0	0.304	0.0	0.211	0.0	0.141	0.0	0.106	0.0	0.062	0.0	0.044
10.0	0.457	10.0	0.352	10.0	0.246	10.0	0.176	10.0	0.088	10.0	0.053
20.0	0.599	20.0	0.475	20.0	0.334	20.0	0.229	20.0	0.123	20.0	0.079
30.0	0.739	30.0	0.642	30.0	0.449	30.0	0.317	30.0	0.185	30.0	0.114
40.0	0.845	40.0	0.836	40.0	0.703	40.0	0.552	40.0	0.176	40.0	0.106
50.0	0.862	50.0	0.862	50.0	0.774	50.0	0.651	50.0	0.202	50.0	0.097
60.0	0.891	60.0	0.891	60.0	0.833	60.0	0.721	60.0	0.211	60.0	0.062
70.0	0.846	70.0	0.804	70.0	0.813	70.0	0.805	70.0	0.079	70.0	0.026
80.0	0.864	80.0	0.806	80.0	0.806	80.0	0.853	80.0	0.044	80.0	0.018
90.0	0.128	90.0	0.132	90.0	0.114	90.0	0.053	90.0	0.009	90.0	0.009
100.0	0.063	100.0	0.053	100.0	0.005	100.0	0.018	100.0	0.000	100.0	0.000
120.0	0.000	120.0	0.000	120.0	0.000	120.0	0.000	120.0	0.000	120.0	0.000

Experiment No. A168: z = 350 mm, Ambient Conc. = 0.063 pph, Jet Nozzle Conc. = 15.568 pph											
z = 1.5 mm	z = 6.5 mm	z = 11.5 mm	z = 16.5 mm	z = 21.5 mm	z = 26.5 mm	z = 31.5 mm	z = 36.5 mm	z = 41.5 mm	z = 46.5 mm		
$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	C
(pph)	(pph)	(pph)	(pph)	(pph)	(pph)	(pph)	(pph)	(pph)	(pph)	(pph)	(pph)
0.0	0.245	0.0	0.211	0.0	0.123	0.0	0.106	0.0	0.079	0.0	0.053
10.0	0.308	10.0	0.255	10.0	0.176	10.0	0.158	10.0	0.106	10.0	0.044
20.0	0.362	20.0	0.334	20.0	0.246	20.0	0.211	20.0	0.158	20.0	0.053
30.0	0.422	30.0	0.413	30.0	0.352	30.0	0.308	30.0	0.228	30.0	0.167
40.0	0.480	40.0	0.493	40.0	0.422	40.0	0.361	40.0	0.273	40.0	0.194
50.0	0.545	50.0	0.554	50.0	0.475	50.0	0.396	50.0	0.282	50.0	0.211
60.0	0.581	60.0	0.572	60.0	0.528	60.0	0.352	60.0	0.255	60.0	0.167
70.0	0.537	70.0	0.484	70.0	0.440	70.0	0.273	70.0	0.202	70.0	0.106
80.0	0.486	80.0	0.399	80.0	0.343	80.0	0.185	80.0	0.079	80.0	0.006
90.0	0.299	90.0	0.228	90.0	0.167	90.0	0.106	90.0	0.062	90.0	0.009
100.0	0.158	100.0	0.132	100.0	0.097	100.0	0.053	100.0	0.000	100.0	0.000
120.0	0.005	120.0	0.006	120.0	0.018	120.0	0.000	120.0	0.000	120.0	0.000

Velocity Ratio ( $U_o/U$ ) = 2  $D/d = 20$ ,  $d = 6.35$  mm (Concentration readings have been corrected for the ambient value)  
 Note: Transverse measurements are referenced from the inner boundary of the deflected jet

Experiment No. A102: $z = 1000$ mm Ambient Conc. = 0.070 ppb Jet Nozzle Conc. = 16.08 ppb											
$z = 13$ mm	$z = 43$ mm	$z = 113$ mm	$z = 163$ mm	$z = 213$ mm	$z = 263$ mm	$z = 313$ mm	$z = 363$ mm	$z = 413$ mm	$z = 463$ mm	$z = 513$ mm	$z = 563$ mm
$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$
C	C	C	C	C	C	C	C	C	C	C	C
(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)
0.0	0.302	0.0	0.105	0.0	0.150	0.0	0.150	0.0	0.150	0.0	0.150
10.0	0.229	10.0	0.201	10.0	0.176	10.0	0.176	10.0	0.176	10.0	0.176
20.0	0.256	20.0	0.229	20.0	0.194	20.0	0.194	20.0	0.194	20.0	0.194
30.0	0.273	30.0	0.255	30.0	0.238	30.0	0.229	30.0	0.229	30.0	0.229
40.0	0.308	40.0	0.282	40.0	0.273	40.0	0.246	40.0	0.238	40.0	0.238
50.0	0.317	50.0	0.290	50.0	0.290	50.0	0.255	50.0	0.250	50.0	0.250
60.0	0.317	60.0	0.280	60.0	0.282	60.0	0.246	60.0	0.229	60.0	0.229
70.0	0.290	70.0	0.255	70.0	0.255	70.0	0.229	70.0	0.194	70.0	0.194
80.0	0.235	80.0	0.238	80.0	0.202	80.0	0.185	80.0	0.150	80.0	0.150
90.0	0.202	90.0	0.185	90.0	0.150	90.0	0.132	90.0	0.097	90.0	0.097
100.0	0.141	100.0	0.132	100.0	0.105	100.0	0.097	100.0	0.070	100.0	0.070
120.0	0.002	120.0	0.003	120.0	0.003	120.0	0.004	120.0	0.004	120.0	0.004

Experiment No. A103: $z = 1500$ mm Ambient Conc. = 0.053 ppb Jet Nozzle Conc. = 18.340 ppb											
$z = 13$ mm	$z = 43$ mm	$z = 113$ mm	$z = 163$ mm	$z = 213$ mm	$z = 263$ mm	$z = 313$ mm	$z = 363$ mm	$z = 413$ mm	$z = 463$ mm	$z = 513$ mm	$z = 563$ mm
$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$
C	C	C	C	C	C	C	C	C	C	C	C
(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)
0.0	0.141	0.0	0.141	0.0	0.125	0.0	0.114	0.0	0.097	0.0	0.053
10.0	0.150	10.0	0.150	10.0	0.132	10.0	0.125	10.0	0.105	10.0	0.053
20.0	0.150	20.0	0.150	20.0	0.141	20.0	0.132	20.0	0.105	20.0	0.053
30.0	0.176	30.0	0.167	30.0	0.167	30.0	0.141	30.0	0.105	30.0	0.053
40.0	0.194	40.0	0.185	40.0	0.176	40.0	0.150	40.0	0.114	40.0	0.053
50.0	0.202	50.0	0.194	50.0	0.185	50.0	0.167	50.0	0.114	50.0	0.053
60.0	0.211	60.0	0.202	60.0	0.194	60.0	0.176	60.0	0.114	60.0	0.053
70.0	0.220	70.0	0.202	70.0	0.194	70.0	0.176	70.0	0.114	70.0	0.053
80.0	0.211	80.0	0.202	80.0	0.194	80.0	0.176	80.0	0.114	80.0	0.053
90.0	0.211	90.0	0.194	90.0	0.185	90.0	0.167	90.0	0.105	90.0	0.053
100.0	0.194	100.0	0.167	100.0	0.150	100.0	0.141	100.0	0.105	100.0	0.053
120.0	0.125	120.0	0.125	120.0	0.114	120.0	0.097	120.0	0.070	120.0	0.009



Velocity Lines (UG7U)=4											
Note: Pressure measurements are referenced from the inner boundary of the ducted jet											
Fig. A.25: $x = 75$ mm, $y = 54$ mm, Ambient Conc. = 0.167 gph, Jet Nozzle Conc. = 13.9 gph											
(Concentration readings have been corrected for the ambient value)											
$U/V = 28$ , $d = 6.35$ mm											
$z = 1.5$ mm	$z = 4.5$ mm	$z = 11.5$ mm	$z = 16.5$ mm	$z = 21.5$ mm	$z = 26.5$ mm	$z = 31.5$ mm	$z = 36.5$ mm	$z = 41.5$ mm			
$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$
(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)
0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
3.0	0.000	3.0	0.000	3.0	0.000	3.0	0.000	3.0	0.000	3.0	0.000
6.0	0.000	6.0	0.000	6.0	0.000	6.0	0.000	6.0	0.000	6.0	0.000
10.0	0.000	10.0	0.000	10.0	0.000	10.0	0.000	10.0	0.000	10.0	0.000
13.0	0.000	13.0	0.000	13.0	0.000	13.0	0.000	13.0	0.000	13.0	0.000
16.0	0.000	16.0	0.000	16.0	0.000	16.0	0.000	16.0	0.000	16.0	0.000
20.0	0.114	20.0	1.144	20.0	1.591	20.0	0.114	20.0	0.000	20.0	0.000
23.0	0.202	23.0	1.200	23.0	1.741	23.0	0.167	23.0	0.000	23.0	0.000
26.0	0.220	26.0	1.200	26.0	1.666	26.0	0.167	26.0	0.000	26.0	0.000
30.0	0.308	30.0	1.300	30.0	1.990	30.0	0.260	30.0	0.000	30.0	0.000
33.0	0.405	33.0	1.300	33.0	1.741	33.0	0.260	33.0	0.000	33.0	0.000
36.0	0.405	36.0	1.204	36.0	1.611	36.0	0.260	36.0	0.000	36.0	0.000
40.0	0.500	40.0	1.200	40.0	1.473	40.0	0.260	40.0	0.000	40.0	0.000
43.0	1.021	43.0	1.221	43.0	1.546	43.0	0.260	43.0	0.000	43.0	0.000
46.0	0.977	46.0	1.406	46.0	1.777	46.0	0.260	46.0	0.000	46.0	0.000
50.0	0.977	50.0	1.605	50.0	2.112	50.0	0.260	50.0	0.000	50.0	0.000
53.0	0.994	53.0	1.535	53.0	2.162	53.0	0.260	53.0	0.000	53.0	0.000
56.0	0.605	56.0	1.204	56.0	1.611	56.0	0.260	56.0	0.000	56.0	0.000
60.0	0.273	60.0	0.774	60.0	0.908	60.0	0.260	60.0	0.000	60.0	0.000
63.0	0.258	63.0	0.431	63.0	0.704	63.0	0.260	63.0	0.000	63.0	0.000
66.0	0.167	66.0	0.211	66.0	0.440	66.0	0.260	66.0	0.000	66.0	0.000
Fig. A.26: $x = 75$ mm, $y = 66$ mm, Ambient Conc. = 0.220 gph, Jet Nozzle Conc. = 12.60 gph											
$z = 1.5$ mm	$z = 4.5$ mm	$z = 11.5$ mm	$z = 16.5$ mm	$z = 21.5$ mm	$z = 26.5$ mm	$z = 31.5$ mm	$z = 36.5$ mm				
$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$
(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)
0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
3.0	0.000	3.0	0.141	3.0	0.273	3.0	0.000	3.0	0.000	3.0	0.000
6.0	0.000	6.0	0.537	6.0	0.677	6.0	0.000	6.0	0.000	6.0	0.000
10.0	0.000	10.0	0.908	10.0	1.126	10.0	0.000	10.0	0.000	10.0	0.000
15.0	0.002	15.0	0.405	15.0	0.908	15.0	0.000	15.0	0.000	15.0	0.000
20.0	0.106	20.0	0.908	20.0	1.126	20.0	0.000	20.0	0.000	20.0	0.000
25.0	0.158	25.0	0.721	25.0	1.252	25.0	0.000	25.0	0.000	25.0	0.000
30.0	0.220	30.0	0.606	30.0	1.179	30.0	0.000	30.0	0.000	30.0	0.000
35.0	0.361	35.0	0.591	35.0	0.908	35.0	0.000	35.0	0.000	35.0	0.000
40.0	0.605	40.0	0.605	40.0	0.908	40.0	0.000	40.0	0.000	40.0	0.000
45.0	0.757	45.0	0.945	45.0	1.056	45.0	0.000	45.0	0.000	45.0	0.000
50.0	0.605	50.0	0.941	50.0	1.108	50.0	0.000	50.0	0.000	50.0	0.000
55.0	0.501	55.0	0.774	55.0	1.021	55.0	0.000	55.0	0.000	55.0	0.000
60.0	0.413	60.0	0.598	60.0	0.750	60.0	0.000	60.0	0.000	60.0	0.000
65.0	0.229	65.0	0.235	65.0	0.343	65.0	0.000	65.0	0.000	65.0	0.000

Velocity Ratio ( $U_0/U$ ) = 4											
Note: Transverse measurements are referenced from the inner boundary of the deflected jet											
Experiment No. A.265: $x = 140$ mm, $y = 64$ mm, Ambient Conc. = 0.167 ppb, Jet Nozzle Conc. = 13.636 ppb											
$D/d = 28$ , $d = 6.35$ mm											
(Concentration readings have been corrected for the ambient value)											
$z = 1.5$ mm	$z = 4.5$ mm	$z = 11.5$ mm	$z = 16.5$ mm	$z = 21.5$ mm	$z = 26.5$ mm	$z = 31.5$ mm	$z = 36.5$ mm	$z = 41.5$ mm	$z = 46.5$ mm		
$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$C$ (ppb)	$C$ (ppb)
0.0	0.009	0.0	0.116	0.0	0.246	0.0	0.158	0.0	0.018	0.0	0.009
5.0	0.079	5.0	0.646	5.0	0.765	5.0	0.545	5.0	0.132	5.0	0.035
10.0	0.114	10.0	0.954	10.0	1.012	10.0	0.977	10.0	0.220	10.0	0.062
15.0	0.246	15.0	1.036	15.0	1.276	15.0	1.179	15.0	0.475	15.0	0.106
20.0	0.105	20.0	0.971	20.0	1.304	20.0	1.296	20.0	0.642	20.0	0.202
25.0	0.255	25.0	0.997	25.0	1.284	25.0	1.249	25.0	0.757	25.0	0.378
30.0	0.258	30.0	0.757	30.0	1.185	30.0	1.268	30.0	0.836	30.0	0.422
35.0	0.449	35.0	0.616	35.0	0.853	35.0	0.968	35.0	0.757	35.0	0.396
40.0	0.537	40.0	0.633	40.0	0.818	40.0	0.962	40.0	0.704	40.0	0.317
45.0	0.572	45.0	0.704	45.0	0.836	45.0	1.083	45.0	0.475	45.0	0.194
50.0	0.545	50.0	0.686	50.0	0.962	50.0	0.990	50.0	0.457	50.0	0.167
55.0	0.526	55.0	0.537	55.0	0.685	55.0	0.765	55.0	0.229	55.0	0.079
60.0	0.282	60.0	0.352	60.0	0.554	60.0	0.573	60.0	0.106	60.0	0.026
65.0	0.106	65.0	0.167	65.0	0.229	65.0	0.194	65.0	0.018	65.0	0.009
Experiment No. A.266: $x = 140$ mm, $y = 76$ mm, Ambient Conc. = 0.264 ppb, Jet Nozzle Conc. = 16.66 ppb											
$z = 1.5$ mm	$z = 4.5$ mm	$z = 11.5$ mm	$z = 16.5$ mm	$z = 21.5$ mm	$z = 26.5$ mm	$z = 31.5$ mm	$z = 36.5$ mm				
$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)				
0.0	0.005	0.0	0.141	0.0	0.273	0.0	0.307	0.0	0.202	0.0	0.132
5.0	0.097	5.0	0.290	5.0	0.501	5.0	0.730	5.0	0.475	5.0	0.317
10.0	0.150	10.0	0.493	10.0	0.827	10.0	0.994	10.0	0.677	10.0	0.493
15.0	0.229	15.0	0.651	15.0	1.029	15.0	1.152	15.0	0.924	15.0	0.721
20.0	0.273	20.0	0.806	20.0	1.073	20.0	1.223	20.0	1.021	20.0	0.845
25.0	0.273	25.0	0.704	25.0	1.073	25.0	1.223	25.0	1.100	25.0	0.915
30.0	0.308	30.0	0.704	30.0	1.038	30.0	1.180	30.0	1.091	30.0	0.941
35.0	0.413	35.0	0.433	35.0	0.915	35.0	1.064	35.0	1.073	35.0	0.915
40.0	0.528	40.0	0.606	40.0	0.897	40.0	1.003	40.0	1.003	40.0	0.836
45.0	0.677	45.0	0.739	45.0	0.818	45.0	0.959	45.0	0.941	45.0	0.704
50.0	0.605	50.0	0.792	50.0	0.800	50.0	0.950	50.0	0.774	50.0	0.509
55.0	0.633	55.0	0.739	55.0	0.818	55.0	0.800	55.0	0.616	55.0	0.378
60.0	0.528	60.0	0.633	60.0	0.739	60.0	0.774	60.0	0.422	60.0	0.264
65.0	0.361	65.0	0.457	65.0	0.591	65.0	0.545	65.0	0.264	65.0	0.123

Property Table (U670) = 4 Note: Temperature dependent properties are determined from the linear boundary of the following fit Density $\rho = 1.13 \text{ g/cc}$ , $T = 0 \text{ K}$ , Ambient Conc. = 0.000 phr, In Vacuo Conc. = 0.000 phr									
D7d = 26, d = 6.35 mm (Conversion readings have been corrected for the ambient value)									
$z = 15 \text{ mm}$	$z = 45 \text{ mm}$	$z = 115 \text{ mm}$	$z = 165 \text{ mm}$	$z = 215 \text{ mm}$	$z = 265 \text{ mm}$	$z = 315 \text{ mm}$	$z = 365 \text{ mm}$	$z = 415 \text{ mm}$	$z = 465 \text{ mm}$
$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$
C	C	C	C	C	C	C	C	C	C
(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)
5.0	0.009	5.0	0.194	5.0	0.194	5.0	0.202	5.0	0.141
10.0	0.126	10.0	0.238	10.0	0.289	10.0	0.325	10.0	0.229
15.0	0.167	15.0	0.331	15.0	0.449	15.0	0.503	15.0	0.597
20.0	0.204	20.0	0.405	20.0	0.537	20.0	0.604	20.0	0.713
25.0	0.239	25.0	0.469	25.0	0.609	25.0	0.677	25.0	0.752
30.0	0.273	30.0	0.525	30.0	0.671	30.0	0.735	30.0	0.801
35.0	0.307	35.0	0.572	35.0	0.729	35.0	0.793	35.0	0.851
40.0	0.337	40.0	0.615	40.0	0.779	40.0	0.841	40.0	0.891
45.0	0.370	45.0	0.656	45.0	0.821	45.0	0.889	45.0	0.937
50.0	0.401	50.0	0.697	50.0	0.862	50.0	0.935	50.0	0.982
55.0	0.431	55.0	0.738	55.0	0.903	55.0	0.980	55.0	1.027
60.0	0.460	60.0	0.779	60.0	0.945	60.0	1.027	60.0	1.072
65.0	0.489	65.0	0.819	65.0	0.986	65.0	1.072	65.0	1.117
70.0	0.518	70.0	0.859	70.0	1.027	70.0	1.117	70.0	1.162
75.0	0.547	75.0	0.899	75.0	1.068	75.0	1.162	75.0	1.207
80.0	0.577	80.0	0.939	80.0	1.109	80.0	1.207	80.0	1.252
85.0	0.606	85.0	0.979	85.0	1.150	85.0	1.252	85.0	1.297
90.0	0.636	90.0	1.019	90.0	1.191	90.0	1.297	90.0	1.342
95.0	0.665	95.0	1.059	95.0	1.232	95.0	1.342	95.0	1.387
100.0	0.695	100.0	1.099	100.0	1.273	100.0	1.387	100.0	1.432
105.0	0.724	105.0	1.139	105.0	1.314	105.0	1.432	105.0	1.477
110.0	0.754	110.0	1.179	110.0	1.355	110.0	1.477	110.0	1.522
115.0	0.783	115.0	1.219	115.0	1.396	115.0	1.522	115.0	1.567
120.0	0.813	120.0	1.259	120.0	1.437	120.0	1.567	120.0	1.612
125.0	0.842	125.0	1.299	125.0	1.478	125.0	1.612	125.0	1.657
130.0	0.872	130.0	1.339	130.0	1.519	130.0	1.657	130.0	1.702
135.0	0.901	135.0	1.379	135.0	1.560	135.0	1.702	135.0	1.747
140.0	0.931	140.0	1.419	140.0	1.601	140.0	1.747	140.0	1.792
145.0	0.960	145.0	1.459	145.0	1.642	145.0	1.792	145.0	1.837
150.0	0.990	150.0	1.499	150.0	1.683	150.0	1.837	150.0	1.882
155.0	1.019	155.0	1.539	155.0	1.724	155.0	1.882	155.0	1.927
160.0	1.049	160.0	1.579	160.0	1.765	160.0	1.927	160.0	1.972
165.0	1.078	165.0	1.619	165.0	1.806	165.0	1.972	165.0	2.017
170.0	1.108	170.0	1.659	170.0	1.847	170.0	2.017	170.0	2.062
175.0	1.137	175.0	1.699	175.0	1.888	175.0	2.062	175.0	2.107
180.0	1.167	180.0	1.739	180.0	1.929	180.0	2.107	180.0	2.152
185.0	1.196	185.0	1.779	185.0	1.970	185.0	2.152	185.0	2.197
190.0	1.226	190.0	1.819	190.0	2.011	190.0	2.197	190.0	2.242
195.0	1.255	195.0	1.859	195.0	2.052	195.0	2.242	195.0	2.287
200.0	1.285	200.0	1.899	200.0	2.093	200.0	2.287	200.0	2.332
205.0	1.314	205.0	1.939	205.0	2.134	205.0	2.332	205.0	2.377
210.0	1.344	210.0	1.979	210.0	2.175	210.0	2.377	210.0	2.422
215.0	1.373	215.0	2.019	215.0	2.216	215.0	2.422	215.0	2.467
220.0	1.403	220.0	2.059	220.0	2.257	220.0	2.467	220.0	2.512
225.0	1.432	225.0	2.099	225.0	2.298	225.0	2.512	225.0	2.557
230.0	1.462	230.0	2.139	230.0	2.339	230.0	2.557	230.0	2.602
235.0	1.491	235.0	2.179	235.0	2.380	235.0	2.602	235.0	2.647
240.0	1.521	240.0	2.219	240.0	2.421	240.0	2.647	240.0	2.692
245.0	1.550	245.0	2.259	245.0	2.462	245.0	2.692	245.0	2.737
250.0	1.580	250.0	2.299	250.0	2.503	250.0	2.737	250.0	2.782
255.0	1.609	255.0	2.339	255.0	2.544	255.0	2.782	255.0	2.827
260.0	1.639	260.0	2.379	260.0	2.585	260.0	2.827	260.0	2.872
265.0	1.668	265.0	2.419	265.0	2.626	265.0	2.872	265.0	2.917
270.0	1.698	270.0	2.459	270.0	2.667	270.0	2.917	270.0	2.962
275.0	1.727	275.0	2.499	275.0	2.708	275.0	2.962	275.0	3.007
280.0	1.757	280.0	2.539	280.0	2.749	280.0	3.007	280.0	3.052
285.0	1.786	285.0	2.579	285.0	2.790	285.0	3.052	285.0	3.097
290.0	1.816	290.0	2.619	290.0	2.831	290.0	3.097	290.0	3.142
295.0	1.845	295.0	2.659	295.0	2.872	295.0	3.142	295.0	3.187
300.0	1.875	300.0	2.699	300.0	2.913	300.0	3.187	300.0	3.232
305.0	1.904	305.0	2.739	305.0	2.954	305.0	3.232	305.0	3.277
310.0	1.934	310.0	2.779	310.0	2.995	310.0	3.277	310.0	3.322
315.0	1.963	315.0	2.819	315.0	3.036	315.0	3.322	315.0	3.367
320.0	1.993	320.0	2.859	320.0	3.077	320.0	3.367	320.0	3.412
325.0	2.022	325.0	2.899	325.0	3.118	325.0	3.412	325.0	3.457
330.0	2.052	330.0	2.939	330.0	3.159	330.0	3.457	330.0	3.502
335.0	2.081	335.0	2.979	335.0	3.200	335.0	3.502	335.0	3.547
340.0	2.111	340.0	3.019	340.0	3.241	340.0	3.547	340.0	3.592
345.0	2.140	345.0	3.059	345.0	3.282	345.0	3.592	345.0	3.637
350.0	2.170	350.0	3.099	350.0	3.323	350.0	3.637	350.0	3.682
355.0	2.199	355.0	3.139	355.0	3.364	355.0	3.682	355.0	3.727
360.0	2.229	360.0	3.179	360.0	3.405	360.0	3.727	360.0	3.772
365.0	2.258	365.0	3.219	365.0	3.446	365.0	3.772	365.0	3.817
370.0	2.288	370.0	3.259	370.0	3.487	370.0	3.817	370.0	3.862
375.0	2.317	375.0	3.299	375.0	3.528	375.0	3.862	375.0	3.907
380.0	2.347	380.0	3.339	380.0	3.569	380.0	3.907	380.0	3.952
385.0	2.376	385.0	3.379	385.0	3.610	385.0	3.952	385.0	3.997
390.0	2.406	390.0	3.419	390.0	3.651	390.0	3.997	390.0	4.042
395.0	2.435	395.0	3.459	395.0	3.692	395.0	4.042	395.0	4.087
400.0	2.465	400.0	3.499	400.0	3.733	400.0	4.087	400.0	4.132
405.0	2.494	405.0	3.539	405.0	3.774	405.0	4.132	405.0	4.177
410.0	2.524	410.0	3.579	410.0	3.815	410.0	4.177	410.0	4.222
415.0	2.553	415.0	3.619	415.0	3.856	415.0	4.222	415.0	4.267
420.0	2.583	420.0	3.659	420.0	3.897	420.0	4.267	420.0	4.312
425.0	2.612	425.0	3.699	425.0	3.938	425.0	4.312	425.0	4.357
430.0	2.642	430.0	3.739	430.0	3.979	430.0	4.357	430.0	4.402
435.0	2.671	435.0	3.779	435.0	4.020	435.0	4.402	435.0	4.447
440.0	2.701	440.0	3.819	440.0	4.061	440.0	4.447	440.0	4.492
445.0	2.730	445.0	3.859	445.0	4.102	445.0	4.492	445.0	4.537
450.0	2.760	450.0	3.899	450.0	4.143	450.0	4.537	450.0	4.582
455.0	2.789	455.0	3.939	455.0	4.184	455.0	4.582	455.0	4.627
460.0	2.819	460.0	3.979	460.0	4.225	460.0	4.627	460.0	4.672
465.0	2.848	465.0	4.019	465.0	4.266	465.0	4.672	465.0	4.717
470.0	2.878	470.0	4.059	470.0	4.307	470.0	4.717	470.0	4.762
475.0	2.907	475.0	4.099	475.0	4.348	475.0	4.762	475.0	4.807
480.0	2.937	480.0	4.139	480.0	4.389	480.0	4.807	480.0	4.852
485.0	2.966	485.0	4.179	485.0	4.430	485.0	4.852	485.0	4.897
490.0	2.996	490.0	4.219	490.0	4.471	490.0	4.897	490.0	4.942
495.0	3.025	495.0	4.259	495.0	4.512	495.0	4.942	495.0	4.987
500.0	3.055	500.0	4.299	500.0	4.553	500.0	4.987	500.0	5.032
505.0	3.084	505.0	4.339	505.0	4.594	505.0	5.032	505.0	5.077
510.0	3.114	510.0	4.379	510.0	4.635	510.0	5.077	510.0	5.122
515.0	3.143	515.0	4.419	515.0	4.676	515.0	5.122	515.0	5.167
520.0	3.173	520.0	4.459	520.0	4.717	520.0	5.167	520.0	5.212
525.0	3.202	525.0	4.499	525.0	4.758	525.0	5.212	525.0	5.257
530.0	3.232	530.0	4.539	530.0	4.799	530.0	5.257	530.0	5.302
535.0	3.261	535.0	4.579	535.0	4.840	535.0	5.302	535.0	5.347
540.0	3.291	540.0	4.619	540.0	4.881	540.0	5.347	540.0	5.392
545.0	3.320	545.0	4.659	545.0	4.922	545.0	5.392	545.0	5.437
550.0	3.350	550.0	4.699	550.0	4.963	550.0	5.437	550.0	5.482
555.0	3.379	55							

Velocity Ratio ( $U_0/U$ ) = 4													
D/d = 20, d = 6.35 mm													
Note: Temperature measurements are referenced from the inner boundary of the diffused jet													
Ambient Air, A-200, $T = 100^\circ\text{F}$ , Ambient Conc. = 0.004 gph, Jet Nozzle Conc. = 16.402 gph													
$z = 1.5$ mm	$z = 4.5$ mm	$z = 16.5$ mm	$z = 21.5$ mm	$z = 26.5$ mm	$z = 31.5$ mm	$z = 41.5$ mm	$z = 51.5$ mm	$z = 61.5$ mm	$z = 71.5$ mm	$z = 81.5$ mm			
$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$
0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
0.025	0.025	0.025	0.025	0.025	0.025	0.025	0.025	0.025	0.025	0.025	0.025	0.025	0.025
0.050	0.050	0.050	0.050	0.050	0.050	0.050	0.050	0.050	0.050	0.050	0.050	0.050	0.050
0.075	0.075	0.075	0.075	0.075	0.075	0.075	0.075	0.075	0.075	0.075	0.075	0.075	0.075
0.100	0.100	0.100	0.100	0.100	0.100	0.100	0.100	0.100	0.100	0.100	0.100	0.100	0.100
0.125	0.125	0.125	0.125	0.125	0.125	0.125	0.125	0.125	0.125	0.125	0.125	0.125	0.125
0.150	0.150	0.150	0.150	0.150	0.150	0.150	0.150	0.150	0.150	0.150	0.150	0.150	0.150
0.175	0.175	0.175	0.175	0.175	0.175	0.175	0.175	0.175	0.175	0.175	0.175	0.175	0.175
0.200	0.200	0.200	0.200	0.200	0.200	0.200	0.200	0.200	0.200	0.200	0.200	0.200	0.200
0.225	0.225	0.225	0.225	0.225	0.225	0.225	0.225	0.225	0.225	0.225	0.225	0.225	0.225
0.250	0.250	0.250	0.250	0.250	0.250	0.250	0.250	0.250	0.250	0.250	0.250	0.250	0.250
0.275	0.275	0.275	0.275	0.275	0.275	0.275	0.275	0.275	0.275	0.275	0.275	0.275	0.275
0.300	0.300	0.300	0.300	0.300	0.300	0.300	0.300	0.300	0.300	0.300	0.300	0.300	0.300
0.325	0.325	0.325	0.325	0.325	0.325	0.325	0.325	0.325	0.325	0.325	0.325	0.325	0.325
0.350	0.350	0.350	0.350	0.350	0.350	0.350	0.350	0.350	0.350	0.350	0.350	0.350	0.350
0.375	0.375	0.375	0.375	0.375	0.375	0.375	0.375	0.375	0.375	0.375	0.375	0.375	0.375
0.400	0.400	0.400	0.400	0.400	0.400	0.400	0.400	0.400	0.400	0.400	0.400	0.400	0.400
0.425	0.425	0.425	0.425	0.425	0.425	0.425	0.425	0.425	0.425	0.425	0.425	0.425	0.425
0.450	0.450	0.450	0.450	0.450	0.450	0.450	0.450	0.450	0.450	0.450	0.450	0.450	0.450
0.475	0.475	0.475	0.475	0.475	0.475	0.475	0.475	0.475	0.475	0.475	0.475	0.475	0.475
0.500	0.500	0.500	0.500	0.500	0.500	0.500	0.500	0.500	0.500	0.500	0.500	0.500	0.500
0.525	0.525	0.525	0.525	0.525	0.525	0.525	0.525	0.525	0.525	0.525	0.525	0.525	0.525
0.550	0.550	0.550	0.550	0.550	0.550	0.550	0.550	0.550	0.550	0.550	0.550	0.550	0.550
0.575	0.575	0.575	0.575	0.575	0.575	0.575	0.575	0.575	0.575	0.575	0.575	0.575	0.575
0.600	0.600	0.600	0.600	0.600	0.600	0.600	0.600	0.600	0.600	0.600	0.600	0.600	0.600
0.625	0.625	0.625	0.625	0.625	0.625	0.625	0.625	0.625	0.625	0.625	0.625	0.625	0.625
0.650	0.650	0.650	0.650	0.650	0.650	0.650	0.650	0.650	0.650	0.650	0.650	0.650	0.650
0.675	0.675	0.675	0.675	0.675	0.675	0.675	0.675	0.675	0.675	0.675	0.675	0.675	0.675
0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700	0.700
0.725	0.725	0.725	0.725	0.725	0.725	0.725	0.725	0.725	0.725	0.725	0.725	0.725	0.725
0.750	0.750	0.750	0.750	0.750	0.750	0.750	0.750	0.750	0.750	0.750	0.750	0.750	0.750
0.775	0.775	0.775	0.775	0.775	0.775	0.775	0.775	0.775	0.775	0.775	0.775	0.775	0.775
0.800	0.800	0.800	0.800	0.800	0.800	0.800	0.800	0.800	0.800	0.800	0.800	0.800	0.800
0.825	0.825	0.825	0.825	0.825	0.825	0.825	0.825	0.825	0.825	0.825	0.825	0.825	0.825
0.850	0.850	0.850	0.850	0.850	0.850	0.850	0.850	0.850	0.850	0.850	0.850	0.850	0.850
0.875	0.875	0.875	0.875	0.875	0.875	0.875	0.875	0.875	0.875	0.875	0.875	0.875	0.875
0.900	0.900	0.900	0.900	0.900	0.900	0.900	0.900	0.900	0.900	0.900	0.900	0.900	0.900
0.925	0.925	0.925	0.925	0.925	0.925	0.925	0.925	0.925	0.925	0.925	0.925	0.925	0.925
0.950	0.950	0.950	0.950	0.950	0.950	0.950	0.950	0.950	0.950	0.950	0.950	0.950	0.950
0.975	0.975	0.975	0.975	0.975	0.975	0.975	0.975	0.975	0.975	0.975	0.975	0.975	0.975
1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000



Velocity Ratio ( $U_0/U$ ) = 4											
D/d = 20, d = 6.35 mm (Concentration readings have been corrected for the ambient value)											
Note: Temperature measurements are referenced from the inner boundary of the deflected jet											
Experiment No. A211: z = 4000 mm, y = 120 mm, Ambient Conc. = 0.150 ppb, Jet Nozzle Conc. = 14.08 ppb											
z = 1.5 mm	z = 6.5 mm	z = 16.5 mm	z = 21.5 mm	z = 26.5 mm	z = 31.5 mm	z = 41.5 mm	z = 51.5 mm	z = 61.5 mm	z = 81.5 mm		
$\eta$ C	$\eta$ C	$\eta$ C	$\eta$ C	$\eta$ C	$\eta$ C	$\eta$ C	$\eta$ C	$\eta$ C	$\eta$ C	$\eta$ C	$\eta$ C
(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)
0.0	0.106	0.0	0.114	0.0	0.123	0.0	0.114	0.0	0.123	0.0	0.097
20.0	0.106	20.0	0.123	20.0	0.132	20.0	0.123	20.0	0.123	20.0	0.097
40.0	0.114	40.0	0.123	40.0	0.132	40.0	0.123	40.0	0.123	40.0	0.106
50.0	0.114	50.0	0.123	50.0	0.141	50.0	0.123	50.0	0.123	50.0	0.106
60.0	0.114	60.0	0.123	60.0	0.141	60.0	0.123	60.0	0.123	60.0	0.097
70.0	0.114	70.0	0.132	70.0	0.141	70.0	0.123	70.0	0.114	70.0	0.106
80.0	0.123	80.0	0.132	80.0	0.132	80.0	0.132	80.0	0.114	80.0	0.106
90.0	0.123	90.0	0.132	90.0	0.132	90.0	0.132	90.0	0.114	90.0	0.097
100.0	0.123	100.0	0.132	100.0	0.132	100.0	0.132	100.0	0.114	100.0	0.097
120.0	0.114	120.0	0.114	120.0	0.123	120.0	0.123	120.0	0.114	120.0	0.097
140.0	0.097	140.0	0.106	140.0	0.106	140.0	0.106	140.0	0.106	140.0	0.088
160.0	0.083	160.0	0.082	160.0	0.082	160.0	0.079	160.0	0.088	160.0	0.079
Experiment No. A212: z = 3000 mm, y = 125 mm, Ambient Conc. = 0.114 ppb, Jet Nozzle Conc. = 12.51 ppb											
z = 1.5 mm	z = 6.5 mm	z = 16.5 mm	z = 21.5 mm	z = 26.5 mm	z = 31.5 mm	z = 41.5 mm	z = 51.5 mm	z = 61.5 mm	z = 81.5 mm		
$\eta$ C	$\eta$ C	$\eta$ C	$\eta$ C	$\eta$ C	$\eta$ C	$\eta$ C	$\eta$ C	$\eta$ C	$\eta$ C	$\eta$ C	$\eta$ C
(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)
0.0	0.083	0.0	0.083	0.0	0.083	0.0	0.083	0.0	0.083	0.0	0.079
20.0	0.083	20.0	0.083	20.0	0.083	20.0	0.083	20.0	0.079	20.0	0.079
40.0	0.083	40.0	0.083	40.0	0.083	40.0	0.083	40.0	0.079	40.0	0.079
50.0	0.083	50.0	0.083	50.0	0.083	50.0	0.083	50.0	0.079	50.0	0.079
60.0	0.083	60.0	0.083	60.0	0.083	60.0	0.083	60.0	0.079	60.0	0.079
70.0	0.083	70.0	0.083	70.0	0.083	70.0	0.083	70.0	0.079	70.0	0.088
80.0	0.083	80.0	0.083	80.0	0.083	80.0	0.083	80.0	0.079	80.0	0.079
90.0	0.083	90.0	0.083	90.0	0.083	90.0	0.083	90.0	0.079	90.0	0.079
100.0	0.083	100.0	0.083	100.0	0.083	100.0	0.083	100.0	0.079	100.0	0.079
120.0	0.083	120.0	0.083	120.0	0.083	120.0	0.083	120.0	0.079	120.0	0.079
140.0	0.083	140.0	0.083	140.0	0.083	140.0	0.083	140.0	0.079	140.0	0.079
160.0	0.083	160.0	0.083	160.0	0.083	160.0	0.083	160.0	0.079	160.0	0.083

Velocity Ratio ( $U_0/U$ ) = 6									
D/d = 20, d = 6.35 mm									
(Concentration readings have been corrected for the ambient value)									
Note: Transverse measurements are referenced from the inner boundary of the deflected jet									
Experiment No. A301: z = 10 mm, y = 40 mm									
Ambient Concentration = 0.185 gph, jet Nozzle Concentration = 14.423 gph									
z = 1.5 mm	z = 4.5 mm	z = 11.5 mm	z = 16.5 mm	z = 21.5 mm	z = 26.5 mm	z = 31.5 mm	z = 36.5 mm	z = 41.5 mm	
$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	
0.0	0.000	0.0	0.000	0.0	0.000	0.0	0.000	0.0	0.000
5.0	0.000	5.0	0.000	5.0	0.000	5.0	0.000	5.0	0.000
10.0	0.000	10.0	0.000	10.0	0.000	10.0	0.000	10.0	0.000
15.0	0.000	15.0	0.000	15.0	0.000	15.0	0.000	15.0	0.000
20.0	0.000	20.0	0.000	20.0	0.000	20.0	0.000	20.0	0.000
25.0	0.000	25.0	0.000	25.0	0.000	25.0	0.000	25.0	0.000
30.0	0.000	30.0	0.000	30.0	0.000	30.0	0.000	30.0	0.000
35.0	0.000	35.0	0.000	35.0	0.000	35.0	0.000	35.0	0.000
40.0	0.000	40.0	0.000	40.0	0.000	40.0	0.000	40.0	0.000
45.0	0.000	45.0	0.000	45.0	0.000	45.0	0.000	45.0	0.000
50.0	0.000	50.0	0.000	50.0	0.000	50.0	0.000	50.0	0.000
55.0	0.000	55.0	0.000	55.0	0.000	55.0	0.000	55.0	0.000
60.0	0.000	60.0	0.000	60.0	0.000	60.0	0.000	60.0	0.000
Experiment No. A302: z = 40 mm, y = 67.5 mm									
Ambient Concentration = 0.229 gph, jet Nozzle Concentration = 17.236 gph									
z = 1.5 mm	z = 4.5 mm	z = 11.5 mm	z = 16.5 mm	z = 21.5 mm	z = 26.5 mm	z = 31.5 mm	z = 36.5 mm	z = 41.5 mm	z = 46.5 mm
$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)
0.0	0.000	0.0	0.000	0.0	0.000	0.0	0.000	0.0	0.000
5.0	0.000	5.0	0.000	5.0	0.000	5.0	0.000	5.0	0.000
10.0	0.000	10.0	0.000	10.0	0.000	10.0	0.000	10.0	0.000
15.0	0.000	15.0	0.000	15.0	0.000	15.0	0.000	15.0	0.000
20.0	0.000	20.0	0.000	20.0	0.000	20.0	0.000	20.0	0.000
25.0	0.000	25.0	0.000	25.0	0.000	25.0	0.000	25.0	0.000
30.0	0.000	30.0	0.000	30.0	0.000	30.0	0.000	30.0	0.000
35.0	0.000	35.0	0.000	35.0	0.000	35.0	0.000	35.0	0.000
40.0	0.000	40.0	0.000	40.0	0.000	40.0	0.000	40.0	0.000
45.0	0.000	45.0	0.000	45.0	0.000	45.0	0.000	45.0	0.000
50.0	0.000	50.0	0.000	50.0	0.000	50.0	0.000	50.0	0.000
55.0	0.000	55.0	0.000	55.0	0.000	55.0	0.000	55.0	0.000
60.0	0.000	60.0	0.000	60.0	0.000	60.0	0.000	60.0	0.000







Velocity Ratio ( $U_0/U$ ) = 6													
D/d = 20, d = 12.7 mm													
(Concentration readings have been corrected for the ambient value)													
Note: Transverse measurements are referenced from the inner boundary of the deflected jet													
Experiment No. B167: z = 145 mm, y = 129 mm, Ambient Conc. = 0.166 ppb, Jet Nozzle Conc. = 16.956 ppb													
z = 11.5 mm	z = 21.5 mm	z = 31.5 mm	z = 41.5 mm	z = 51.5 mm	z = 71.5 mm	z = 91.5 mm	z = 121.5 mm						
$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)						
C (ppb)	C (ppb)	C (ppb)	C (ppb)	C (ppb)	C (ppb)	C (ppb)	C (ppb)						
0.0	0.609	0.0	2.007	0.0	1.705	0.0	0.633	0.0	0.035	0.0	0.000	0.0	0.000
30.0	1.451	20.0	2.563	20.0	2.400	20.0	1.201	20.0	0.132	20.0	0.000	20.0	0.000
50.0	1.701	30.0	2.434	30.0	2.369	30.0	1.201	30.0	0.097	30.0	0.000	30.0	0.000
60.0	1.423	40.0	2.007	40.0	2.063	40.0	1.118	40.0	0.062	40.0	0.000	40.0	0.000
50.0	1.204	50.0	1.674	50.0	1.894	50.0	1.034	50.0	0.053	50.0	0.000	50.0	0.000
60.0	1.590	60.0	1.703	60.0	2.007	60.0	0.701	60.0	0.035	60.0	0.000	60.0	0.000
70.0	1.952	70.0	1.994	70.0	1.924	70.0	0.300	70.0	0.009	70.0	0.000	70.0	0.000
80.0	1.701	80.0	1.618	80.0	1.360	80.0	0.097	80.0	0.000	80.0	0.000	80.0	0.000
100.0	0.720	100.0	1.396	100.0	0.230	100.0	0.000	100.0	0.000	100.0	0.000	100.0	0.000
Experiment No. B168: z = 259 mm, y = 139 mm, Ambient Conc. = 0.159 ppb, Jet Nozzle Conc. = 15.964 ppb													
z = 11.5 mm	z = 31.5 mm	z = 51.5 mm	z = 61.5 mm	z = 71.5 mm	z = 91.5 mm	z = 111.5 mm	z = 141.5 mm	z = 171.5 mm					
$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)	$\eta$ (mm)					
C (ppb)	C (ppb)	C (ppb)	C (ppb)	C (ppb)	C (ppb)	C (ppb)	C (ppb)	C (ppb)					
0.0	0.000	0.0	0.300	0.0	0.290	0.0	0.273	0.0	0.097	0.0	0.000	0.0	0.000
30.0	0.000	30.0	1.546	30.0	1.510	30.0	1.204	30.0	0.606	30.0	0.150	30.0	0.000
50.0	0.176	50.0	1.900	50.0	1.704	50.0	1.454	50.0	0.941	50.0	0.246	50.0	0.000
60.0	0.255	60.0	1.963	60.0	1.649	60.0	1.426	60.0	0.905	60.0	0.202	60.0	0.000
70.0	0.202	70.0	1.991	70.0	1.769	70.0	1.390	70.0	0.950	70.0	0.259	70.0	0.000
80.0	0.422	80.0	1.832	80.0	1.657	80.0	1.287	80.0	0.906	80.0	0.230	80.0	0.010
90.0	0.605	90.0	1.546	90.0	1.463	90.0	1.176	90.0	0.862	90.0	0.220	90.0	0.010
100.0	0.924	100.0	1.200	100.0	1.207	100.0	1.065	100.0	0.721	100.0	0.167	100.0	0.000
110.0	0.994	110.0	1.010	110.0	1.009	110.0	0.870	110.0	0.545	110.0	0.106	110.0	0.000
130.0	0.977	130.0	0.823	130.0	0.740	130.0	0.481	130.0	0.246	130.0	0.010	130.0	0.000
150.0	0.774	150.0	0.378	150.0	0.317	150.0	0.194	150.0	0.097	150.0	0.000	150.0	0.000
180.0	0.220	180.0	0.043	180.0	0.044	180.0	0.000	180.0	0.000	180.0	0.000	180.0	0.000

Velocity Ratio ( $U_0/U$ ) = 6												
$D/d = 20$ , $d = 12.7$ mm												
(Concentration readings have been corrected for the ambient value)												
Standard No. 1000, $z = 400$ mm, $y = 140$ mm, Ambient Conc. = 0.196 gph, Jet Nozzle Conc. = 19.182 gph												
$z = 1.5$ mm	$z = 21.5$ mm	$z = 41.5$ mm	$z = 61.5$ mm	$z = 81.5$ mm	$z = 101.5$ mm	$z = 121.5$ mm	$z = 141.5$ mm	$z = 161.5$ mm	$z = 181.5$ mm	$z = 201.5$ mm	$z = 221.5$ mm	$z = 241.5$ mm
$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$
C	C	C	C	C	C	C	C	C	C	C	C	C
0.0	0.044	0.0	0.273	0.0	0.591	0.0	0.657	0.0	0.528	0.0	0.255	0.0
30.0	0.100	30.0	0.871	30.0	1.109	30.0	1.057	30.0	0.937	30.0	0.713	30.0
50.0	0.194	50.0	1.196	50.0	1.200	50.0	1.224	50.0	1.021	50.0	0.713	50.0
60.0	0.273	60.0	1.100	60.0	1.335	60.0	1.200	60.0	1.049	60.0	0.704	60.0
70.0	0.334	70.0	1.100	70.0	1.300	70.0	1.335	70.0	0.993	70.0	0.686	70.0
80.0	0.343	80.0	1.224	80.0	1.335	80.0	1.474	80.0	0.965	80.0	0.651	80.0
90.0	0.370	90.0	1.194	90.0	1.363	90.0	1.474	90.0	0.965	90.0	0.625	90.0
100.0	0.390	100.0	1.005	100.0	1.200	100.0	1.391	100.0	0.802	100.0	0.563	100.0
110.0	0.404	110.0	0.940	110.0	1.194	110.0	1.224	110.0	0.790	110.0	0.466	110.0
120.0	0.400	120.0	0.897	120.0	0.897	120.0	0.752	120.0	0.576	120.0	0.317	120.0
130.0	0.590	130.0	0.905	130.0	0.474	130.0	0.591	130.0	0.250	130.0	0.132	130.0
140.0	0.400	140.0	0.299	140.0	0.105	140.0	0.264	140.0	0.079	140.0	0.010	140.0
Standard No. 1010, $z = 360$ mm, $y = 210$ mm, Ambient Conc. = 0.080 gph, Jet Nozzle Conc. = 16.187 gph												
$z = 1.5$ mm	$z = 21.5$ mm	$z = 41.5$ mm	$z = 61.5$ mm	$z = 81.5$ mm	$z = 101.5$ mm	$z = 121.5$ mm	$z = 141.5$ mm	$z = 161.5$ mm	$z = 181.5$ mm	$z = 201.5$ mm	$z = 221.5$ mm	$z = 241.5$ mm
$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$
C	C	C	C	C	C	C	C	C	C	C	C	C
0.0	0.122	0.0	0.370	0.0	0.300	0.0	0.370	0.0	0.370	0.0	0.317	0.0
30.0	0.200	30.0	0.520	30.0	0.500	30.0	0.475	30.0	0.475	30.0	0.360	30.0
50.0	0.264	50.0	0.537	50.0	0.537	50.0	0.545	50.0	0.563	50.0	0.422	50.0
60.0	0.200	60.0	0.500	60.0	0.590	60.0	0.563	60.0	0.590	60.0	0.449	60.0
70.0	0.317	70.0	0.600	70.0	0.604	70.0	0.651	70.0	0.625	70.0	0.466	70.0
80.0	0.343	80.0	0.640	80.0	0.721	80.0	0.604	80.0	0.677	80.0	0.493	80.0
90.0	0.370	90.0	0.640	90.0	0.740	90.0	0.713	90.0	0.604	90.0	0.493	90.0
100.0	0.370	100.0	0.643	100.0	0.705	100.0	0.740	100.0	0.677	100.0	0.493	100.0
110.0	0.340	110.0	0.425	110.0	0.740	110.0	0.730	110.0	0.651	110.0	0.493	110.0
120.0	0.340	120.0	0.537	120.0	0.605	120.0	0.642	120.0	0.563	120.0	0.475	120.0
130.0	0.430	130.0	0.400	130.0	0.554	130.0	0.404	130.0	0.413	130.0	0.360	130.0
140.0	0.300	140.0	0.273	140.0	0.343	140.0	0.260	140.0	0.230	140.0	0.211	140.0

Velocity Ratio ( $U_0/U$ ) = 6		D/d = 28, d = 12.7 mm																	
(Conversion readings have been corrected for the ambient value)																			
Note: Pressure measurements are referenced from the inner boundary of the deflected jet																			
Experiment No. 1311: $x = 130$ mm, $y = 230$ mm, Ambient Conc. = 0.114 gph, Jet Nozzle Conc. = 15.023 gph																			
$z = 15$ mm		$z = 31.5$ mm		$z = 61.5$ mm		$z = 71.5$ mm		$z = 81.5$ mm		$z = 101.5$ mm		$z = 131.5$ mm		$z = 171.5$ mm		$z = 211.5$ mm			
$\eta$	C	$\eta$	C	$\eta$	C	$\eta$	C	$\eta$	C	$\eta$	C	$\eta$	C	$\eta$	C	$\eta$	C		
0.0	0.211	0.0	0.209	0.0	0.259	0.0	0.308	0.0	0.255	0.0	0.282	0.0	0.141	0.0	0.053	0.0	0.002		
30.0	0.275	30.0	0.304	30.0	0.352	30.0	0.361	30.0	0.326	30.0	0.282	30.0	0.194	30.0	0.053	30.0	0.002		
50.0	0.308	50.0	0.434	50.0	0.440	50.0	0.422	50.0	0.405	50.0	0.308	50.0	0.228	50.0	0.052	50.0	0.002		
60.0	0.320	60.0	0.440	60.0	0.457	60.0	0.466	60.0	0.440	60.0	0.334	60.0	0.225	60.0	0.053	60.0	0.002		
70.0	0.345	70.0	0.466	70.0	0.484	70.0	0.510	70.0	0.501	70.0	0.343	70.0	0.225	70.0	0.053	70.0	0.002		
80.0	0.352	80.0	0.500	80.0	0.510	80.0	0.543	80.0	0.537	80.0	0.404	80.0	0.228	80.0	0.053	80.0	0.002		
90.0	0.361	90.0	0.528	90.0	0.537	90.0	0.581	90.0	0.581	90.0	0.361	90.0	0.228	90.0	0.053	90.0	0.002		
100.0	0.387	100.0	0.554	100.0	0.581	100.0	0.572	100.0	0.510	100.0	0.361	100.0	0.228	100.0	0.053	100.0	0.002		
110.0	0.387	110.0	0.563	110.0	0.572	110.0	0.528	110.0	0.404	110.0	0.352	110.0	0.194	110.0	0.044	110.0	0.002		
130.0	0.405	130.0	0.528	130.0	0.528	130.0	0.493	130.0	0.440	130.0	0.259	130.0	0.174	130.0	0.035	130.0	0.002		
150.0	0.413	150.0	0.440	150.0	0.405	150.0	0.370	150.0	0.361	150.0	0.238	150.0	0.132	150.0	0.026	150.0	0.002		
160.0	0.352	160.0	0.308	160.0	0.275	160.0	0.238	160.0	0.211	160.0	0.141	160.0	0.044	160.0	0.002	160.0	0.002		

**Velocity Ratio ( $U_0/U$ ) = 6** **D/d = 16, d = 12.7 mm**

(Conversion readings have been corrected for the ambient value)

Note: Pressure measurements are referenced from the inner boundary of the deflected jet

Experiment No. 1312:  $x = 35$  mm,  $y = 85$  mm

Experiment No. 1313:  $x = 55$  mm,  $y = 115$  mm

Experiment No. 1314:  $x = 85$  mm,  $y = 145$  mm

Experiment No. 1315:  $x = 115$  mm,  $y = 175$  mm

Experiment No. 1316:  $x = 145$  mm,  $y = 205$  mm

Experiment No. 1317:  $x = 175$  mm,  $y = 235$  mm

Experiment No. 1318:  $x = 205$  mm,  $y = 265$  mm

Experiment No. 1319:  $x = 235$  mm,  $y = 295$  mm

Experiment No. 1320:  $x = 265$  mm,  $y = 325$  mm

Experiment No. 1321:  $x = 295$  mm,  $y = 355$  mm

Experiment No. 1322:  $x = 325$  mm,  $y = 385$  mm

Experiment No. 1323:  $x = 355$  mm,  $y = 415$  mm

Experiment No. 1324:  $x = 385$  mm,  $y = 445$  mm

Experiment No. 1325:  $x = 415$  mm,  $y = 475$  mm

Experiment No. 1326:  $x = 445$  mm,  $y = 505$  mm

Experiment No. 1327:  $x = 475$  mm,  $y = 535$  mm

Experiment No. 1328:  $x = 505$  mm,  $y = 565$  mm

Experiment No. 1329:  $x = 535$  mm,  $y = 595$  mm

Experiment No. 1330:  $x = 565$  mm,  $y = 625$  mm

Experiment No. 1331:  $x = 595$  mm,  $y = 655$  mm

Experiment No. 1332:  $x = 625$  mm,  $y = 685$  mm

Experiment No. 1333:  $x = 655$  mm,  $y = 715$  mm

Experiment No. 1334:  $x = 685$  mm,  $y = 745$  mm

Experiment No. 1335:  $x = 715$  mm,  $y = 775$  mm

Experiment No. 1336:  $x = 745$  mm,  $y = 805$  mm

Experiment No. 1337:  $x = 775$  mm,  $y = 835$  mm

Experiment No. 1338:  $x = 805$  mm,  $y = 865$  mm

Experiment No. 1339:  $x = 835$  mm,  $y = 895$  mm

Experiment No. 1340:  $x = 865$  mm,  $y = 925$  mm

Experiment No. 1341:  $x = 895$  mm,  $y = 955$  mm

Experiment No. 1342:  $x = 925$  mm,  $y = 985$  mm

Experiment No. 1343:  $x = 955$  mm,  $y = 1015$  mm

Experiment No. 1344:  $x = 985$  mm,  $y = 1045$  mm

Experiment No. 1345:  $x = 1015$  mm,  $y = 1075$  mm

Experiment No. 1346:  $x = 1045$  mm,  $y = 1105$  mm

Experiment No. 1347:  $x = 1075$  mm,  $y = 1135$  mm

Experiment No. 1348:  $x = 1105$  mm,  $y = 1165$  mm

Experiment No. 1349:  $x = 1135$  mm,  $y = 1195$  mm

Experiment No. 1350:  $x = 1165$  mm,  $y = 1225$  mm

Experiment No. 1351:  $x = 1195$  mm,  $y = 1255$  mm

Experiment No. 1352:  $x = 1225$  mm,  $y = 1285$  mm

Experiment No. 1353:  $x = 1255$  mm,  $y = 1315$  mm

Experiment No. 1354:  $x = 1285$  mm,  $y = 1345$  mm

Experiment No. 1355:  $x = 1315$  mm,  $y = 1375$  mm

Experiment No. 1356:  $x = 1345$  mm,  $y = 1405$  mm

Experiment No. 1357:  $x = 1375$  mm,  $y = 1435$  mm

Experiment No. 1358:  $x = 1405$  mm,  $y = 1465$  mm

Experiment No. 1359:  $x = 1435$  mm,  $y = 1495$  mm

Experiment No. 1360:  $x = 1465$  mm,  $y = 1525$  mm

Experiment No. 1361:  $x = 1495$  mm,  $y = 1555$  mm

Experiment No. 1362:  $x = 1525$  mm,  $y = 1585$  mm

Experiment No. 1363:  $x = 1555$  mm,  $y = 1615$  mm

Experiment No. 1364:  $x = 1585$  mm,  $y = 1645$  mm

Experiment No. 1365:  $x = 1615$  mm,  $y = 1675$  mm

Experiment No. 1366:  $x = 1645$  mm,  $y = 1705$  mm

Experiment No. 1367:  $x = 1675$  mm,  $y = 1735$  mm

Experiment No. 1368:  $x = 1705$  mm,  $y = 1765$  mm

Experiment No. 1369:  $x = 1735$  mm,  $y = 1795$  mm

Experiment No. 1370:  $x = 1765$  mm,  $y = 1825$  mm

Experiment No. 1371:  $x = 1795$  mm,  $y = 1855$  mm

Experiment No. 1372:  $x = 1825$  mm,  $y = 1885$  mm

Experiment No. 1373:  $x = 1855$  mm,  $y = 1915$  mm

Experiment No. 1374:  $x = 1885$  mm,  $y = 1945$  mm

Experiment No. 1375:  $x = 1915$  mm,  $y = 1975$  mm

Experiment No. 1376:  $x = 1945$  mm,  $y = 2005$  mm

Experiment No. 1377:  $x = 1975$  mm,  $y = 2035$  mm

Experiment No. 1378:  $x = 2005$  mm,  $y = 2065$  mm

Experiment No. 1379:  $x = 2035$  mm,  $y = 2095$  mm

Experiment No. 1380:  $x = 2065$  mm,  $y = 2125$  mm

Experiment No. 1381:  $x = 2095$  mm,  $y = 2155$  mm

Experiment No. 1382:  $x = 2125$  mm,  $y = 2185$  mm

Experiment No. 1383:  $x = 2155$  mm,  $y = 2215$  mm

Experiment No. 1384:  $x = 2185$  mm,  $y = 2245$  mm

Experiment No. 1385:  $x = 2215$  mm,  $y = 2275$  mm

Experiment No. 1386:  $x = 2245$  mm,  $y = 2305$  mm

Experiment No. 1387:  $x = 2275$  mm,  $y = 2335$  mm

Experiment No. 1388:  $x = 2305$  mm,  $y = 2365$  mm

Experiment No. 1389:  $x = 2335$  mm,  $y = 2395$  mm

Experiment No. 1390:  $x = 2365$  mm,  $y = 2425$  mm

Experiment No. 1391:  $x = 2395$  mm,  $y = 2455$  mm

Experiment No. 1392:  $x = 2425$  mm,  $y = 2485$  mm

Experiment No. 1393:  $x = 2455$  mm,  $y = 2515$  mm

Experiment No. 1394:  $x = 2485$  mm,  $y = 2545$  mm

Experiment No. 1395:  $x = 2515$  mm,  $y = 2575$  mm

Experiment No. 1396:  $x = 2545$  mm,  $y = 2605$  mm

Experiment No. 1397:  $x = 2575$  mm,  $y = 2635$  mm

Experiment No. 1398:  $x = 2605$  mm,  $y = 2665$  mm

Experiment No. 1399:  $x = 2635$  mm,  $y = 2695$  mm

Experiment No. 1400:  $x = 2665$  mm,  $y = 2725$  mm

Experiment No. 1401:  $x = 2695$  mm,  $y = 2755$  mm

Experiment No. 1402:  $x = 2725$  mm,  $y = 2785$  mm

Experiment No. 1403:  $x = 2755$  mm,  $y = 2815$  mm

Experiment No. 1404:  $x = 2785$  mm,  $y = 2845$  mm

Experiment No. 1405:  $x = 2815$  mm,  $y = 2875$  mm

Experiment No. 1406:  $x = 2845$  mm,  $y = 2905$  mm

Experiment No. 1407:  $x = 2875$  mm,  $y = 2935$  mm

Experiment No. 1408:  $x = 2905$  mm,  $y = 2965$  mm

Experiment No. 1409:  $x = 2935$  mm,  $y = 2995$  mm

Experiment No. 1410:  $x = 2965$  mm,  $y = 3025$  mm

Experiment No. 1411:  $x = 2995$  mm,  $y = 3055$  mm

Experiment No. 1412:  $x = 3025$  mm,  $y = 3085$  mm

Experiment No. 1413:  $x = 3055$  mm,  $y = 3115$  mm

Experiment No. 1414:  $x = 3085$  mm,  $y = 3145$  mm

Experiment No. 1415:  $x = 3115$  mm,  $y = 3175$  mm

Experiment No. 1416:  $x = 3145$  mm,  $y = 3205$  mm

Experiment No. 1417:  $x = 3175$  mm,  $y = 3235$  mm

Experiment No. 1418:  $x = 3205$  mm,  $y = 3265$  mm

Experiment No. 1419:  $x = 3235$  mm,  $y = 3295$  mm

Experiment No. 1420:  $x = 3265$  mm,  $y = 3325$  mm

Experiment No. 1421:  $x = 3295$  mm,  $y = 3355$  mm

Experiment No. 1422:  $x = 3325$  mm,  $y = 3385$  mm

Experiment No. 1423:  $x = 3355$  mm,  $y = 3415$  mm

Experiment No. 1424:  $x = 3385$  mm,  $y = 3445$  mm

Experiment No. 1425:  $x = 3415$  mm,  $y = 3475$  mm

Experiment No. 1426:  $x = 3445$  mm,  $y = 3505$  mm

Experiment No. 1427:  $x = 3475$  mm,  $y = 3535$  mm

Experiment No. 1428:  $x = 3505$  mm,  $y = 3565$  mm

Experiment No. 1429:  $x = 3535$  mm,  $y = 3595$  mm

Experiment No. 1430:  $x = 3565$  mm,  $y = 3625$  mm

Experiment No. 1431:  $x = 3595$  mm,  $y = 3655$  mm

Experiment No. 1432:  $x = 3625$  mm,  $y = 3685$  mm

Experiment No. 1433:  $x = 3655$  mm,  $y = 3715$  mm

Experiment No. 1434:  $x = 3685$  mm,  $y = 3745$  mm

Experiment No. 1435:  $x = 3715$  mm,  $y = 3775$  mm

Experiment No. 1436:  $x = 3745$  mm,  $y = 3805$  mm

Experiment No. 1437:  $x = 3775$  mm,  $y = 3835$  mm

Experiment No. 1438:  $x = 3805$  mm,  $y = 3865$  mm

Experiment No. 1439:  $x = 3835$  mm,  $y = 3895$  mm

Experiment No. 1440:  $x = 3865$  mm,  $y = 3925$  mm

Experiment No. 1441:  $x = 3895$  mm,  $y = 3955$  mm

Experiment No. 1442:  $x = 3925$  mm,  $y = 3985$  mm

Experiment No. 1443:  $x = 3955$  mm,  $y = 4015$  mm

Experiment No. 1444:  $x = 3985$  mm,  $y = 4045$  mm

Experiment No. 1445:  $x = 4015$  mm,  $y = 4075$  mm

Experiment No. 1446:  $x = 4045$  mm,  $y = 4105$  mm

Experiment No. 1447:  $x = 4075$  mm,  $y = 4135$  mm

Experiment No. 1448:  $x = 4105$  mm,  $y = 4165$  mm

Experiment No. 1449:  $x = 4135$  mm,  $y = 4195$  mm

Experiment No. 1450:  $x = 4165$  mm,  $y = 4225$  mm

Experiment No. 1451:  $x = 4195$  mm,  $y = 4255$  mm

Experiment No. 1452:  $x = 4225$  mm,  $y = 4285$  mm

Experiment No. 1453:  $x = 4255$  mm,  $y = 4315$  mm

Experiment No. 1454:  $x = 4285$  mm,  $y = 4345$  mm

Experiment No. 1455:  $x = 4315$  mm,  $y = 4375$  mm

Experiment No. 1456:  $x = 4345$  mm,  $y = 4405$  mm

Experiment No. 1457:  $x = 4375$  mm,  $y = 4435$  mm

Experiment No. 1458:  $x = 4405$  mm,  $y = 4465$  mm

Experiment No. 1459:  $x = 4435$  mm,  $y = 4495$  mm

Experiment No. 1460:  $x = 4465$  mm,  $y = 4525$  mm

Experiment No. 1461:  $x = 4495$  mm,  $y = 4555$  mm

Experiment No. 1462:  $x = 4525$  mm,  $y = 4585$  mm

Experiment No. 1463:  $x = 4555$  mm,  $y = 4615$  mm

Experiment No. 1464:  $x = 4585$  mm,  $y = 4645$  mm

Experiment No. 1465:  $x = 4615$  mm,  $y = 4675$  mm

Experiment No. 1466:  $x = 4645$  mm,  $y = 4705$  mm

Experiment No. 1467:  $x = 4675$  mm,  $y = 4735$  mm

Experiment No. 1468:  $x = 4705$  mm,  $y = 4765$  mm

Experiment No. 1469:  $x = 4735$  mm,  $y = 4795$  mm

Experiment No. 1470:  $x = 4765$  mm,  $y = 4825$  mm

Experiment No. 1471:  $x = 4795$  mm,  $y = 4855$  mm

Experiment No. 1472:  $x = 4825$  mm,  $y = 4885$  mm

Experiment No. 1473:  $x = 4855$  mm,  $y = 4915$  mm

Experiment No. 1474:  $x = 4885$  mm,  $y = 4945$  mm

Experiment No. 1475:  $x = 4915$  mm,  $y = 4975$  mm

Experiment No. 1476:  $x = 4945$  mm,  $y = 5005$  mm

Experiment No. 1477:  $x = 4975$  mm,  $y = 5035$  mm

Experiment No. 1478:  $x = 5005$  mm,  $y = 5065$  mm

Experiment No. 1479:  $x = 5035$  mm,  $y = 5095$  mm

Experiment No. 1480:  $x = 5065$  mm,  $y = 5125$  mm

Experiment No. 1481:  $x = 5095$  mm,  $y = 5155$  mm

Experiment No. 1482:  $x = 5125$  mm,  $y = 5185$  mm

Experiment No. 1483:  $x = 5155$  mm,  $y = 5215$  mm

Experiment No. 1484:  $x = 5185$  mm,  $y = 5245$  mm

Experiment No. 1485:  $x = 5215$  mm,  $y = 5275$  mm

Experiment No. 1486:  $x = 5245$  mm,  $y = 5305$  mm

Experiment No. 1487:  $x = 5275$  mm,  $y = 5335$  mm

Experiment No. 1488:  $x = 5305$  mm,  $y = 5365$  mm

Experiment No. 1489:  $x = 5335$  mm,  $y = 5395$  mm

Experiment No. 1490:  $x = 5365$  mm,  $y = 5425$  mm

Experiment No. 1491:  $x = 5395$  mm,  $y = 5455$  mm

Experiment No. 1492:  $x = 5425$  mm,  $y = 5485$  mm

Experiment No. 1493:  $x = 5455$  mm,  $y = 5515$  mm

Experiment No. 1494:  $x = 5485$  mm,  $y = 5545$  mm</



Velocity Ratio (U <sub>6</sub> /U) = 6									
D/d = 10, d = 12.7 mm									
(Concentration readings have been corrected for the ambient value)									
Experiment No. E336: z = 330 mm									
Ambient Conc. = 0.105 gph, Jet Nozzle Conc. = 17.236 gph									
Chamber = 0.105 gph, Chamber = 17.236 gph									
z = 11.5 mm	z = 31.5 mm	z = 41.5 mm	z = 51.5 mm	z = 61.5 mm	z = 71.5 mm	z = 81.5 mm	z = 91.5 mm	z = 101.5 mm	z = 111.5 mm
η	C	η	C	η	C	η	C	η	C
0.0	0.000	0.0	0.174	0.0	0.352	0.0	0.530	0.0	0.708
30.0	0.320	30.0	1.305	30.0	0.920	30.0	0.905	30.0	0.941
50.0	0.374	50.0	1.504	50.0	0.959	50.0	1.022	50.0	0.994
60.0	0.390	60.0	1.550	60.0	1.007	60.0	1.038	60.0	1.038
70.0	1.000	70.0	1.500	70.0	1.073	70.0	1.164	70.0	1.144
80.0	1.000	80.0	1.500	80.0	1.100	80.0	1.179	80.0	1.161
90.0	0.905	90.0	1.400	90.0	1.090	90.0	1.100	90.0	1.161
100.0	0.800	100.0	1.257	100.0	1.073	100.0	1.170	100.0	1.126
110.0	0.774	110.0	1.000	110.0	0.933	110.0	1.073	110.0	1.030
120.0	0.790	120.0	0.800	120.0	0.770	120.0	0.740	120.0	0.704
130.0	0.800	130.0	0.300	130.0	0.563	130.0	0.500	130.0	0.466
140.0	0.320	140.0	0.105	140.0	0.077	140.0	0.240	140.0	0.211
D/d = 5, d = 12.7 mm									
(Concentration readings have been corrected for the ambient value)									
Experiment No. E337: z = 30 mm, y = 70 mm									
Ambient Conc. = 0.220 gph, Chamber = 16.950 gph									
Chamber = 0.220 gph, Chamber = 16.950 gph									
z = 11.5 mm	z = 31.5 mm	z = 41.5 mm	z = 51.5 mm	z = 61.5 mm	z = 71.5 mm	z = 81.5 mm	z = 91.5 mm	z = 101.5 mm	z = 111.5 mm
η	C	η	C	η	C	η	C	η	C
0.0	0.000	0.0	0.000	0.0	0.000	0.0	0.000	0.0	0.000
30.0	0.170	30.0	2.720	30.0	2.500	30.0	2.700	30.0	2.400
50.0	0.420	50.0	2.877	50.0	2.900	50.0	2.857	50.0	2.200
60.0	2.377	60.0	3.120	60.0	4.077	60.0	2.800	60.0	1.800
70.0	4.320	70.0	4.000	70.0	5.015	70.0	3.420	70.0	1.800
80.0	3.970	80.0	4.077	80.0	4.135	80.0	3.420	80.0	1.800
90.0	1.900	90.0	1.000	90.0	2.970	90.0	2.812	90.0	1.800
100.0	0.450	100.0	0.000	100.0	0.000	100.0	1.700	100.0	0.000
110.0	0.000	110.0	0.000	110.0	0.000	110.0	0.000	110.0	0.000
Experiment No. E338: z = 140 mm									
Ambient Conc. = 0.105 gph, Jet Nozzle Conc. = 17.236 gph									
Chamber = 0.105 gph, Chamber = 17.236 gph									
z = 11.5 mm	z = 31.5 mm	z = 41.5 mm	z = 51.5 mm	z = 61.5 mm	z = 71.5 mm	z = 81.5 mm	z = 91.5 mm	z = 101.5 mm	z = 111.5 mm
η	C	η	C	η	C	η	C	η	C
0.0	0.000	0.0	0.000	0.0	0.000	0.0	0.000	0.0	0.000
30.0	0.170	30.0	2.720	30.0	2.500	30.0	2.700	30.0	2.400
50.0	0.420	50.0	2.877	50.0	2.900	50.0	2.857	50.0	2.200
60.0	2.377	60.0	3.120	60.0	4.077	60.0	2.800	60.0	1.800
70.0	4.320	70.0	4.000	70.0	5.015	70.0	3.420	70.0	1.800
80.0	3.970	80.0	4.077	80.0	4.135	80.0	3.420	80.0	1.800
90.0	1.900	90.0	1.000	90.0	2.970	90.0	2.812	90.0	1.800
100.0	0.450	100.0	0.000	100.0	0.000	100.0	1.700	100.0	0.000
110.0	0.000	110.0	0.000	110.0	0.000	110.0	0.000	110.0	0.000
Experiment No. E339: z = 130 mm									
Ambient Conc. = 0.105 gph, Jet Nozzle Conc. = 17.236 gph									
Chamber = 0.105 gph, Chamber = 17.236 gph									
z = 11.5 mm	z = 31.5 mm	z = 41.5 mm	z = 51.5 mm	z = 61.5 mm	z = 71.5 mm	z = 81.5 mm	z = 91.5 mm	z = 101.5 mm	z = 111.5 mm
η	C	η	C	η	C	η	C	η	C
0.0	0.000	0.0	0.000	0.0	0.000	0.0	0.000	0.0	0.000
30.0	0.170	30.0	2.720	30.0	2.500	30.0	2.700	30.0	2.400
50.0	0.420	50.0	2.877	50.0	2.900	50.0	2.857	50.0	2.200
60.0	2.377	60.0	3.120	60.0	4.077	60.0	2.800	60.0	1.800
70.0	4.320	70.0	4.000	70.0	5.015	70.0	3.420	70.0	1.800
80.0	3.970	80.0	4.077	80.0	4.135	80.0	3.420	80.0	1.800
90.0	1.900	90.0	1.000	90.0	2.970	90.0	2.812	90.0	1.800
100.0	0.450	100.0	0.000	100.0	0.000	100.0	1.700	100.0	0.000
110.0	0.000	110.0	0.000	110.0	0.000	110.0	0.000	110.0	0.000

Velocity Ratio ( $U_0/U$ ) = 8																							
D/d = 20, d = 6.35 mm																							
(Concentration readings have been corrected for the ambient value)																							
Note: Transverse measurements are referenced from the inner boundary of the deflected jet																							
Experiment No. A401: z = 5 mm, y = 21 mm, Ambient Conc. = 0.079 ppb, Jet Nozzle Conc. = 15,600 ppb																							
z = 1.5 mm			z = 6.5 mm			z = 11.5 mm			z = 16.5 mm			z = 21.5 mm			z = 26.5 mm			z = 31.5 mm					
b	C	(ppb)	b	C	(ppb)	b	C	(ppb)	b	C	(ppb)	b	C	(ppb)	b	C	(ppb)	b	C	(ppb)	b	C	(ppb)
(mm)			(mm)			(mm)			(mm)			(mm)			(mm)			(mm)			(mm)		
0.0	0.009		0.0	0.009		0.0	0.009		0.0	0.009		0.0	0.009		0.0	0.000		0.0	0.009		0.0	0.000	
5.0	0.009		5.0	0.009		5.0	0.009		5.0	0.009		5.0	0.009		5.0	0.009		5.0	0.009		10.0	0.000	
10.0	0.009		10.0	0.009		10.0	0.009		10.0	0.009		10.0	0.009		10.0	0.000		10.0	0.009		20.0	0.000	
15.0	0.009		15.0	0.009		15.0	0.009		15.0	0.009		15.0	0.009		15.0	0.009		15.0	0.009		30.0	0.009	
20.0	0.018		20.0	0.009		20.0	0.009		20.0	0.026		20.0	0.018		20.0	0.009		20.0	0.009		40.0	0.009	
25.0	0.018		25.0	0.009		25.0	0.026		25.0	0.026		25.0	0.026		25.0	0.018		25.0	0.018		50.0	0.009	
30.0	0.114		30.0	0.095		30.0	0.070		30.0	0.070		30.0	0.053		30.0	0.053		30.0	0.026		60.0	0.000	
35.0	0.959		35.0	3.147		35.0	0.194		35.0	0.194		35.0	0.088		35.0	0.070		35.0	0.035		70.0	0.000	
40.0	0.703		40.0	10.654		40.0	1.172		40.0	1.172		40.0	0.114		40.0	0.062		40.0	0.035		80.0	0.000	
45.0	9.952		45.0	13.267		45.0	0.757		45.0	0.757		45.0	0.106		45.0	0.070		45.0	0.009		90.0	0.000	
50.0	2.395		50.0	0.369		50.0	0.097		50.0	0.097		50.0	0.062		50.0	0.018		50.0	0.018				
55.0	0.009		55.0	0.053		55.0	0.044		55.0	0.044		55.0	0.044		55.0	0.009		55.0	0.009				
60.0	0.009		60.0	0.009		60.0	0.009		60.0	0.009		60.0	0.009		60.0	0.000		60.0	0.009				
65.0	0.009		65.0	0.000		65.0	0.000		65.0	0.000		65.0	0.009		65.0	0.000		65.0	0.009				
70.0	0.000		70.0	0.000		70.0	0.000		70.0	0.000		70.0	0.009		70.0	0.000		70.0	0.000				
75.0	0.009		75.0	0.000		75.0	0.000		75.0	0.000		75.0	0.000		75.0	0.000		75.0	0.000				
80.0	0.000		80.0	0.000		80.0	0.000		80.0	0.000		80.0	0.000		80.0	0.000		80.0	0.000				
85.0	0.000		85.0	0.000		85.0	0.000		85.0	0.000		85.0	0.000		85.0	0.000		85.0	0.000				
90.0	0.000		90.0	0.000		90.0	0.000		90.0	0.000		90.0	0.000		90.0	0.000		90.0	0.000				
95.0	0.000		95.0	0.000		95.0	0.000		95.0	0.000		95.0	0.000		95.0	0.000		95.0	0.000				



Velocity Ratio ( $U_0/U$ ) = 1											
Note: Pressure measurements are referenced from the inner boundary of the diffused jet											
Experiment No. A404: $z = 1.26$ mm, $Y = 107.9$ mm, Ambient Conc. = 0.005 gph, Jet Nozzle Conc. = 16.187 gph											
$D/d = 28$ , $d = 6.35$ mm (Concentration readings have been corrected for the ambient value)											
$z = 1.5$ mm	$z = 6.5$ mm	$z = 11.5$ mm	$z = 16.5$ mm	$z = 21.5$ mm	$z = 26.5$ mm	$z = 31.5$ mm	$z = 36.5$ mm	$z = 41.5$ mm	$z = 46.5$ mm	$z = 51.5$ mm	$z = 56.5$ mm
$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$
$C$	$C$	$C$	$C$	$C$	$C$	$C$	$C$	$C$	$C$	$C$	$C$
(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)
0.0 0.000	0.0 0.000	0.0 0.000	0.0 0.000	0.0 0.000	0.0 0.000	0.0 0.000	0.0 0.000	0.0 0.000	0.0 0.000	0.0 0.000	0.0 0.000
20.0 0.000	20.0 0.106	20.0 0.106	20.0 0.343	20.0 0.616	20.0 0.897	20.0 1.374	20.0 1.402	20.0 1.249	20.0 0.748	20.0 0.018	20.0 0.000
40.0 0.000	40.0 0.004	40.0 0.141	40.0 0.396	40.0 0.924	40.0 1.337	40.0 1.457	40.0 1.457	40.0 1.117	40.0 0.845	40.0 0.035	40.0 0.000
60.0 0.000	60.0 0.289	60.0 0.176	60.0 0.457	60.0 1.328	60.0 1.459	60.0 1.068	60.0 1.068	60.0 0.809	60.0 0.827	60.0 0.044	60.0 0.000
80.0 0.364	80.0 0.317	80.0 0.469	80.0 0.440	80.0 0.959	80.0 1.337	80.0 0.512	80.0 0.508	80.0 0.651	80.0 0.739	80.0 0.026	80.0 0.000
100.0 0.309	100.0 0.352	100.0 0.308	100.0 0.308	100.0 0.537	100.0 0.792	100.0 0.404	100.0 0.399	100.0 0.465	100.0 0.528	100.0 0.009	100.0 0.000
120.0 0.282	120.0 0.308	120.0 0.211	120.0 0.229	120.0 0.406	120.0 0.579	120.0 0.211	120.0 0.235	120.0 0.228	120.0 0.299	120.0 0.000	120.0 0.000
140.0 0.158	140.0 0.211	140.0 0.000	140.0 0.200	140.0 0.317	140.0 0.405	140.0 0.079	140.0 0.079	140.0 0.079	140.0 0.079	140.0 0.000	140.0 0.000
160.0 0.079	160.0 0.000	160.0 0.000	160.0 0.000	160.0 0.000	160.0 0.000	160.0 0.000	160.0 0.000	160.0 0.000	160.0 0.000	160.0 0.000	160.0 0.000

Experiment No. A405: $z = 1.26$ mm, $Y = 135$ mm, Ambient Conc. = 0.005 gph, Jet Nozzle Conc. = 17.135 gph											
$z = 1.5$ mm	$z = 6.5$ mm	$z = 11.5$ mm	$z = 16.5$ mm	$z = 21.5$ mm	$z = 26.5$ mm	$z = 31.5$ mm	$z = 36.5$ mm	$z = 41.5$ mm	$z = 46.5$ mm	$z = 51.5$ mm	$z = 56.5$ mm
$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$
$C$	$C$	$C$	$C$	$C$	$C$	$C$	$C$	$C$	$C$	$C$	$C$
(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)
0.0 0.000	0.0 0.000	0.0 0.000	0.0 0.000	0.0 0.000	0.0 0.000	0.0 0.000	0.0 0.000	0.0 0.000	0.0 0.000	0.0 0.000	0.0 0.000
20.0 0.000	20.0 0.000	20.0 0.132	20.0 0.194	20.0 0.229	20.0 0.229	20.0 0.282	20.0 0.282	20.0 0.282	20.0 0.282	20.0 0.282	20.0 0.282
40.0 0.000	40.0 0.000	40.0 0.422	40.0 0.545	40.0 0.616	40.0 0.616	40.0 0.677	40.0 0.677	40.0 0.677	40.0 0.677	40.0 0.677	40.0 0.677
60.0 0.000	60.0 0.273	60.0 0.625	60.0 0.713	60.0 0.765	60.0 0.765	60.0 0.765	60.0 0.765	60.0 0.765	60.0 0.765	60.0 0.765	60.0 0.765
80.0 0.000	80.0 0.364	80.0 0.739	80.0 0.809	80.0 0.809	80.0 0.809	80.0 0.809	80.0 0.809	80.0 0.809	80.0 0.809	80.0 0.809	80.0 0.809
100.0 0.106	100.0 0.405	100.0 0.792	100.0 0.792	100.0 0.792	100.0 0.792	100.0 0.792	100.0 0.792	100.0 0.792	100.0 0.792	100.0 0.792	100.0 0.792
120.0 0.114	120.0 0.309	120.0 0.616	120.0 0.616	120.0 0.616	120.0 0.616	120.0 0.616	120.0 0.616	120.0 0.616	120.0 0.616	120.0 0.616	120.0 0.616
140.0 0.107	140.0 0.308	140.0 0.308	140.0 0.308	140.0 0.308	140.0 0.308	140.0 0.308	140.0 0.308	140.0 0.308	140.0 0.308	140.0 0.308	140.0 0.308
160.0 0.211	160.0 0.211	160.0 0.211	160.0 0.211	160.0 0.211	160.0 0.211	160.0 0.211	160.0 0.211	160.0 0.211	160.0 0.211	160.0 0.211	160.0 0.211
180.0 0.105	180.0 0.176	180.0 0.176	180.0 0.176	180.0 0.176	180.0 0.176	180.0 0.176	180.0 0.176	180.0 0.176	180.0 0.176	180.0 0.176	180.0 0.176
200.0 0.105	200.0 0.000	200.0 0.000	200.0 0.000	200.0 0.000	200.0 0.000	200.0 0.000	200.0 0.000	200.0 0.000	200.0 0.000	200.0 0.000	200.0 0.000
220.0 0.000	220.0 0.000	220.0 0.000	220.0 0.000	220.0 0.000	220.0 0.000	220.0 0.000	220.0 0.000	220.0 0.000	220.0 0.000	220.0 0.000	220.0 0.000



Velocity Ratio ( $U_0/U$ ) = 8											
D/d = 20, d = 6.35 mm											
Note: Temperature measurements are referenced from the inner boundary of the deflected jet											
(Concentration readings have been corrected for the ambient value)											
Ambient No. A400: $z = 4000$ mm, $y = 200$ mm, Ambient Conc. = 0.070 gph, Jet Nozzle Conc. = 16.124 gph											
$z = 1.5$ mm	$z = 4.5$ mm	$z = 16.5$ mm	$z = 26.5$ mm	$z = 31.5$ mm	$z = 36.5$ mm	$z = 46.5$ mm	$z = 66.5$ mm	$z = 96.5$ mm	$z = 121.5$ mm		
$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$C$
(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(mm)	(gph)
0.0	0.123	0.0	0.114	0.0	0.123	0.0	0.106	0.0	0.088	0.0	0.088
20.0	0.123	20.0	0.114	20.0	0.123	20.0	0.114	20.0	0.097	20.0	0.088
40.0	0.132	40.0	0.132	40.0	0.123	40.0	0.123	40.0	0.097	40.0	0.088
50.0	0.132	50.0	0.132	50.0	0.132	50.0	0.123	50.0	0.097	50.0	0.079
60.0	0.132	60.0	0.132	60.0	0.132	60.0	0.123	60.0	0.088	60.0	0.079
70.0	0.132	70.0	0.132	70.0	0.141	70.0	0.123	70.0	0.088	70.0	0.070
80.0	0.132	80.0	0.132	80.0	0.141	80.0	0.123	80.0	0.079	80.0	0.070
90.0	0.132	90.0	0.132	90.0	0.141	90.0	0.114	90.0	0.079	90.0	0.062
100.0	0.132	100.0	0.132	100.0	0.123	100.0	0.114	100.0	0.079	100.0	0.062
120.0	0.123	120.0	0.106	120.0	0.123	120.0	0.106	120.0	0.070	120.0	0.053
140.0	0.097	140.0	0.088	140.0	0.088	140.0	0.088	140.0	0.062	140.0	0.044
170.0	0.070	170.0	0.062	170.0	0.070	170.0	0.070	170.0	0.044	170.0	0.026
Ambient No. A400: $z = 1500$ mm, $y = 177$ mm, Ambient Conc. = 0.070 gph, Jet Nozzle Conc. = 19.182 gph											
$z = 1.5$ mm	$z = 11.5$ mm	$z = 21.5$ mm	$z = 26.5$ mm	$z = 31.5$ mm	$z = 36.5$ mm	$z = 41.5$ mm	$z = 46.5$ mm	$z = 66.5$ mm	$z = 91.5$ mm	$z = 121.5$ mm	
$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$C$
(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(mm)	(gph)
0.0	0.141	0.0	0.105	0.0	0.202	0.0	0.211	0.0	0.202	0.0	0.176
20.0	0.167	20.0	0.211	20.0	0.229	20.0	0.238	20.0	0.229	20.0	0.176
40.0	0.194	40.0	0.229	40.0	0.264	40.0	0.273	40.0	0.255	40.0	0.176
50.0	0.202	50.0	0.246	50.0	0.273	50.0	0.273	50.0	0.255	50.0	0.176
60.0	0.202	60.0	0.246	60.0	0.273	60.0	0.273	60.0	0.255	60.0	0.167
70.0	0.211	70.0	0.246	70.0	0.273	70.0	0.273	70.0	0.255	70.0	0.158
80.0	0.229	80.0	0.258	80.0	0.264	80.0	0.264	80.0	0.211	80.0	0.088
90.0	0.229	90.0	0.258	90.0	0.264	90.0	0.258	90.0	0.194	90.0	0.079
100.0	0.229	100.0	0.211	100.0	0.211	100.0	0.202	100.0	0.176	100.0	0.097
120.0	0.165	120.0	0.158	120.0	0.141	120.0	0.141	120.0	0.106	120.0	0.062
140.0	0.097	140.0	0.088	140.0	0.079	140.0	0.079	140.0	0.062	140.0	0.026
170.0	0.035	170.0	0.035	170.0	0.026	170.0	0.026	170.0	0.018	170.0	0.000

Velocity Ratio (U <sub>0</sub> /U) = 12											
(Concentration readings have been corrected for the ambient value)											
Note: Temperature concentrations are referenced from the inner boundary of the diffuser jet											
1 = 1.5 mm, 2 = 3.0 mm, 3 = 4.5 mm, 4 = 6.0 mm, 5 = 7.5 mm, 6 = 9.0 mm, 7 = 10.5 mm, 8 = 12.0 mm, 9 = 13.5 mm, 10 = 15.0 mm, 11 = 16.5 mm, 12 = 18.0 mm											
z = 1.5 mm		z = 3.0 mm		z = 4.5 mm		z = 6.0 mm		z = 7.5 mm		z = 9.0 mm	
$\eta$	C	$\eta$	C	$\eta$	C	$\eta$	C	$\eta$	C	$\eta$	C
10.0	0.000	5.0	0.000	5.0	0.000	5.0	0.000	5.0	0.000	5.0	0.000
20.0	0.000	10.0	0.000	10.0	0.000	10.0	0.000	10.0	0.000	10.0	0.000
30.0	1.200	15.0	0.000	15.0	0.000	15.0	0.000	15.0	0.000	15.0	0.000
40.0	0.000	20.0	0.000	20.0	0.000	20.0	0.000	20.0	0.000	20.0	0.000
50.0	0.000	25.0	0.000	25.0	0.000	25.0	0.000	25.0	0.000	25.0	0.000
60.0	0.000	30.0	0.000	30.0	0.000	30.0	0.000	30.0	0.000	30.0	0.000
70.0	0.000	35.0	0.000	35.0	0.000	35.0	0.000	35.0	0.000	35.0	0.000
80.0	0.000	40.0	0.000	40.0	0.000	40.0	0.000	40.0	0.000	40.0	0.000
90.0	0.000	45.0	0.000	45.0	0.000	45.0	0.000	45.0	0.000	45.0	0.000
		50.0	0.000	50.0	0.000	50.0	0.000	50.0	0.000	50.0	0.000
		55.0	0.000	55.0	0.000	55.0	0.000	55.0	0.000	55.0	0.000
		60.0	0.000	60.0	0.000	60.0	0.000	60.0	0.000	60.0	0.000
		65.0	0.000	65.0	0.000	65.0	0.000	65.0	0.000	65.0	0.000
		70.0	0.000	70.0	0.000	70.0	0.000	70.0	0.000	70.0	0.000
		75.0	0.000	75.0	0.000	75.0	0.000	75.0	0.000	75.0	0.000
		80.0	0.000	80.0	0.000	80.0	0.000	80.0	0.000	80.0	0.000
		85.0	0.000	85.0	0.000	85.0	0.000	85.0	0.000	85.0	0.000
		90.0	0.000	90.0	0.000	90.0	0.000	90.0	0.000	90.0	0.000
		95.0	0.000	95.0	0.000	95.0	0.000	95.0	0.000	95.0	0.000
1 = 1.5 mm, 2 = 3.0 mm, 3 = 4.5 mm, 4 = 6.0 mm, 5 = 7.5 mm, 6 = 9.0 mm, 7 = 10.5 mm, 8 = 12.0 mm, 9 = 13.5 mm, 10 = 15.0 mm, 11 = 16.5 mm, 12 = 18.0 mm											
z = 1.5 mm		z = 3.0 mm		z = 4.5 mm		z = 6.0 mm		z = 7.5 mm		z = 9.0 mm	
$\eta$	C	$\eta$	C	$\eta$	C	$\eta$	C	$\eta$	C	$\eta$	C
10.0	0.000	5.0	0.000	5.0	0.000	5.0	0.000	5.0	0.000	5.0	0.000
20.0	0.000	10.0	0.000	10.0	0.000	10.0	0.000	10.0	0.000	10.0	0.000
30.0	0.000	15.0	0.000	15.0	0.000	15.0	0.000	15.0	0.000	15.0	0.000
40.0	0.000	20.0	0.000	20.0	0.000	20.0	0.000	20.0	0.000	20.0	0.000
50.0	0.000	25.0	0.000	25.0	0.000	25.0	0.000	25.0	0.000	25.0	0.000
60.0	0.000	30.0	0.000	30.0	0.000	30.0	0.000	30.0	0.000	30.0	0.000
70.0	0.000	35.0	0.000	35.0	0.000	35.0	0.000	35.0	0.000	35.0	0.000
80.0	0.000	40.0	0.000	40.0	0.000	40.0	0.000	40.0	0.000	40.0	0.000
90.0	0.000	45.0	0.000	45.0	0.000	45.0	0.000	45.0	0.000	45.0	0.000
		50.0	0.000	50.0	0.000	50.0	0.000	50.0	0.000	50.0	0.000
		55.0	0.000	55.0	0.000	55.0	0.000	55.0	0.000	55.0	0.000
		60.0	0.000	60.0	0.000	60.0	0.000	60.0	0.000	60.0	0.000
		65.0	0.000	65.0	0.000	65.0	0.000	65.0	0.000	65.0	0.000
		70.0	0.000	70.0	0.000	70.0	0.000	70.0	0.000	70.0	0.000
		75.0	0.000	75.0	0.000	75.0	0.000	75.0	0.000	75.0	0.000
		80.0	0.000	80.0	0.000	80.0	0.000	80.0	0.000	80.0	0.000
		85.0	0.000	85.0	0.000	85.0	0.000	85.0	0.000	85.0	0.000
		90.0	0.000	90.0	0.000	90.0	0.000	90.0	0.000	90.0	0.000
		95.0	0.000	95.0	0.000	95.0	0.000	95.0	0.000	95.0	0.000





Velocity heads (0.67U) <sup>2</sup> = 12 Note: Transverse measurements are referenced from the inner boundary of the deflected jet (Concentration readings have been corrected for the ambient value)														
Fig. 7.5.2.1: $z = 100$ mm, $y = 126.5$ mm, Ambient Conc. = 0.105 gph, Jet Nozzle Conc. = 11.025 gph														
$z = 15$ mm	$z = 41.5$ mm	$z = 68.5$ mm	$z = 95.5$ mm	$z = 122.5$ mm	$z = 149.5$ mm	$z = 176.5$ mm	$z = 203.5$ mm	$z = 230.5$ mm	$z = 257.5$ mm	$z = 284.5$ mm	$z = 311.5$ mm	$z = 338.5$ mm	$z = 365.5$ mm	$z = 392.5$ mm
$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$
C	C	C	C	C	C	C	C	C	C	C	C	C	C	C
(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)
0.0	0.000	0.0	0.300	0.0	1.002	0.0	1.307	0.0	1.331	0.0	1.303	0.0	1.220	0.0
30.0	0.000	30.0	0.300	30.0	1.145	30.0	1.425	30.0	1.349	30.0	1.349	30.0	0.941	30.0
60.0	0.125	60.0	0.404	60.0	1.118	60.0	1.479	60.0	1.402	60.0	1.367	60.0	0.899	60.0
90.0	0.357	90.0	0.422	90.0	0.812	90.0	1.314	90.0	1.349	90.0	1.341	90.0	0.748	90.0
120.0	0.400	120.0	0.398	120.0	0.756	120.0	1.276	120.0	1.331	120.0	1.274	120.0	0.545	120.0
150.0	0.504	150.0	0.300	150.0	0.857	150.0	1.056	150.0	1.202	150.0	1.175	150.0	0.326	150.0
180.0	1.021	180.0	0.924	180.0	0.912	180.0	0.979	180.0	1.149	180.0	1.137	180.0	0.167	180.0
210.0	0.509	210.0	0.509	210.0	0.509	210.0	0.897	210.0	1.036	210.0	0.999	210.0	0.044	210.0
240.0	0.537	240.0	0.246	240.0	0.607	240.0	0.842	240.0	0.998	240.0	0.970	240.0	0.000	240.0
							45.0	45.0	0.924	45.0	0.889	45.0	0.777	
							90.0	90.0	0.831	90.0	0.805	90.0	0.747	
							135.0	135.0	0.674	135.0	0.646	135.0	0.554	
							180.0	180.0	0.664	180.0	0.633	180.0	0.409	
							225.0	225.0	0.424	225.0	0.343	225.0	0.202	
							270.0	270.0	0.352	270.0	0.246	270.0	0.185	
							315.0	315.0	0.167	315.0	0.132	315.0	0.088	
							360.0	360.0	0.046	360.0	0.009	360.0	0.000	
							405.0	405.0	0.000	405.0	0.000	405.0	0.000	
Fig. 7.5.2.2: $z = 150$ mm, $y = 173$ mm, Ambient Conc. = 0.043 gph, Jet Nozzle Conc. = 17.236 gph														
$z = 15$ mm	$z = 41.5$ mm	$z = 68.5$ mm	$z = 95.5$ mm	$z = 122.5$ mm	$z = 149.5$ mm	$z = 176.5$ mm	$z = 203.5$ mm	$z = 230.5$ mm	$z = 257.5$ mm	$z = 284.5$ mm	$z = 311.5$ mm	$z = 338.5$ mm	$z = 365.5$ mm	$z = 392.5$ mm
$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$
C	C	C	C	C	C	C	C	C	C	C	C	C	C	C
(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)	(gph)
0.0	0.000	0.0	0.000	0.0	0.004	0.0	0.079	0.0	0.097	0.0	0.132	0.0	0.185	0.0
30.0	0.000	30.0	0.150	30.0	0.510	30.0	0.905	30.0	1.003	30.0	1.029	30.0	1.003	30.0
60.0	0.044	60.0	0.349	60.0	0.908	60.0	1.240	60.0	1.152	60.0	1.091	60.0	0.994	60.0
90.0	0.079	90.0	0.578	90.0	0.948	90.0	1.179	90.0	1.100	90.0	0.994	90.0	0.871	90.0
120.0	0.246	120.0	0.282	120.0	0.713	120.0	0.953	120.0	0.897	120.0	0.818	120.0	0.739	120.0
150.0	0.440	150.0	0.317	150.0	0.486	150.0	0.806	150.0	0.677	150.0	0.609	150.0	0.616	150.0
180.0	0.554	180.0	0.431	180.0	0.451	180.0	0.554	180.0	0.501	180.0	0.554	180.0	0.510	180.0
210.0	0.600	210.0	0.528	210.0	0.510	210.0	0.510	210.0	0.519	210.0	0.457	210.0	0.396	210.0
240.0	0.677	240.0	0.554	240.0	0.404	240.0	0.422	240.0	0.413	240.0	0.343	240.0	0.264	240.0
270.0	0.681	270.0	0.535	270.0	0.449	270.0	0.398	270.0	0.282	270.0	0.229	270.0	0.158	270.0
300.0	0.506	300.0	0.194	300.0	0.407	300.0	0.444	300.0	0.403	300.0	0.355	300.0	0.265	300.0
330.0	0.035	330.0	0.035	330.0	0.000	330.0	0.000	330.0	0.000	330.0	0.035	330.0	0.035	330.0
											100.0	100.0	0.026	100.0
											150.0	150.0	0.026	150.0
											200.0	200.0	0.026	200.0
											250.0	250.0	0.026	250.0
											300.0	300.0	0.026	300.0

Velocity Ratio (US/70) = 12 Note: Transverse measurements are referenced from the inner boundary of the deflected jet U/d = 28, d = 0.35 mm (Concentration readings have been corrected for the ambient value)											
Fig. A-367: L = 300 mm, Y = 225 mm, Ambient Conc. = 0.007 ppb, Jet Nozzle Conc. = 17,792 ppb											
z = 15 mm	z = 115 mm	z = 215 mm	z = 315 mm	z = 365 mm	z = 415 mm	z = 465 mm	z = 515 mm	z = 565 mm	z = 615 mm	z = 915 mm	z = 1215 mm
$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$
C	C	C	C	C	C	C	C	C	C	C	C
(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)
0.0	0.003	0.0	0.114	0.0	0.176	0.0	0.238	0.0	0.308	0.0	0.211
30.0	0.105	30.0	0.275	30.0	0.431	30.0	0.431	30.0	0.422	30.0	0.351
50.0	0.176	50.0	0.361	50.0	0.466	50.0	0.537	50.0	0.564	50.0	0.493
60.0	0.194	60.0	0.378	60.0	0.485	60.0	0.563	60.0	0.651	60.0	0.605
70.0	0.202	70.0	0.378	70.0	0.501	70.0	0.607	70.0	0.677	70.0	0.598
80.0	0.211	80.0	0.369	80.0	0.485	80.0	0.589	80.0	0.651	80.0	0.572
90.0	0.220	90.0	0.361	90.0	0.484	90.0	0.563	90.0	0.598	90.0	0.484
100.0	0.234	100.0	0.343	100.0	0.422	100.0	0.495	100.0	0.591	100.0	0.396
110.0	0.275	110.0	0.308	110.0	0.369	110.0	0.422	110.0	0.413	110.0	0.317
120.0	0.289	120.0	0.299	120.0	0.317	120.0	0.352	120.0	0.308	120.0	0.235
130.0	0.229	130.0	0.229	130.0	0.211	130.0	0.211	130.0	0.176	130.0	0.097
140.0	0.141	140.0	0.158	140.0	0.114	140.0	0.114	140.0	0.062	140.0	0.006
Fig. A-368: L = 1500 mm, Y = 200 mm, Ambient Conc. = 0.116 ppb, Jet Nozzle Conc. = 13,965 ppb											
z = 15 mm	z = 115 mm	z = 215 mm	z = 315 mm	z = 365 mm	z = 415 mm	z = 465 mm	z = 515 mm	z = 565 mm	z = 615 mm	z = 915 mm	z = 1115 mm
$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$
C	C	C	C	C	C	C	C	C	C	C	C
(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)	(ppb)
0.0	0.176	0.0	0.194	0.0	0.228	0.0	0.264	0.0	0.275	0.0	0.282
30.0	0.105	30.0	0.211	30.0	0.264	30.0	0.317	30.0	0.317	30.0	0.334
50.0	0.202	50.0	0.229	50.0	0.264	50.0	0.299	50.0	0.317	50.0	0.308
60.0	0.211	60.0	0.229	60.0	0.264	60.0	0.299	60.0	0.299	60.0	0.282
70.0	0.229	70.0	0.238	70.0	0.264	70.0	0.264	70.0	0.275	70.0	0.258
80.0	0.220	80.0	0.229	80.0	0.229	80.0	0.264	80.0	0.246	80.0	0.238
90.0	0.202	90.0	0.211	90.0	0.211	90.0	0.229	90.0	0.211	90.0	0.211
100.0	0.105	100.0	0.202	100.0	0.211	100.0	0.185	100.0	0.194	100.0	0.185
110.0	0.158	110.0	0.185	110.0	0.167	110.0	0.176	110.0	0.176	110.0	0.158
120.0	0.158	120.0	0.176	120.0	0.132	120.0	0.158	120.0	0.158	120.0	0.158
130.0	0.079	130.0	0.097	130.0	0.079	130.0	0.079	130.0	0.079	130.0	0.079
140.0	0.005	140.0	0.005	140.0	0.005	140.0	0.005	140.0	0.005	140.0	0.005

Velocity Ratio $(U_5/U) = 12$ <span style="float: right;"><math>D/d = 20, d = 12.7 \text{ mm}</math></span>											
(Concentration readings have been corrected for the ambient values)											
Note: Temperature measurements are referenced from the inner boundary of the deflected jet											
Experiment No. 1461: $z = 150 \text{ mm}, y = 265 \text{ mm}, \text{Ambient Conc.} = 0.150 \text{ gph, Jet Nozzle Conc.} = 17.792 \text{ gph}$											
$z = 1.5 \text{ mm}$	$z = 21.5 \text{ mm}$	$z = 41.5 \text{ mm}$	$z = 61.5 \text{ mm}$	$z = 81.5 \text{ mm}$	$z = 101.5 \text{ mm}$	$z = 121.5 \text{ mm}$	$z = 141.5 \text{ mm}$	$z = 161.5 \text{ mm}$	$z = 181.5 \text{ mm}$	$z = 191.5 \text{ mm}$	$z = 221.5 \text{ mm}$
$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$
$C$	$C$	$C$	$C$	$C$	$C$	$C$	$C$	$C$	$C$	$C$	$C$
(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)
0.0 0.000	0.0 0.132	0.0 0.009	0.0 0.025	0.0 0.309	0.0 0.675	0.0 0.300	0.0 0.369	0.0 0.000	0.0 0.000	0.0 0.000	0.0 0.000
20.0 0.010	20.0 0.520	20.0 1.993	20.0 1.565	20.0 1.417	20.0 1.417	20.0 1.353	20.0 1.130	20.0 0.000	20.0 0.000	20.0 0.000	20.0 0.000
30.0 0.003	30.0 0.704	30.0 1.649	30.0 1.732	30.0 1.895	30.0 1.723	30.0 1.742	30.0 1.436	30.0 0.000	30.0 0.000	30.0 0.000	30.0 0.000
40.0 0.070	40.0 0.600	40.0 1.565	40.0 1.732	40.0 1.770	40.0 1.834	40.0 1.826	40.0 1.540	40.0 0.000	40.0 0.000	40.0 0.000	40.0 0.000
50.0 0.235	50.0 0.301	50.0 1.315	50.0 1.621	50.0 1.805	50.0 1.751	50.0 1.770	50.0 1.631	50.0 1.000	50.0 1.000	50.0 1.000	50.0 1.000
60.0 0.519	60.0 0.405	60.0 1.009	60.0 1.454	60.0 1.529	60.0 1.612	60.0 1.631	60.0 1.603	60.0 1.000	60.0 1.000	60.0 1.000	60.0 1.000
70.0 0.720	70.0 0.510	70.0 0.926	70.0 1.140	70.0 1.334	70.0 1.390	70.0 1.381	70.0 1.575	70.0 1.144	70.0 1.144	70.0 1.144	70.0 1.144
80.0 0.830	80.0 0.704	80.0 0.926	80.0 1.037	80.0 1.167	80.0 1.270	80.0 1.106	80.0 1.402	80.0 1.064	80.0 1.064	80.0 1.064	80.0 1.064
90.0 0.900	90.0 0.853	90.0 0.954	90.0 1.065	90.0 1.004	90.0 1.223	90.0 1.150	90.0 1.436	90.0 1.047	90.0 1.047	90.0 1.047	90.0 1.047
100.0 0.945	100.0 0.904	100.0 0.981	100.0 1.176	100.0 1.112	100.0 1.195	100.0 1.214	100.0 1.381	100.0 0.871	100.0 0.871	100.0 0.871	100.0 0.871
120.0 0.500	120.0 0.713	120.0 0.759	120.0 1.000	120.0 1.004	120.0 1.004	120.0 1.106	120.0 1.150	120.0 0.607	120.0 0.607	120.0 0.607	120.0 0.607
			125.0 0.981	125.0 0.856		125.0 1.103					
Experiment No. 1462: $z = 250 \text{ mm}, y = 221.5 \text{ mm}, \text{Ambient Conc.} = 0.150 \text{ gph, Jet Nozzle Conc.} = 20.850 \text{ gph}$											
$z = 1.5 \text{ mm}$	$z = 21.5 \text{ mm}$	$z = 41.5 \text{ mm}$	$z = 61.5 \text{ mm}$	$z = 81.5 \text{ mm}$	$z = 101.5 \text{ mm}$	$z = 121.5 \text{ mm}$	$z = 141.5 \text{ mm}$	$z = 161.5 \text{ mm}$	$z = 181.5 \text{ mm}$	$z = 191.5 \text{ mm}$	$z = 221.5 \text{ mm}$
$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$
$C$	$C$	$C$	$C$	$C$	$C$	$C$	$C$	$C$	$C$	$C$	$C$
(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)
0.0 0.000	0.0 0.000	0.0 0.200	0.0 0.501	0.0 0.317	0.0 0.220	0.0 0.035	0.0 0.009	0.0 0.009	0.0 0.009	0.0 0.009	0.0 0.009
30.0 0.000	30.0 0.220	30.0 1.213	30.0 1.435	30.0 1.170	30.0 0.815	30.0 0.352	30.0 0.150	30.0 0.070	30.0 0.070	30.0 0.000	30.0 0.000
50.0 0.000	50.0 0.503	50.0 1.005	50.0 1.574	50.0 1.300	50.0 1.005	50.0 0.590	50.0 0.300	50.0 0.070	50.0 0.070	50.0 0.010	50.0 0.010
60.0 0.000	60.0 0.700	60.0 1.790	60.0 1.546	60.0 1.300	60.0 1.120	60.0 0.651	60.0 0.361	60.0 0.097	60.0 0.097	60.0 0.010	60.0 0.010
70.0 0.000	70.0 0.800	70.0 1.804	70.0 1.491	70.0 1.315	70.0 1.120	70.0 0.730	70.0 0.370	70.0 0.114	70.0 0.114	70.0 0.010	70.0 0.010
80.0 0.114	80.0 0.810	80.0 1.790	80.0 1.435	80.0 1.287	80.0 1.120	80.0 0.845	80.0 0.413	80.0 0.097	80.0 0.097	80.0 0.009	80.0 0.009
90.0 0.340	90.0 0.677	90.0 1.713	90.0 1.352	90.0 1.176	90.0 1.065	90.0 0.802	90.0 0.409	90.0 0.106	90.0 0.106	90.0 0.009	90.0 0.009
100.0 0.422	100.0 0.440	100.0 1.491	100.0 1.157	100.0 1.140	100.0 0.981	100.0 0.809	100.0 0.334	100.0 0.106	100.0 0.106	100.0 0.009	100.0 0.009
110.0 0.520	110.0 0.300	110.0 1.101	110.0 1.018	110.0 1.037	110.0 0.890	110.0 0.703	110.0 0.317	110.0 0.097	110.0 0.097	110.0 0.009	110.0 0.009
130.0 0.730	130.0 0.387	130.0 0.604	130.0 0.851	130.0 0.926	130.0 0.815	130.0 0.721	130.0 0.255	130.0 0.062	130.0 0.062	130.0 0.009	130.0 0.009
150.0 0.757	150.0 0.405	150.0 0.712	150.0 0.700	150.0 0.676	150.0 0.620	150.0 0.509	150.0 0.141	150.0 0.000	150.0 0.000	150.0 0.000	150.0 0.000
180.0 0.500	180.0 0.440	180.0 0.434	180.0 0.490	180.0 0.264	180.0 0.202	180.0 0.246	180.0 0.026	180.0 0.000	180.0 0.000	180.0 0.000	180.0 0.000

Velocity Ratio ( $U_0/U$ ) = 12 <span style="float: right;"><math>D/d = 20</math>, <math>d = 12.7</math> mm</span>											
(Concentration readings have been corrected for the ambient values)											
Note: Transverse measurements are referenced from the inner boundary of the deflected jet											
Experiment No. 1045: $z = 420$ mm, Ambient Conc. = 0.035 gph, Jet Nozzle Conc. = 16.958 gph											
$z = 1.5$ mm	$z = 21.5$ mm	$z = 41.5$ mm	$z = 61.5$ mm	$z = 81.5$ mm	$z = 101.5$ mm	$z = 131.5$ mm	$z = 161.5$ mm	$z = 191.5$ mm	$z = 221.5$ mm	$z = 251.5$ mm	
$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	C
(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)
0.0	0.004	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.026
30.0	0.019	30.0	0.071	30.0	0.083	30.0	0.090	30.0	0.093	30.0	0.026
50.0	0.025	50.0	0.090	50.0	0.093	50.0	0.095	50.0	0.095	50.0	0.035
60.0	0.055	60.0	0.073	60.0	0.094	60.0	0.095	60.0	0.095	60.0	0.026
70.0	0.053	70.0	0.073	70.0	0.094	70.0	0.094	70.0	0.094	70.0	0.026
80.0	0.088	80.0	0.072	80.0	0.097	80.0	0.097	80.0	0.097	80.0	0.026
90.0	0.125	90.0	0.094	90.0	0.093	90.0	0.093	90.0	0.093	90.0	0.035
100.0	0.225	100.0	0.093	100.0	0.093	100.0	0.093	100.0	0.093	100.0	0.026
110.0	0.282	110.0	0.094	110.0	0.094	110.0	0.094	110.0	0.094	110.0	0.018
130.0	0.352	130.0	0.238	130.0	0.431	130.0	0.308	130.0	0.282	130.0	0.009
150.0	0.388	150.0	0.299	150.0	0.388	150.0	0.264	150.0	0.167	150.0	0.000
160.0	0.238	160.0	0.282	160.0	0.225	160.0	0.194	160.0	0.079	160.0	0.000

Experiment No. 1046: $z = 1250$ mm, Ambient Conc. = 0.114 gph, Jet Nozzle Conc. = 16.011 gph											
$z = 1.5$ mm	$z = 21.5$ mm	$z = 41.5$ mm	$z = 61.5$ mm	$z = 81.5$ mm	$z = 101.5$ mm	$z = 131.5$ mm	$z = 161.5$ mm	$z = 191.5$ mm	$z = 221.5$ mm	$z = 251.5$ mm	
$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	$\eta$	C
(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)	(mm)
0.0	0.055	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.085
30.0	0.070	30.0	0.361	30.0	0.361	30.0	0.370	30.0	0.282	30.0	0.167
50.0	0.097	50.0	0.398	50.0	0.398	50.0	0.413	50.0	0.282	50.0	0.114
60.0	0.125	60.0	0.378	60.0	0.405	60.0	0.457	60.0	0.264	60.0	0.114
70.0	0.114	70.0	0.361	70.0	0.457	70.0	0.466	70.0	0.282	70.0	0.114
80.0	0.125	80.0	0.352	80.0	0.391	80.0	0.493	80.0	0.282	80.0	0.114
90.0	0.150	90.0	0.352	90.0	0.354	90.0	0.510	90.0	0.282	90.0	0.114
100.0	0.150	100.0	0.398	100.0	0.466	100.0	0.537	100.0	0.282	100.0	0.114
110.0	0.150	110.0	0.398	110.0	0.466	110.0	0.537	110.0	0.282	110.0	0.114
130.0	0.132	130.0	0.361	130.0	0.466	130.0	0.475	130.0	0.255	130.0	0.079
150.0	0.150	150.0	0.352	150.0	0.466	150.0	0.388	150.0	0.225	150.0	0.079
160.0	0.167	160.0	0.255	160.0	0.352	160.0	0.264	160.0	0.132	160.0	0.000

### **APPENDIX III**

#### **Centerline Wall Jet Trajectories for the Momentum Dominated Flow Regimes**

**( Figures ( a ) - ( u ) )**

### **Appendix III**

#### **Diffusion of Circular Wall Jet in Crossflows**

##### **General**

The analysis on this section is based on the photographic trajectory data from an experimental study by M. Diebel and N. Rajaratnam which was carried out in the T. Blench hydraulics laboratory, University of Alberta. The results predict both the path and the growth rate of the deflected wall jet and were used to approximate the location of the jet during the dilution investigations.

Diebel's experiments were conducted in the same rectangular channel, 0.91 m wide, 0.76 m deep and 36.6 m long, used in the present study. Well-designed nozzles of diameters equal to 6.35 mm and 19.05 mm, located at a distance of about 21 m from the flume entrance were used to generate the wall jet discharges from one side of the flume. Diluted solution of cochineal food color dye used was introduced into the piping system near the jet nozzle by gravity to produce a colored jet. The specific gravity of the dye was 1.020 at a temperature of 16.5 °C and with significant dilution, its density was assumed to approach the freestream water density.

Photographs of the coloured jets with exposure time of a 1/2 to 1 second were taken from above the flume to provide the plan view of the deflected wall jet. Measurements of the jet centerline and its total width  $B$  at different locations along the  $\xi$  - axis were carried out using a 2 cm x 2 cm grid painted on the bed of the flume at the study section. The mid point between the inner and the outer jet penetration boundaries at each location was taken as the jet centerline. Photographs taken for the

side elevation were used to obtain the vertical thickness  $h$  of the deflected jet at locations along the axial distance.

### **Growth of the Deflected Wall Jet**

The deflected jet centerline in the work of Diebel was defined by the  $x$  and  $y$  co-ordinates where  $x$  represents the longitudinal distance along the stream and  $y$  represents the perpendicular distance to the stream with the origin at the jet nozzle. The axial distance  $\xi$  was measured from the nozzle along the centerline of the deflected jet for which the  $y$  co - ordinate was written as  $y_c$ .

The analysis of the jet trajectory showed no sensitivity to the magnitude of  $D / d$ , the ratio of freestream depth to the jet nozzle diameter which was generally in the range of 20-37, in the lateral growth. The present study on deeply submerged jets therefore, would show minimal dependence on the parameter. However the jet growth in the vertical ( depth wise ) direction would be influenced by the surface effects for relatively low values of  $D / d$ .

### **The Present Investigation**

The objectives of the study were to define the flow regimes of the deflected circular wall jet using the photographic data of Diebel and to compare the trajectory relations with those established by Wright ( 1977 ). Diebel's data give the co-ordinates of the jet centerline.

The investigation of the flow regimes were carried out by plotting the dimensionless centerline co - ordinates,  $x / l_m$  against  $y_c / l_m$  and then superimposing the known trajectory solutions for the momentum dominated near and far fields. Based on the trajectory analysis of Wright ( 1977 ), the path of a free deflected circular jet in crossflow was fitted by a  $1/2$  - slope and  $1/3$  - slope for the MDNF and the MDFF respectively. Diebel's wall jet data are presented graphically in Figures III ( a ) - ( s ) for the two jet nozzle diameters used. The plots indicate that most of the data fall on the far field flow regime. The transition point was found to vary in the range of  $y_c / l_m = 1.0$  to  $2.0$  and approximated the value obtained from the work of Wright ( 1977 ) of  $y_c / l_m = 1.5$ .

The dependence of the proportionality coefficients  $C_1$  and  $C_2$  on the velocity ratio  $\alpha$  was also analyzed based on the two slopes for the MDNF and the MDFF respectively. The variation of each of these coefficients against  $\alpha$  is presented in Figures III ( t ) and ( u ). The coefficients are fitted by the equations:

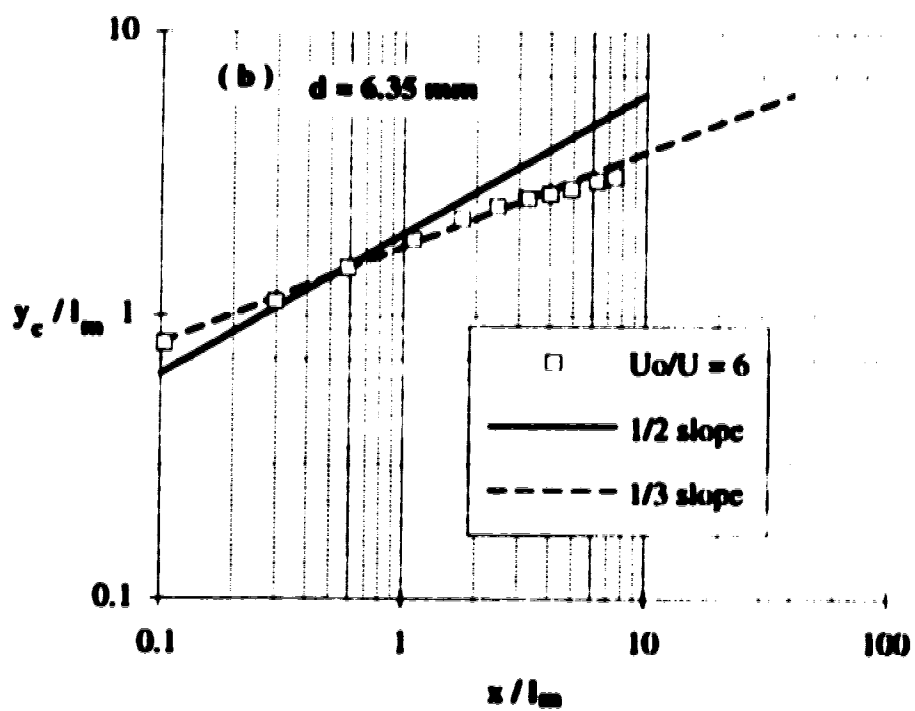
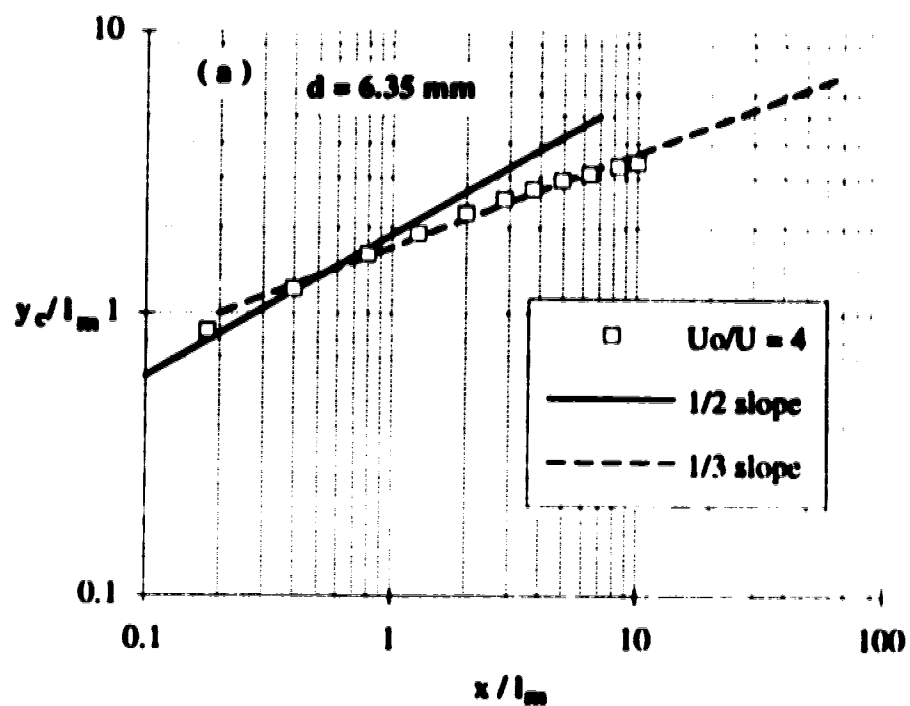
$$C_1 = 1.11 \alpha^{0.29} \quad (\text{III-1})$$

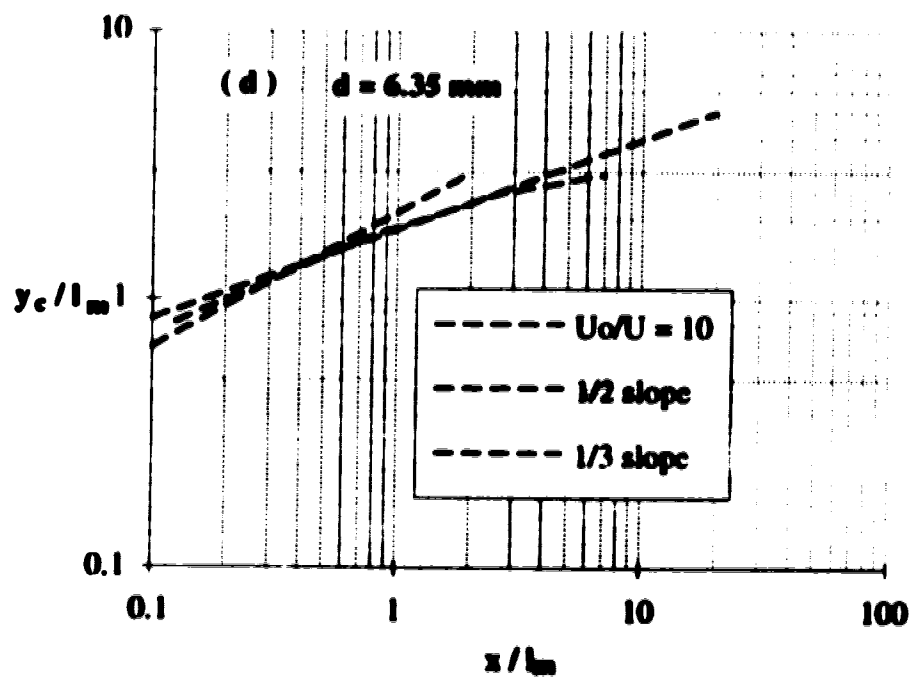
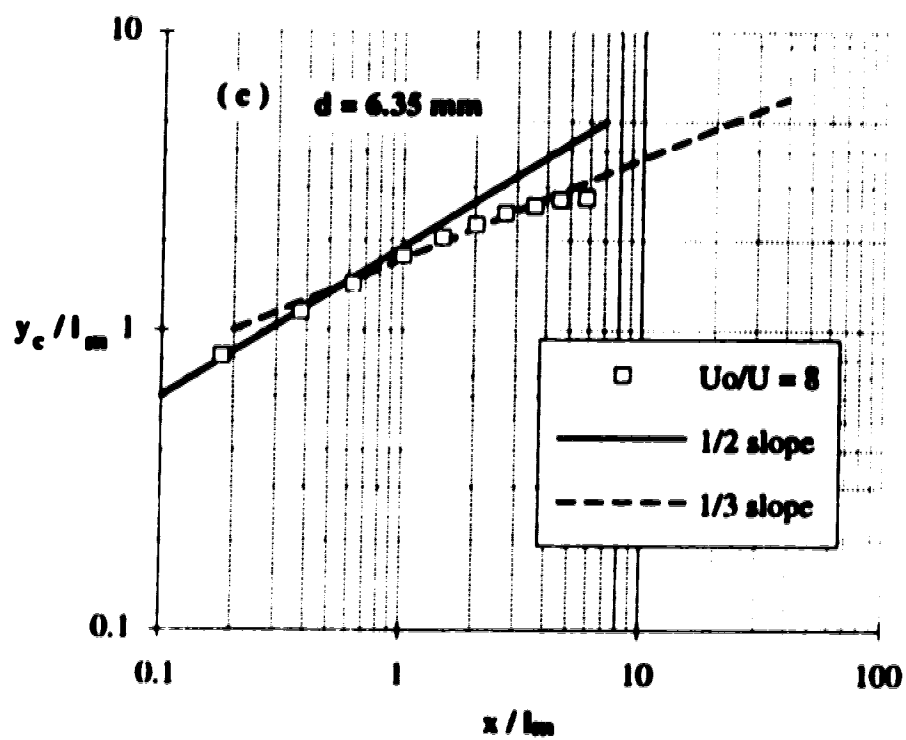
$$C_2 = 0.98 \alpha^{0.28} \quad (\text{III-2})$$

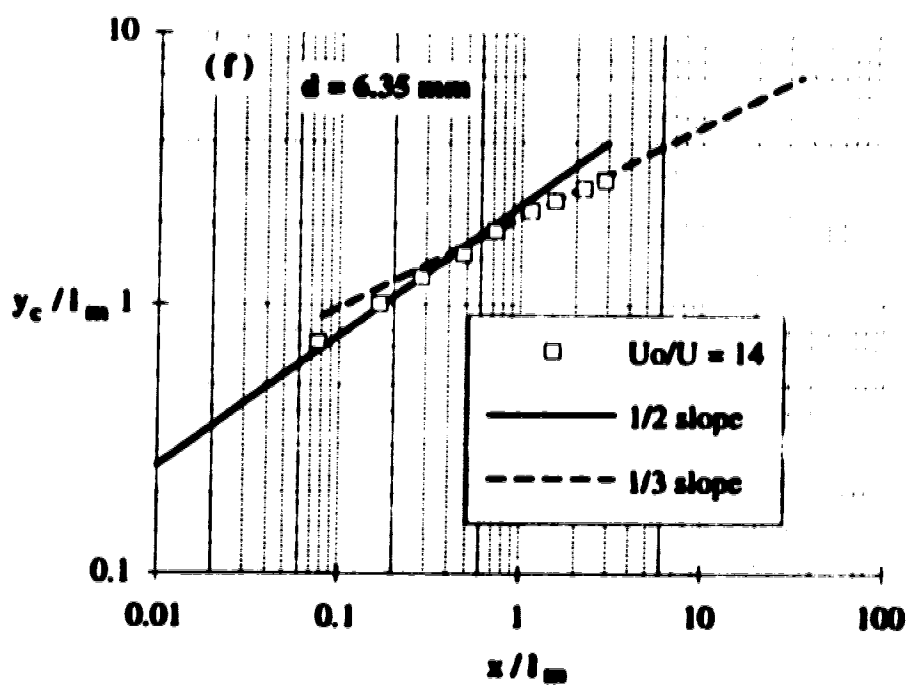
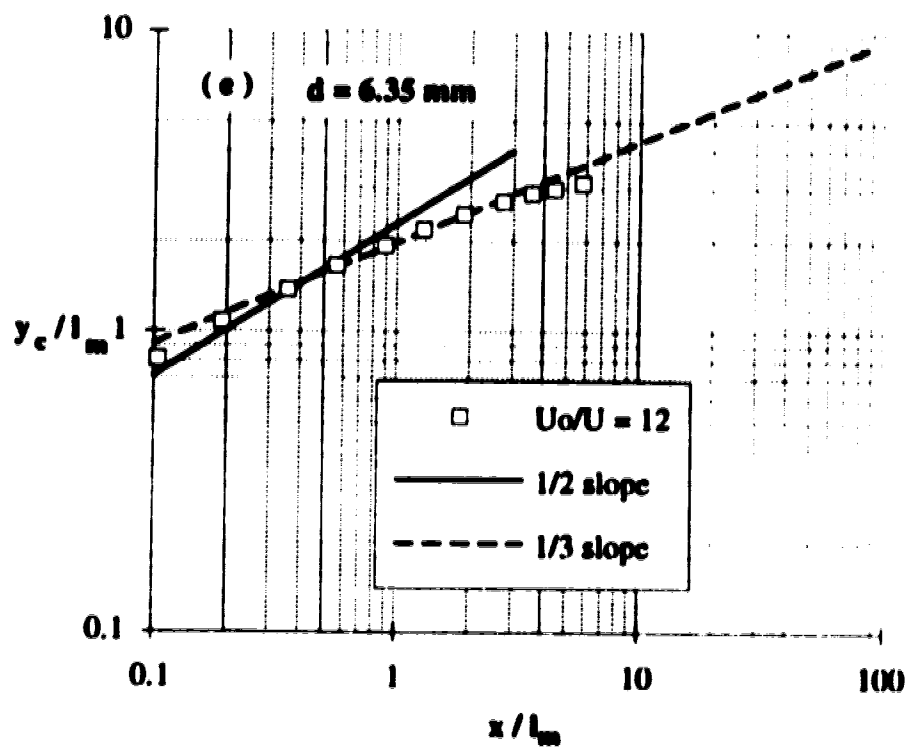
The results indicate that both these coefficients are not constants but are approximately linear functions of  $\alpha$ . The increase of  $C_1$  tends to an asymptotic value of 3, while  $C_2$  approaches a constant value of about 2.5 for  $\alpha$  above 20. The results given by the work of Wright showed similar trends but both the coefficients asymptotically approached a constant value of 2 for very high velocity ratios of about  $\alpha = 100$ . Hodgson ( 1991 ) carried out similar analysis for river - like shallow crossflows for  $\alpha$  less than 15. The present results from Diebel's data closely approximated Hodgson's results for  $\alpha$  less than 10 but about 30 % greater than

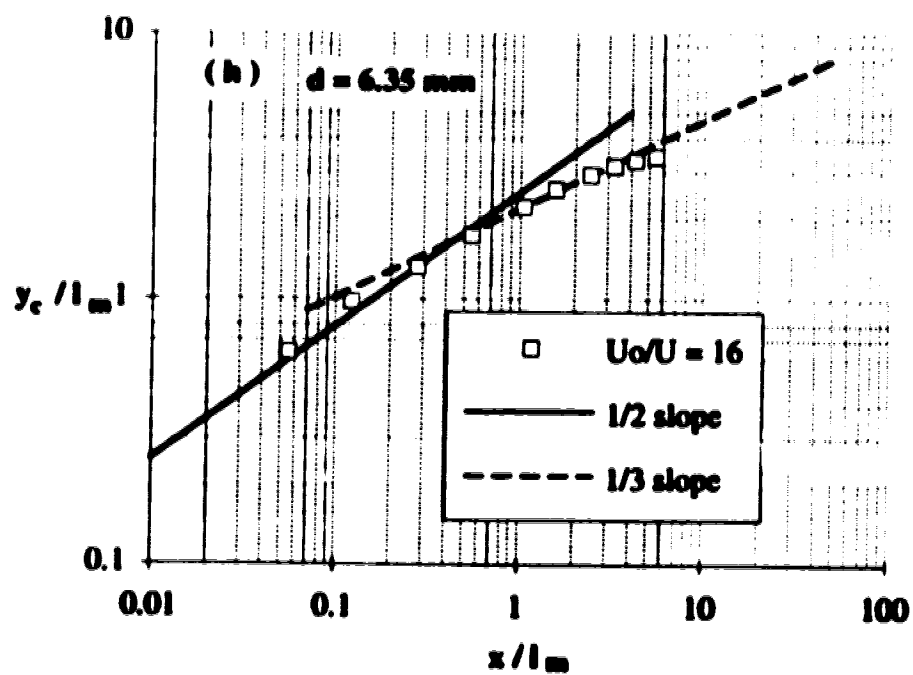
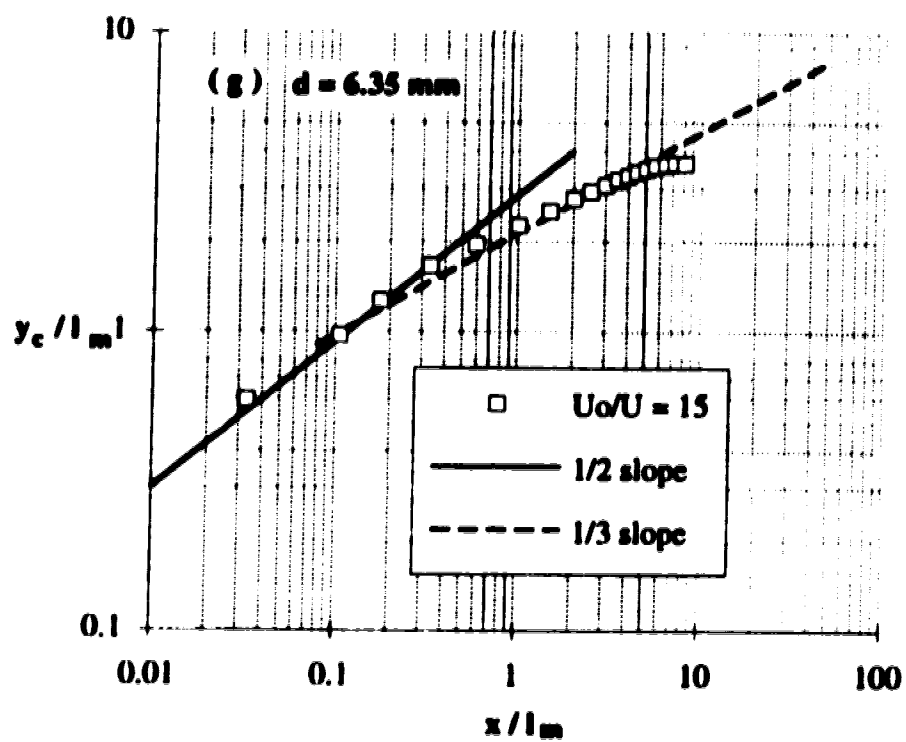


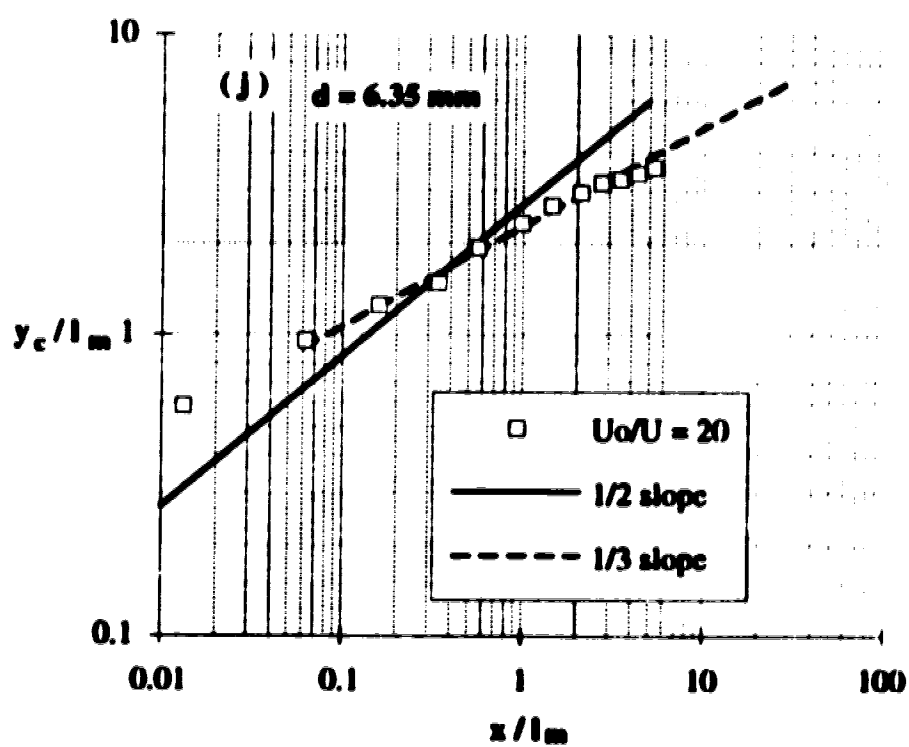
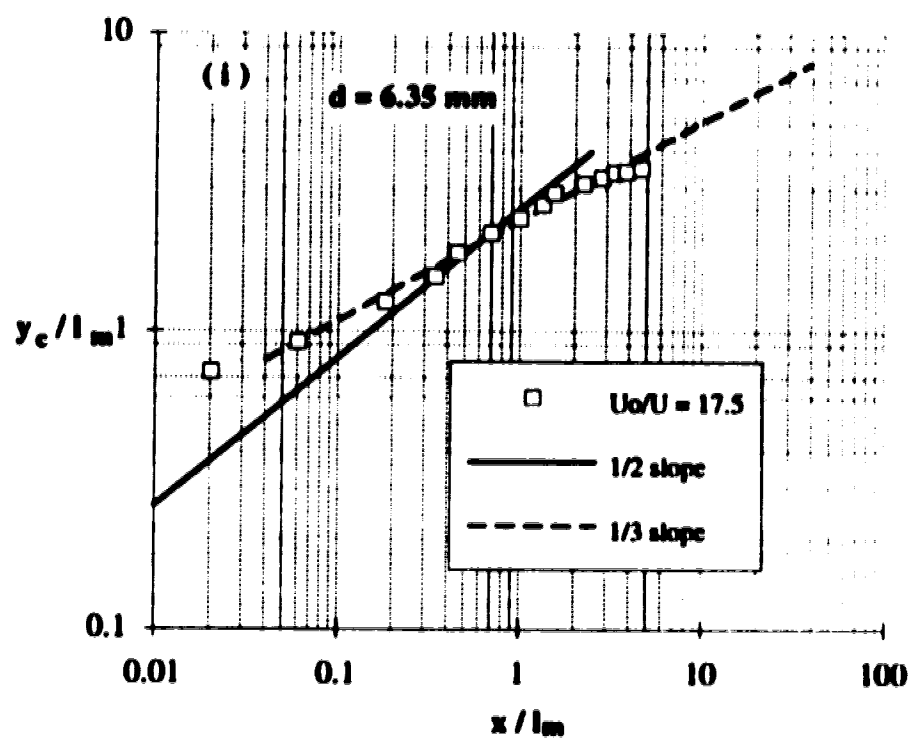
Wright's results. The comparisons in the momentum dominated far field regime indicates that the wall jet coefficient  $C_2$  tends to increase faster than values given by the work of Hodgson. These results indicate that the wall jet penetration is greater than that of the corresponding free deflected jet. Low velocity of freestream flow near the bed might be responsible for this difference.

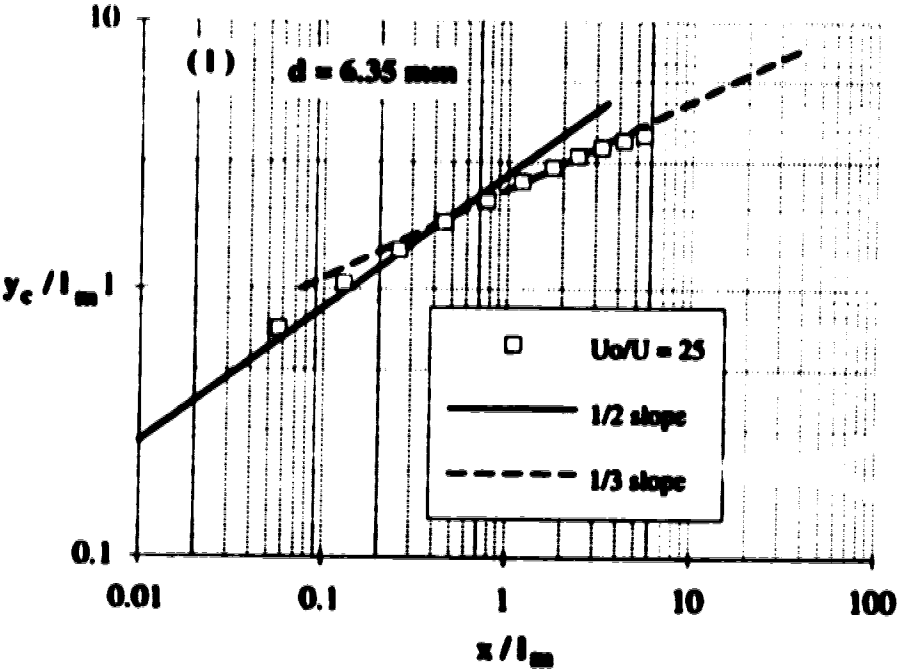
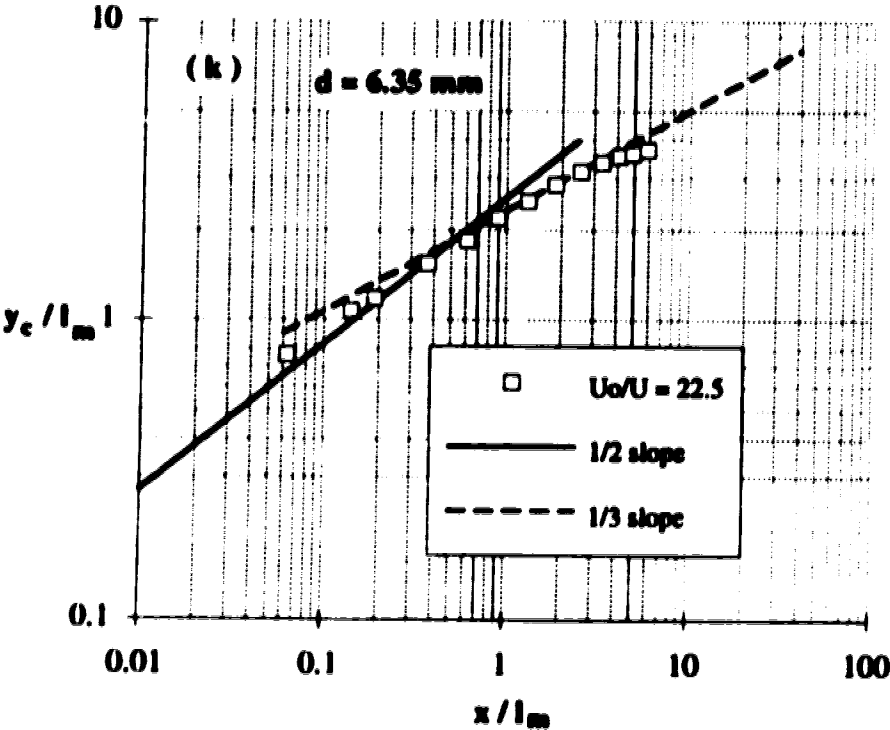


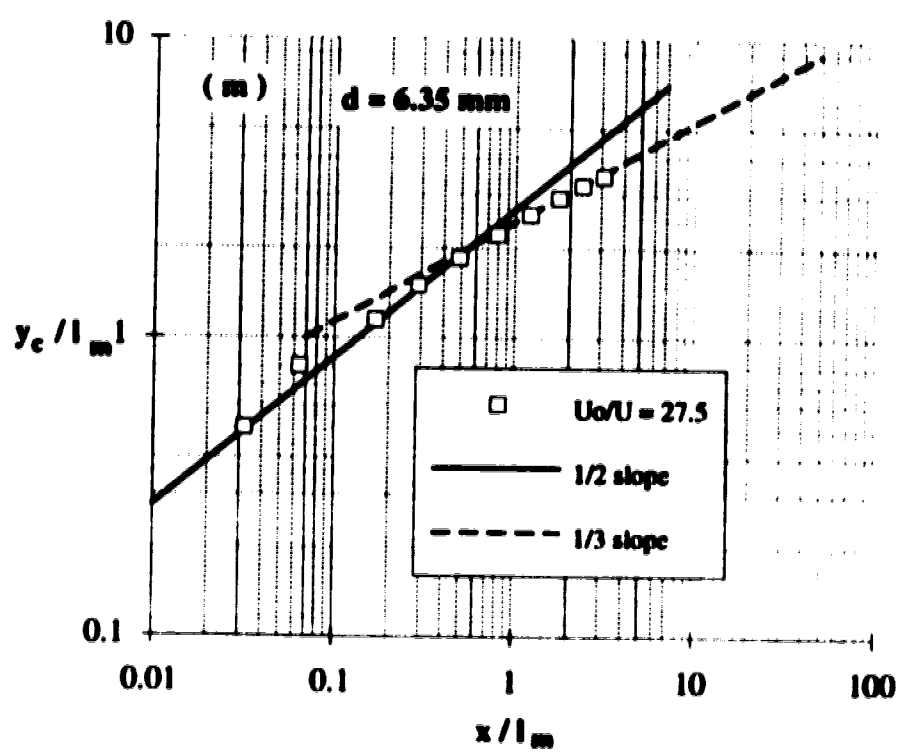




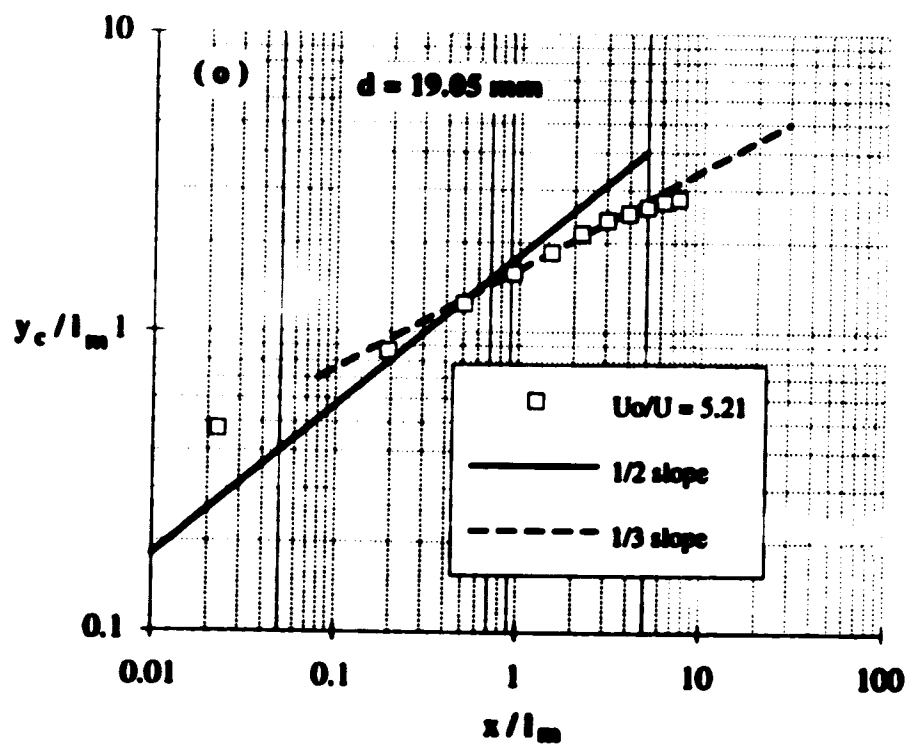
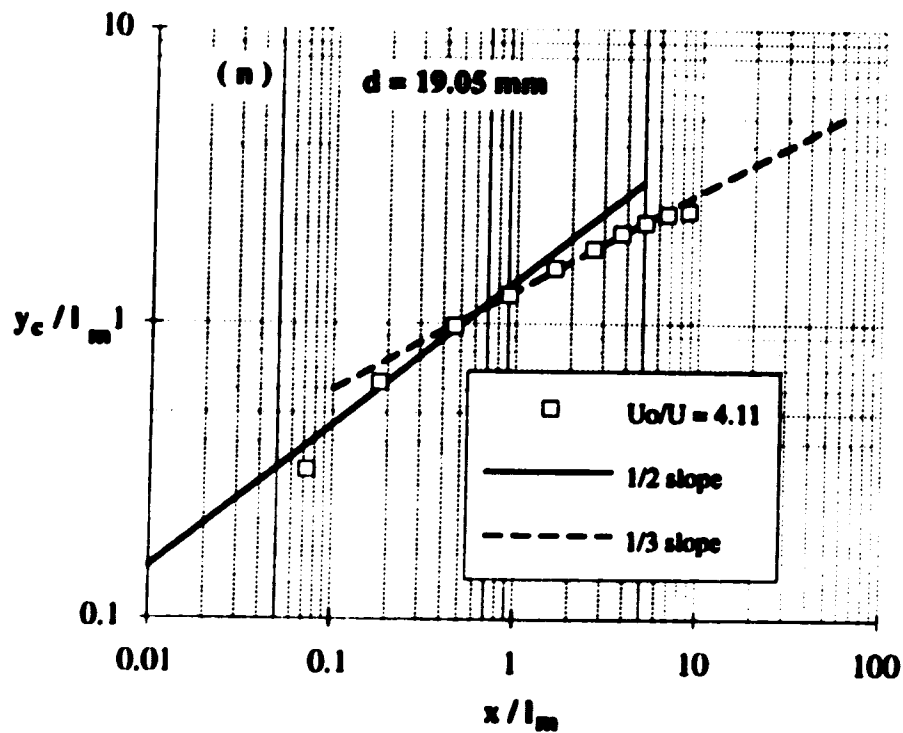


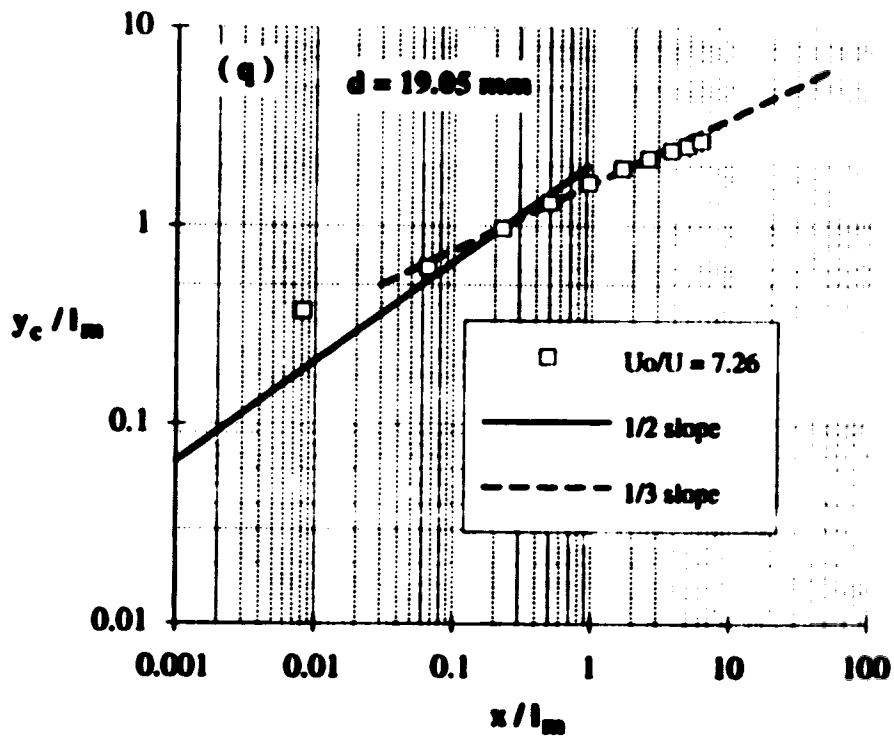
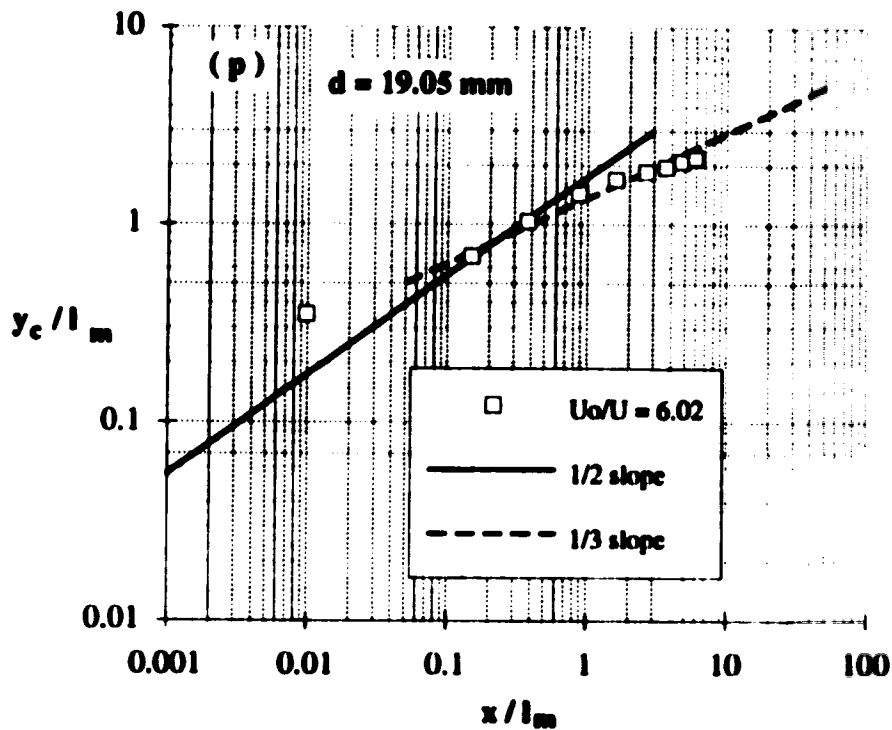


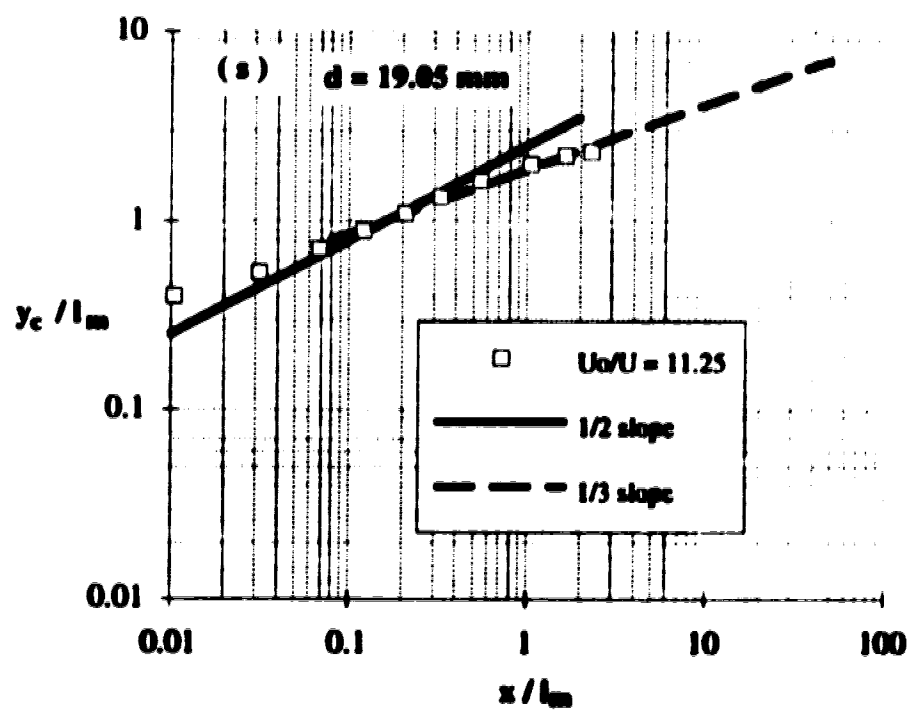
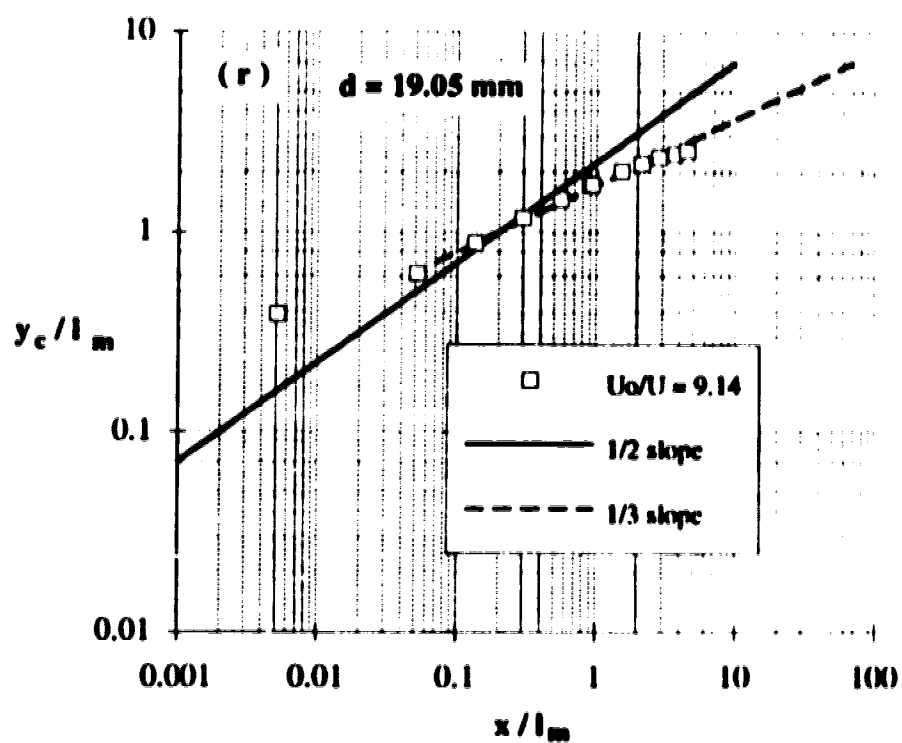












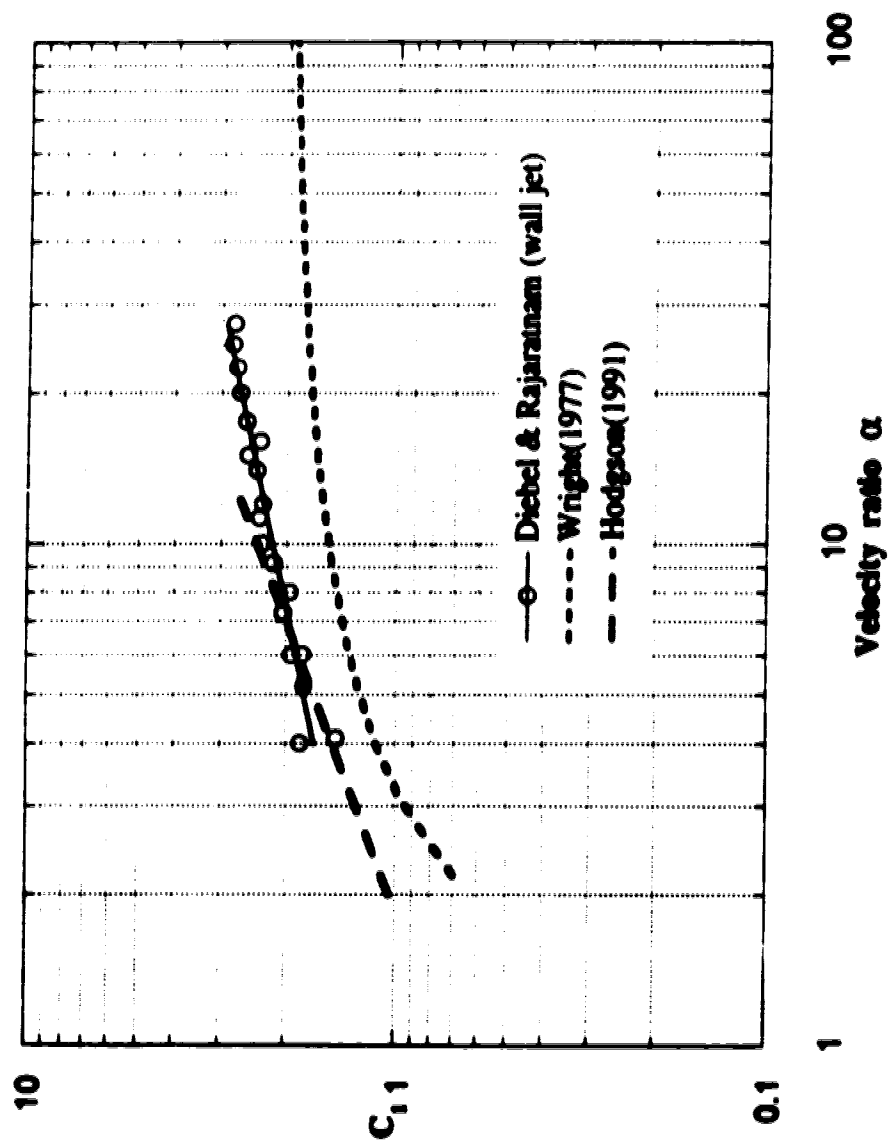
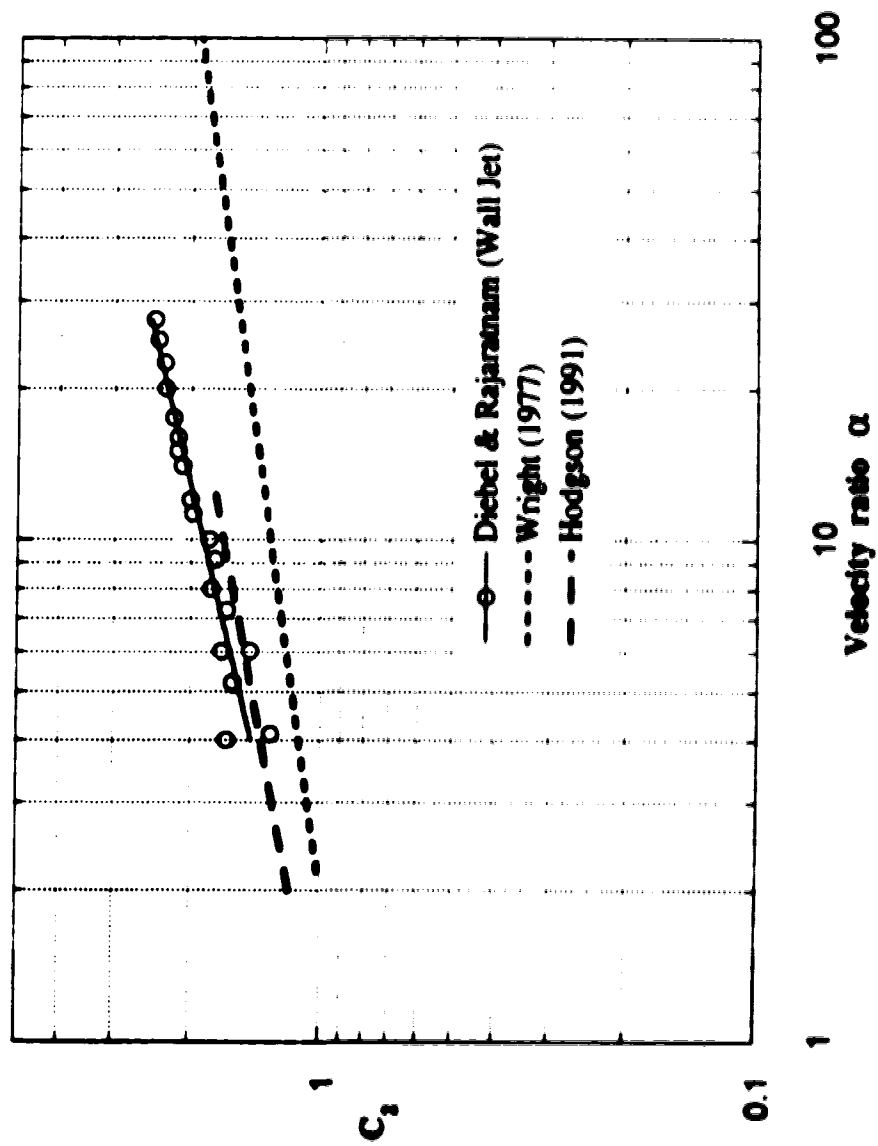


Fig. III (i) Momentum Dominated Near Field Coefficients



**Fig. III (u) Momentum Dominated Far Field Coefficients**