## Investigations of Bismuth- and Cobalt-based Electrocatalysts for Carbon Dioxide Reduction Reactions

by

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### Abstract

The electrochemical reduction of carbon dioxides (CO<sub>2</sub>RR) is a promising solution for mitigating CO<sub>2</sub> emissions while simultaneously generating value-added chemicals. From the perspective of materials engineering, understanding the structure-function relationships is crucial in guiding the rational design of electrocatalysts and advancing CO<sub>2</sub>RR technologies. Considering its significance attached, this thesis endeavors to investigate the i) BaBiO<sub>3</sub> (BBO) perovskite, ii) Bi- and iii) Co-based electrocatalysts with atomically distributed active sites, with particular focus on how the key structural features including potential-driven reconstructions, coordination environment, and local geometry affect the catalytic performances of CO<sub>2</sub>RR.

The first part of this thesis delves into the investigation of the voltage-driven structural reconstructions in the perovskite BBO, resulting in the generation of Bi metallene (eBBO) that manifests an efficient production of formate/formic acid (FA) with appreciable selectivity and partial current densities. Furthermore, Ba<sup>2+</sup> ions are released into the electrolyte during the course of reconstructions owing to the irreversible exsolution of Bi cations and phase transformations. The combined insights from the time-resolved Fourier-transform infrared spectroscopy (FTIR) and in situ Raman analysis reveal that the adsorption of Ba<sup>2+</sup> ions at eBBO surface facilitates CO<sub>2</sub> adsorption, leading to an enhanced CO<sub>2</sub>-to-FA conversion. This work is of direct significance in uncovering the structural evolutions during electrolysis and elucidating the cooperative catalysis between A- and B- site cations in perovskites for room-temperature CO<sub>2</sub>RR.

The second part of this thesis presents a simple and versatile nanosecond pulsed lasers method for the simultaneous confinement of the Bi "single atom" (SA) on graphene-based support for CO<sub>2</sub>RR. The outcomes of the reactions could be controlled by adjusting the compositions of the graphene support. Electrochemical studies disclose that the Bi ensemble supported by pristine or nitrogenated graphene preferably produces FA or syngas, respectively, as the dominant CO<sub>2</sub>RR products. X-ray absorption spectroscopy (XAS) and theoretical modeling collectively reveal that the product tunability originates from the distinct electronic characteristics of the doped Bi SAs induced by their different first-shell coordination (either carbon or nitrogen), which modify the hybridizations between the Bi center and \*OCHO/\*COOH intermediates, alter the energy barriers of the rate-determining steps and ultimately trigger bifurcated reaction pathways. This study demonstrates a practical and scalable ultrafast laser approach to tailoring the fine-structures and catalytic properties of supported catalysts and offers atomic-level insights into the mechanisms of CO<sub>2</sub>RR on ligand-modified Bi SAs with potential applications in various fields.

The third part of this thesis presents the geometric tuning of the CoN8C8 motif in cobalt phthalocyanine (CoPc) through varying the radius of carbon nanotubes (CNTs) supports, revealing the underlying volcanic correlations between the magnitude of compressive deformation/curvature within CoN8C8 and its catalytic performance in CO<sub>2</sub>RR. The optimally curved CoN8C8 boosts the turnover frequency by 2.4-fold at a potential of -0.8 V vs RHE *via* regulating the energy barrier of the rate-determining step (RDS), as supported by Tafel analysis and computational simulations. Such structural features further secure a near 4-fold CoPc mass preservation, affording a halved degradation rate in CO partial current density in the optimally strained sample in contrast to the least strained one by virtue of the slower CoPc demetallation and more efficient charge transfer.

## Preface

This thesis is an original work by Mengnan Zhu (Meng-Nan Zhu) under the supervision of Dr. Jing-Li Luo.

Chapter 1 is the introduction to the background knowledge and fundamentals of electrochemical carbon dioxide reduction reactions at room temperatures and pressures.

Chapter 2 is a Review with reference to the up-to-date literature reports in electrochemical carbon dioxide reduction reactions.

Chapter 3 introduces the methodologies and characterization techniques.

Chapter 4 of this thesis has been published as Meng-Nan Zhu, Bo-Wen Zhang, Min-Rui Gao, Peng-Fei Sui, Chenyu Xu, Lu Gong, Hongbo Zeng, Karthik Shankar, Steven Bergens, Jing-Li Luo. Electrochemically reconstructed perovskite with cooperative catalytic sites for CO<sub>2</sub>-to-formate conversion, Applied Catalysis Environmental: B, 2022, 306, 121101.

J.L.L. is responsible for project administration, supervision, funding acquisition, review and editing the manuscript. J.L.L., M.N.Z and B.W.Z conceived the work. M.N.Z synthesized the materials, performed electrochemical studies, data analysis and interpretation, the DFT analysis, and wrote the manuscript draft. B.W.Z synthesized the materials. M.R.G participated in DFT data analysis. P.F.S and C.X helped with data curation. L.G. performed the AFM analysis. H.Z, K.S and S.B reviewed and edited the manuscript. Chapter 5 of this thesis has been published as Meng-Nan Zhu, Haoqing Jiang, Bo-Wen Zhang, Minrui Gao, Peng-Fei Sui, Renfei Feng, Karthik Shankar, Steven H. Bergens, Gary J. Cheng, and Jing-Li Luo. Nanosecond Laser confined bismuth moiety with tunable structures on graphene for carbon dioxide reduction, ACS Nano, 2023, 17, 8705–8716.

J.L.L supervised and directed the study, contributed to the funding acquisition, edited, and revised the manuscript. G.J.C directed the study, edited, and revised the manuscript. J.L.L, M.N.Z and H.J conceived the work. M.N.Z performed the DFT analysis, electrochemical studies, data analysis and interpretation, and wrote the manuscript draft. H.J contributed to the material synthesis and revised the manuscript. B.W.Z participated in electrochemical studies, XAFS data analysis and revised the manuscript. M.R.G conducted the XRD analysis. P.F.S participated in the data discussions and gave constructive comments of this work. R.F performed the synchrotron X-ray spectroscopy and gave constructive comments on XAFS data interpretation measurements. K.S and S.B gave constructive comments of this work. M.N.Z and H.J contributed equally.

Chapter 6 of this thesis, entitled Volcano-shaped Carbon Dioxide Reduction on Cobalt Phthalocyanine with Curvature Induced Atomic Spacing Regulation, is ready for submission.

J.L.L supervised and directed the study, contributed to the funding acquisition, edited, and revised the manuscript. J.L.L and M.N.Z conceived the work. M.N.Z performed the DFT analysis, electrochemical studies, data analysis and interpretation, and wrote the manuscript draft. B.W.Z contributed to the material synthesis and XAFS data analysis. S.Z performed the ICP-OES analysis. M.R.G contributed to DFT data analysis. R.F performed the synchrotron X-ray spectroscopy and

V

gave constructive comments on XAFS data interpretation measurements. K.S and S.B gave constructive comments of this work.

Chapter 7 of this thesis includes the summary and prospects.

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# List of Symbols

$FE_x$	Faradaic efficiency
I <sub>x</sub>	Partial current density of product x
Ι	Total current
n	The number of electrons transferred
c <sub>x</sub>	Concentration of product x
F	Faraday constant
$V_m^{-1}$	Unit molar volume at 298.15 K
V	Total volume of the electrolyte
e	1.6 x 10 <sup>-19</sup> C mol <sup>-1</sup>
N <sub>A</sub>	Avogadro number
Q <sub>total</sub>	Total amount of charge passed through the system
j	Current density
j <sub>x</sub>	Partial current density toward product x
Ĵ <sub>ecsa</sub>	ECSA-normalized j
j <sub>x-ecsa</sub>	ECSA-normalized $j_x$
C <sub>dl</sub>	Double-layer capacitance
I <sub>a</sub>	Anodic charging current
Ic	Cathodic charging current
ν	Scan rate
C <sub>REF</sub>	Capacitance of the smooth planar surface

S	Surface area of the electrodes
ω	The content of the active sites
m	Mass
Μ	Atomic mass
η	Overpotential
E	Applied potential
E <sup>0</sup>	Thermodynamic equilibrium potential
G	Gibbs free energy
$\Delta G^0$	Gibbs free energy change
E <sub>DFT</sub>	DFT calculated electronic energy
E <sub>ZPE</sub>	Zero-point energy
$\int C_{\rm p} dT$	Enthalpy correction
TS	Entropy correction
E <sub>b</sub>	Binding energy
$\nu_1 CO_3^{2-}$	Symmetric stretching oscillation of carbonate
UL	Thermodynamic limiting potentials
R	Bond length
$\sigma^2$	Debye-Waller factors
$\Delta E_0$	Inner potential correction
I <sub>photo</sub>	Photocurrent

## List of Abbreviations

CO <sub>2</sub> RR	Carbon dioxide reduction reaction
BBO	BaBiO <sub>3</sub>
eBBO	Electricity-induced Bi metallene from BaBiO <sub>3</sub>
FA	Formic acid/Formate
FTIR	Fourier-transform infrared spectroscopy
SA	Single atom
XAS	X-ray absorption spectroscopy
СоРс	Cobalt phthalocyanine
CNTs	Carbon nanotubes
RDS	Rate-determining step
OER	Oxygen evolution reaction
GC	Gas chromatography
IC	Ion chromatography
EC	Electrochemical cell
HER	Hydrogen evolution reaction
ECSA	Electrochemically active surface area
CV	Cyclic voltammetry
ОСР	Open-circuit potential
TOF	Turnover frequency
RHE	Reversible hydrogen electrode

DFT	Density Functional Theory
СНЕ	Computational hydrogen electrode
SERS	Surface-enhanced Raman scattering
HEAs	High entropy alloys
ORR	Oxygen reduction reaction
LCO	La <sub>2</sub> CuO <sub>4</sub>
SACs	Single atom-based catalysts
XANES	X-ray Absorption Near Edge Spectroscopy
EDTA	Ethylenediaminetetraacetic acid
BVO	BiVO <sub>4</sub>
BVOh	H <sub>2</sub> treated BiVO <sub>4</sub>
BVOh-FN	$H_2$ treated $BiVO_4$ with FeOOH and NiOOH
XRD	X-ray diffraction
FE-SEM	Field emission scanning electron microscopy
TEM	Transmission electron microscopy
XPS	X-ray photoelectron spectroscopy
EDX	Energy dispersive X-ray spectrometry
AFM	Atomic force microscope measurements
ICP-OES	Inductively coupled plasma optical emission spectrometry
LSV	Linear sweep voltammetry
VASP	Vienna Ab initio Simulation Package
BBO100	BBO reduced for 100 s

BBO500	BBO reduced for 500 s	
BBO1000	BBO reduced for 1000 s	
BBO3000	BBO reduced for 3000 s	
BBO5000	BBO reduced for 5000 s	
Bi-C	Bi SA coordinated to C	
Bi-NC	Bi SA coordinated to N	
CN	Coordination number	
r-FE <sub>CO</sub>	FE <sub>CO</sub> retention	
r-j <sub>co</sub>	j <sub>CO</sub> retention	

### **Chapter 1. Introduction**

#### 1.1. Overview of Carbon Dioxide Recycling

The dependence on fossil fuels and the resultant emissions of carbon dioxide (CO<sub>2</sub>) are pressing issues in the present-day energy landscape. According to the data released by the National Oceanic and Atmospheric Administration of the US Department of Commerce, the average concentration of CO<sub>2</sub> in the atmosphere reached 419.47 parts per million by January 2023, which almost doubles the CO<sub>2</sub> level recorded during the Industrial Revolution.<sup>1</sup> The persistent increase in atmospheric CO<sub>2</sub> levels not only poses significant threats to the environment, but also results in the inefficient utilization of carbon, a vital component in fuels. In light of this, many nations, such as Canada, have pledged to achieve net-zero emissions by 2050 and are making efforts to transition to a sustainable energy system.<sup>2</sup>

Carbon neutrality, otherwise referred to as the net-zero CO<sub>2</sub> emission, entails a delicate balance between the emission and removal of CO<sub>2</sub> from the atmosphere. To achieve the goal, efficient carbon recycling schemes, e.g., CO<sub>2</sub>-fuels-CO<sub>2</sub> loop, should be integrated to energy-intensive industries. The cornerstone of the CO<sub>2</sub> removal process is the reduction of captured CO<sub>2</sub> into value-added substances that can either be used directly as raw materials or serve as reactants in numerous chemical processes. However, the conversion of CO<sub>2</sub> molecules poses a significant challenge due to its chemical inertness, and cannot be achieved without the presence of an external driving force under standard temperature and pressure conditions.<sup>3</sup> To tackle the challenges, various man-made CO<sub>2</sub> conversion processes have been devised in recent years, incorporating a diversity of functional units such as solar energy, electricity, thermo, among others. The processes aim to expedite the  $CO_2$  recycling and the utilization process are depicted in Figure 1.1a.



**Figure 1.1** (a)  $CO_2$  conversion strategies. (b) Comparison of the cost of various  $CO_2$ -derived chemicals between the current market price and the levelized cost from  $CO_2$  reduction.<sup>4</sup> Reprinted with permission from Reference [4]. Copyright (2018) Elsevier Ltd.

The electrochemical CO<sub>2</sub>RR technique has made rapid progress in recent years, standing out among its counterparts due to its several advantages, including mild reaction conditions such as ambient temperature and pressure and the use of aqueous-based non-toxic electrolytes. Additionally, its ability to easily control electrode potential results in the products with high activity and stability, making it suitable for large-scale implementation when integrated with renewable energy sources such as photovoltaic, biomass, and hydroelectric power. Recent techno-economic evaluations of room temperature CO<sub>2</sub> electrolysis conducted by several independent research groups have reached similar conclusions, reinforcing the feasibility of room temperature CO<sub>2</sub>RR as a solution to the current carbon crisis.<sup>4,5</sup> In particular, the production of CO and formic acid/formate (FA) through present-day techniques has already become commercially competitive with conventional processes. According to a reported by Shin et al., the base production costs of CO and FA are approximately US\$0.44 and US\$0.59 per kilogram, respectively.<sup>5</sup> These costs are comparable to their respective market prices of US\$0.80 and US\$0.50 per kilogram, thereby indicating the commercial viability of CO and FA produced via CO<sub>2</sub>RR. Although the large-scale productions of high-order C2+ feedstocks for economic gain are not immediately feasible, it holds promise for the near future, provided that electricity prices continue to decrease, and energy efficiency is improved. Bushuyev and co-workers conducted a separate study, taking into account the factors such as the costs of  $CO_2$ , electricity, separation, capital/maintenance, and operation, as well as the known product selectivity (Figure 1.1b).<sup>4</sup> They obtained similar conclusions as Shin et al., stating that current CO<sub>2</sub>RR technologies are already more cost-effective than traditional processes in the production of major C1 products (e.g., CO and FA), and that the continued use of low-cost, renewable electricity has the potential to further enhance the economic viability of CO<sub>2</sub>RR. While it is acknowledged that certain scientific hurdles still persist, the roadmap for CO<sub>2</sub> neutralization through the utilization of CO<sub>2</sub>RR at room temperature and pressure exhibits great promise over the long term.

#### **1.2.** Fundamentals of Carbon Dioxide Reduction Reaction (CO<sub>2</sub>RR)

#### **1.2.1.** The working systems

CO<sub>2</sub> electrolysis is usually carried out in specialized electrochemical reactors that continuously convert CO<sub>2</sub> to fuels at the cathode side, driven by external cathodic potentials. This process is frequently paired with the oxygen evolution reaction (OER) from water splitting at the anode,

thereby completing the overall reaction of  $CO_2 + H_2O \rightarrow fules + O_2$ . To analyze the products obtained from  $CO_2RR$ , the cathode is directly connected to the gas chromatography (GC) spectrometer for online detection of gaseous products, while the liquid products are collected and subsequently analyzed by ion chromatography (IC). To prevent products crossover and reoxidation during the reaction, a proton-exchange membrane (e.g., Nafion 117) is placed between the two chambers. The cathodic electrode is equipped with a reference electrode near its surface to accurately regulate the external potentials applied to the cathode. In lab-scale research, the H-type cell (Figure 1.2) has been widely adopted due to its simple cell fabrication, efficient prescreening of the catalyst performances, and easy access to probe the reaction mechanisms when combined with advanced *in situ* spectroscopy techniques.



**Figure 1.2** Digital image of the H-type cell used in electrochemistry studies (1. CO<sub>2</sub> inlet. 2. counter electrode. 3. working electrode. 4. CO<sub>2</sub> inlet. 5. reference electrode. 6. Connection to GC).

#### 1.2.2. Figures of Merit for CO<sub>2</sub>RR

#### • Faradaic efficiency

Faradaic efficiency (FE<sub>x</sub>, *x* is target product) measures the fraction of the current used to generate a specific product *x* over the total current flowed through the system.<sup>6,7</sup> For a system to exhibit optimal efficiency in generating a target product, it is desirable to attain a 100% FE, meaning that all the charges flowing through the circuit will be consumed in the production of the desired product. The FE<sub>x</sub> of gaseous product *x* is calculated based on Equation 1.1:

$$FE_{x} = \frac{I_{x}}{I} = \frac{n \cdot v_{co_{2}} \cdot c_{x} \cdot F \cdot V_{m}^{-1}}{I}$$

$$(1.1)$$

Where  $I_x$  and I stand for the partial current density of product x and the overall current flow through the system. n represents the number of electron transfer for the formation of 1 mol of x.  $v_{co_2}$  denotes the flow rate of CO<sub>2</sub> feeding gas.  $c_x$  is the concentration of x . F and  $V_m^{-1}$  refer to the Faraday constant (96,485 C mol<sup>-1</sup>) and unit molar volume (24.5 L mol<sup>-1</sup>) at 298.15 K.

The  $FE_{FA}$  of FA is calculated based on Equation 1.2:

$$FE_{FA} = \frac{2 \cdot c_{FA} \cdot V \cdot e \cdot N_A \cdot (0.001)}{Q_{total}}$$
(1.2)

Where  $c_{FA}$  (mol L<sup>-1</sup>) is the measured concentration of FA. V stands for the total volume of the electrolyte, which is around 30-35 mL in this study. e is 1.6 x 10<sup>-19</sup> C mol<sup>-1</sup>. N<sub>A</sub> is the Avogadro number (6.02 x 10<sup>23</sup>). Q<sub>total</sub> represents the total amount of charge passed through the system.

#### • Total current density

Total current density (j) is the measurement of the number of electrons flowing through the electrochemical cell (EC) per unit surface area. The observed j is mainly attributed to the two simultaneous reactions, i.e., hydrogen evolution reaction (HER) and CO<sub>2</sub>RR on the electrode surface in aqueous-based electrolytes, and thus the increase in j can not be directly translated to an increase in catalytic activities for generating product x. To distinguish the capability of electrocatalysts to drive CO<sub>2</sub>RR and HER, the values of j obtained in both CO<sub>2</sub> and argon saturated electrolyte should be reported and compared.

#### • Partial current density

Partial current density of x ( $j_x$ ) reflects the current density for forming product x, which is determined by multiplying the steady j and FE<sub>x</sub> at the same potential.  $j_x$  can be used as the descriptor to evaluate the production rates/activities of the electrocatalysts. Typically, the j and  $j_x$  are normalized with respect to the geometric area of the electrode, which sometimes fail to reflect the intrinsic activity of catalyst due to the surface roughness effect.<sup>8</sup> Therefore, the electrochemically active surface area (ECSA)-normalized j and  $j_x$ , namely the  $j_{ECSA}$  and  $j_{x-ECSA}$ , has been employed to probe the intrinsic activity of the electrocatalysts. ECSA can be obtained by measuring the double-layer capacitance ( $C_{dl}$ ) with cyclic voltammetry technique (CV) in the non-Faradaic regime, which is typically a 100 mV window centered as the open-circuit potential (OCP) based on Equations 1.3 and 1.4.<sup>9</sup>

$$C_{dl} = \frac{I_a - I_c}{2\nu}$$
(1.3)

$$ECSA = \frac{C_{dl}}{C_{REF}}$$
(1.4)

Where  $I_a$  and  $I_c$  is the anodic and cathodic charging current, respectively.  $\nu$  represents the scan rate.  $C_{REF}$  stands for the capacitance of the reference smooth planar surface.

#### • Turnover Frequency (TOF)

Turnover frequency (TOF) is defined as the mole of products generated per electrocatalytic active sites per unit time, as shown in Equation 1.5:

$$TOF = \frac{j_x \cdot S/nF}{\omega m/M}$$
(1.5)

Where S is the surface area of the electrodes.  $\omega$  is the content of the active sites. m is the total mass of electrocatalysts. M is the atomic mass of the active element.

#### • Overpotential

Overpotential ( $\eta$ ) refers to the potential difference between the thermodynamic equilibrium potential of a certain reaction and the applied potential, as shown in Equation 1.6:

$$\eta = E - E^0 \tag{1.6}$$

where E and  $E^0$  refer to the applied potential and the standard potential of the target CO<sub>2</sub>RR reaction.

#### • Stability

The long-term durability is evaluated by assessing the values of  $FE_x$  and  $j/j_x$  of certain products periodically over the course of electrolysis. For practical applications, the service lifetime of electrodes should reach to several thousands of hours; meanwhile, the degradation rate of  $j/j_x$ and  $FE_x$  overtime should reside in a reasonable range.<sup>10,11</sup> In lab experiments, the stability tests are typically performed up to at least a few hours.

#### 1.2.3. Thermodynamics of CO<sub>2</sub>RR

The electrochemical CO<sub>2</sub>RR are essentially multiple proton–electron reactions that result in the generation of a diverse range of carbonaceous products and water. A clear correlation exists between the external potentials applied and the electrocatalytic products in the context of CO<sub>2</sub>RR. The standard redox potentials ( $E^0 \vee vs$  RHE, reversible hydrogen electrode) for the CO<sub>2</sub>RR products can be calculated based on Equation 1.7 and the results are presented in Table 1.1 (all potential hereafter is referred to RHE scale unless otherwise specified).

$$\Delta G^0 = -nFE^0 \tag{1.7}$$

where  $\Delta G^0$  is the Gibbs free energy change.

Reaction	E <sup>0</sup> (V vs RHE)		
CO <sub>2</sub> RR			
$CO_2 + 2H^+ + 2e^- \rightarrow HCOOH_{(aq)}$	-0.20 (for pH < 4).		
	-0.20 + 0.059 * [pH-4] (for pH > 4)		
$\mathrm{CO}_2 + 2\mathrm{H}^+ + 2\mathrm{e}^- \rightarrow \mathrm{CO}_{(\mathrm{g})} + \mathrm{H}_2\mathrm{O}$	-0.11		
$\mathrm{CO}_2 + 8\mathrm{H}^+ + 8\mathrm{e}^- \rightarrow \mathrm{CH}_{4(\mathrm{g})} + 2\mathrm{H}_2\mathrm{O}$	0.17		
$\mathrm{CO}_2 + 6\mathrm{H}^+ + 6\mathrm{e}^- \rightarrow \mathrm{CH}_3\mathrm{OH}_{(\mathrm{aq})} + \mathrm{H}_2\mathrm{O}$	0.03		
$2CO_2 + 12H^+ + 12e^- \rightarrow C_2H_{4(g)} + 4H_2O$	0.07		
$2CO_2 + 12H^+ + 12e^- \rightarrow C_2H_5OH_{(aq)} + 4H_2O$	0.08		
Water splitting			
$2H_20 \rightarrow 0_2 + 4H^+ + 4e^-$	1.23		
$2H^+ + 2e^- \rightarrow H_2$	0		

Table 1.1 Equilibrium Potentials of the representative CO<sub>2</sub>RR.<sup>12,13</sup>

It is noteworthy that several of the reduction potentials of the CO<sub>2</sub>RR are similar, which exacerbates the challenges of low selectivity and thus product diversity for the desired product during the CO<sub>2</sub>RR process. Furthermore, the HER can further undermine the selectivity of CO<sub>2</sub>RR, leading to decreased efficiency. The fact that a broad range of products can be generated indicates the presence of different reactions mechanisms as well as the branched reaction pathways on the electrocatalysts surface. Hence, fine-tuning the properties of electrocatalysts to achieve the selective and stable production of target products remains as a central objective CO<sub>2</sub>RR research.

#### 1.2.4. Mechanistic insights of CO<sub>2</sub>RR

The comprehensive understanding of the mechanisms behind CO<sub>2</sub>RR is of utmost importance to the advancement of the field. Experimental and theoretical approaches are thus indispensable in providing a thorough investigation of the complex reaction process and pathways. The application of *in situ* spectroscopy techniques offers direct evidence to the nature of reaction intermediates,<sup>14</sup> yet the intricacy of CO<sub>2</sub>RR often poses limitations to the decoding of spectra. As a complementing tool, atomic-scale density-functional-theory (DFT) calculations based on the computational hydrogen electrode (CHE) model have proven to be instrumental in yielding insights into the reaction mechanisms and pathways. Within this formalism, the concerted proton-electron transfer is assumed at each elementary step. The pH and potential effects are not directly considered by DFT but can be added in a linear fashion.<sup>15,16</sup>

#### • Mechanisms of C1 production

CO and FA are the simplest products of CO<sub>2</sub>RR, requiring the transfer of only two electrons/protons to complete the reaction. In practice, large overpotentials are required to initiate these reactions because the first step to form adsorbed \*CO2<sup>•-</sup> with bended structure is both thermodynamically and kinetically limited (\* stands for the adsorption site).<sup>17</sup> After this step, the \*CO2<sup>•-</sup> will react with H<sub>2</sub>O to form either \*COOH and \*OCHO as the first protonated intermediate (Figure 1.3).<sup>18</sup> Feaster et al. reported that the \*COOH binding energy can be used as the descriptor for the production of CO, whereas the \*OCHO binding energy shows a clear correlation to the FA production.<sup>18</sup> To produce CO, a carbophilic catalyst is generally required to initiate the metal-C bonding and the subsequent formation of \*COOH, and further protonation

of \*COOH can lead to a variety of products; in contrast, the formation of \*OCHO requires a oxyphilic catalyst and FA is a "dead-end" and cannot be further reduced.<sup>19,20</sup> These results collectively suggested that the production of CO and FA proceeds through different intermediates. In a recent work conducted by Chernyshova et al., the cutting-edge techniques including the operando surface-enhanced Raman scattering (SERS), Tafel analysis, and DFT simulations collectively confirmed that the FA and CO production on Cu proceeds through a carboxylate intermediate with the  $\eta^2(C, O) - CO_2^-$  structure, which can be used as the common descriptor of the CO<sub>2</sub>-to-CO and CO<sub>2</sub>-to-FA.<sup>14</sup>



**Figure 1.3** CO<sub>2</sub>-to-CO and CO<sub>2</sub>-to-FA reaction pathways involving two different intermediates of \*COOH and \*OCHO.<sup>18</sup> Reprinted with permission from Reference [18]. Copyright (2017) American Chemical Society.

 $CH_4$  and  $CH_3OH$ , another two major C1 products, are preferably observed over Cu-based electrocatalysts. It has been generally accepted that the production of  $CH_4$  undergoes two stages: the production of \*CO and its further protonation. Peterson and co-workers, through DFT calculations, predicted that protonation of the \*CO to \*CHO is the RDS (0.39 eV), which experiences the "\*CHO-\*CH2O-\*CH3O-CH4" pathway (Figure 1.4, pathway a), leaving \*O on the surface of electrocatalysts that is subsequently converted to H<sub>2</sub>O. The selectivity between CH<sub>4</sub> over CH<sub>3</sub>OH has been proposed to be the final reduction of \*CH3O. However, their calculation results were merely based on thermodynamic analysis and the kinetics contributions were not accounted for. By explicitly incorporating the role of water alongside the kinetic analysis of each elementary step, Ni et al. further proposed a different reaction mechanism involving the formation of \*COH intermediate, which requires a lower energy of 0.21 eV, and the complete pathway follows "\*CO-\*COH-\*C-\*CH-\*CH2-\*CH3-\*CH4-CH4" (Figure 1.4, pathway b).<sup>21</sup> In addition, studies have shown that the protonation steps follow a Langmuir-Hinshelwood mechanism where the surface adsorbed \*H directly participates in the reaction, in good agreement with the experimentally observed concerted increase/decrease in HER and CO<sub>2</sub>-to-CH<sub>4</sub> reaction.


**Figure 1.4** (a and b) The proposed reaction pathways for CO<sub>2</sub>-to-CH<sub>4</sub>. (c) The proposed reaction pathway for CO<sub>2</sub>-to-C<sub>2</sub>H<sub>4</sub>.<sup>21</sup> Reprinted with permission from Reference [21]. Copyright (2013) WILEY-VCH Verlag GmbH & Co. KGaA, Weinheim.

## • Mechanisms of C2+ production

The reaction pathways of CO<sub>2</sub>RR toward various high-order C2+ hydrocarbon/oxygenated products are even more complicated and there is currently no consensus in the research community, and yet it has been widely accepted that the production of C2+ requires the formation of C-C bonds. Some detailed mechanistic routes have been suggested, showing the bifurcated reaction pathways from the common intermediate  $*CO.^{22}$  Cite C<sub>2</sub>H<sub>4</sub> as an example: the formation of C<sub>2</sub>H<sub>4</sub> involves the \*CO dimerization with an electron transfer to render the \*C2O2 as key species, followed by the subsequent protonation to produce \*CO-CHO

intermediate. The final intermediate of ethenol ( $C_2H_4O$ ) can be further reduced to  $C_2H_4$  or  $CH_3CHO$ . Although the equilibrium potentials of  $CO_2$  reduction toward hydrocarbon or alcohol products are thermodynamically more favorable than toward CO and FA, the RDS, which is the formation of C-C bonds, limits some of these reactions kinetically. This explains the experimentally observed low C2+ yield. In addition to the \*CO-CO step, Ni et al. also suggested a different  $C_2H_4$  pathways involving the coupling of \*CH2-CH2 (Figure 1.4, pathway c). Overall, future studies are required to clarify the reaction mechanisms in terms of the C2+ generations.

# **Chapter 2. Literature Review**

## 2.1. General Material-Function Relations in CO<sub>2</sub>RR

Since the seminal studies by Hori et al., extensive research efforts by various research organizations have contributed to establishing a general consensus among the scientific community that there exists a clear relation between the chemical properties of metal-based electrocatalysts and the resultant yields from CO<sub>2</sub>RR.<sup>23</sup> As shown in Figure 2.1a, noble metalbased electrocatalysts (mainly Ag and Au) and metal Zn are generally highly active toward CO generation. The p-blocking metal-based electrocatalysts, mainly Sn, In, Bi, Sb, etc., predominantly yield FA from CO<sub>2</sub>RR. Cu, intriguingly, is the only metal-based catalyst capable of reducing CO<sub>2</sub> to hydrocarbons and oxygenates with appreciable production rates. Main group transition metals, e.g., Fe, Co, Mn, etc., are almost inert to CO<sub>2</sub>RR but are active toward the competitive HER.<sup>24</sup> These experimental findings can be correlated to the distinctive metal-intermediate interactions that are characterized by the adsorption energy of a specific species. As demonstrated in Figure 2.1b, the group of metals that exhibit high production of CO (Ag and Zn) displays a relatively weak \*CO binding, which tends to desorb from the catalysts' surface and form CO. Au exhibits the highest activity toward CO production, being situated at the peak of the graph. The metals on the left side of the figure (Pt and Ni) exhibit a strong binding to \*CO and are prone to poisoning and deactivation. Cu presents a favorable balance of \*CO adsorption energy, neither too strong nor too weak, making it a promising candidate for deep reduction of CO, as depicted in Figure 2.1c.



**Figure 2.1** (a) Metal electrocatalysts and their major  $CO_2RR$  products.<sup>24</sup> Reprinted with permission from Reference [24]. Copyright (2021) Elsevier Ltd. (b, and c) Volcano plot of  $CO_2RR$  current density at –0.8 V as a function of the CO binding strength (b) and onset potentials of  $CO_2RR$  and methane/methanol as a function of the CO binding strength (c).<sup>16</sup> Reprinted with permission from Reference [16]. Copyright (2014) American Chemical Society.

Metal derivatives, such as metal alloys, metal (oxides/sulfides) composites, have been investigated for  $CO_2RR$  as they provide extra dimensions (e.g., electronic effect, ligand effect, etc.) in tuning the electronics features of electrocatalysts compared to the mono-component ones. Despite delivering similar product distributions for  $CO_2RR$  compared to the metals, the values of  $FE_x$  and  $j_x$  are subjected to variations based on the factors like the physiochemical properties (e.g., morphology, particle sizes, surface chemistries, etc.) of the electrocatalysts, the type of electrolyser, and testing conditions, etc. P-blocking metal-based derivatives mostly take on the similar selectivity/product distributions as their metal forms. For example, Yang et al. synthesized the Sn<sub>0.80</sub>Bi<sub>0.20</sub> alloy that was reconstructed to Bi doped SnOx under cathodic potentials, exhibiting much enhanced FA production compared to that of the untreated SnOx samples

(Figure 2.2a-2.2c).<sup>25</sup> Xing et al. fabricated the Bi@Sn core-shell nanoparticles (Bi core and Sn shell) by the electroreduction of Bi<sub>2</sub>Sn<sub>2</sub>O<sub>7</sub> precursor.<sup>26</sup> The as-obtained electrocatalysts could convert  $CO_2$  to FA with a  $FE_{FA}$  around 90% from -0.9 to -1.2 V whereas  $SnO_2$  delivered a much lower FE<sub>FA</sub> of less than 60% within the same potential range. In addition to the p-blocking metal-based materials, Cu alloys could deliver the more diverse product distributions in CO<sub>2</sub>RR. Zhong et al., using DFT calculations in combination with active machine learning, identified the Cu-Al electrocatalysts as the excellent electrocatalysts for C<sub>2</sub>H<sub>4</sub> production from a series Cu-based alloys.<sup>27</sup> The as-obtained Cu-Al reduced CO<sub>2</sub> to C<sub>2</sub>H<sub>4</sub> with a high FE of over 80% at a current density of 400 mA cm<sup>-2</sup> and a half-cell ethylene power conversion efficiency of 55  $\pm$  2% at 150 mA cm<sup>-2</sup>, representing the state-of-the-art electrocatalysts for CO<sub>2</sub>-to-C<sub>2</sub>H<sub>4</sub> conversion. Beyond alloys, dual-component catalysts, where a second phase is only mechanically/physically introduced without the formation of the alloy, have been investigated in a few other studies. For instance, Ag-Cu and Au-Cu based heterostructures were developed and showed promising C2+ production rates through the so-called "tandem" reaction mechanisms.<sup>28,29</sup> In such a tandem configuration, the CO<sub>2</sub> is firstly reduced to CO on Ag or Au sites, generating the microenvironment with high local CO concentrations. In this regard, the sequential CO-CO dimerization step over Cu surface would be easily initiated for enhanced C2+ products (Figure 2.2 d and 2.2e).



**Figure 2.2** (a) EDS elemental mapping images of Sn<sub>0.80</sub>Bi<sub>0.20</sub> alloy NPs. (b)  $j_{FA}$  of Sn<sub>0.80</sub>Bi<sub>0.20</sub> @Bi-SnOx and Sn@SnOx nanoparticles. (c) FEs of Sn<sub>0.80</sub>Bi<sub>0.20</sub>@Bi-SnOx.<sup>25</sup> Reprinted with permission from Reference [25]. Copyright (2020) Wiley – VCH Verlag GmbH & Co. KGaA, Weinheim. (d) Schematics of interdigitated bimetallic electrodes in the interdigitated design. (e) FEx for Cu lines on Ag system as a function of Cu areal coverage.<sup>28</sup> Reprinted with permission from Reference [28]. Copyright (2017) American Chemical Society. (f) Schematic of the HEA and catalysis reaction.<sup>30</sup> Reprinted with permission from Reference [30]. Copyright (2020) American Chemical Society.

High entropy alloys (HEAs), composing of various different elements, have been recently applied to  $CO_2RR$ . Nellaiappan et al.<sup>30</sup> and Pederson et al.<sup>31</sup> independently reported the AuAgPtPdCu HEAs for  $CO_2RR$ , based on the joint of experimental results and theoretical simulations. According to the findings of Nellaiappan et al., the electrocatalytic activity of AuAgPtPdCu was predominated by the redox-active Cu species (Cu<sup>2+</sup>/Cu<sup>0</sup>) and the other metals only contributed synergistically. As a result, a 100% conversion of CO<sub>2</sub> to gaseous products could be achieved at a low voltage of -0.3 V (Figure 2.2f). Pederson et al. applied DFT methods with supervised machine learning to predict the \*CO and \*H adsorption energy of all sites in the (111) facet of disordered CoCuGaNiZn and AgAuCuPdPt HEAs, thereby identifying the locally optimal HEAs for CO<sub>2</sub>RR. In addition to these efforts, Li and colleagues recently developed the HEAs aerogels with the enrichment of p-blocking metals, and the optimal sample was identified as PdCuAuAgBiln. On this specific catalyst, FA was the predominant product, achieving a maximum FE<sub>FA</sub> of 98.1% at - $1.1 \text{ V.}^{32}$  The selective FA production was ascribed to the strong interactions between different metal species and the presence of abundant surface unsaturated sites.

## 2.2. Perovskites- based Electrocatalysts

Perovskites are a family of organic and inorganic materials possessing similar crystal structures of ABX<sub>3</sub>. In general, the A-site elements in a perovskite are comprised of rare earth or alkali metal ions, while the B-sites are occupied by transition metals such as Fe, Ni, Co, Mn, among others, which typically possess smaller radius than A-site elements. X generally represents O, F, or halide elements. The ideal ABO<sub>3</sub> structures could be depicted as a continuous network of corner-sharing BO<sub>6</sub> octahedral, with A occupying the cubo-octahedral voids (Figure 2.3a). The versatility and flexibility of the A-site and B-site combinations, including their types and ratios, render perovskites highly promising candidates for a multitude of redox processes, such as oxygen reduction reaction (ORR), OER and HER. It has been widely recognized that the B-site elements in perovskites play a crucial role in dictating the catalytic outcomes, thereby providing a fundamental guideline for selecting appropriate perovskites to initiate CO<sub>2</sub>RR. In a recent study, Pi et al. applied SrSnO<sub>3</sub> nanowires to convert CO<sub>2</sub> to FA, showcasing an appreciable FE<sub>FA</sub> > 75% over a broad potential range from -1.1 V to -1.3 V and the highest j<sub>FA</sub> of 21.6 mA cm<sup>-2</sup> at -1.3 V.<sup>33</sup> The catalytic outcomes of SrSnO<sub>3</sub> are invariably dictated by the Sn ions as Sr is almost inert toward CO<sub>2</sub>RR, however, whether SrSnO<sub>3</sub> is intrinsically more active than SnO<sub>2</sub> in the context of CO<sub>2</sub>RR remains underexplored (Figure 2.3b). Zhu et al. reported a LalnO<sub>3</sub> perovskite for FA production, reaching the maximum FE<sub>FA</sub> of 91.4% along with a j<sub>FA</sub> of 106.8 mA cm<sup>-2</sup> at -0.9 V.<sup>34</sup> In addition to Sn- and In-based perovskites, Yan et al. demonstrated that a near-unity FA selectivity can be acquired on YbBiO<sub>3</sub> perovskite at -0.9 V, as well as a wide potential window range with FE<sub>FA</sub> > 90% from -0.8 to -1.2 V.<sup>35</sup>

Cu-based perovskites, particularly La<sub>2</sub>CuO<sub>4</sub> (LCO) with the tetragonal layered K<sub>2</sub>NiF<sub>4</sub> structure, have been shown to be able to catalyze multi-electron transfer reactions in CO<sub>2</sub>RR with a variety of products beyond CO and FA. In early studies, researchers adopted La<sub>2</sub>CuO<sub>4</sub> as the cathodes on the belief that it would maintain the high oxidation states of Cu<sup>2+</sup>/Cu<sup>+</sup> during CO<sub>2</sub>RR electrolysis, which are crucial to produce C2+ products. Schwart et al. showed that CO<sub>2</sub> could be reduced to CH<sub>3</sub>OH, C<sub>2</sub>H<sub>5</sub>OH, and n-propanol up to = 40% at current density of 180 mA cm<sup>-2</sup> on La<sub>1.8</sub>Sr<sub>0.2</sub>CuO<sub>4</sub> with similar device setup and operating environment, but the electrocatalysts variably yielded CH<sub>4</sub> and C<sub>2</sub>H<sub>4</sub> as the major products and only a negligible amount of C<sub>2</sub>H<sub>5</sub>OH had been detected.<sup>37</sup> A few other studies reported similar product distributions over LCO-based electrocatalysts with hydrocarbons being the major products of CO<sub>2</sub>RR. For instance, Chen et al. reported that La<sub>2</sub>CuO<sub>4</sub> underwent structural transformation to form the Cu/La<sub>2</sub>CuO<sub>4</sub> heterostructures under extreme cathodic potentials; such unique interface accounted for the observed CO<sub>2</sub>-to-CH<sub>4</sub> conversion with a high  $FE_{CH_4}$  of 56.3% alongside a  $j_{CH_4}$  of 117 mA cm<sup>-2</sup> for CH<sub>4</sub> production at an external potential of –1.4 V (Figure 2.3c).<sup>38</sup> Wang et al. demonstrated good C<sub>2</sub>H<sub>4</sub> selectivity ( $FE_{C_2H_4} \sim 60\%$ ) over nano-bamboo LCO with rich twin boundaries synthesized from electrospinning. Furthermore, in situ XAS revealed that the Cu<sup>2+</sup> was well maintained during the catalytic process. Recently, Zhu et al. investigated the effect of A-site deficiency on the CO<sub>2</sub>RR performances and unveiled a volcano-type "A deficiency – performance" relation, where L<sub>1.9</sub>CuO<sub>4-x</sub> exhibited the optimal current density (51.3 mA cm<sup>-2</sup>) and selectivity ( $FE_{C_2H_4} \sim 51.4\%$ ) for C2+ products, and yet L<sub>1.7</sub>CuO<sub>4-x</sub> favours CH<sub>4</sub>.<sup>39</sup> The non-stoichiometry induced tunable oxygen vacancies and/or the formation of CuO/Ruddlesden-Popper hybrids are considered the main contributors to the tunable selectivity in LCO.

Given the cathodic operating potential inherent to CO<sub>2</sub>RR, the B-site elements reduction to lowvalence phases during electrolysis appears unavoidable. The initial reduction of perovskite can pose stabilities issues, rendering the  $FE_x / j_x$  obtained during this period unreliable. As demonstrated by a study conducted by Whittingham et al., LCO remained functionally stable within the voltage ranges between -0.4 - 1.1 V, but further decreasing the voltage down below -0.4 V led to amorphization of the LCO structures.<sup>40</sup> Singh et al. revisited the structural evolution of LCO and showed that it underwent dissociation to La<sub>2</sub>O<sub>3</sub> and Cu<sub>2</sub>O under relatively mild cathodic potentials, and further disintegrated to metallic Cu at even more negative potentials below -0.5 V.<sup>41</sup>



**Figure 2.3** (a) Illustrations of the ABX<sub>3</sub> structures of perovskite.<sup>43</sup> Reprinted with permission from Reference [43]. Copyright (2020) Wiley - VCH Verlag GmbH & Co. KGaA, Weinheim. (b) Comparisons of the  $FE_x$  and current densities in SrSnO<sub>3</sub> and SnO<sub>2</sub>.<sup>33</sup> Reprinted with permission from Reference [33]. Copyright (2019) Elsevier Ltd. (c) Schematic illustration of the transformation from LCO to form the Cu/La<sub>2</sub>CuO<sub>4</sub>.<sup>38</sup> Reprinted with permission from Reference [38]. Copyright (2020) American Chemical Society. (d) Correlations between the A-site deficiency in LCO and  $FE_{C_{2+}}/FE_{CH_4}$ .<sup>39</sup> Reprinted with permission from Reference [39]. Copyright (2021) Wiley - VCH GmbH.

In addition to La<sub>2</sub>CuO<sub>4</sub>, a Ca<sub>2</sub>CuO<sub>3</sub> perovskite oxide with undercoordinated Cu sites generated due to partial Ca<sup>2+</sup> release and strong basic strength endowed by A site, delivering a high  $j_{CH_4}$  of 517 ± 23 mA cm<sup>-2</sup> as the potential of -0.3 V. DFT calculations suggested that the hydrogenation of \*CO and \*CHO at the undercoordinated Cu sties was more easier, thus enabling the high  $CH_4$  production rates.<sup>42</sup> Until now, the potential-induced reconstructions of perovskites remain largely under-researched, and further in-depth examination is required to determine the potential benefits of this effect on  $CO_2RR$ .

## 2.3. Single Atom-based Electrocatalysts

Atomic metal ions supported by substrates demonstrate great potentials in heterogeneous catalysis due to their unique chemical environment and potentially maximum atom efficiency, which opens a new horizon of possibilities in the field.<sup>44</sup> Previous studies have engineered the type of central metal atom to steer the production distributions, which can be readily achieved through the manipulation of the precursor metal ions during the manufacturing process. Carbon supported Ni,<sup>45,46</sup> Fe,<sup>47–49</sup> Co,<sup>50</sup> and Mn-based<sup>51,52</sup> single-atom-based catalysts (SACs) coordinated by nitrogen atoms have been shown to exhibit favourable CO generation, in stark contrast to the bulk forms of these materials, which primarily display activity toward HER. A comprehensive analysis conduced by Ju et al. demonstrated that Fe-N-C and Ni-N-C electrocatalysts, among a series of catalyst materials composed of MNx moieties (M= Mn, Fe, Co, Ni, Cu), rival traditional Au- and Ag-based electrocatalysts in terms of the intrinsic catalytic reactivity, turnover frequency, and FE<sub>CO</sub>.<sup>53</sup> Park et al. used DFT-based calculations to evaluate the potentials of 23 SACs, each possessing an "M-N-C" structure, for CO<sub>2</sub>-to-CO reaction. Fe-N-C, Co-N-C and Ni-N-C were identified as highly promising transition metal-based SACs candidates based on the critical performance metrics, including the maximum reaction energy, differences in the \*H and \*CO binding energy ( $\Delta G^*H - \Delta G^*CO$ ), and \*CO desorption energy ( $\Delta G^*CO \rightarrow CO$ ).<sup>54</sup> More recently, pblocking metal-based SACs, including Sn-N4,<sup>55,56</sup> In-N4,<sup>57–60</sup> and Sb-N4,<sup>61,62</sup> have draw attention due to their capability in delivering both FA and CO (Figure 2.4b-2.4d). In addition to basic products requiring the transfer of two electrons, a more diverse array of products, including CH<sub>3</sub>OH, CH<sub>4</sub>,<sup>63</sup> C<sub>2</sub>H<sub>4</sub>,<sup>63,64</sup> CH<sub>3</sub>COCH<sub>3</sub>,<sup>65</sup> etc., has been observed on Cu-based SACs. However, these catalysts display a much lower efficiency for the production of higher-order C2+ species compared to their bulk counterparts, primarily due to the low concentrations of Cu centers and the increased distances between adjacent Cu centers, which retard the \*CO-CO dimerization. It is noteworthy that several studies have reported the dynamic formation of Cu aggregation under operando CO<sub>2</sub>RR studies,<sup>66,67</sup> leading to the identification of Cu clusters, rather than Cu SAs, as the true active centers. Xu et al. reported a Cu SAC for CO<sub>2</sub>-to-ethanol conversion, during which the Cu SAs could transform to Cu<sub>n</sub> clusters (n = 3 and 4), as evidenced by the leftward shifts in the operando Cu k-edge X-ray Absorption Near Edge Spectroscopy (XANES) spectra (Figure 2.4e).<sup>66</sup> DFT calculations collectively revealed that the reactions are most possibly carried out over Cu clusters (Figure 2.4f). The formation of Cu clusters (Cu < 4 atoms) has also been identified in Cu-in-Ag alloy system (about 1 atomic per cent of Cu) when applied to CO reduction.<sup>68</sup> Bai et al., through DFT simulations, predicted that the adsorption of H acts as a critical step driving the leaching of Cu atoms from the graphene lattice. Such process would accelerate at more negative potentials where stronger H adsorption took place.<sup>69</sup> The leached Cu atoms would aggregate and redisperse on the graphene surface, functioning as the true active centers dictating the catalytic outcomes. Therefore, further studies are imperative to examine the structural reconstruction of Cu SACs under cathodically relevant potentials and to gain a deeper understanding of the structure-performance relationships of SACs under in situ conditions.



**Figure 2.4** (a) The difference in \*CO and \*H binding energy ( $\Delta G^*H-\Delta G^*CO$ ) versus the maximum CO<sub>2</sub>RR reaction energy ( $-\Delta Gmax$ ).<sup>54</sup> Reprinted with permission from Reference [54]. Copyright (2021) Wiley-VCH GmbH. (b) FEs and TOF of FA at different potentials for In-SAs/NC, In-NPs/NC, and NC. (c)  $j_{FA}$  at different potentials for In-SAs/NC, In-NPs/NC, In-NPs/NC, and NC. (c)  $j_{FA}$  at different potentials for In-SAs/NC, In-NPs/NC, and NC.<sup>70</sup> Reprinted with permission from Reference [70]. Copyright (2020) Wiley - VCH GmbH. (d) FE<sub>CO</sub> of In@NC-1000 and In@NC-900.<sup>60</sup> Reprinted with permission from Reference [60]. Copyright (2022) American Chemical Society. (e) In situ Cu k-edge XANES spectra of pre Cu/C-0.4, Cu/C-0.4 at -0.7 V and -1.0 V vs RHE and post Cu/C-0.4.<sup>66</sup> (f) The hypothesized reaction mechanism suggested by the operando measurements.<sup>66</sup> Reprinted with permission from Reference [66]. Copyright (2020) Springer Nature.

Beyond the atom identity, the modulation of ligand functionality, including the number and type of coordinated atoms, can also change the bonding configuration and the electron distributions

of the active sites, which in turn influence the adsorption and activation of the CO<sub>2</sub> molecule and intermediates. In an effort to enhance the electrocatalytic performance and stability of SACs, early investigations primarily centered around understanding the M-N4 pyramidal structures with a symmetrical nitrogen coordination environment due to the simplicity of the structure and ease of synthesis. However, as the field has progressed, a plethora of studies have been carried out to investigate the impact of asymmetrical and/or non-nitrogen coordination environments on the M-Nx structures and their effects on the CO<sub>2</sub>RR. Pan et al. exploited the Co-N4 and Co-N5 with different coordination number and found that Co-N5 exhibited superior CO2RR performances with  $FE_{CO}$  of 99.2% and 99.4% at -0.73 and -0.79 V, respectively, equivalent to a 15.5-fold enhancement of Co-N4 in activity.<sup>50</sup> Ni et al. fabricated a Sn-C2O2F SACs which actively converted CO<sub>2</sub> to CO with a  $FE_{CO}$  > 90.0% over a potential window from -0.2 to - -0.6 V, in contrast to the Sn-N4 where FA was identified as the major product.<sup>55</sup> DFT calculations indicated that C/O coordination regulates the adsorption of intermediates, resulting the RDS shift from \*CO desorption on Sn-N4 to the \*CO2 activation on Sn-C2O2 and Sn-C2O2F, thereby changing the selectivity of CO<sub>2</sub>RR. Lakshmanan et al. recently reported an unique Fe SACs configuration where the central Fe atom is surrounded by three -SO<sub>3</sub> groups via the oxygen atoms in Nafion coated functionalized multi-wall carbon nanotubes (Fe-n-f-CNTs), as shown in Figure 2.5.71 Interestingly, the as-obtained Fe-n-f-CNTs achieved a high FE<sub>C2H5OH</sub> of 45% and a production rate of 56.42 µmol cm<sup>-2</sup> h<sup>-1</sup> at -0.8 V. The near +3 oxidation states of Fe and the unique catalytic features induced by oxygen coordination collectively contributed to the high yields of C<sub>2</sub>H<sub>5</sub>OH. Li et al. synthesized the P,N co-coordinated Fe SACs (Fe–N/P–C) on commercial carbon black, which demonstrated enhanced activity and stability toward CO<sub>2</sub>RR compared to the N coordinated Fe

SACs (Fe-N-C).<sup>48</sup> *Ex situ* XAS analyses of Fe–N/P–C and Fe-N-C before and after CO<sub>2</sub> electrolysis suggest the more severe Fe clustering in the latter sample, which indicates that the P,N co-coordinated Fe is more resilient toward aggregation. Therefore, the coordination-tunning strategy presents a general approach to regulating the intrinsic activities of the metal center and can be more broadly applied to other electrochemical processes.



**Figure 2.5** Graphical illustration of the synthesis process of Fe-n-f-CNTs.<sup>71</sup> Reprinted with permission from Reference [71]. Copyright (2022) Wile - VCH GmbH.

An interesting phenomenon worth mentioning is the reported variability in CO<sub>2</sub>RR performance over SACs that possess identical coordinating atoms. This suggests that the activity of these SACs is not only determined by the metal/ligand pairing but may also rise from the overarching microstructures of these SACs. Through DFT simulations, Zhu et al. predicted a curvaturedependent CO<sub>2</sub>RR selectivity using cobalt porphyrin nanotubes with various radius of 2.93/2.42 (CoPrNT-2), 4.17 (CoPrNT-3) and 5.25 (CoPrNT-4) Å. The simulated results showed that CO<sub>2</sub>-to-CO could be readily initiated on the catalyst with larger diameters, while the high curved nanotubes with smaller radii would preferably enable further CO hydrogenation to CH<sub>4</sub>.<sup>72</sup> Xiong et al. synthesized Ni-N4 single atom structures on a series of carbon shell with different shell thickness.<sup>73</sup> They found that the electrocatalysts displayed the highest CO selectivity when the Ni-N4 was loaded on 12 nm shell (thinnest). Hao et al. reported that Zn SACs anchored on the highly curved carbon nano-onions (CNO) support displayed much higher CO<sub>2</sub>RR activity compared to the ones on two-dimensional planar graphene substrate, which was ascribed to the reduced thickness of electrochemical double layer and stronger electric field strength on the surface of the former Zn SACs.<sup>74</sup> Zhang and colleagues reported that the atomically dispersed Sn on the tensile-strained ZnO nanosheets demonstrated enhanced activity and selectivity in comparison to ZnO in terms of CO<sub>2</sub>-to-FA conversions.<sup>75</sup> These studies point to the critical roles of the geometric structures in dictating the CO<sub>2</sub>RR, which remain less explored in SACs for CO<sub>2</sub>RR.

#### 2.4. Current Status and Remaining Challenges

In the past decades, tremendous efforts have been devoted to CO<sub>2</sub>RR research which represents one the most promising solutions to the ultimate carbon neutrality. The enrichment of commercially available electrocatalysts that are low-cost, high active and durable remain as the prioritized work aimed at the enhancement of CO<sub>2</sub>RR technology on a broad scale. The prevalent methods of material development are primarily predicated on a process of repeated experimentation that follows a trail-and-error approach, while a deeper understanding of the underlying principles dictating their effectiveness remains inadequately explored. In this regard, elucidating the correlations between structure and performance of electrocatalysts is a paramount aspect of research and requires further investigations.

In order to address these challenges, the objectives of this thesis are outlined into two major segments as follows. First, for practical applications, it is crucial to design low-cost catalysts with facile synthesis procedures. Perovskites, which offer tunable A-site and B-site combinations,

present significant opportunities for regulating the selectivity and activity of CO<sub>2</sub>RR. In addition, perovskites can be prepared using versatile methods, including the widely used and straightforward "sol-gel" approach, enabling the large-scale production of perovskite powders. However, the systematic investigations into the application of perovskites for room temperature CO<sub>2</sub>RR has been lacking, and one crucial aspect that remains unexplored is how the evolved perovskite structure influences performance and stability under cathodic reductions relevant to CO<sub>2</sub>RR. To fill the gap, the structure-performance relations in a representative perovskite, BaBiO<sub>3</sub> (BBO), are to be systematically explored in this thesis. Under cathodic potentials, the structural evolution during electrolysis and the catalytic roles of both A-site and B-site elements are investigated to shed lights on the utilization of perovskites in room-temperature CO<sub>2</sub>RR. Moreover, the cooperative catalytic scheme of A- and B- sites has been proposed to enhance the formate production *via* distinct mechanisms. The conclusions drawn from these studies can serve as valuable guidance in designing other potential perovskite systems for highly active CO<sub>2</sub>.

To enhance the cost-effectiveness and atom utilization of catalysts, there is a growing interest in downsizing nano-bulk materials to an extreme extent where all metal atoms are discretely embedded in a certain matrix. This involves exposing only a single active atom to the reactants. In the ideal scenario, the atomic utilization efficiency would be maximized, as inactive atoms are eliminated, and all catalytically active sites are effectively utilized. The structure-performance of SACs, especially the coordination effects and the geometry effects, are to be studied on two representative SACs including Bi SACs and Co SACs. The coordination effects are to be examined on a series of Bi SACs, owing to the capabilities of p-blocking metal-based materials to catalyze both CO and FA production. In terms of the geometry effects, Co SACs anchored on curved CNT

substrates will be adopted as model electrocatalysts. These catalysts hold significant promise for advancing the field of catalysis and opening up new opportunities for sustainable and efficient chemical processes.

# **Chapter 3. Experimental Methodologies**

#### 3.1. Materials Synthesis

#### **3.1.1.** Sol-gel synthesis of BaBiO<sub>3</sub> (BBO)

BBO powder was prepared by a facile sol-gel method. Stoichiometric amounts of  $Ba(NO_3)_2$  and  $Bi(NO_3)_3$ ·5H<sub>2</sub>O were firstly dissolved in 300 mL deionized water and then, nitric acid was introduced dropwise until  $Bi(NO_3)_3$ ·5H<sub>2</sub>O was completely dissolved. Afterwards, ethylenediaminetetraacetic acid (EDTA) and citric acid were added (the molar ratio of EDTA and citric acid to total metal ions was set as 1:2:1), and the pH of the solution was adjusted to be around 7 by NH<sub>3</sub>·H<sub>2</sub>O. The precursor solution was slowly evaporated on a hot plate to yield viscous gel which further underwent a self-combustion reaction. Finally, the obtained powder was annealed at 850 °C for 4 h in air, and the as-obtained powder was further ball milled in ethanol for 6 hours to achieve smaller particle size distribution.

#### 3.1.2. Synthesis of BVOh-FN photoanode

Nanoporous BiVO<sub>4</sub> (BVO) photoanode was prepared according to the pioneering work by Kim and Choi with slight modifications.<sup>76</sup> Briefly, 0.73 g Bi(NO<sub>3</sub>)<sub>3</sub>·5H<sub>2</sub>O was dissolved in 50 mL 0.4 M KI solution, and its pH was adjusted to ~ 1.7 by HNO<sub>3</sub>. The precursor was further mixed with a separate ethanol solution (20 mL) containing 0.23 M p-benzoquinone and stirred for 5 mins to form the BiOI deposition precursor solution. To obtain BiOI nanosheets, a piece of clean FTO (2 \* 3 cm<sup>2</sup>), Pt foil and Ag/AgCl (sat.) electrode were employed as the working, counter, and reference electrodes, respectively. The potential was kept at - 0.1 V vs Ag/AgCl for 10 - 12 minutes to deposit BiOI. To convert BiOI to BiVO<sub>4</sub>, 0.6 mL of 0.2 M VO(acac)<sub>2</sub> dissolved in dimethyl sulfoxide was pipetted onto BiOI, which was further annealed at 450 °C for 2 hours at a ramping rate of 2 °C min<sup>-1</sup>. Afterwards, the as-obtained material was soaked in 1.0 M KOH for 30 mins to remove excess  $V_2O_5$ . Finally, the BVO substrate was dried and annealed at 270 °C at a ramping rate of 2 °C min<sup>-1</sup> in Ar/H<sub>2</sub>(5%) for 20 minutes to generate excessive oxygen vacancies (BVOh). FeOOH and NiOOH co-catalyst layer was further deposited on BVOh to enhance water oxidation kinetics. FeOOH thin layer was photo-deposited onto BiVO<sub>4</sub> from a 0.1 M FeSO<sub>4</sub> solution. To assist photo-deposition, an external bias of 0.3 V vs Ag/AgCl was applied. The deposition proceeded for 20 mins prior to increasing the potential to 1.2 V vs Ag/AgCl and maintained there for another 1 min. Subsequently, NiOOH was photo-deposited from a 0.1 M NiSO<sub>4</sub> solution (pH ~ 7) with an external potential of 0.11 V vs Ag/AgCl for 15 mins, followed by a sequential electrodeposition of NiOOH at 1.2 V vs Ag/AgCl for 1 min. The as-prepared samples are denoted as BVOh-FN. The BVOh-FN photoelectrode was washed with deionized water, and naturally dried overnight.

## 3.1.3. Synthesis of Bi-C and Bi-NC

## • Synthesis of nitrogen-doped reduced graphene:

N doped rGO was synthesized by annealing the rGO and dicyandiamide mixture (in a mass ratio of 1:10) at 900 °C in argon flow for 1 h at a ramping rate of 2 °C min<sup>-1</sup>. After cooling down naturally in the argon flow, the nitrogen doped graphene powder was obtained.

#### • Synthesis of Bi-C and Bi-NC:

The synthesis of Bi-based SACs was achieved by a three-step synthesis process including (i). precursor powder preparation, (ii). laser irradiation process, and (iii). the final acid refluxing treatment.

(i). The precursor powder was obtained by dispersing 20 mg of rGO/NrGO to the 10 mL of ethanol solution containing 4mM of  $Bi(NO_3)_3 \cdot 5H_2O$  or  $BiCl_3$  salts, and the dispersion solution was subsequently subjected to constant ultrasound treatment for 20 min. The obtained mixture was then dried and degassed under vacuum at room temperature overnight. Finally, the powdery precursor was obtained and preserved in a vacuum oven.

(ii). The Bi ions/graphene complex was subjected to pulsed laser irradiation, and the details are described as follows:

<u>Sample preparation</u>: 50 mg of the powdery precursor was loaded in a glass vial with a volume of 20 ml and then covered by a glass slide on the opening from which laser pulses were penetrated through.

<u>Laser system setup</u>: the nanosecond pulse laser was operated at a wavelength of 1064 nm and pulse duration of 5 ns (Nd:YAG, Surelite III Q-switch, Continuum). Three reflective mirrors and a focus lens were used to reflect and focus the laser beam. The reflective mirrors changed the laser pulse direction from horizontal to vertical and thus, the laser beam passed through the focus lens and irradiated into the opening of the vial containing precursors. The spot size of the laser beam could be adjusted by changing the distance between the focus lens and the glass vial. In a typical procedure, the spot size of the laser beam was 5 mm, and the laser pulse energy was 620 mJ to produce a power density of 0.64 GW cm<sup>-2</sup>. For a typical experiment, 50 laser pulses were used to convert 50 mg precursor.

<u>Laser processing</u>: in the typical laser treatment, the glass vial containing the precursor was placed under the focus lens. The laser pulses were delivered to the precursors automatically with a frequency of 2 Hz. Once the laser contacted the precursor, a bright light was observed along with floating black smoke saturated across the whole vial. The light was caused by the plasma plume and the black smoke was generated by the powdery precursor thrusted by the ejection of plasma from the precursor during laser irradiation. In the optimized protocol for the synthesis Bi SACs, the laser irradiation dose was 1 pule per mg of the precursor. After laser treatment, the obtained product was soaked 3 times in fresh ethanol to dissolve residual metal salts. The final product was obtained by vacuum drying overnight at room temperature.

The overall ultrafast laser-based method can be concluded as follows: initially, laser photons were absorbed by both the carbonaceous support and metal ions, resulting in the generation of electrons. High-temperature conditions were achieved simultaneously, leading to the reduction, and etching of the carbonaceous support. The laser-induced plume, characterized by localized high temperature and a reductive atmosphere, effectively reduces the metal ions, enabling the entire process to be conducted in ambient air. Following this, the reduced metal atoms were rapidly cooled upon laser irradiation, embedding into the defect sites of the carbon support. This laser-induced ultrafast reduction and cooling process occurs within nanoseconds, facilitating the swift reduction of metal salts and the formation of highly enriched Bi SACs with wide distribution

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on the supports. Importantly, the non-contact nature of laser interaction makes this method particularly suitable for processing powdery precursors, which aligns well with modern industrial fabrication practices with significant cost reduction.

(iii). To obtain the final Bi SACs, the as-obtained powder was washed with 0.5 M  $H_2SO_4$  three times to remove the Bi-based nanoclusters.

#### **3.1.4.** Synthesis of CoPc-CNTx

#### • Synthesis of acid functionalized CNTs

CNTs with various radii (XFNANO Materials Tech Co., Ltd) were annealed in air at 450 - 500 °C for 5 h in air to oxidize the amorphous carbon layer, followed by acid wash (5% w/w HCl) to remove the Ni reside. 150 mg of the pre-annealed CNTs powder was dispersed in 15 mL of concentrated H<sub>2</sub>SO<sub>4</sub>, following the slow addition of 5 mL of concentrated HNO<sub>3</sub> with mild magnetic agitation to improve hydrophilicity. The CNTs suspension was cooled down naturally and washed extensively with deionized water until the pH of the suspension approached 7. The powder was freeze-dried overnight.

### • Synthesis of CoPc-CNTx

The synthesis of CoPc-CNTx was based on the previous report with slight modifications.<sup>77</sup> In details, 20 mg of the functionalized CNTs powder was dispersed in 20 mL of dimethylformamide solution and sonicated for 30 mins to achieve homogenous distributions. 10 mL of the CoPc stock solution (0.12 mg mL<sup>-1</sup>) was then added dropwise to the CNTs suspension and sonicated for 30

mins, followed by magnetic stirring for another 24 h to allow complete CoPc-CNTx hybridization. The CoPc-CNTx was then filtered with polypropylene membrane and washed with dimethylformamide two times and ethanol one time. The as-obtained powder was dried in a vacuum oven overnight to yield the final products. The synthesis of CoPc-rGO follows the same protocols but replacing the CNTs powder with graphene nanosheets.

### **3.2.** Physical Characterizations

To study the physicochemical properties of materials, the following characterization techniques were adopted:

- X-ray Diffraction (XRD): The X-ray diffraction (XRD) analysis was acquired on a Rigaku Ultima IV equipped with a Cu-K<sub> $\alpha$ </sub> radiation source (K $\alpha$  = 1.540598 Å) operating at 40 kV and 44 mA with a scan speed of 8° min<sup>-1</sup>. The XRD data was deconvoluted by Jade Software.
- Field Emission Scanning Electron Microscopy (FE-SEM): the microstructures of the materials were recorded using the Zeiss Sigma FE-SEM configured with in-lens secondary electron detector and a backscatter detector.
- Transmission Electron Microscopy (TEM): the TEM images were acquired using the JEOL JEM-ARM200CF, which is a probe aberration corrected S/TEM (scanning TEM) with a cold field emission gun at 200 kV. Energy dispersive X-ray spectrometry (EDX) elemental mapping and aberration-corrected high angle annular dark field scanning transmission electron microscopy (AC-HAADF-STEM) was also acquired using JEOL JEM-ARM200CF.

- X-ray photoelectron spectroscopy (XPS): the XPS analysis was performed on a Krato AXIS Ultra with the carbon C 1s at the binding energy of 284.8 eV as the calibration. The XPS data were analyzed using CasaXPS.<sup>78</sup>
- Fourier-transform infrared spectroscopy (FTIR): FTIR was performed on the Nicolet 8700
   Fourier Transform Infrared Spectrometer equipped with an in situ cell with constant CO<sub>2</sub>/H<sub>2</sub>
   flow (CO<sub>2</sub>: H<sub>2</sub> = 0.2 : 20 sccm) during signal collections.
- Raman: Raman spectroscopy was conducted on the Renishaw inVia Qontor Confocal Raman Microscope with a laser wavelength of 532 nm. Surface-enhanced Raman spectroscopy (SERS) was conducted by dipping materials onto the Au-based SERS substrates (Ocean Insight).
- Atomic force microscope measurements (AFM): suitable amounts of the ethanol suspension of electrocatalysts were deposited on a clean silicon wafer. The MFP-3D-Bio AFM system (Asylum Research, Santa Barbara, CA) was exploited to characterize the thickness of electrocatalysts.
- X-ray absorption spectroscopy (XAFS): The XAFS data were collected at VESPERS, Canadian Light Source. The data were processed using Demeter software package.<sup>79</sup>
- Inductively Coupled Plasma Optical Emission spectroscopy (ICP-OES): The samples were digested, and the ions concentrations were measured by Thermo iCAP6300 Duo (N. America) inductively coupled plasma-optical emission spectrometer.

### 3.3. Electrochemical Characterizations

#### 3.3.1. Electrolyser setup

The electrolyser used in the experiments of this thesis is a customized gas-tight twocompartment H-cell in a three-electrode configuration. The anode and cathode compartments were separated by a piece of activated proton-exchange Nafion 117 membrane. The catalyst ink was prepared by dispersing the suitable amount of catalyst powder in the homogeneous solution containing ethanol/water mixture, with the addition of Nafion solution (5 wt%, Sigma-Aldrich) to enhance the viscosity. The ink was subjected to ultrasonic treatment for at least 1h before usage. The as-prepared ink was pipetted onto carbon paper to achieve desirable loading mass (c.a. 0.04 – 0.1 mg cm<sup>-2</sup>). A graphite rod and the Ag/AgCl (sat.) electrode were employed as the counter and reference electrodes, respectively. Prior to the start of electrolysis, CO<sub>2</sub> was fed to electrolyte until saturated (around 30 mins). During the experiment, the flow rate of CO<sub>2</sub> was fixated at 20 mL min<sup>-1</sup>. The CO<sub>2</sub> saturated 0.1 M and 0.5 M KHCO<sub>3</sub> electrolyte have the pH of 6.8 and 7.4, respectively.

#### **3.3.2.** Electrochemical analysis

Linear sweep voltammetry (LSV) polarization curves and the CV scans were obtained in CO<sub>2</sub> and/or Ar saturated KHCO<sub>3</sub> electrolyte. Gaseous and liquidous products were analyzed using the Agilent 6890 N GC and Metrohm 850 Professional IC Cation–HP-Gradient IC, respectively, as described in section 1.2.2. All potentials reported in aqueous electrolytes were converted to the RHE scale:  $E_{RHE}(V) = E_{Ag/AgCl}(V) + 0.059 * pH + 0.197$ . All electrochemical studies were performed on Autolab worksation unless otherwise specified. Electrochemical Impedance

Spectroscopy (EIS) was performed in  $10^5 - 0.1$  Hz. The EIS data was fitted using suitable equivalent circuits.

#### **3.4.** Density Functional Theory

#### 3.4.1. Calculation parameters

The first-principles calculations were performed based on the DFT with the generalized gradient approximation in the form of Perdew-Burke-Ernzerhof implemented in the Vienna Ab initio Simulation Package (VASP). The electron ion interaction was described with the projector augmented wave method. Vaspkit package was used to generate input files.<sup>80</sup> Vesta software was used for visualization and model constructions.<sup>81</sup>

Before calculations, the convergence tests were performed to determine the values of K points and cutoff energy ( $E_{cutoff}$ ) for each system. The Gibbs free energy change of each step during CO<sub>2</sub>RR and HER was determined based on the CHE model.<sup>15</sup> The Gibbs free energy of the slabs with different adsorbents was determined by the following equation Equation 3.1:

$$G = E_{DFT} + E_{ZPE} + \int C_p dT - TS$$
(3.1)

where  $E_{DFT}$ ,  $E_{ZPE}$ ,  $\int C_p dT$  and TS stand for the DFT calculated electronic energy, zero-point energy, enthalpy correction and entropy correction, respectively.

• Calculation details for BBO

For unit cell optimization, a cutoff energy of 520 eV was set. Spin polarization was considered in all calculations. Based on the optimized cells, the following calculations were performed on a (3

× 3) Bi (003) slab, (3 × 1) BBO (100) and (3 × 1) BBO (001) slab with a 15 Å vacuum layer on the top (Table S4.2). Brillouin Zone k points (3 × 3×1), (6 × 5×1) and (4 × 5×1) were generated for Bi (003) slab, BBO (100) and BBO (001) slab, respectively, and the cutoff energy was set as 500 eV. The criterion of convergence for electronic step was set as  $10^{-5}$ . The two upper layers of the slab were allowed to fully relax until a maximum force component of 0.02 eV Å<sup>-1</sup> was reached, and the positions of other atoms were fixed. To obtain the optimized model with \*OCHO adsorption, the different supercell models with various adsorption locations were considered, and the configuration with the lowest energy was used in the subsequent calculations (Table S4.3).

Calculation details for Bi-C and Bi-NC

The Bi single atom embedded at the vacancy site of C and NC was modeled by replacing the carbon atom(s) with Bi atom(s) or/and N atoms in a 4 \* 4 graphene supercell based on the previous reports.<sup>82,83</sup> The configurations were diversified by filling single and double vacancies with Bi atom, followed by replacing the coordinated carbon atom(s) with nitrogen atom(s) in the initial BiC3 and BiC4 models. There are two different configurations when two nitrogen atoms are doped in the double vacancy models, which are labeled as BiC2N2-1 adjacent (N) and BiC2N2-2 (opposite N). A 15 Å vacuum layer was placed along Z direction in all the models to minimize the interactions between the periodic graphene sheets. A plane-wave basis cutoff energy was set as 500 eV for spin polarization calculations, and Brillouin Zone K points (4\*4\*1) were generated by Gamma centered grid based on the results of convergence tests. The criterion of convergence for electronic step was set as 1e<sup>-5</sup>, and all atoms were allowed to relax during the geometry optimizations until a maximum force component of 0.02 eV Å<sup>-1</sup> was reached. Gaussian smearing

was adopted for calculations based the previous reports.<sup>83,84</sup> DFT-D3 semi-empirical van der Waals corrections were considered during structural optimization to compile with the deficiencies of DFT in dealing with dispersion interactions.<sup>85</sup> Furthermore, a correction of -0.45 eV for gaseous CO<sub>2</sub> molecule was added to compensate the deviation between theoretical and experimental results of gas-phase molecules.<sup>86</sup> The thermodynamic stabilities of Bi SAs were evaluated by calculating the E<sub>b</sub> of different models with  $E_b = E_{total} - E_g - E_a$ , where  $E_{total}$ indicates the total energy of the Bi-graphene systems,  $E_g$  refers to the energy of graphene substrate,  $E_a$  stands for the energy of one atom which is calculated by dividing the Bi bulk energy by the number of Bi atoms.<sup>84</sup> Within this definition, the more negative values of  $E_b$  indicate the stronger bonding strength between Bi SA and the substrate.

#### Calculation details for Co-CNT

For the structural optimization and electronic property calculations of CoPc-CNT, a plane wave basis set with a cutoff energy of 520 eV and the Gamma 2 × 2 × 1 K points was used to sample the Brillouin zone. The criterion of convergence for electronic step was set as 1e<sup>-5</sup>. The atoms can relax freely during the geometry optimizations until the forces were lower than 0.02 eV Å<sup>-1</sup>. Gaussian smearing with a smearing width of 0.05 eV was adopted based on the previous reports. The vacuum thickness was set as 20 Å along the Z-axis. For the calculations of the simplified CoN4C8N4 embedded in graphene, a  $\sqrt{2} * \sqrt{2}$  graphene unit cell (rectangular cell) was employed to construct a (7 x 3 x 1) supercell to ensure applications of the biaxial strain, and to avoid the interactions between adjacent CoN4C8N4 motifs. During the application of strain, the a/b value of the supercell was fixated. The Gamma 2 × 3 × 1 K points was used, and the vacuum thickness was set as 15 Å along the Z-axis. For all the calculations, the Van der Waals interactions were corrected using DFT-D3 semi-empirical to cope with the deficiencies of DFT in dealing with dispersion interactions. Spin polarizations were also considered in all the calculations. Furthermore, a correction of -0.45 eV for gaseous CO<sub>2</sub> molecule was added to compensate the deviation between the theoretical and experimental results of gas-phase molecules.

#### **3.4.2.** Reaction pathways

## • FA pathway

the elementary reaction step along FA pathway can be represented by Equations 3.2 and 3.3:

$$CO_2 + * + H^+ + e^- \leftrightarrow ^*OCHO$$
(3.2)

$$^{*}\text{OCHO} + \text{H}^{+} + \text{e}^{-} \leftrightarrow * + \text{HCOOH}$$
(3.3)

where \* stands for the adsorption site. The  $\Delta G$  for each step can be calculated using the Equations 3.4 and 3.5:

$$\Delta G1[^{*}OCHO] = G[^{*}OCHO] - G[^{*}] - G[CO_{2}] - G[H^{+}] - G[e^{-}]$$
(3.4)

$$\Delta G2[HCOOH] = G[HCOOH] - G[CO_2] - 2G[H^+] - 2G[e^-]$$
(3.5)

The free energy change diagrams were plotted based on  $\Delta$ G1 and  $\Delta$ G2.

### • CO pathway

$$CO_2 + * + H^+ + e^- \leftrightarrow *COOH \tag{3.6}$$

$$*COOH + H^+ + e^- \leftrightarrow *CO + H_2O$$
(3.7)

$$^{*}CO \leftrightarrow * + CO \tag{3.8}$$

where \* stands for the adsorption site. The  $\Delta G$  for each step can be calculated using the Equations 3.9-3.11:

$$\Delta G3[^*COOH] = G[^*COOH] - G[^*] - G[CO_2] - G[H^+] - G[e^-]$$
(3.9)

$$\Delta G4[*CO] = G[*CO] + G[H_2O] - G[CO_2] - G[*] - 2G[H^+] - 2G[e^-]$$
(3.10)

$$\Delta G5[CO] = G[CO] + G[H_2O] - G[CO_2] - 2G[H^+] - 2G[e^-]$$
(3.11)

The free energy change diagrams were plotted based on  $\Delta$ G3,  $\Delta$ G4 and  $\Delta$ G5.

## • H<sub>2</sub> pathway

$$* + H^+ + e^- \leftrightarrow {}^*H \tag{3.12}$$

$$\mathrm{H}^{+} + {}^{*}\mathrm{H} + \mathrm{e}^{-} \leftrightarrow * + \mathrm{H}_{2} \tag{3.13}$$

The Gibbs free energy change for HER can be calculated using the Equation 3.14:

$$\Delta G6[^*H] = G[^*H] - G[^*] - G[H^+] - G[e^-]$$
(3.14)

The free energy change diagrams were plotted based on  $\Delta G6$ .

# **Chapter 4. Electrochemically Reconstructed Perovskite with**

# Cooperative Catalytic Sites for CO<sub>2</sub>-to-formate Conversion



**Figure 4.1** Illustration of the structural evolution of BBO under cathodic potentials (colors of the atom, orange: Ba; purple: Bi; white: oxygen).

### 4.1. Introduction

 $CO_2RR$  driven by sustainable energy resources holds great promise for alleviating the adverse effects of  $CO_2$  accumulation by converting  $CO_2$  to value-added chemicals in order to realize zero net emission of  $CO_2$  in the carbon cycle of  $CO_2$ -fuel- $CO_2$  <sup>12,87–89</sup>. FA is an important liquid product of  $CO_2RR$  and plays an indispensable part in various industrial processes <sup>90–93</sup>. For the past few years, substantial efforts have been devoted to boosting the  $CO_2$ -to-FA conversion using different nanostructured catalysts, however, the complicated synthesis procedures and low product yields are usually associated with many of these catalysts, which hinder their scalability. Therefore, it is imperative to synthesize electrocatalysts through rational design with easy fabrication process and economic feasibility to advance  $CO_2RR$  technology for its large-scale implementation. Inspired by the multiple advantages of perovskites (e.g., structural/compositional flexibility, good scalability, etc.), we pursue initiating the room-temperature electrochemical conversion of CO2 on perovskite-based catalysts owing to their excellent activity and easy production <sup>94–96</sup>. It has been well recognized that B-site cations of perovskites play major catalytic roles, and this knowledge provides a basis when choosing appropriate perovskite. For instance, Cu-based perovskites have been shown to favorably produce hydrocarbon products, i.e. CH<sub>4</sub> <sup>38</sup>, C<sub>2</sub>H<sub>4</sub> <sup>97</sup>, while Sn-based perovskites, in sharp contrast, tend to selectively produce FA <sup>33</sup>. According to these studies, a close correlation can be established between the type of B-site species and production distributions in CO<sub>2</sub>RR. The second concern that needs to be addressed is the potential-induced reconstruction of perovskites at catalytically relevant voltages. Electricitydriven reconstructions in electrocatalysts have been actively investigated in binary metal compounds (e.g., oxides, sulfides, etc.) for various applications including OER, HER, etc. 98-100, but rarely discussed in perovskites for room-temperature CO<sub>2</sub>RR. In general, the voltage-driven reconstructions in perovskites could lead to the change of crystal phase accompanied by the evolution of geometrical structures (e.g., enlarged surface area, more exposed active sites, etc.); and/or give rise to new electronic features that stabilize certain intermediates and lead to the promoted activity of reactions <sup>101–104</sup>. Finally, it should be noted that the electrochemical reduction of perovskite will trigger the rearrangement of all or a portion of A-site elements due to the "diffusion - re-nucleation - growth" of B-site ions <sup>105,106</sup>. Since A-site elements in perovskites are usually considered to be non-active in  $CO_2RR$  (i.e., Pr, Ba, La, and Sr, etc.), the role of A-site elements in CO<sub>2</sub> conversion under room-temperature conditions has been overlooked so far.

Therefore, the reconstructions of perovskites under cathodic potentials may be of great significance for CO<sub>2</sub>RR and require further investigations.

In this work, the BBO perovskite is fabricated by crystallization of the sol-gel  $Ba^{2+}/Bi^{3+}$  nitrate crosslinkers. Bi cations placed at B-site is expected to facilitate FA production, whereas Ba at A-site is determined due to its suitable ionic radius and valence state to form perovskite structure. Our studies show that under negative potentials, BBO pre-catalysts undergo irreversible structural and phase transformations, giving rise to electricity induced BBO (eBBO) that leads to high FA selectivity in both EC and PEC cells. Further investigations reveal that A-site element (Ba) can diffuse to the electrolyte and remain as  $Ba^{2+}$  ions, and the effects of  $Ba^{2+}$  on  $CO_2RR$  are co-dependent on the type of electrolyte, the external potentials, and the concentration of  $Ba^{2+}$  in the electrolyte. Our study proposes that the utilization of both A- and B- sites in BBO to benefit  $CO_2$  conversion could be possible, which may be extended to other perovskite electrocatalysts for  $CO_2RR$ .

## 4.2. Results and Discussion

Gram-scale BBO powder was synthesized by annealing 0.01 mol BBO sol-gel precursor under high temperature followed by ball-milling for 6 hours to achieve the smaller particle size distributions of BBO. The XRD pattern of the sintered powder matches well with the standard monoclinic BBO phase (JCPDS: 035-1020, Figure 4.1a) with no discernable impurity phase. The successful synthesis of BBO is further corroborated by the Raman scattering spectrum where the three fingerprint vibrations emerged at 300.0, 492.1, and 556.4 cm<sup>-1</sup> can be well assigned to the superstition of Bi-O bending mode, Bi-O stretching mode, and the [BiO<sub>6</sub>] breathing with Ag

symmetry in monoclinic BBO, respectively (Figure 4.1b).<sup>107</sup> The FE-SEM and TEM reveal that the ball-milled BBO composes of the irregularly shaped nanoparticles (Figure 4.1c and 4.1d).

Considering the cathodic working potential nature of CO<sub>2</sub>RR, we performed the CV analysis in Argon-saturated 0.1 M KHCO<sub>3</sub> with a scan rate of 20 mV s<sup>-1</sup> to initially probe the redox capabilities of fresh BBO (Figure 4.1e). No distinguishable reduction peak could be observed in the initial cathodic sweep, but starting from the second scan, a cathodic peak merged at 0.04 V, indicative of the reduction of Bi ions. The inter-crossing point located at - 0.07 V is attributed to the insulating nature of BBO and the high energy requirement to deconstruct BBO scaffold.<sup>108</sup> In anodic scans, three anodic peaks located at 0.23 V (point C), 0.43 V (point D) and 0.63 V (point E) represent the oxidation reactions from Bi<sup>0</sup> to Bi<sup>3+</sup>. The presence of Bi<sup>0</sup> phase is further supported by performing the XRD analysis over catholically reduced BBO electrodes at - 1.2 V for various time periods of 100, 500, 1000, 3000 and 5000 s (denoted as BBO100, BBO500, BBO1000, BBO3000, and BBO5000, respectively, Figure 4.1f). The peaks emerged at 23.8°, 27.2°, 37.9° and 39.6° are well indexed to the (003), (012), (104) and Bi (110) facets of metallic Bi, respectively, thus confirming the formation of rhombohedral Bi<sup>0</sup> (JCPDS: 44-1426) in all reduced BBO samples. Notably, the readily observed Bi<sup>0</sup> phase in BBO100 imply that voltage-driven Bi reduction is an extremely efficient process compared to the traditional high-temperature annealing method in reducing atmosphere (which usually takes up to hours).<sup>106</sup> Based on these results, we further performed Raman spectroscopy over a typical phase-changed BBO3000 (Figure 4.1g). Clearly, the absence of all three representative BBO Raman shifts in BBO3000 confirms the deconstruction of BBO architecture upon deep reductions.

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**Figure 4.1** (a) XRD pattern, (b) Raman spectrum, (c) FE-SEM and (d) TEM of fresh BBO powder. (e) CV curves of fresh BBO electrode. (f) *Ex situ* XRD analysis of BBO electrodes reduced at various time periods of 100, 500, 1000, 3000, and 5000 s (green: JCPDS Bi: 44-1246; blue: JCPDS Bi<sub>2</sub>O<sub>2</sub>CO<sub>3</sub>: 41-1448; red: JCPDS BaBiO<sub>3</sub>: 035-1020). (g) Raman spectrum of BBO3000.

The surface chemistry of BBO3000 was studied by the XPS. As shown in Figure 4.2, the Bi 4f spectra of BBO3000 and the control sample Bi-3000 (where the commercial Bi nanoparticles were reduced at - 1.2 V for 3000s) exhibit the similar features, and the two peaks located at ca. 159 eV and 164 eV can be ascribed to the Bi<sup> $\delta$ +</sup> (0 <  $\delta$  < 3) resulting from the oxidation of surface Bi species. The surface oxides of the BBO3000 and Bi-3000 were then partly removed by the Ar<sup>+</sup> sputter etching for three minutes (denoted as BBO3000-etch and metal Bi-3000-etch, respectively). After surface etching, the original XPS peaks split into four new peaks. The new peaks located at around 157.1 and 162.4 eV can be ascribed to metallic Bi; the other two peaks at around 159.6 and 165.0
eV can be assigned to Bi<sup>3+</sup>.The resembled Bi 4f scans of BBO3000 and metal Bi suggest similar chemical states of Bi atoms in BBO3000 and metallic Bi. These results confirm that the fresh BBO was reduced to Bi<sup>0</sup> phase when subjected to the external potential of - 1.2 V for 3000 s. Moreover, the Ba signals are completely vanished after cathodic polarization, as observed from XPS, which is presumably explained by the release of Ba<sup>2+</sup> into the surrounding electrolyte, rather than the formation of relevant Ba species (i.e., BaO) at the electrode surface.

Ex situ FESEM images of the different BBO samples during the reduction process were captured to examine the surface morphology changes (Figure 4.3). Upon a short reduction time of 100 s, no apparent morphological changes have been observed, but the surface of BBO100 is clearly roughened, which is assigned to the partial Bi exsolution from BBO lattice. Starting from BBO500, all samples show the nanosheets structures, indicating that the cathodic potentials could not only modify the electronic properties of Bi centers, but also lead to rapid self-reconstruction in nanostructures. HRTEM in conjunction with EDX mapping and the corresponding line scans were employed to characterize three representative samples (Figure 4.4), namely, BBO100, BBO1000 and BBO3000, to uncover the evolution process of BBO. In the initial stage of reduction (BBO100), nanosized Bi were clearly exsolved on the surface of BBO, leading to the intermediate Bi/BBO structures where the unreacted BBO core is covered by the Bi shell. This observation is in accordance with XRD and FESEM results. As the reduction prolongs to 1000 s, the BBO phase is hardly maintained, as revealed by the much weaker intensity of Ba signal compared to BBO100. Noteworthy, the majority of BBO should have converted to Bi at this point due to the severe BBO dissolution. As the reaction time extends to 3000 s, only the Bi nanosheets can be identified.



**Figure 4.2** (a) XPS survey scans of BBO and BBO3000. (b) High-resolution Bi 4f spectra of metal Bi-3000 and BBO3000 before and after Ar etching for 3 mins. (c, d) High-resolution Ba 3d spectra of (c) BBO and (d) BBO3000, respectively.



**Figure 4.3** (a-e) FE-SEM images of catholically reduced BBO powder with various reduction times of (a) 100, (b) 500, (c) 1000, (d) 3000, and (e) 5000 s at three different magnifications.



**Figure 4.4** (a-c) HAADF-STEM dark field images, the EDX mappings and the corresponding schematic illustration of the structures of (a) BBO100, (b) BBO1000 and (c) BBO3000 to uncover the BBO reduction (cartoon: orange: Ba; purple: Bi; white: oxygen).

The dissolution of BBO scaffolds is further evidenced by comparing the C<sub>dl</sub> values obtained over BBO samples with various reduction times (Figure 4.5). Interestingly, the C<sub>dl</sub> value gradually decreases as the reduction reaction proceeds over BBO, i.e., the C<sub>dl</sub> was calculated as 5.93 and 2.30 mF cm<sup>-2</sup> over BBO100 and BB05000, respectively, and this can be attributed to the gradual loss of Ba sites. The ECSA value of all BBO-based samples was determined, as shown in Figure 4.5f. Despite the gradual loss of Ba sites, all BBO samples possess larger ECSA compared to that of the commercial Bi nanoparticles. Such morphology of 2D nanosheets is desirable for CO<sub>2</sub>RR due to the maximized specific surface area, which guarantees larger contact areas between the catalysts surface and electrolyte. Moreover, the lamellar structures also endow the reduced catalyst thickness on electrode and lower the mass transfer resistance at the solid/liquid interface during CO<sub>2</sub>RR, which in turn leads to a higher current density/reaction rate. In addition, the atomic sites at the edges of the 2D nanosheets possess multiple unsaturated chemical bonds and the dangling bonds, therefore, are more active in comparison to the atoms residing in the metal core, 104,109 thus achieving the higher catalytic activities. The edge atoms of the ultrathin nanosheets could also help reduce the activation barrier and stabilize certain reaction intermediates, making the reaction more feasible.<sup>110</sup>

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Figure 4.5 (a-e) CV analysis over BBO100, 500, 1000, 3000, and 5000 in non-Faradaic region. (f) The corresponding  $C_{dl}$  values.

The validity of the gradual Ba<sup>2+</sup> loss is supported by quantifying the Ba<sup>2+</sup> concentration in the used KHCO<sub>3</sub> (referred to the electrolyte used for BBO3000 preparation) by ICP-OES. The average Ba<sup>2+</sup> concentration is determined to be 3.69 mg L<sup>-1</sup> after reducing 1.0 mg BBO for 3000s. We repeated the electrolysis in CO<sub>2</sub>-saturated DIW without KHCO<sub>3</sub> additive, and only identified a much lower Ba<sup>2+</sup> concentration (0.097 mg L<sup>-1</sup>). Therefore, both the external bias and the high conductivity of electrolyte appear to facilitate the Ba<sup>2+</sup> release from BBO backbones. Furthermore, to rule out the self-dissolution of BBO in DIW, a fresh piece of BBO was placed in DIW for 3000 s without applied voltage and as expected, no detectable among of Ba<sup>2+</sup> has been obtained, suggesting the structural stability of BBO under potential-free conditions in DIW. The analyses of XRD, Raman, XPS, and ICP-OES collectively confirmed the BBO-to-Bi conversion upon extended electrochemical

conditioning, accompanied by the Ba<sup>2+</sup> release from the perovskite scaffolds due to the overall structural rearrangement. Based on these results, an overwhelming amount of BBO in the BBO3000 sample has been reduced to metallic Bi, denote as eBBO, and will be subjected to further electrolysis characterizations.

To briefly sum up, conventional exsolution process generally produces nanoparticles grown homogeneously on the surface of host perovskites, and the mild exsolution of B-site elements produces suitable number of vacancies while maintaining structural integrity.<sup>106</sup> However, from the above results and discussions, it is concluded that electrochemical conditioning can trigger Bi exsolution from BBO backbones in an instantaneous manner. Furthermore, Bi exsolution only ceases upon complete reorganization of BBO, which results in the complete phase transformation from BBO to Bi. The catalyst reconstruction route is, in essence, a Bi dissolution-renucleation-growth pathway. At the moderate potential of - 1.2 V, Bi in BBO is continuously reduced, and any remaining exsolvable Bi ions would keep diffusing from interior toward electrode/electrolyte interface until reaching an equilibrium, leading to the nucleation of Bi at electrode surface followed by the in situ preferential growth of Bi nanosheets. Meanwhile, the released Ba<sup>2+</sup> ions are dissolved into the aqueous electrolyte and remain in the ionic form.

To understand whether the phase change of BBO affects the CO<sub>2</sub>RR from a thermodynamic point of view, DFT-based calculations were performed to examine the Gibbs free energy changes of CO<sub>2</sub>-to-FA conversion and HER on pristine BBO and the reconstructed BBO surface (Figure 4.6). BBO (100) and BBO (001) slabs were employed to represent the pristine BBO surface because Bi atoms, which are the active centers, can be well exposed on these two surfaces. Bi (003) slab was adopted to represent BBO surface based on the previous HR-TEM results. The computational results show that the RDS for CO<sub>2</sub>-to-FA conversion on Bi (003) is the first protonation step to produce \*OCHO, which requires an energy of 1.050 eV, and the subsequent formation of FA is a barrierless step. For BBO (100), the \*OCHO intermediate will adsorb to Bi atoms in all considered configurations. The RDS is also the first protonation step to form \*OCHO but with a higher energy barrier of 1.21 eV compared to that of the eBBO, indicating that the activation of \*CO<sub>2</sub> molecule to form \*OCHO is more difficult on BBO (100). For BBO (001), we observed an interesting phenomenon: the \*OCHO intermediate tends to coordinate with sub-surface Ba atoms rather than Bi atoms regardless of the initial adsorption site, and this is perhaps owing to the strong alkalinity of Ba atoms. However, it should be noted that Ba atoms are not the true active centers despite the easiest formation of \*OCHO among all surfaces. We also simulated the free energy change of HER on these three different surfaces. For eBBO and BBO (100), the adsorption energies of \*OCHO and \*H show similar trend due to the existence of the scaling relation. Based on these results, we conclude that the reconstruction of BBO to produce eBBO is desirable, and the eBBO surface favors the FA production by providing suitable \*OCHO adsorption energy and the barrierless desorption of FA.



**Figure 4.6** (a) Free energy diagrams of the CO<sub>2</sub>-to-FA conversion. (b) Free energy diagrams of the HER. eBBO (red line), BBO (100) (blue line) and BBO (001) (green line).

To comprehensively evaluate the CO<sub>2</sub>RR activity of the eBBO and to compare eBBO with the reported Bi-based catalysts, we firstly evaluated the electrocatalytic activities of eBBO in 0.1 M KHCO<sub>3</sub> electrolytes using the H-cell separated by a Nafion 117 membrane. As shown from the LSV curves in Figure 4.7a, the *j* of eBBO obtained in CO<sub>2</sub> bubbled electrolytes is comparatively higher than those in the argon bubbled media, indicating the occurrence of CO<sub>2</sub> conversion. The external potential was stepped down from -0.7 to -1.3 V to detect the product distributions of potentiostatic CO<sub>2</sub>RR electrolysis (Figure 4.7b). The results unveil that the liquid phase is composed of FA over the entire measured voltage range, whereas H<sub>2</sub> and CO account for the rest gaseous phases. The FE<sub>FA</sub> exceeds 90.0% as the potential shifts more negatively to -0.9 V, and the maximum FE<sub>FA</sub> approaching 100% has been achieved at -1.2 V, accompanied with 0.3% of H<sub>2</sub> and 1.0% of CO. The FE<sub>FA</sub> slightly deteriorates to 93.1% by further raising the potential to -1.3 V, and the enhanced HER at - 1.3 V may be ascribed to the limited CO<sub>2</sub> mass transfer. Furthermore, the high *j*<sub>FA</sub> of - 20.7 mA cm<sup>-2</sup> can be obtained at a moderate potential of -1.2 V, along with a FA

production rate of 533.2 µmol h<sup>-1</sup> cm<sup>-2</sup>. A control experiment using only argon as the feed gas produced almost exclusively H<sub>2</sub> and a trace amount of CO and FA (Figure S4.1a). The minor amounts of CO and FA came from the electrolysis of  $HCO_3^-$ , which is a common phenomenon in KHCO<sub>3</sub> based electrolyte owing to the dynamic equilibrium between dissolved CO<sub>2</sub> and HCO $_3^-$ . Furthermore, no FA has been acquired over bare carbon paper substrate (Figure S4.1b), affirming the catalytic roles of eBBO rather than carbon substrate. It is well known that the evolution of H<sub>2</sub> from water splitting always outcompetes the CO<sub>2</sub>RR and consequently, hampers the efficiency and selectivity of CO<sub>2</sub>RR in aqueous media. For example, the maximum FE<sub>FA</sub> has been identified as 85.7% at - 1.2 V for commercial Bi nanoparticles with larger particle sizes (Figure S4.1c and S4.1d). Clearly, the Bi ultrathin nanosheets benefit the CO<sub>2</sub>RR by effectively suppressing the HER. Overall, the eBBO developed in this study exhibits a well-suppressed HER with FE<sub>H<sub>2</sub></sub> maintaining at lower than 3.0% from -1.0 – -1.3, and FE<sub>FA</sub> > 90% over a wide potential range of at least 400 mV in 0.1 M KHCO<sub>3</sub> solution, suggesting that the eBBO derived from perovskite is a good catalyst capable of selectively acquiring FA with high activity.

The electrochemical stability of catalysts is another important criterion to evaluate a catalyst for  $CO_2RR$  in addition to the catalytic selectivity. Thus, we examined the long-term durability of eBBO at the negative bias of -1.2 V, and the electrolyte was replaced with fresh ones periodically (around every 6.5 hours) during the test (Figure 4.4c). The eBBO achieves the stable operation over 60 h at an average current density of -21.0 mA cm<sup>-2</sup> with a FE<sub>FA</sub> retention of 90.0% (which corresponds to a FE<sub>FA</sub> = 90.1% at the end of the 60h test). The above analysis indicates that eBBO possesses a great potential as a promising candidate for  $CO_2RR$  with the superior FA selectivity (FE<sub>FA</sub>  $\approx$  99% at - 1.2 V) and durability (60h at - 1.2V with a FE<sub>FA</sub> retention of 90%). The post-mortem

characterizations after the long-term stability tests of 12h and 60h (denoted as eBBO-12 and eBBO-60) were performed to study the eBBO at the different stages of CO<sub>2</sub>RR.



**Figure 4.7** (a) LSV curves of eBBO at a scan rate of 0.05 V s<sup>-1</sup>. (b) Potential-dependent FEs of H<sub>2</sub>, CO, and FA on eBBO. (c) Long-term stability tests of eBBO at - 1.2 V in 0.1 M KHCO<sub>3</sub> electrolyte.

As shown in Figure 4.8a and 4.8b, the XRD and Raman spectra confirm the dominance of Bi<sup>0</sup> phase after long-time electrolysis of CO<sub>2</sub>. The SEM image of eBBO-12 reveals the well-preserved lamellar structure of eBBO, which gradually evolved to porous Bi sheets composed of ultrasmall nanoparticles upon the extended reaction time of 60 h (Figure 4.8c-e), as further confirmed by the exposed (110) facet of Bi and EDX mappings (Figure 4.8f). Despite the emergence of the ultrasmall Bi nanoparticles, the nanosheets structures are still partly preserved. Therefore, the eBBO obtained in this study shows a good stability during the long-term tests at a very negative potential of -1.2 V. For comparison, the important merits of the recently reported Bi-based catalysts have been summarized in Table S1. More practically, the facile synthesis procedure and the low cost of BaBiO<sub>3</sub> render it suitable for industrial-scale implementations.



**Figure 4.8** (a-f) Post-mortem characterizations eBBO-12 and eBBO-60. (a) XRD, (b) Raman, (c, d) SEM, (e) HR-TEM lattice fringes and (f) HAADF-STEM dark field image and the corresponding EDX mappings of eBBO-60h.

As stated before, zero net emission of CO<sub>2</sub> can be realized by utilizing renewable energy to drive CO<sub>2</sub>RR. Inspired by the excellent CO<sub>2</sub>-to-FA conversion on eBBO surface, we explored the opportunity to drive the reaction partially using clean and renewable solar energy by wiring the eBBO dark cathode with a low-cost BiVO<sub>4</sub> photoanode (deposited with FeOOH and NiOOH layers) for the OER reaction to construct a PEC (BVOh-FN|0.1 M KHCO<sub>3</sub>|eBBO, Figure 4.9a). Thus, to unveil the optimal working conditions of BVOh-FN|0.1 M KHCO<sub>3</sub>|eBBO, the illuminated/dark LSV signals of eBBO coupled with BVOh-FN were firstly collected at the cell potentials from 0 to 3.5 V (Figure 4.9b). It is observed that the dark current of BVOh-FN|0.1 M KHCO<sub>3</sub>|eBBO remains

comparably small when the cell potentials stay below 2.0 V. As the potentials shift upward, the dark currents start to contribute a non-negligible portion to the I. The photocurrent, Iphoto, determined by finding the difference between the currents measured under dark and light conditions in BVOh-FN|0.1M KHCO<sub>3</sub>|eBBO is shown in Figure 4.9c (blue line). A closer examination reveals that I<sub>photo</sub> reaches the maximal value at a cell voltage of around 2.75 V, which is the vertex of the parabola. To better distinguish between the contributions of solar and electricity energy inputs, the cathode potential and the corresponding I are monitored as a function of the applied potentials on photoanode, and the results are shown in Figure 4.9d. Apparently, the potential of dark cathode increases rapidly when the anodic potential increases from 0.5 to 1.1 V, but the rate gradually decreases as the anode potential exceeds 1.1 V (Point K). Furthermore, the current increase rate in the anodic potential range of 0.5 - 1.1 V is clearly much higher than that in the 1.1 - 2 V range, suggesting a more efficient utilization of solar energy in the potential range of 0.5 – 1.1 V. These results collectively point out that the maximal utilization of solar energy can be accomplished approximately at the point K where the cell voltage of around 2 V with a total current of 2.5 mA is achieved. This result is slightly at variance with the data obtained from LSV results, which is presumably ascribed to the rapid scan rate of LSV. In light of all the experimental evidence, the overall operational voltages should be in the range of 2.0 – 2.75 V in the BVOh-FN|0.1 M KHCO<sub>3</sub>|eBBO for PEC device to truly benefit from solar energy.



**Figure 4.9** (a) Schematic illustration of the PEC device. (b) Illustration of the optimal working condition of BVOh-FN|0.1 M KHCO3|eBBO PEC cell. (c) LSV curves for BVOh-FN-illu|0.1 M KHCO3|eBBO, BVOh-FN-dark|0.1 M KHCO3|eBBO, and corresponded I<sub>photo</sub> (photocurrent) as a function of cell potential in two-electrode cells. (d) Monitored potentials of eBBO cathode and the applied potential on photoanode as a function of the current. (e) Potential-dependent FEs and partial current densities for FA in BVOh-FN|0.1 M KHCO3|eBBO PEC and EC cells. (f) Short-term electrochemical stabilities of BVOh-FN|0.1 M KHCO3|eBBO PEC cell measured at different potentials.

The selectivity of products in PEC and EC under the optimized working conditions is shown in Figure 4.9e. It is found that FA can be generated with the FE<sub>FA</sub> of 59.0% and 63.3% at the cell voltages of 1.5 and 2 V in PEC device, respectively, and the FE<sub>FA</sub> gradually raises to 80.0% at a cell voltage of 2.5 V with  $j_{FA}$  of -2.1 mA cm<sup>-2</sup>. Further increasing cell potential to 3 V yields a higher

FE<sub>FA</sub> of 81.0%, and the  $j_{FA}$  reaches -2.9 mA cm<sup>-2</sup>. Contrarily, no FA is detected in EC at 1.5 nor at 2 V, and FE<sub>FA</sub> < 1.0 % is detected at 2.5 V with a negligible  $j_{FA}$  of - 0.015 mA cm<sup>-2</sup>. It is only when the external bias reaches 3.0 V that the EC cell will start to contribute significantly to FA production (i.e., FE<sub>FA</sub> = 60.1%). For reference, the total current densities are depicted in Figure 4.9f. Based on the above results, it can be concluded that solar energy can compensate for a portion of the external bias needed to drive the CO<sub>2</sub>RR and can favorably shift the onset potential for FA generation to a smaller value, thereby achieving an appreciable current and FEs for target products compared to the pure electricity-driven approach. Consequently, the PEC cell realizes a high FA selectivity of 80% at the cell voltage of 2.5 V where trivial amount of FA is detected at the same potential in EC cell without solar irradiation.

The electrochemical performance of the eBBO electrode was examined in fresh electrolytes to preclude any possible perturbations of any surface or and naturally released Ba<sup>2+</sup> in the electrolyte. For practical applications, the effects of Ba<sup>2+</sup> should not be ignored since previous studies showed that the alkaline metal ions play a significant role in dictating the FE.<sup>111–113</sup> While many studies have focused on the monovalent cations (e.g., Li<sup>+</sup>, Na<sup>+</sup>, K<sup>+</sup>, etc.), recent studies by Koper et al. showed that the multivalent with larger hydration radii might have even stronger impact over the performances of CO<sub>2</sub>RR since they are more likely to stabilize CO<sub>2</sub>, which is the key to initiate CO<sub>2</sub>RR.<sup>114</sup> The hydrated radii of K<sup>+</sup> and Ba<sup>2+</sup> are 3.31 and 4.04 Å at 25 °C,<sup>115</sup> respectively, and theoretically, the Ba<sup>2+</sup>-CO<sub>2</sub> interactions should be more pronounced compared to that of the K<sup>+</sup>-CO<sub>2</sub>. However, in another study by Wallace et al., the CO<sub>2</sub>RR can be greatly suppressed in the seawater-like electrolyte containing 20 mM CaCl<sub>2</sub> due to the formation of

calcium carbonate at the electrode surface at applied cathodic potentials.<sup>116</sup> Therefore, the concentration of certain multivalent cations must be well controlled to benefit CO<sub>2</sub>RR.

To gain insights into how the released Ba<sup>2+</sup> from BBO affects CO<sub>2</sub>RR, a series of potentialcontrolled electrolysis from - 0.7 - - 1.3 V were conducted to examine the product distributions in 0.1 M KHCO<sub>3</sub> containing 0.025 mM BaCl<sub>2</sub> to mimic the naturally released Ba<sup>2+</sup> when reducing 1.0 mg BBO. As shown in Figure 4.10a, the FE of FA,  $H_2$  and CO obtained in the two electrolytes are almost overlapped, suggesting that the low Ba<sup>2+</sup> concentration (i.e., 0.025 mM) has negligible effects on the CO<sub>2</sub> reduction in 0.1 M KHCO<sub>3</sub> media. However, in 0.1 M KCl-based electrolytes with/without 0.025 mM Ba<sup>2+</sup> additive, a stark difference in FEs can be observed (Figure 4.10b). In general, the FE<sub>H2</sub> values in Ba<sup>2+</sup>-containing 0.1 M KCl solutions are always lower than that of the Ba<sup>2+</sup>-free ones in the potential range of -0.9 to - 1.2 V, and meanwhile, the FE<sub>FA</sub> is clearly boosted by Ba<sup>2+</sup> in the electrolyte, especially at less negative potentials (i.e., -0.8 – -1.1 V). This observation is in accordance with previous studies.<sup>117</sup> The changes in the selectivity for FA at these potentials are closely related to the attenuated HER as the FE<sub>co</sub> remains relatively constant over the studied potential range (fluctuating within a relatively small range of  $\pm$  1.5 %), which is presumably owing to the capability of Ba<sup>2+</sup> ions to repel H<sup>+</sup> near the electrode surface. Increasing the Ba<sup>2+</sup> concentration to 2.5 mM (which is 100 times higher than the actual concentration detected in this study) has led to an even more prominent growth in FA production (Figure 4.10c), suggesting the Ba<sup>2+</sup> additive has indeed contributed to the CO<sub>2</sub>RR reaction in 0.1 M KCl. Notably, further increasing Ba<sup>2+</sup> concentration to 25.0 mM results in the formation of BaCO<sub>3</sub> precipitates when the electrolysis was performed at - 1.3 V for 3000 s (Figure S4.2), which can be detrimental to CO<sub>2</sub>RR since BaCO<sub>3</sub> could block the Bi active sites, retard efficient mass and electron transfers and thus,

impede efficient  $CO_2RR$  electrolysis. It should be noted that in real cases, however, such a high  $Ba^{2+}$  concentration in the electrolyte is unlikely to occur.



**Figure 4.10** (a, b) Potential dependent FEs over eBBO in (a) 0.1 M KHCO<sub>3</sub> and (b) 0.1 M KCl electrolyte with (solid lines) or without 0.025 mM BaCl<sub>2</sub> (dash lines) addition. (c, d) Time-resolved FTIR studies of (c) eBBO and (d) Ba<sup>2+</sup> - eBBO. (c) FEs of eBBO electrodes in 0 mM, 2.5 mM, 7.5 mM and 2.5 mM BaCl<sub>2</sub> in KCl-based electrolytes. (d, e) Time-resolved FTIR studies of (c) eBBO and (d) Ba<sup>2+</sup> - eBBO in 0.1 M KCl and Ba<sup>2+</sup>-0.1 M KCl performed under various external potentials.

The understand how  $Ba^{2+}$  interplays with the CO<sub>2</sub> molecules, the time-resolved FTIR studies were carried out. Certain amount of  $BaCl_2$  was dipped on the clean eBBO electrode and then dried overnight prior to usage (named  $Ba^{2+}$ -eBBO, assuming all the released  $Ba^{2+}$  has been adsorbed to the surface). As shown in Figure 4.10d and 4.10e, both eBBO and  $Ba^{2+}$ -eBBO samples show prominent peaks at 2200 – 2400 cm<sup>-1</sup>, which can be attributed to the physical adsorption of CO<sub>2</sub>.

The CO<sub>2</sub> adsorption responses of both samples could stabilize at around 60 mins, however, the signal intensities in Ba<sup>2+</sup>-eBBO sample are apparently higher than that of the bare eBBO surface. For example, the peak heights in Ba<sup>2+</sup>-eBBO were already larger than the bare eBBO when the reaction only proceeded for 10 mins. Therefore, the intensified FTIR signals in Ba<sup>2+</sup>-eBBO indicate that Ba<sup>2+</sup> favors the CO<sub>2</sub> adsorption, in line with previous studies.<sup>118</sup> To identify possible reaction intermediates of CO<sub>2</sub>RR in 0.1 M KCl and 0.025 mM Ba<sup>2+</sup> added 0.1 M KCl (Ba<sup>2+</sup>-KCl), in situ Raman analysis was then performed over eBBO to gain mechanistic insights. As shown in Figure 4.10f, both the samples exhibit two characteristic Raman shifts at 1313 and 1616 cm<sup>-1</sup> which are assigned to the glassy carbon substrate. In Ba<sup>2+</sup>-KCl media, a marked Raman peak at around 1061 cm<sup>-1</sup> can be clearly observed in a wide potential range, i.e., at - 0.8 V and more negative potentials. This peak is ascribed to the symmetric stretching oscillation of carbonate ( $\nu_1 CO_3^{2-}$ ); whereas no  $v_1 CO_3^{2-}$  bands can be identified on the eBBO surface measured in pure KCl electrolyte.<sup>14,119</sup> The formation of BaCO<sub>3</sub> can be ruled out, since the  $v_1 CO_3^{2-}$  band gradually decreases and eventually vanishes upon releasing the applied potential (- 1.2 V). This observation indicates that the Ba<sup>2+</sup> in the 0.1 M KCl electrolyte has led to enhanced adsorption of carbonate intermediate, which evidently promotes the CO<sub>2</sub>-to-FA conversion. Song et al. reported similar results over S-doped Cu for highly selective production of FA, and their study shows that S-doped Cu exhibit much enhanced  $v_1 C O_3^{2-}$  adsorption.<sup>120</sup>

In fact, previous studies have also carefully examined cation effects by analyzing their perturbations on internal electric field.<sup>121–123</sup> Although most of the reported studies are based on the monovalent cations/anions (e.g., Li<sup>+</sup>, K<sup>+</sup>, Cs<sup>+</sup>, Na<sup>+</sup>, Cl<sup>-</sup>, I<sup>-</sup>, Br<sup>-</sup>), one can still expect the roles of multivalent ions in the electrical field to be even more significant. The "electrolyte-defined

selectivity" for CO<sub>2</sub>RR is perhaps related to the different local CO<sub>2</sub> environment and CO<sub>2</sub>-cation interactions near the catalyst surface in the two electrolytes. It is well acknowledged that KHCO3 solutions can create a high local CO<sub>2</sub> concentration due to the equilibrium between bicarbonate and dissolved CO<sub>2</sub>, meaning that the CO<sub>2</sub> consumed at surface can be rapidly replenished by bicarbonate.<sup>124</sup> As a result, the Ba<sup>2+</sup> mediated CO<sub>2</sub> adsorption could only contribute a negligible amount to the total CO<sub>2</sub> concentration on electrode surface, and therefore the FEs of all products remain very similar in the electrolytes with/without Ba<sup>2+</sup> addition. However, in 0.1 M KCl, the CO<sub>2</sub> is replenished by the dissolved CO<sub>2</sub>, which is insufficient in amount compared to that in the  $KHCO_3$ -based solutions considering the low  $CO_2$  solubility in the water-based electrolyte. In such a case, even the trace amount of Ba<sup>2+</sup> (i.e., 0.025 – 2.5 mM) in 0.1 M KCl may lead to an effective enhancement in the local CO<sub>2</sub> concentration and therefore remarkably boost CO<sub>2</sub>RR over HER, since Ba<sup>2+</sup> has been shown to favor CO<sub>2</sub> adsorption based on the previous analysis. In a recent study by Bell et al., they also suggested that the local CO<sub>2</sub> concentration can be regulated by the hydrolysis of alkaline metal ions, and the CO<sub>2</sub> concentration improves with increasing the cation size.<sup>125</sup> To confirm our hypothesis, further studies that incorporate multiple in situ techniques are required to fully unveil the effects of Ba<sup>2+</sup>. Nonetheless, based on our extensive electrochemical characterizations, it can therefore be concluded that the Ba<sup>2+</sup> released from BBO should be beneficial to FA production in general despite that these effects are collectively dependent on the external potentials, type of electrolytes, as well as the Ba<sup>2+</sup> concentration. It should be emphasized that final concentration of Ba<sup>2+</sup> in the electrolytes is determined by the loading mass of catalyst, as well as the total volume of electrolyte, and these parameters may vary depending on the real operation conditions of CO<sub>2</sub>RR.

Finally, we consider the eBBO with naturally released  $Ba^{2+}$  as one system, and the working mechanisms for CO<sub>2</sub>-to-FA are proposed, as shown in Figure 4.11. Firstly, the adsorption of  $Ba^{2+}$  will take place at the eBBO surface at cathodic potentials. Secondly, the CO<sub>2</sub> dissolved in the electrolyte can be adsorbed more easier on  $Ba^{2+}$  sites and/or Bi sites adjacent to  $Ba^{2+}$ , leading to higher local CO<sub>2</sub> concentration compared to that of the bare Bi surface. Afterwards, the adsorbed CO<sub>2</sub> would gain one electron and form CO<sub>2</sub><sup>--</sup> intermediate, following the hydrogenation step to form HCOO<sup>-</sup> (ads) which further proceeds the elementary step of HCOO<sup>-</sup> (ads) +  $e^- \rightarrow$  HCOO<sup>-</sup> (ads), as proposed in the CO<sub>2</sub>-to-FA mechanisms on Bi surface by a previous study.<sup>126</sup> In the final step, the HCOO<sup>-</sup> (ads) desorbs from the surface and form the final product HCOO<sup>-</sup> (aq). Over the entire process, both the Bi catalytic active sites and  $Ba^{2+}$  ions participate in the CO<sub>2</sub>RR and work cooperatively to drive CO<sub>2</sub>-to-FA conversion, and this mechanism could be extended to other perovskite-based materials for electrocatalytic CO<sub>2</sub>RR at room temperature.



**Figure 4.11** Proposed working mechanism of the eBBO with natural released Ba<sup>2+</sup> in the electrolyte for the selective FA production from CO<sub>2</sub>RR (cartoon: orange: Ba; purple: Bi; white: oxygen; grey: carbon; pink: hydrogen).

### 4.3. Conclusions

In summary, by a series of extensive physical and electrochemical characterizations, we are able to unveil: 1) the structural and phase evolution of pristine BBO perovskite under cathodic potentials, and that is, the electrochemical conditioning of pristine BBO leads to the in operando "dissolution-nucleation-growth" of Bi ions. The resulting eBBO with atomic-scale thickness provides an enlarged active area and more unsaturated active centers, which is among one of the best Bi-based catalysts for FA production reported so far. 2) The cooperative working mechanisms of A- and B- site species in voltage-reconstructed BBO perovskite that regulate the surface reactions. In contrast to the commonly accepted concept that only B-site elements are actively involved in CO<sub>2</sub>RR, our experimental results and systematic analyses demonstrate that the multivalent A-site elements can concurrently participate in CO<sub>2</sub>RR and benefit FA production and furthermore, the Ba<sup>2+</sup> concentration, external potentials and the type of electrolyte play the critical roles in enhancing the beneficial effect of Ba<sup>2+</sup> on CO<sub>2</sub>RR. Our studies show that perovskite-based materials that integrate both A- and B- site elements in one structure, should serve as an effective platform for efficient CO<sub>2</sub>RR with mutual benefits coming from both elements.



#### 4.4. Supporting information

**Figure S4.1** (a) Potential dependent FEs of products: H<sub>2</sub> (green), CO (yellow), and FA (blue) and current densities obtained over eBBO in argon saturated 0.1 M KHCO<sub>3</sub>. (b) Potential dependent FEs of products: H<sub>2</sub> (grey) and CO (red) and total current densities obtained over bare carbon paper in CO<sub>2</sub> saturated 0.1 M KHCO<sub>3</sub>. (c) LSV curve and (d) potential dependent FEs of H<sub>2</sub> (green), CO (yellow), and FA (blue) and current densities (red line) (b) of commercial Bi nanoparticles in 0.1 M KHCO<sub>3</sub> electrolyte.



**Figure S4.2** (a) Digital images of eBBO reduced in 25 mM BaCl<sub>2</sub> electrolyte at -1.3 V for 3000 s. (b) XRD patten of eBBO electrode reduced in 25 mM BaCl<sub>2</sub> for 3000 s.

Electrocatalysts	Electrolyte	E with FEmax	FEmax		Potential window (FE > 90%)	Stability (h)
Bi <sub>2</sub> O <sub>3</sub> NSs@MCCM carbon matrix <sup>126</sup>	0.1 M KHCO₃	1.256 V	93.8%		300 mV	12h @- 0.956V
Bi <sub>2</sub> S <sub>3</sub> derived Bi (SD-Bi)	0.5 M NaHCO <sub>3</sub>	-0.75V	84%		N.A.	24h@- 0.75V
Bi <sub>2</sub> S <sub>3</sub> -Bi <sub>2</sub> O <sub>3</sub> @rGO <sup>128</sup>	0.1 M KHCO3	-0.9 V	90.1%		< 100 mV	24h@- 0.9 V
curved Bi nanotubes <sup>129</sup>	0.5 M KHCO₃	-1.0 V	97%		400 mV	10 h @- 1.0 V
Bi-rGO <sup>130</sup>	0.1 M KHCO₃	–0.8 V	98%		100 mV	15 h @ -0.8 V
Few-layer Bi <sub>2</sub> O <sub>2</sub> CO <sub>3</sub> <sup>131</sup>	0.5 M NaHCO₃	-0.7 V	85%		N.A.	12 h @-0.7 V
BiOCI nanoplates <sup>132</sup>	0.5 M KHCO₃	-0.9 V	92%		300 mv	12 h @ -0.9 v
2D Bi metal–organic framework <sup>133</sup>	0.1 M KHCO₃	-0.9 V	92.9%		100 mV	30h@- 0.9 V
Metal–organic framework derived Bi <sup>108</sup>	0.5 M KHCO₃	-0.97 V	95(±3)%		200 mV	32h@- 0.97 V
Bi Metal–organic framework Bi-BTC-D <sup>134</sup>	0.5 M KHCO₃	-0.86 V	95.5%		300 mV	12h@- 0.86 V
Ag <sub>0.95</sub> BiS <sub>0.75</sub> O <sub>3.1</sub> nanorods <sup>135</sup>	0.1 M KHCO₃	-0.7 V	94.3	3%	300 mV	12h@- 0.7V
This work	0.1 M KHCO₃	V	FE <sub>HCOO</sub> -	FEtotal	400 mV	60 h@
		-1.3 V -1.2 V -1.1 V -1.0 V	93.1% ~100.0 % 92.5% 93.0%	98.8% 103.9% 96.9% 99.0%		-1.2 V (final FE <sub>HCOO</sub> - was
		-0.9 V -0.8 V -0.7 V	90.3% 84.0% 81.6%	98.4% 94.2% 100.1%		90.1%)

**Table S 4.1** Summary and comparison of Bi-based catalysts reported in literatures.

**Table S 4.2** BBO (001) and BBO (100) slabs viewed from the a-axis, b-axis, and c-axis (red: oxygen,purple: bismuth, green: barium).



**Table S 4.3** Summary of the configurations and energies of \*OCHO and \*H intermediate adsorbed on BBO (001), BBO (100), and Bi (003) surface.





# Chapter 5. Nanosecond Laser Confined Bismuth Moiety with Tunable



# **Structures on Graphene for Carbon Dioxide Reduction**

**Figure 5.1** Illustration of the structure-performance relation over two Bi SACs (color of the atoms, purple: Bi; yellow: nitrogen; light grey: carbon on the substrates; dark grey: carbon coordinated to Bi).

### 5.1. Introduction

CO<sub>2</sub>RR driven by renewable energy resources is a promising strategy to accelerate the advent of the ultimate carbon neutrality.<sup>136</sup> Catalysts supported by suitable substrates possess the well exposed active centers and unique metal-support interactions, rendering them a promising group of catalysts to drive CO<sub>2</sub>RR.<sup>3,137</sup> Among all the candidates, Bi metal-based materials demonstrate overall excellent capabilities of converting CO<sub>2</sub> to versatile products, including FA and CO, with appreciable current density and selectivity.<sup>92,138,139</sup> To further improve atom turnover efficacy, mass-specific activity and reduce the production cost, the sizes of the supported catalyst can be downsized from nano- to atomic-scale to expose more active sites for enhanced interplay between active sites and reactant. However, at the atomic dimension, the performance of the catalysts becomes extremely sensitive to the local environment where any subtle variations could lead to a paradigm-shift in the CO<sub>2</sub>RR performances due to the modification of the electronic structure of the active speices.<sup>140</sup> This sheds light on the opportunities to fine-regulate the catalytic outcomes by rationally designing the metal-support interactions.

Previous studies have shown that coordination engineering is an effective strategy to regulate the metal-support interactions, thereby steering the catalytic outcomes. For instance, the nitrogen coordinated Sn SACs can produce FA in general while the Sn SA embedded in C<sub>2</sub>O<sub>2</sub>F can facilitate CO production.<sup>55,141</sup> Compared to Sn, Bi is even more attractive due to their better longterm stability and higher selectivity over FA in bulk forms.<sup>142</sup> Recent studies by Li et al.<sup>82</sup> and Wu et al.<sup>143</sup> reported that Bi atoms coordinated by nitrogen and/or sulfur atoms are promising toward CO production, in sharp contrast to another recent study claiming that only FA has been detected from CO<sub>2</sub>RR over the Bi loaded carbon spheres.<sup>144</sup> The precise identification of the coordination effects requires the delicate control during materials synthesis to exclude other effects, which remains challenging. For instance, the conventional high-temperature annealing for coordination tuning would simultaneously affect the degree of the graphitization of carbon support. This, in turn, leads to the modification of both matrix and coordination structures, which complicates the understanding of these coordination effects. Furthermore, many of the reported synthesis routes reply on the initial synthesis of relevant metal organic frameworks, followed by the annealing, which oftentimes involve the usage of expensive linkers and/or solvents. Thus,

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despite the achievements, the mechanisms of CO<sub>2</sub>RR on Bi SACs currently remain elusive, and it is critical to completely understand the coordination effects on the activity of materials at the atomic level in order to advance CO<sub>2</sub>RR technology.

In this study, the coordination-tuned CO<sub>2</sub>RR has been comprehensively investigated using supported Bi as model catalysts. This is achieved by tailoring the type of the "glue atoms" (C and N) to Bi center via ultrafast laser agitation in nanoseconds. In our method, the graphene nanosheets absorb the photon energy and generate rich vacancy defects which serve as anchoring sites for Bi SAs immobilization; the bismuth salts simultaneously decompose under the high local temperature and in the reductive atmosphere induced by laser irradiation.<sup>145</sup> By applying graphene nanosheets with or without N dopants, the coordination structures of Bi SAs on graphene can be engineered, generating either carbon- (Bi-C) or nitrogen- (Bi-NC) bound Bi SACs, and the former catalysts selectively deliver FA as the major CO<sub>2</sub>RR product with a TOF of 2.64 s<sup>-1</sup> at 1.05 V with a high partial current density of ca. -29.3 mA cm<sup>-2</sup>, exceeding most SACs reported in the literature. Theoretical simulations explicitly uncover that the coordination atoms modulate the electronic features of the Bi centers, thus determining the interactions between Bi and the intermediate species during the reaction. Consequently, Bi-C samples require the lowest energy to drive the CO<sub>2</sub>-to-\*OCHO (RDS), thus favouring the FA production, whereas the CO<sub>2</sub>-to-\*COOH (RDS) conversion to produce CO can be more easily achieved over Bi-NC with the lowest energy penalty associated with this step.

#### 5.2. Results and Discussion

In general, the un-anchored Bi adatom supported by defect-free graphene nanosheets requires a low migration barrier energy of around 0.0 eV to move freely (0.5 eV is roughly the threshold energy of atom migration at ambient temperature).<sup>146</sup> In the presence of defects, vacancies or dopant atoms, in graphene, the trapping of Bi SA at such sites would occur more readily, thus inhibiting clustering and ultimately resulting in the enhanced stability owing to the robust covalency between Bi and the neighbouring atoms. We start by predicting the thermodynamic stability of Bi SA doped in ten different defective graphene models (in either single vacancy or double vacancies sites), using the  $E_b$  as the metric, and the results are shown in Figure 5.2a. The red-highlighted rectangular region at the bottom denotes the thermodynamic stability region ( $E_b$ < 0), wherein most of the investigated configurations exhibit good stability, with the exception of the BiN<sub>3</sub> structure that possesses a positive E<sub>b</sub> and has therefore been excluded from further evaluation. Figure 5.2b reports the Bader charge of various models plotted as a function of their corresponding carbon content within the first-shell coordination sphere. Notably, a linear scaling relation is observed in four-atom coordinated Bi models, and an increase in the C percentage results in a corresponding decrease in the Bader charge of Bi atom, whereas no clear dependence of this nature is identified in the case of three-atom coordinated models. Electron-enriched Bi centers have been reported to exhibit higher activity toward FA conversion,<sup>147</sup> pointing to the feasibilities of coordination engineering for achieving higher FA productions.



**Figure 5.2** (a) DFT calculated  $E_b$  of Bi SAs trapped by various defective sites. Ten different models with Bi SAs occupying either single or double vacancies were evaluated (color, purple: carbon; blue: bismuth; silver: nitrogen). (b) Bader Charge as a function of the concentration of C atoms in all the first shell coordinated atoms. (c) DFT predicted  $\Delta U_L$  over the surfaces of all models. Both CO2-to-FA (red) and CO2-to-CO (blue) pathways were computed. (d) DFT optimized Bi-C/N bond length and Bader charge analysis of BiC3, BiC4 and BiN4 (cyan and yellow regions refer to electron depletion and accumulation, respectively). (e) DFT calculated bond lengths of Bi -\*OCHO and Bi -\*COOH intermediates over BiC3, BiC4 and BiN4.

To gain the theoretical insights at the atomistic level, the Gibbs free energy diagrams of  $CO_2RR$ and HER were simulated on the basis of the well-accepted CHE model to elucidate the structurefunction correlations of Bi-based SACs.<sup>18,20</sup> The complete Gibbs free energy diagrams of the three reaction pathways, including CO<sub>2</sub>-to-FA, CO<sub>2</sub>-to-CO and H<sub>2</sub>O-to-H<sub>2</sub> (HER) with the critical intermediates of \*OCHO, \*COOH/\*CO and \*H, were computed to provide an overview of the CO<sub>2</sub>RR and HER reactions (Figure S5.1). We utilize the  $\Delta U_L$  between CO<sub>2</sub>RR (both FA and CO) and HER, defined as  $\Delta U_L = U_L(CO_2RR) - U_L(HER)$ , as a descriptor to compare their preferred occurrence, and higher CO<sub>2</sub>RR selectivity is indicated by a more positive  $\Delta U_L$ .<sup>148</sup> As depicted in Figure 5.2c, in order to selectively catalyze a particular reaction, the target catalysts should possess a positive  $\Delta U_L$  value for that specific reaction. According to this criterion, BiC3 and BiC4 apparently stand out for the CO<sub>2</sub>-to-FA reaction. BiC2N2-2 also meets the requirement, albeit with a less negative  $\Delta U_L$  for CO. BiN4 appears to be the only viable catalyst suitable for the CO<sub>2</sub>-to-CO reaction. Consequently, our attention is directed toward three exemplary catalysts, namely, BiC3, BiC4 and BiN4, for which the Bader charge distributions and DFT-optimized bond distances of Bi-C or Bi-N within the first coordination shell are depicted in Figure 5.2d.

In more details, the  $*CO_2 \rightarrow *OCHO$  conversion is determined as the endothermic process in both BiC3 and BiC4 samples, and their RDS have been identified as the production of \*OCHO with the energy barriers of 0.58 and 0.62 eV, respectively, both are lower than the energy required to produce\*COOH (1.50, and 2.26 eV, respectively). In addition, the second elementary step is barrierless over the BiC3 and BiC4 samples, thus confirming the favourable production of FA over CO at carbon-bound Bi centers. The binding of Bi atoms to the two O atoms in \*OCHO is favored over binding to a single O atom, with an energy difference of 0.41 eV (taking BiC4 as an example), while Bi atom tends to coordinate with one C atom in \*COOH. In contrast,  $*CO_2 \rightarrow *OCHO$ becomes downhill over BiN4 (-0.85 eV), and the further protonation of \*OCHO to yield desorbed FA requires an energy of 1.05 eV. We further compare the CO<sub>2</sub>-to-CO route over BiC3, BiC4 and BiN4. The first elementary step to produce \*COOH in the reaction is endothermic and is the RDS in all the studied models; the energy penalties associated with the \*COOH generation over BiN4, BiC3, and BiC4 samples are 0.61, 1.50, and 2.26 eV, respectively. The second and third elementary steps from \*COOH to \*CO and the subsequent \*CO release are exergonic over all the samples. The electronic interactions between Bi centers and intermediate species during the reaction are further rationalized by finding the bond lengths between the two components, with shorter distance predicting the stronger interactions. As demonstrated in Figure 5.2e, the BiC3 (2.32 Å) and BiC4 (2.35 Å) exhibit the shorter Bi-O (\*OCHO) bond distance compared to BiN4 (2.51 Å), clearly indicating the enhancement of Bi-O interactions on BiC3 and BiC4. In contrast, the Bi-C (\*COOH) bond lengths of both BiC3 (2.79 Å) and BiC4 (2.81 Å) are comparably longer than that of the BiN4 (2.46 Å), which points to the more enhanced interplay between BiN4 and \*COOH. Furthermore, the orbital interactions between Bi centers and \*OCHO/\*COOH intermediate are examined by plotting the projected density of states (PDOS) of Bi p orbitals and \*OCHO/\*COOH over BiC3, BiC4 and BiN4, as shown in Figure 5.3. The Bi p orbitals, rather than the d orbitals which are commonly adopted for transition metals, were chosen based on the previous studies in which good correlations between the p orbital and \*OCHO adsorption had been described over Bi surface.<sup>109,149</sup> As is shown, the interaction of \*OCHO and Bi is stronger in BiC3 and BiC4 than in BiN4, as evidenced by the much larger overlapping area (S) of Bi p orbitals and \*OCHO (S = 0.435 and 0.450 in BiC3 and BiC4, respectively). Additionally, the sharp coupling peak near Fermi energy level further manifests the preferred hybridization between Bip orbital and \*OCHO and thus the enhanced electronic interactions between Bi-C and \*OCHO.<sup>134</sup> Consequently, the Bi centers in the BiC3 and BiC4 display stronger Bi-\*OCHO interplay that benefits the charge transfer via the Bi-O bond. Likewise, the larger orbital peak overlap of Bi-\*COOH alongside the near-Fermi level coupling peaks in BiN4 (compared to those of the BiC3 and BiC4) collectively points to the more efficient charge transfer between Bi center and \*COOH intermediate in BiN4 catalysts.

Based on this analysis, it becomes known that tuning the microenvironment around Bi centers can substantially influence the electronic interplay between central Bi atoms and the matrix, leading to different hybridizations between Bi and intermediates and therefor enabling the distinct catalytic capabilities of Bi SACs.



**Figure 5.3** PDOS of Bi p orbitals and \*OCHO and \*COOH and their overlapped area after the adsorption of the two species over BiC3, BiC4 and BiN4.

To achieve a rational synthesis of the catalysts, we devised a systematic, two-step method that comprised of wet impregnation of a predetermined amount of metal ions precursor solutions onto carbonaceous matrix, followed by vacuum drying. The metal salt-impregnated carbon supports were further subjected to high-energy laser pulses to decompose and reduce the metal ions (Figure 5.4).



carbonaceous support 
 Metal ion seeds on support
 INanoclusters-SAs hybrids
 SAs on rGO

**Figure 5.4** (a-c) Schematic illustration of (a) the laser setup, (b) the synthesis procedure (picture: the real-life images captured during laser irradiation) and (c) the evolution of "metal ion loaded graphene" hybrids during laser shocks.

The nanosecond pulse laser with a wavelength of 1064 nm was operated at the pulse duration of 5 ns. The spot size of the laser beam could be adjusted by changing the distance between the focus lens and the sample surface. The optimized spot size of the laser beam was 5 mm, and the laser pulse energy was 620 mJ to produce a power density of 0.64 GW cm<sup>-2</sup>. The feasibility of this laser confinement strategy roots in the efficient adsorption of the photon energy and conversion to heat by graphene-based support, allowing for the creation of a transient and localized region with alternating heating and quenching environment as the laser switches on and off. The temperature rise was observed when reaching above 1500 K, thereby promoting the instant
reduction and nucleation of metal cations.<sup>150</sup> Due to the band structure of graphene, electrons from the valence band were excited to the conduction band when laser pulses were absorbed by graphene, leading to the ejection and liberation of electrons which further drive the reduction of metal cations through Auger-like mechanisms.<sup>151</sup> The digital images captured the graphene powder movement and the emergent of bright light resulted from the thermionic emission induced by laser stimulation. The method was firstly exemplified using 0.004  $\times$  of Bi(NO<sub>3</sub>)<sub>3</sub>·5H<sub>2</sub>O as the Bi source, pristine or nitrogenated graphene as substrates (denoted as C and NC, respectively). To analyze the crystalline phase of the laser-treated samples, XRD was performed, as depicted in Figure 5.5. The broad peaks in the XRD spectra suggest the limited crystallinity and low concentrations of the Bi-related phases, which cannot be accurately indexed as metallic or Bi oxides. These samples are denoted as BiOx-C ( $0 \le x \le 1.5$ ) for pristine graphene and BiOx-NC for nitrogenated graphene considering that surface Bi atoms would preferably coordinate with oxygen atoms due to their oxyphilic nature.



**Figure 5.5** XRD patterns of as-synthesized BiOx-NC (red) and BiOx-C (green). The standard XRD patterns of Bi (JCPDS: 44-1246) and Bi<sub>2</sub>O<sub>3</sub> (JCPDS: 27-0050) are provided for reference.

The morphologies of the catalysts were then analyzed using high-angle annular dark-field scanning transmission electron microscopy (HAADF-STEM), as illustrated in Figure 5.6. The images exhibit the presence of sub-5nm nanoclusters alongside a substantial number of bright atoms distributed on the free-standing nanosheets, which are discernable due to the different Z contrasts of Bi and adjacent light elements. The mean diameter of the luminous spots was determined to be 0.289 nm (with the diameter of a single Bi atom being 0.230 nm), thereby substantiating that the isolated dots are Bi SAs. Cluster-free Bi SAs samples can be obtained by refluxing BiOx-C and BiOx-NC with 0.5 m H<sub>2</sub>SO<sub>4</sub>, denoted as Bi-C and Bi-NC, respectively. HAADF-STEM images (Figure 5.6c and 5.6g) in conjunction with EDX elemental mappings in TEM (Figure 5.6d and 5.6h) further evidence the prevalence of Bi SAs across the entire architectures with a high degree of homogeneity and uniformity, reinforcing the excellent stability of Bi SAs against acid leaching. The loading mass of Bi has been measured using ICP-OES (Table S5.1). The slightly higher loading concentrations of Bi has been observed when using NC as the substrate, which can be attributed to the increased number of defects resulted from the introduction of N dopants to graphene. This is critical to stabilize and anchor the metal cations.



**Figure 5.6** (a-c, e-g) HRTEM images of (a-c) Bi-C and (e-g) Bi-NC. (d, h) The corresponding EDX mappings of (d) Bi-C and (h) Bi-NC.



**Figure 5.7** (a) XRD pattern of the sample before and after acid washing. (b-e) HAADF-STEM images. (f) The corresponded EDX mappings of Bi and Cl elements.

In the next series of experiments, the Bi(NO<sub>3</sub>)<sub>3</sub>·5H<sub>2</sub>O precursor solution was substituted with BiCl<sub>3</sub> while keeping other parameters unchanged to investigate the possible impact of the precursor type on materials synthesis (Figure 5.7). The XRD peaks acquired from the irradiated  $BiCl_3/C$ exhibit the enhanced crystallinity and narrower width which can be unambiguously ascribed to the BiOCI phase, in contrast to the broad peak feature and low crystallinity obtained over  $Bi(NO_3)_3 \cdot 5H_2O/C$ . This phenomenon can be explained by the hydrolysis of  $BiCl_3$  in the presence of atmospheric moisture.<sup>152</sup> The coexistence of Bi SAs and BiOCl clusters with the (101) facet exposed has been revealed by HR-TEM and EDX mapping, whereas no well-defined lattice plane has been identified in  $Bi(NO_3)_3$ ·5H<sub>2</sub>O/C samples. It appears that the type of metal ions precursor has a significant role to play on the phase and crystallinity of the nanocrystals, while the generation of metal SAs is comparatively less influenced. The effectiveness of our method was also demonstrated using BiCl<sub>3</sub>-CNTs (carbon nanotubes) and BiCl<sub>3</sub>-CB (carbon black) precursor hybrids (Figure 5.8). As anticipated, a combination of Bi nanoclusters and SAs can be observed. Nevertheless, considering that the Cl source in BiCl<sub>3</sub> may be co-doped into the graphene lattice, the Bi(NO<sub>3</sub>)<sub>3</sub>·5H<sub>2</sub>O precursor solution was chosen in order to exclude any possible interference with the graphene compositions.



**Figure 5.8** (a, b) HAADF-STEM images of Bi loaded on carbon nanotubes (Bi-CNTs) and (c, d) Bi loaded on carbon spheres (Bi-CS).

Compared to the traditional high-temperature annealing methods for catalyst synthesis, the laser treatment confers unique self-etching capabilities that promote the stabilization of metal atoms through the strong covalent bonds with neighboring defects generated *in situ*.<sup>153</sup> More specifically, graphene-based substrates tend to undergo etching in the presence of loaded metal ions, resulting in the generation of more defects.<sup>154</sup> In the annealing process, auxiliary etching agents are oftentimes required to modify the carbonaceous substrates to introduce more

defects,<sup>55</sup> whereas the ultrafast laser bombardment circumvents this requirement, reducing the metal ions and producing defects in a straightforward and simultaneous manner, as substantiated in the following Raman analysis, using the Bi(NO<sub>3</sub>)<sub>3</sub>·5H<sub>2</sub>O/C sample as an example. As shown in Figure 5.9, the I<sub>D</sub>/I<sub>G</sub> values, which indicate the degree of defects (I<sub>D</sub> at around 1355 cm<sup>1</sup> and I<sub>G</sub> at around 1580 cm<sup>-1</sup>), were determined as 0.78, 0.88 for the untreated C and NC powders, respectively, and these values increase to 0.95 and 0.99 after laser treatment in BiOx-C and BiOx-NC, respectively, indicating the creation of rich defects in the samples upon laser dosages. In brief, the ultrafast laser shock method proves to be an efficient means of synthesizing either SACs materials or cluster-SACs hybrids with flexible metal-substrate combinations within a short period of time, offering a promising path toward the fabrication of the SACs-based catalysts tailorable for various catalytic processes.



Figure 5.9 Raman spectra of Bi-C, Bi-NC, C and NC, and the corresponded ID/IG values.

To investigate the surface chemistries and electronic properties of the Bi atoms in the asobtained samples, XPS was conducted, as shown in Figure S5.2. The high-resolution Bi 4f scans exhibit two peaks at the binding energies of 165.0 and 159.7 eV in BiOx-C; these peaks slightly shift to 165.4 and 160.0 eV in BiOx-NC, owing to the different electronegativities of N and C elements. In parallel, these peaks appear at 164.4 and 159.1 eV in Bi-C, and slightly shift to 164.8 and 159.4 eV in Bi-NC. These results may indicate that the C atom(s) coordinated to the Bi SA, if any, have been partially substituted by N atom(s), resulting in an elevated oxidation state of Bi<sup> $\delta$ +</sup> (0 <  $\delta$  < 3) species caused by the electron flow from Bi to N atoms. Hence, the individual Bi atoms in Bi-C and Bi-NC may possess varying coordination environment based on the choice of C or NC as supports.



**Figure 5.10** (a) Bi L-edge XANES spectra of Bi-C, Bi-NC,  $Bi_2O_3$  and metallic Bi references (inset shows the enlarged near-edge patterns). (b) Fourier transformed  $\kappa$ 3-weight EXAFS spectrum of Bi-C, Bi-NC,  $Bi_2O_3$  and metallic Bi. (c, d) Fourier transformed  $\kappa$ 3-weight EXAFS spectrum with the best fitting results of (c) Bi-C and (d) Bi-NC, respectively.

However, there is no direct evidence suggesting the Bi-C or Bi-N coordination species from XPS results, probably due to the low concentration of Bi atoms. To further gain insights into the electronic properties and local geometries of Bi-C and Bi-NC, XANES and EXAFS were performed. To semi-quantitatively determine the Bi oxidation states, the absorption edges of Bi-C and Bi-NC at  $\mu$  = 0.5 are adopted and compared with references of Bi and Bi<sub>2</sub>O<sub>3</sub> (Figure 5.10a).<sup>155</sup> The adsorption edges of both Bi-C and Bi-NC situate between the Bi powder and Bi<sub>2</sub>O<sub>3</sub> references, implying the low-valency of  $Bi^{\delta+}$  (0 <  $\delta$  < 3). Moreover, the Bi-C spectrum slightly shifts toward lower energy compared to that of the Bi-NC, thus pointing to lower oxidation states of Bi atoms in the Bi-C powder. The intensities of the white lines in the spectra of Bi-C and Bi-NC also fall between the references of Bi and Bi<sub>2</sub>O<sub>3</sub>, providing additional evidence for these conclusions on oxidation states, consistent with the XPS analysis. FT-EXAFS spectra of Bi-NC, Bi-C and the reference Bi and  $Bi_2O_3$  powder are plotted and analyzed to elucidate the possible structural information of Bi SAs (Figure 5.10b). The EXAFS of R-space for Bi powder reveals two the predominant peaks located at 2.59 and 3.21 Å, assigned to the scattering of Bi-Bi interatomic feature.<sup>156</sup> The absence of metallic Bi-Bi signals and the presence of only primary peaks located at 1.60 Å in Bi-C and 1.69 Å in Bi-NC suggest the discrete dispersion of Bi in both samples. The predominant peak in the FT-EXAFS spectrum of Bi-C symbolizes the scattering trajectory of Bi and its proximal light elements and can be attributed to the scattering of the Bi-C bonds. The major peak in the Bi-C spectrum shows a slight shift toward the lower energy compared to that of the Bi-NC, signifying a reduction in the first-shell scattering distance in the former samples. Although EXAFS method is not able to differentiate between N and C atoms in the first coordination sphere, the predominant peak can be tentatively associated with the first shell Bi-C path due to its

comparatively shorter distance, as simulated by DFT simulations (Table S5.2).<sup>157,158</sup> Due to the variability in the coordination environment of Bi, it is insufficient to accurately determine the fine structures of Bi-C and Bi-NC solely through EXAFS. Therefore, a combination of the EXAFS modeling and DFT calculations was performed to quantitatively assess the bond lengths and the coordination numbers around the central Bi atoms in Bi-C and Bi-NC (Figure 5.10c and Figure 5.10d). The results of the simulations are summarized in Table S3 in terms of fitting parameters, such as bond lengths, coordination numbers, and Debye Waller factors. The simulations indicate that a Bi atom in Bi-C is directly coordinated with C and the best fitting coordination number is  $3.73 \pm 0.17$ , indicating the coexistence of BiC3 and BiC4 species in Bi-C as the EXAFS is an average result. Therefore, we cautiously assign the primary peak at 1.60 Å to the Bi-C bonds. In the case of Bi-NC, the optimized fittings show that Bi center is coordinated by four N atoms (BiN4), leading to a coordination number of 4.02  $\pm$  0.21. In a nutshell, the agreement among DFT calculations, XAFS and XPS findings unambiguously confirms the successful synthesis of Bi SACs with Bi-C and Bi-N coordination structures. In the following discussions, we use Bi-C for BiC3 and BiC4 samples, Bi-NC for BiN4 for simplicity.

The electrochemical performances of the Bi-C, Bi-NC, BiOx-C and BiOx-NC electrodes were evaluated in a gas-tight H-type cell using KHCO<sub>3</sub> as the electrolyte. CV scans were firstly performed in argon-saturated 0.1 M KHCO<sub>3</sub> electrolyte to probe the Bi<sup>3+</sup>/Bi<sup>0</sup> redox capabilities (Figure 5.11). The well-defined redox peaks at approximately 0.50 and -0.06 V are attributed to the Bi<sup>3+</sup>/Bi<sup>0</sup> conversions. These characteristic peaks are discernible over BiOx-C and BiOx-NC but are absent in the Bi-C and Bi-NC electrodes. This is due to the low concentrations of Bi species, in line with the characteristic "single atom" features in the Bi-C and Bi-NC samples. The absence of

the Bi<sup>3+</sup>/Bi<sup>0</sup> redox peaks promoted us to compare the ECSA of Bi-C and Bi-NC electrodes by utilizing their C<sub>dl</sub> values, which were extrapolated from the slope of the " $\Delta j/2$  – scan rate" plot acquired in non-Faradaic region. The Bi-C and Bi-NC apparently possess larger electrochemical surface areas (ECSA) values compared to the Bi-free substrates, suggesting the enhancement of ECSA by the incorporation of Bi heteroatoms. It is worth mentioning that the catalytic activity/selectivity of electrodes are not necessarily dependent on their ECSA values,<sup>74,159</sup> thus, more detailed characterizations need to be carried out to comprehensively evaluate the CO<sub>2</sub>RR performances of Bi-C and Bi-NC.



**Figure 5.11** (a, b) CV scans of BiOx-C and Bi-C (a), and BiOx-NC and Bi-NC (b) at a scan rate of 20 mV s<sup>-1</sup> in argon-saturated 0.1  $\mu$  KHCO<sub>3</sub>. (c) C<sub>dl</sub> values of Bi-C, Bi-NC, C and NC electrodes.

Next, LSV was carried out in CO<sub>2</sub>-saturated 0.1 and 0.5 M KHCO<sub>3</sub> electrolytes to distinguish the activities of the four samples (Figure 5.12a). The Bi-C and Bi-NC electrodes display considerably higher current responses and thus higher overall activities compared to BiOx-C and BiOx-NC electrodes, including both CO<sub>2</sub>RR and HER, when the external potential surpasses -0.8 V. The potential-dependent FE toward the gas and liquid products in CO<sub>2</sub>RR, obtained from the average of three independent tests, are presented in Figure 5.12b which highlights significant differences

in product distributions. To begin with, in 0.5  $mathbf{M}$  KHCO<sub>3</sub>, the Bi-C electrodes show overall high selectivity toward CO<sub>2</sub>RR-to-FA conversion. Raising the potential from -0.7 to -0.9(5) V results in an enhancement in the FE<sub>FA</sub> from 47.1 ± 1.2 % to 82.6 ± 0.3 % (peak value) on Bi-C, while further increasing the potentials from -0.9(5) to -1.2 V leads to the decline in FE<sub>FA</sub> alongside the promotion of FE<sub>H2</sub>. In contrast, Bi-NC demonstrates limited selectivity toward FA with the maximum FE<sub>FA</sub> of less than 33 ± 2.1 % (at -1.0 V), significantly lower than that of the Bi-C. As the external potential shifts more anodically, we start to observe a promotion of CO over Bi-NC, reaching the maximum FE<sub>CO</sub> of 81.8 ± 3.0 % at - 0.5 V. The selectivity toward CO is even more enhanced when switching the 0.5 m KHCO<sub>3</sub> to 0.1 m KHCO<sub>3</sub>, wherein the peaking FE<sub>CO</sub> of 90.8 ± 2.6% at - 0.5 V alongside an ultrasmall overpotential of 0.190 V with appreciable FE<sub>CO</sub> onset of 70.3% can be detected, accompanied by negligible amount of FA (less than 2.6%) over the entire measured potential range. On the other hand, the maximum FE<sub>FA</sub> on Bi-C drops to 57.4 ± 0.1 % at a potential of -1.0 V with a simultaneous increase in FE<sub>H2</sub> in 0.1 m KHCO<sub>3</sub>, probably owing to the insufficient proton activation in more diluted electrolytes.<sup>160</sup>



**Figure 5.12** (a) LSV curves of BiOx-C, BiOx-NC, Bi-C and Bi-NC electrodes in CO<sub>2</sub>-saturated 0.1 and 0.5 M KHCO<sub>3</sub>. (b) FEs of FA or CO obtained over Bi-C and Bi-NC in either 0.1 or 0.5 M KHCO<sub>3</sub>. (c)  $j_{FA-geo}$  and  $j_{CO-geo}$  of Bi-C and Bi-NC electrodes acquired in 0.5 M KHCO<sub>3</sub>. (d) FE<sub>FA</sub> obtained over BiOx-C and Bi-C in 0.5 M KHCO<sub>3</sub>. (e)  $j_{FA-geo}$  and  $j_{FA-mass}$  of BiOx-C and Bi-C electrodes acquired in 0.5 M KHCO<sub>3</sub>. (f) Long-term stabilities of Bi-C at a cathodic potential of - 0.85 V in 0.5 M KHCO<sub>3</sub>.

It has been noticed that the area-specific current densities decrease considerably in 0.1  $\times$  KHCO<sub>3</sub>, contributing to the decreased production rates over both FA and CO, albeit the apparent enhancement of FE<sub>CO</sub> achieved in this case. Since the production rate is an important metric attesting the performance and potentials for industrialization of a catalyst, we further calculate the partial current densities of FA or CO obtained in 0.5  $\times$  KHCO<sub>3</sub>, normalized by the geometric area of the electrodes ( $j_{FA-geo}$  or  $j_{CO-geo}$ ), and the results are presented in Figure 5.12c. Bi-C clearly stands out as the best catalyst driving the FA production with the maximum  $j_{FA-geo}$  of -

29.3 mA cm<sup>-2</sup> at -1.05 V. The Bi-NC, on the other hand, demonstrates the higher  $j_{CO-geo}$  at more positive potential ranges (i.e., -0.3 - -0.7 V) but with insignificant values.

Subsequently, we compare the performance of Bi-C to BiOx-C electrodes with the anticipation that the latter sample would also exhibit good catalytic properties, as suggested by previous research highlighting the potentials of Bi-based clusters/bulk materials.<sup>161,162</sup> As shown in Figure 5.12d, both Bi-C and BiOx-C show overall appreciable selectivity toward CO<sub>2</sub>RR-to-FA conversion. On BiOx-C, the formation of FA accounts for more than 90% of the total FEs across a wide potential range of -0.8 to -1.2 V, with only minor amounts of CO and H<sub>2</sub> (less than 5%) in presence. Regarding j<sub>FA-geo</sub>, the Bi-C exhibits the highest j<sub>FA-geo</sub> between cathodic potentials of -0.7 to -1.05 V, as illustrated in Figure 5.12e. As the potential decreases further to -1.2 V, the  $j_{FA-geo}$ plateaus and then slightly decreases probably due to mass transfer limitations. On the other hand, the j<sub>FA-geo</sub> of BiOx-C continues to grow as the potential shifts more negatively, exceeding that of the Bi-C at -1.1 V. We postulate that these disparities can be attributed to the different concentrations of Bi in the BiOx-C and Bi-C samples. It is generally acknowledged that highly negative potentials can significantly enhance the charge transfer and reaction kinetics of FA, thus resulting in a state of saturation for the number of available sites in Bi-C when the potential surpasses -1.05 V. Conversely, in the case of BiOx-C, a surplus of sites for CO<sub>2</sub> adsorption and turnover remains available. Therefore, the j<sub>FA-geo</sub> of BiOx-C keeps increasing even when further reducing the potentials. In addition, Bi-C exhibits the highest FA partial current density normalized by mass (j<sub>FA-mass</sub>), thus indicating the highest cost-effectiveness of the Bi-C. In order to estimate the intrinsic activities of Bi atoms in Bi-C, the TOF was calculated based on the total mass of Bi (Figure 5.13). The results reinforce the high intrinsic activity of Bi atoms in the Bi-C for

the CO<sub>2</sub>-to-FA conversion with the TOF of Bi-C reaching a peak value of 2.6 s<sup>-1</sup> at -1.05 V. Considering the much higher current densities achieved in 0.5  $\times$  KHCO<sub>3</sub> electrolyte and the high activities of CO<sub>2</sub>-to-FA conversion over Bi-C, the long-term stability has been assessed over a period of 40 hours (Figure 5.12f). The results reveal that the Bi-C catalyst demonstrates appreciable long-term durability, maintaining an average FE<sub>CO</sub> (ca. 2.5%) and FE<sub>H<sub>2</sub></sub> (ca. 18%) values with the average total current density of -16.5 mA cm<sup>-2</sup> and achieving a total FE<sub>FA</sub> of 81.2% at the end of the measurement. The obtained total FE<sub>FA</sub> is slightly higher than the FE<sub>FA</sub> measured during potentiostatic analysis, which could be the systematic error from different batches of samples.



Figure 5.13 TOF of Bi-C at various applied potentials.

# 5.3. Supporting information



**Figure S5.1** DFT computed Gibbs free energy of the individual reaction steps of CO, FA, and H<sub>2</sub> pathway over ten different Bi SACs models.



Figure S5.2 XPS analysis of BiOx-C, BiOx-NC, Bi-C and Bi-NC.

**Table S 5.1** Bi loading mass of BiOx-C, BiOx-NC, Bi-C and Bi-NC.

Sample	Loading Mass (w.t.%)
BiOx-C	6.3 %
BiOx-NC	8.8 %
Bi-C	0.9 %
Bi-NC	2.1 %

**Table S 5.2** EXAFS fitting parameters for Bi-NC and Bi-C.

Sample	Scattering	CN	R (Å)	σ² (10 <sup>-3</sup> Ų)	$\Delta E_0$ eV)	R factor
	Path(s)					
Bi-NC	Bi-N	4.02 <u>+</u>	2.25 <u>+</u>	13	-6	0.008
		0.21	0.06			
Bi-C	Bi-C	3.73	2.29 <u>+</u>	6	-2.3	0.005
		±	0.025			
		0.17				

# **Chapter 6. Volcano-shaped Carbon Dioxide Reduction on Cobalt**

# Phthalocyanine with Curvature Induced Atomic Spacing Regulation



**Figure 6.1** Illustration of the curvature-tuned geometric deformation in CoPc (color of the atoms: red: Co; yellow: nitrogen; light grey: carbon on the substrates; blue: carbon in CoPc).

## 6.1. Introduction

Electrocatalysts with the atomically distributed "metal-ligand" active centers (e.g., MNxCy, M = metal, N = nitrogen and C = carbon), mainly the metal macrocycle-based catalysts (e.g., n=metalloporphyrin, metallophthalocyanines, etc.) and inorganic SACs have been actively investigated in CO<sub>2</sub>RR for their high catalytic activities, efficient atom utilization and low cost compared to the noble metal-based counterparts.<sup>163</sup> "Ideal" MNxCy generally adopts the planar, and centrosymmetric geometry with equal M-N/C bond length and N/C(1)-M-N/C(2) bond angle. In practical scenarios, however, MNxCy motif tends to deviate from the "perfect" structure and deforms, as widely observed in the materials synthesized/pyrolyzed at different temperatures,<sup>164,165</sup> to the MNxCy with asymmetrical coordination (different atom type and number),<sup>166,167</sup> and MNxCy immobilized on supports with different porosities and curvatures,<sup>72,73</sup> etc. Under non-static conditions, MNxCy deforms even more severely due to adsorption/desorption behaviours.<sup>168,169</sup> Bond length of M-N/C, among the other geometric

parameters, has been previously used as a useful indicator, predicting the CO<sub>2</sub>RR activities. For instance, Wang et al. reported that Zn-N distances vary depending on the annealing temperature, which affect the electronic properties of Zn centers and further dictate the catalytic activities.<sup>170</sup> On the basis of DFT, Zhu et al. predicted that cobalt porphyrin nanotubes with larger/smaller curvatures afford longer/shorter first-shell Co-N distances, which could preferably reduce the CO<sub>2</sub> to CO or CH4, respectively.<sup>72</sup> Despite these understandings, the net effects of local structures of MNxCy on CO<sub>2</sub>RR performance are oftentimes overlooked due to the performance enhancement brought about by other factors, mainly the ligand/coordination effects, and thus remain largely elusive.

One interpretation for the "structure-dictated" CO<sub>2</sub>RR in the MNxCy upon geometric deformation is the "strain effect". In the simplest case, the deviations in bond length from its equilibrium state would lead to compressed/tensile MNxCy, further affecting metal-intermediate hybridizations and ultimately the CO<sub>2</sub>RR performances, in resemble to the well-known "strain engineering" in bulk catalysts. However, strain engineering in MNxCy-based materials has been lagging mainly due to the entanglement between strain and other effects as mentioned above. The ligand effect, for instance, occurs readily when local strain is introduced *via* doping heteroatoms,<sup>171</sup> or annealing MOF-based precursors at various temperatures. The latter is a convenient synthesis method but tends to modify the physiochemical properties of support, the number of coordinated atoms, and/or to introduce catalytic inequivalent species (e.g., nanoclusters, etc.).<sup>172</sup> Many previous studies have demonstrated that the annealing temperature greatly affects the degree of the graphitization of carbon support, which changes the CO<sub>2</sub>RR performances.<sup>46,170</sup> In addition, the lack of synthesis methods to achieve effective build-up of

internal strain in MNxCy as well as the limited access to advanced techniques to probe the local deformations further restrains the understanding of strain-performance relations.

In an attempt to unveil the potential links between local structures and CO<sub>2</sub>RR in MNxCy, a series of cobalt phthalocyanine/carbon nanotubes (CoPc-CNTs) are chosen as ideal platforms in this study to introduce deformation around central Co atoms, and the magnitude is controlled by varying the radii/curvatures of the CNTs matrix. The CoPc-CNTs are prepared via self-assembly at room temperatures without harsh conditionings, thus preserving the intact CoN8C8 structures with identical and well-defined coordination inherited from the CoPc molecule. This eliminates any potential ligand effects caused by different coordination environment. The nonplanar distortion and symmetry reduction of this structure in CoPc can be readily interpreted as the buildup of strain around the Co centers. With this model electrocatalyst, we applied systematic and comprehensive physical and electrochemical characterizations in conjunction with DFT simulations to fully uncover their strain-function relations. A typical volcano trend over the intrinsic CO<sub>2</sub>RR activities and the magnitude of strain around Co centres based on interatomic distance has been established, where the apex point is a mildly compressed CoN8C8 with reduced Co-N/C bond lengths. This optimal sample (Co-CNT2) yields a 1.2-fold and 2.4-fold *j*co-ECSA and TOF, respectively, at a typical potential of - 0.8 V compared to its least strained counterparts (Co-CNT4). Furthermore, it is shown that the long-term stability of Co-CNT2 has been greatly improved owing to the retarded CoPc demetallation process during CO<sub>2</sub> electrolysis. This study highlights and confirms the importance of controlling the internal strain and geometric distortion of catalysts in the applications of  $CO_2RR$ , which demonstrates the untapped potentials of strain engineering in MNxCy-based structures to realize further achievements in CO<sub>2</sub>RR.

#### 6.2. Results and Discussion

We started by optimizing the structures of CoPc/CNT and CoPc/rGO via DFT-based methods to provide sight into whether CNT could effectively generate deformed structures. The armchair (7\*7) CNT passivated with H at the edge sites and  $\sqrt{2}$  (8\*5) rGO were employed to model the curved and planar substrates, respectively. Although the size of CNTs was smaller than the one in practical cases (to cope with the limited computational resources), the goal is to provide basic insights into the CoPc/support interactions, and the conclusion can serve as a basis for the rational design of Co-CNTx series with the structures of varying degree of distortion. Two typical CoPc orientations (denoted as CoPc-CNT-o1 and CoPc-CNT-o2, with a 45° difference), each with three different adsorption sites (top, bridge, and hex), were explored to determine the most energetically stable configurations.<sup>173</sup> As shown in Figure 6.1, the dome-shaped conformation of the CoPc molecule was obtained upon its hybridization with CNT. For Co-rGO, no apparent distortion/bending of CoPc was observed, in line with the previous studies.<sup>173</sup> Next, we examined the bond distance change in the first (Co-N<sub>1st</sub>), second (Co-C<sub>2nd</sub>), and third (Co-N<sub>3rd</sub>) coordination shells of Co, and this local structure is denoted as CoN8C8 for simplicity. Using Co-rGO as the reference, we observed anisotropic bond length reductions in both Co-CNT-o1 and Co-CNT-o2, where the largest degree of bond change takes place along the radial direction (X), and the medium/moderate bond shrinkage occurs along the 45° direction (green arrows). No apparent changes were observed along axial direction (Y). Take the Co-N1<sub>st</sub> for example: In CoPc-rGO, the Co-N1<sub>st</sub> is 1.932 Å. In Co-CNT-o1, this value reduces to 1.926 Å. In Co-CNT-o2, the Co-N1<sub>st</sub> along X and Y direction is 1.931 and 1.914 Å, respectively. The same propensity applies to the Co-C<sub>2nd</sub> and Co-N<sub>3rd</sub>. The trends in bond length changes (in whichever shell) follow the same trends in the

degree of CoPc curving in the three different directions, suggesting the positive correlations between CoPc curvature and bond reduction. Therefore, we can postulate that regulating the CNT radii could effectively induce various anisotropic curvature in CoPc, leading to average bond distance reduction and thus intramolecular strain.



**Figure 6.1** (a) Illustrations of the CoPc structure and the optimized bond distance in CoPc-rGO, Co-CNT-o1 and Co-CNT-o2. (b) Co k-edge XANES spectra, (c) enlarged Co k-edge XANES spectra at the near edge region and (d) Fourier transformed κ3-weight EXAFS spectra of CoPc and CoPc-CNTx. (e) Magnitude of the average bond distance change with respect to the equilibrated bond distance in CoPc-CNTx.

Co-CNTx electrocatalysts (x = 1, 2, 3, 4, pre-cleaned CNT with the average radii of 2, 4, 10 and 20 nm) and the control sample Co-rGO were synthesized through the hybridization of CoPc molecules and carbon substrates in dimethylformamide at room temperature and pressure.<sup>77</sup> Further reducing the radius of CNTs to < 1 nm leads to apparent CoPc aggregation and therefore, they are excluded in the next series of experiments. As presented in the XRD (Figure 6.2), all the as-obtained samples exhibit the characteristic diffraction peaks of CNT, and no CoPc phase has

been detected, indicating the molecular dispersion and relatively low concentration of the loaded CoPc molecules.



Figure 6.2 XRD spectra of Co-CNTx, Co-rGO, bare CNTs and CoPc powder.

TEM and SE-TEM discloses the aggregates-free morphologies of the electrocatalysts (Figure 6.3), which is critical (i) to reduce the inter-molecule interactions among CoPc and preserve its molecular dispersion, (ii) to guarantee efficient charge transfer between CoPc and support. The presence of the atomically distributed Co ions is confirmed by the Z-contrast AC-HAADF STEM graphs. The loading mass of Co atoms in Co-CNTx is determined ICP-OES (Table S1), suggesting a CoPc concentration of 2.0 - 3.5 nmol cm<sup>-2</sup>. This is consistent with the non-stacking and monodispersing features of CoPc, which is important to understand their geometrical effects.<sup>174,175</sup>



Figure 6.3 TEM and SE-TEM images of Co-CNT1 (a), Co-CNT2 (b), Co-CNT3 (c), Co-CNT4 (d) and Co-rGO (e).

*Ex situ* Co K-edge XAS was performed owing to its high sensitivity toward the three-dimensional atomistic arrangement around the X-ray absorber, which provides opportunities in decoding the atomic structures of around Co centers.



**Figure 6.4** (a) Co k-edge XANES spectra and (b) enlarged Co k-edge XANES spectra at the near edge region of CoPc and CoPc-CNTx.

As shown in Figure 6.4a, the weaker pre-edge peak (peak *a*) at ca. 7709 eV is assigned to the dipole forbidden 1s  $\rightarrow$  3d transitions which reflect the hybridization of the empty 3d metal states, the amplitude of which increases with the decrease in symmetry in CoN4.<sup>176</sup> Co-CNT1 exhibits the strongest peak intensity (insert), thus affording the most severe metal site distortion from centrosymmetric to non-centrosymmetric coordination environment.<sup>177,178</sup> The gradual decrease in peak intensity from Co-CNT2 to Co-CNT3 and Co-CNT4 indicates the continuous reduction in the degree of distortions. As further demonstrated in Figure 6.4b, the second pre-edge peak (peak *b*) in XANES emerged at ca. 7715 eV represents the electric dipole transition of 1s  $\rightarrow$  4p<sub>z</sub>, a fingerprint feature that probes the square-planar bonding motif of CoN4 with *D*<sub>4h</sub> symmetry in CoPc molecules. The intensity of this peak is the strongest in Co-CNT1 and attenuates in the other samples. This is a sign of the presence of symmetry-breaking and deformed CoN4 geometry,

alongside the changes in the  $\pi$ -electron conjugation in molecularly dispersed CoPc, which are presumably triggered by the different magnitude of strain within CoPc. In addition to these features, the valence states of Co can be extrapolated from the adsorption edge energy of XANES spectrum, which is determined by finding the energy shifts in adsorption edge. The adsorption edges slightly shift rightward as the CNT radius increases from Co-CN1 to Co-CNT2. This variation, albeit subtle, indicates more localized electrons around the Co centers as the CNTs radius decreases, thus lowering oxidation states of Co ions. The Co-CNT3 and Co-CNT4 take on similar values, suggesting the similar oxidation states in these two samples. These observations agree well with the previous reports on the Zn-N4 geometries and Zn K-edge XAS studies, which suggests a correlation between Zn-N4 bond length and valence states of Zn.<sup>170</sup> The high-resolution Co 2p XPS spectra possess similar profiles (Figure 6.5), indicating the prevailing +2 oxidation states of Co ions. However, insignificant peak shifts have been detected by XPS, this is probably due to the different sensitivities of XPS and XAS techniques.



Figure 6.5 XPS high resolution Co 2p spectra of Co-CNTx and Co-rGO.

The Co K-edge κ3 weighted FT-EXAFS, which directly reflect the distances between Co center and adjacent atoms, are presented to support the hypothesis on the strained CoN8C8 motifs in Co-CNTx (Figure 6.6a). The FT-EXAFS spectrum of bare CoPc exhibits one major peak at ca. 1.44 Å, assigned to the Co-N<sub>1st</sub> scattering path in CoPc. The position of this primary peak gradually shifts leftward as the radius of CNTs decreases. These are clear indications of the Co-N<sub>1st</sub> distance decrease and bond shrinkage. In addition to the decreased Co-N<sub>1st</sub> bond lengths, similar trend is also observed over the Co- $C_{2nd}$  and Co- $N_{3rd}$  shell.<sup>176,179,180</sup> This suggests that the overall CoPc molecular is subjected to certain degree of compression when hybridized with CNT, leading to the more compact molecules with altered bond length. The bond distance reduction when coupled with highly curved substrates has been identified in another recent study.<sup>181</sup> The magnitude of deformation within the CoN8C8 can be interpreted with shearing and/or linear strain induced by the changes in bond angle and/or bond length. Probing the bond distance in CoPc is more straightforward and experimentally feasible compared to bond angel and thus, the magnitude of linear strain is adopted as a descriptor and calculated based on the R values of all three shells:  $\varepsilon = (\Delta R)/R_{zero}$ , where  $\Delta R$  stands for the difference in final (strained) and equilibrium  $(R_{zero})$  bond distance, respectively. The R value measured from Co-CNT4 was adopted as the equilibrium/initial distance, considering that the radius of CNT4 is large enough to afford a near-planar surface and thus, the  $\varepsilon$  around Co center in Co-CNT4 is set as a reference point and equals to zero (Co-rGO is ruled out for comparison, as will be discussed in the following section). Based on the above rationale, the magnitude of  $\bar{\varepsilon}$  around Co is semi-quantitatively determined based on the value of bond distance change averaged from three different shells adopted from the XAFS results (Figure 6.6b). To briefly sum up, the magnitude of strain within

CoPc molecules changes as a function of the radius of the CNT. Co-CNT1 and Co-CNT2 are categorized as group 1, where these geometric effects are more prominent. Co-CNT3 and Co-CNT4 possess similar geometric properties and are categorized as group 2.



**Figure 6.6** (a) Fourier transformed κ3-weight EXAFS spectra of CoPc and CoPc-CNTx. (b) Magnitude of the average bond distance change with respect to the equilibrated bond distance in CoPc-CNTx.

The LSV was collected in CO<sub>2</sub> saturated 0.5 M KHCO<sub>3</sub> to pre-examine the area-specific catalytic capabilities toward CO<sub>2</sub>RR and HER over different samples. As shown in Figure 6.7a, Co-CNT1 demonstrates the highest overall activity, followed by Co-CNT2. Co-CNT3 and Co-CNT4 show similar LSV results, both are lower than Co-CNT1 and Co-NT2. Co-rGO delivers the lowest *j*<sub>total-geo</sub>. Chronoamperometric CO<sub>2</sub> electrolysis covering a range of cathodic potentials (-0.5 - -1.05 V) was performed. Potentials beyond -1.05 V progressively erode the catalysts, which rises severe stability issues, when it is below -0.5 V the current density is too low and may lead to significant errors. Therefore, -0.5 - -1.05 V is an appropriate range for CO<sub>2</sub>RR studies. In details, Co-CNT2 delivers optimal Faradic Efficiency toward CO among all samples, particularly at more cathodic potentials from - 0.95 to - 1.05 V. Co-CNT3 also demonstrates good FEco, but it only delivers

comparable FEco to Co-CNT2 within a narrower potential range (-0.6 - -0.9 V). Mass transfer limitations due to different specific surface areas/porosities of carbon support cannot sufficiently explain the observed FEco differences at -0.9 - -1.05 V, as Co-CNT1 possesses the smallest radius which would otherwise delivers the highest FEco. Co-CNT4, Co-rGO and CoPc display inferior FEco compared to Co-CNT2 at all the measured potentials.



**Figure 6.7** (a) LSV obtained in Co-CNTx and Co-rGO. (b) FEco of Co-CNTx, Co-rGO and CoPc averaged from three independent measurements. (c)  $j_{co-geo}$  of Co-CNTx and Co-rGO. (d)  $j_{co-ECSA} - \overline{\epsilon}$  plot, and (e) TOF -  $\overline{\epsilon}$  plot over measured potential range.

As shown in Figure 6.7c, Co-CNT1 shows the highest  $j_{co-geo}$ , followed by Co-CNT2. Co-CNT3 and Co-CNT4 demonstrate comparable  $j_{co-geo}$  while Co-rGO shows the smallest  $j_{co-geo}$ . Note that ideally, Co-rGO is suitable to study the geometry-induced effects owing to the planar surface of rGO,<sup>182</sup> however, the apex FEco in Co-rGO emerges at ca. - 0.6 - - 0.7 V, slightly deviates from the - 0.8 V observed in the Co-CNTx series. This may be presumably explained by the different electron transfer patterns within CNT/rGO supported catalysts, as further evidenced by the EIS (Figure 6.8, Table S2). The fitted results show that all the samples possess similar Rs values (which reflect the resistance of electrolyte), but different Rp values with Co-rGO (99.47  $\Omega$  cm<sup>2</sup>) being considerably larger than the others. As the charge transfer strongly affects the reaction kinetics on the catalyst's surface,<sup>183,184</sup> the Co-rGO will be ruled out to ensure fair comparisons of the electrocatalysts' performances. It is noted that Co-CNTx samples also show different Rp, which increases monotonically as the radius of CNTs increases, similar to the trends observed in  $j_{total-geo}$ and  $j_{co-geo}$ .



Figure 6.8 (a) EIS of Co-CNTx and Co-rGO. (b) Tafel slope of Co-CNTx.

In addition to the measurements of *j*<sub>total-geo</sub>, *j*<sub>co-geo</sub> and FE<sub>co</sub>, the intrinsic activities remain as the most important metrics attesting the performances of the electrocatalysts. The activities were firstly determined by calculating the  $j_{co-ECSA}$ , which is more pertinent to our goal.<sup>185,186</sup> As shown in Figure 6.7d, the  $j_{co-ECSA}$  as a function of the  $\bar{\varepsilon}$  was plotted to unveil the activity-strain relation. A volcano-type relation can be clearly observed between the magnitude of  $\bar{\varepsilon}$  and the values of  $j_{co-ECSA}$ . At the representative potential of - 0.8 V where the mass transfer limitations can be generally neglected, the *j<sub>co-ECSA</sub>* in Co-CNT2 is approximately 1.22-fold improvement compared to that in the Co-CNT4 at the same voltage. To further assess the TOF as a function of deformation, the values of TOF were calculated based on the total mass of Co atoms. Using the total mass of Co for TOF calculations generally gives its lower bound values, but it is reasonable in this study due to the high-level molecular dispersion and excellent exposure of CoPc.<sup>187</sup> As shown in Figure 6.7e, the volcanic relation has also been spotted in the TOF-strain plot where Co-CNT2 shows the maximum TOF value at all the measured potentials. Moreover, such a relation is more prominent in the kinetically limited region (-0.5 - -0.8 V). For instance, at - 0.8 V, Co-CNT2 shows a TOF of 4.1 s<sup>-1</sup>, which is 2.4-fold (1.7 s<sup>-1</sup>), 1.6-fold (2.5 s<sup>-1</sup>) and 1.2-fold (3.3 s<sup>-1</sup>) enhancement compared to Co-CNT4, Co-CNT3 and Co-CNT1, respectively, corroborating the highest intrinsic activities of Co atoms in the Co-CNT2 samples. To probe the reaction kinetics of CO formation, Tafel analysis derived from the  $j_{co-ECSA}$  and overpotentials (E<sup>0</sup>(CO<sub>2</sub>/CO) = -0.11 V vs RHE, pH 7.3) is presented in Figure 6.8b. Co-CNT2 shows the smallest Tafel slope of 118 mV dec<sup>-1</sup> among Co-CNT1 (139 mV dec<sup>-1</sup>) and Co-CNT4 (155 mV dec<sup>-1</sup>), comparable to Co-CNT3 (119 mV dec<sup>-1</sup>), indicating the same RDS of CO<sub>2</sub> activation and concurrent electron transfer step in all Co-CNTx. The Tafel values are close to the theoretical value of 118 mV dec<sup>-1</sup>, further verifying the highly molecular distributions

of CoPc with negligible mass transfer limitations, which is the premise to study the geometric effect on CO<sub>2</sub>RR.

To provide mechanistic insights to the experimental observations, we seek to model the process using DFT-based methods. Studying the real systems (where the radii of the CNT could be up to ca. 20 nm) is quite challenging, therefore, we seek to mimic the various deformed CoN8C8 structures with a series of simplified models (Figure 6.9a), where the pyrrolic-type CoN8C8 motifs are embedded in graphene, and then regulating bond length by applying certain amount of "compressive strain" (i.e., -1%, -2%, -3%, -4%, -5%, -6%) and "tensile strain" (i.e., +1% and +2%). In these models, we could achieve: 1) fine regulation of the inter-atomic distance, which is the major observation in our previous discussion, and 2) perseverance of the whole basic CoN8C8 motif, including the characteristic isoindole nitrogen (N<sub>i</sub>) and meso-nitrogen (N<sub>m</sub>) sites. Thus, the calculations should provide useful insights into the local geometric effects on CO<sub>2</sub>RR. As shown in Figure 6.9b, all models share the same RDS which is the protonation of  $CO_2$  to form \*COOH, but with different energy penalty associated with the RDS. When the ε changes stepwise from 0% to -3%, the energy barrier reduces correspondingly, suggesting that the CO<sub>2</sub>RR has become easier to occur as the bond length decreases. For models with  $-4\% < \epsilon < -6\%$ , the strain effects are less prominent toward Gibbs free energy change, as manifested by the similar energy barriers of each individual step. The RDS results are also in line with Tafel results, suggesting that the barrier energy associated with the RDS step can be readily tuned by applying compression, thus enabling higher activity and catalytic turnover.

To gain further insight into the long-term performances of Co-CNTx, the stability tests at the cathodic potential of -0.95 V were conducted over a time span of 4 hours to initially probe the degradation patterns. The samples are donated as Co-CNTx-4h. The expedited degradation of MNxCy-rich catalysts has been reported to occur at more negative potentials, e.g., -0.9 V <sup>188</sup> and -1.0V <sup>189</sup>; this allows the easier observations of the degradation patterns within reasonable timescale.



**Figure 6.9** (a) Simplified models with CoN8C8 embedded in graphene. (b) Gibbs free energy change of  $CO_2$ -to-CO calculated based on simplified models with different degree of compression or tension.



**Figure 6.10** (a) r-FEco and (b) r-jco of Co-CNTx measured at -0.95 V in the initial four hours. (c) The r-jco-av-4h with respect to the magnitude of deformation. (d) r-jco of Co-CNT2 and Co-CNT4 over the course of 10 h electrolysis.

As shown in Figure 6.10a, the FEco values were monitored and normalized with respect to their stable values acquired at 0.5 h, defined as the FEco retention (r-FEco). The r-FEco continuously decreases in all samples over time, while Co-CNT2 and Co-CNT3 retain the r-FEco above 90%. The discrepancies in the CO degrading profiles are further strengthened by comparing the retention of jco (denoted as r-jco, taking the jco at 0.5 h as the initial value) during electrolysis, which could more accurately reflect the changes in activity (Figure 6.10b). Co-CNT2 shows the highest r-jco, following the Co-CNT1, while Co-CNT3 and Co-CNT4 possess similar r-jco. A volcanic feature can be extrapolated based on the average r-jco (r-jco-av-4h, Figure 6.10c). We mapped the

degradation profiles of Co-CNT2 and Co-CNT4, the two catalysts with the highest and lowest rjco, respectively, by extending the reaction time to 10h (denoted as Co-CNTx-10h). As shown in Figure 6.10d, the Co-CNT2 degrades at a rather homogeneous and mild rate while the Co-CNT4 demonstrates a more aggressive degradation profile over the course of  $CO_2RR$ . The rate of degradation, *r*, calculated based on the slope of Figure 3c takes on the values of 3.6% and 6.7% h<sup>-1</sup> in Co-CNT2 and Co-CNT4, respectively, pointing to a nearly doubled degradation rate in Co-CNT4.



Figure 6.11 Co centration in the electrolyte of Co-CNT2-10h and Co-CNT4-10h.

An assortment of degradation mechanisms are intertwined and collectively contribute to the overall performance decay in catalysts with monomerically distributed active centers.<sup>190–192</sup> ICP-OES reveals that the Co-CNT2-10 and Co-CNT4-10 have the Co leaching rates of 7e-5 and 1.4e-4 mg h<sup>-1</sup>, respectively, corresponding to the overall Co mass losses of 54.6% and 88.5% (Figure 6.11). One route for the Co leaching is the "direct" Co release from the macrocycle core, <sup>190</sup> which leaves behind the base-free H<sub>2</sub>Pc matrix. As shown in Figure 6.12, the SERS of Co-CNT2-10h and Co-CNT4-10h can hardly be indexed into the H<sub>2</sub>Pc spectrum colored in grey and yet, a few newly

emerged peaks (blue dots) at 1600, 1030, 998, 850 and 800 cm<sup>-1</sup> closely pertain to the C-C stretching, ring breathing and deformation in benzene-related vibrations.<sup>193,194</sup> This strongly supports the "indirect" leaching pathway, which is likely promoted by the irreversible electricity-driven fragmentation of the CoPc and the simultaneous generation of benzene-based units.<sup>77</sup> In addition, the CoPc and benzene-related vibrations coexist in Co-CNT2-10h, whereas in Co-CNT4-10h, no CoPc has been detected because the majority of CoPc has eroded and the amount of remaining CoPc fallen below the SERS detection limit. Metallic Co formation can be ruled by XAFS and TEM (Figure S6.1).<sup>17,173</sup> Physical detachment is unlikely the major cause differentiating the *r* values based on the analysis of the reaction rates and binding energy.<sup>72,173</sup> Therefore, the various CoPc fragmentation rates in these samples are the major contributor to the different decay rates.



**Figure 6.12** SERS spectra of Co-CNT2 and Co-CNT4 before, and after degradation studies of 4h and 10h.

While the origin of CoPc fragmentation under cathodic potentials is still open for discussion, we tentatively discuss the possible reasons leading to different CoPc demetallation rates when coupled with different CNTs. The emergence of the benzene-related signals in SERS alongside ICP-OES results collectively suggest that certain bonds have dissociated and yielded the free-

standing benzene-related pieces and Co ions. The possible pathways of CoPc fragmentation reported previously point to the protonation of the N<sub>i</sub> and/or N<sub>m</sub> atoms, further leading to weakened Co-N<sub>i</sub>, C-N<sub>i</sub> and/or C-N<sub>m</sub> bond strength.<sup>195,196</sup> The absence of H<sub>2</sub>Pc vibrations in SERS rules out the sole rapture of Co-N<sub>i</sub>. The protonation attack at N<sub>m</sub> and scission of C-N<sub>m</sub> bonds are more probably based on the SERS results and DFT calculations.<sup>195</sup> Hence, Bader charge analysis was performed to examine the charge transfer between  $C-N_m$  bonds in two model catalysts with either planar or curved CoPc geometries. On average, the  $N_m$  atoms gain 0.80 and 0.86 |e| in flat and curved samples, respectively, suggesting that the charge transfer from C to  $N_m$  in the strained samples is indeed more favorable due to its stronger C-N<sub>m</sub> interactions. In addition, the overall charge transfer capabilities in Co-CNTx could also affect stability (see EIS results). Given the same number of total electrons, Co-CNT2 is inclined to allocate a relatively larger portion of electrons to reduce CO<sub>2</sub>, owing to its more efficient charge transfer and higher intrinsic activities. As a result, fewer electrons will be utilized to drive the detrimental self-corrosion process. Therefore, we postulate that the more compact CoPc structure and efficient charge transfer endowed by the local deformation helps improve the stability of catalysts during electrolysis. More investigations will be needed to fully uncover the degradation mechanisms of the CoPc-CNTx systems.

### 6.3. Conclusions

This study reports the enhanced intrinsic activity and stability of CoPc-CNT hybrids with the curvature-induced compressively distorted CoN8C8 moiety in the application of CO<sub>2</sub>RR. The conclusions made based on the results from this study are threefolds: Firstly, CNTx with various radii can induce different magnitude of curvature/deformation/bond length reduction in CoPc, which can be readily interpreted as the intramolecular strain within the CoC8N8 motif, and such

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strain effects are more prominent when the radius of CNT is below 4 nm. Secondly, the optimal magnitude of strain could boost the intrinsic activity of the Co centers in terms of CO<sub>2</sub>-to-CO conversion, displaying the volcanic feature in the activity-strain relations. Thirdly, optimal strain is one of the parameters contributing to the stabilization the overall CoPc structures against demetallation during CO<sub>2</sub>RR.



## **6.4.** Supporting information

Figure S6.1 (a-d) Ex situ XAFS (a-b) and EXAFS (c-d) of Co-CNT2-4h, Co-CNT2-10h, Co-CNT4-4h,

Co-CNT4-10h. (e, f) of STEM images of Co-CNT2-10h and Co-CNT4-10h.

Sample	Co (mg L <sup>-1</sup> )
Co-CNT1	0.514
Co-CNT2	0.322
Co-CNT3	0.276
Co-CNT4	0.398

**Table S6.1** Co concentrations in Co-CNTx and obtained by ICP-OES analysis.

# **Table S6.2** Fitted Rs and Rp values in Co-CNTx and Co-rGO.

Sample	Rs	Rp
Co-CNT1	5.92	12.88
Co-CNT2	6.11	20.32
Co-CNT3	4.81	22.46
Co-CNT4	6.65	28.66
Co-rGO	5.81	99.47

# **Chapter 7. Summary and Future Prospects**

## 7.1. Summary

The work in this dissertation focused on the development of innovative electrocatalysts and the investigations of their structure-performance correlations. Bismuth-based materials have attracted significant research interest as efficient catalysts for producing value-added chemicals, primarily FA and CO, from CO<sub>2</sub>. However, their scalability and industrialization have been hindered by complex production procedures and low product yields. To tackle these challenges, a perovskite-type catalyst, BBO, has been synthesized using a facile sol-gel approach and identified as a suitable candidate for CO<sub>2</sub>RR. Through a combination of XRD, SEM, TEM and XPS techniques, the dynamic evolution of BBO under applied potentials was revealed, leading to the formation of Bi nanosheets (eBBO) alongside the release of A-site element (Ba) during electrolysis, both of which accounted for the phase transition from BBO to metallic Bi with layered structures (eBBO/Bi nanosheets). Another advantage of BBO is the ability to release Ba<sup>2+</sup> naturally. The FA production can be significantly boosted in the Ba<sup>2+</sup>-contained electrolyte, particularly at low cathodic potentials. Time-resolved FTIR and *in situ* Raman analysis reveal that the Ba<sup>2+</sup> benefits the CO<sub>2</sub> adsorption, which ultimately contributes to the improved CO<sub>2</sub>-to-FA conversion.

To further enhance atom turnover efficacy, mass-specific activity, and reduce the production cost, downsizing the catalysts from nano- to atomic-scale to expose more active sites has been identified as a viable approach. This strategy involves exposing more active sites to promote better interaction between active sites and reactants. However, at the atomic dimension, the performance of the catalysts becomes extremely sensitive to the local environment, where any subtle variations could lead to a paradigm-shift in the CO2RR performances due to the modifications of the electronic structure of the active species. Using supported Bi as model catalysts, the coordination-tuned CO<sub>2</sub>RR has been comprehensively investigated by tailoring the type of the "glue atoms" (C and N) to Bi center. Through DFT calculations, the mechanistic bifurcation routes have been identified over Bi SAs, which selectively produces either FA or syngas when bound to C or N atoms, respectively. Theoretical analysis suggests that the tunable selectivity arises from the different coupling states and metal-supported interactions between the central Bi atom and adjacent atoms, which modify the hybridizations between the Bi center and \*OCHO/\*COOH intermediates, alter the energy barriers of the rate-determining steps and ultimately trigger branched reaction pathways after CO<sub>2</sub> adsorption. A novel ultrafast laser shock method was developed to achieve the immobilization of Bi SAs with tunable ligand atoms. Particularly, Bi-C with carbon atoms as the ligand atoms tend to produce the FA from CO<sub>2</sub>RR with negligible account of CO detected, and Bi-NC with nitrogen atoms as the ligand atoms can drive the CO production at small over potentials and achieve the maximal CO selectivity at a low cathodic potential of - 0.5 V. There are two important implications of this work. First, an annealing-free method was developed to fabricate the SACs within short periods of time. This strategy can be broadly applied to prepared SACs electrocatalysts with different types of metal atoms that are tailorable to various electrochemical process. Second, the mechanistic insights of the aqueous-based  $CO_2RR$  performances on the surface of p-blocking Bi SAs were provided, and a general classification of p-blocking SACs were proposed based on the selectivity toward CO<sub>2</sub>RR. In the case of Bi-C and Bi-NC, it has been assumed that these SACs would adopt ideal geometric structures with equal bond length angle. However, in practical scenarios, local deformations

around the central active atoms in SACs often occur due to the presence of different ligand atoms. The net effects of geometric variations have largely been overlooked due to the challenges in disentangling geometric effects from other factors. Additionally, there is a lack of synthesis methods that can effectively regulation the geometries, and advanced techniques are also needed to probe the local deformations. To address the challenges, a series of CoPc-CNTs are chosen as ideal platforms in this study to introduce deformation around central Co atoms, and the magnitude is controlled by varying the radii/curvatures of the CNTs matrix. With this model electrocatalyst, we applied systematic and comprehensive physical and electrochemical characterizations in conjunction with DFT simulations to fully uncover their strain-function relations. A typical volcano trend over the intrinsic CO<sub>2</sub>RR activities and the magnitude of strain around Co centres based on interatomic distance has been established, where the apex point is a mildly compressed CoN8C8 with reduced Co-N/C bond lengths. This study highlights and confirms the importance of controlling the geometric distortion of catalysts in the applications of CO<sub>2</sub>RR, which demonstrates the untapped potentials of strain engineering in MNxCy-based structures to realize further achievements in CO<sub>2</sub>RR.

### 7.2. Future Prospects

Multiple future directions can be proposed for the room-temperature CO<sub>2</sub>RR research, which possess the potential to enhance our comprehension of the operational mechanisms of CO<sub>2</sub>RR in practical systems and expedite the lab-to-fab transfer of CO<sub>2</sub>RR methodology and ultimately achieve global carbon neutrality.

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#### 7.2.1. Operando CO<sub>2</sub>RR study

Operando study provides value insights into both the mechanisms of CO<sub>2</sub>RR and the everevolving dynamics of electrocatalysts in practical scenarios. On one hand, future research could focus on examining the *in situ* physiochemical features of catalyst to uncover the connections between CO<sub>2</sub>RR activity and materials properties, as this knowledge is essential for the rational design of electrocatalysts to reach the desired performance. On the other hand, efforts should be exerted into investigating the reaction pathways, particularly the C<sub>2+</sub> products, which remain elusive nowadays.

### 7.2.2. Stability study

The unsatisfactory long-term stability (>1000 h) of electrocatalysts in the context of CO<sub>2</sub>RR has significantly impeded the practical implementation of this technique. The degradation of materials represents a critical concern for the industry, which has been unfortunately overlooked for some time. In contrast to the well-established electrocatalysts employed in other chemical synthesis reactions, those utilized in CO<sub>2</sub>RR are comparatively less understood with regard to their degradation mechanisms.

### 7.2.3. Materials development based on artificial intelligence

The conventional trial-and-error approach to developing well-performing electrocatalysts toward a target reaction is considerably inefficient and time-consuming. The exploration of novel, unknown and untested materials could be greatly expedited through the implementation of big data analysis, drawing from the vast data pool of theoretical simulation results, and established experiential data in the literature. The integration of artificial intelligence into materials design represents a new epoch in the advancement of next-generation electrocatalysts for CO<sub>2</sub>RR.

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# 7.2.4. New electrolyser configurations

To enable large-scale operation of CO<sub>2</sub>RR, electrolysers must be meticulously designed to surmount the challenges of low CO<sub>2</sub> solubility and sluggish CO<sub>2</sub> mass transfer in liquid-based electrolytes. While the implementation of a flow cell configuration does partially address these issues, other hindrances such as flooding, and carbonate depositions require careful considerations. Hence, substantial progress in the design of electrolysers is vital to propel the study of CO<sub>2</sub>RR going forward.

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